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The study of phase separation in the miscibility gap and ion specific effects on the aggregation of soft matter system

Li Zhang

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Par

Mme Li Zhang

The study of phase separation in the miscibility gap and ion specific effects on the aggregation of soft matter systems

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Chapter 1 Introduction

Many common industrial products and processes are composed of multiple phases that are incompatible. Depending on the processes the systems can be required to remain separate, such as foams and emulsions (mixtures of gas and fluid or 2 fluids) where the dispersions are stabilized through the use of interfacial active molecules or particles. Such systems also include particulate suspensions (such as paints, paper, soil, clays and so on), which are often stabilised by surface charges. However, in other cases the mixtures are not stabilised and phase separation occurs through coarsening. The phase separation process can be important as it determines the structure of the final material. For example, metal alloys with special microstructure are made by cooling from a temperature above the melting temperature, similarly to many polymer systems. Meanwhile, particles can aggregate as the solid phase comes out.

There is a wide range of systems that exhibit phase separation and my thesis has concentrated on the study of various types of such systems. I have studied the phase separation of a transparent system in the miscibility gap in China, but in 09.2013 as I got the opportunity to spend one and a half years in France as part of my studies I concentrated on slightly different systems. My project is to study the ion specific

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effects on the aggregation of soft matter systems. Therefore, in my thesis, Chapter 4 is my work in China and Chapter 5, 6, 7 and 8 are the work in France.

My work in China concentrated on studying the phase separation in the miscibility gap. When the temperature is quenched into the miscibility gap, a phase separation process occurred. Which is either nucleation growth (NG) or spinodal decomposition (SD). The study of the phase separation pattern in the miscibility gap is significant from a practical viewpoint for providing a novel approach to create special regular microstructures. This suggests that it is necessary to study the evolution of microstructure under certain conditions and formation kinetics of minority phase. In this dissertation, a transparent system with a miscibility gap is used to investigate the aging of microstructure for SD and NG type with the thermal gradient and the growth rate of minority phase with isothermal field.

In France I worked on making stable foam through the formation of a gel inside the foam. Adding salt to the dispersion of colloidal particles can lead to aggregation due to screening of repulsive electrostatic force between particles and make gels, which have many applications such as in food and material science. It's important to know how the gel ages with time, which has already been widely studied. However, previous studies tend to observe the macroscopic gelation time and using the same salt at various concentrations when comparing the gel properties. In this dissertation, we first observe the microscopic gelation time and then compare the gel properties in the presence of different types of salts.

Obtaining stable foams is an important issue in the view of their large variety of applications. There are many ways to make stable foams up to now. However, many of them are complicated. In this dissertation, by adding high concentrations of salt (NaCl or KCl) to surfactant SDS, ultrastable foam can be made and the foam is temperature sensitive. In addition, solid foams also have numerous applications due to their low mass density and high surface area properties. This indicates that it's important to know how the aging of bubbles during the foam changes as the continuous phase goes from a liquid to a solid (gel). In this dissertation, gel phase is used to modify the foam stability.

Outline of the thesis is as follows:

Chapter 2 gives an overview of the different concepts that are used in the rest of

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the manuscript.

Chapter 3 describes the experimental methods and materials used.

Chapter 4 Presents SD and NG type phase separation in the miscibility gap. Under the temperature gradient, layer structures can be formed with both types but their morphologies are not the same due to the higher growth rate and volume fraction of minority phase with SD type. If the parameters are controlled appropriately, multilayer structure can be formed as well. In the high speed solidification process, the initial network like structure of SD type can be preserved. So these two types can produce different morphologies both in the early and late stages of phase separation.

Chapter 5 describes the gelation process in the presence of salt NaCl or KCl. Macroscopic and microscopic timescales show that the solidification with KCl is much faster than with NaCl. But their properties can be scaled onto a single master curve, both the local structure and rheology. This suggests that the ion types only change the kinetics but not the final structure of gels. At the same timescale, the gel structure formed is more flexible with NaCl and more robust with KCl.

Chapter 6 continues the study started in Chapter 5 and explores the kinetics of gel formation using a wider range of salts, but restricting the experiments to light transmission. The transmitted light intensities can be scaled onto single master curve, showing that (at least at the length-scales probed using light transmission) the gelation process differs only in the kinetics even with a wider range of salts.

Chapter 7 shows that ultrastable foams can be made below the Krafft temperature through adding a high salt concentration NaCl or KCl to SDS. The foams are stable or not dependant on the kinetics of crystal formation. If crystallization is too slow, the foam has time to disappear. If the crystals have time to form on the surfaces of the bubbles the foams are stable over months or until they are heated to melt the crystals at which point they start to age and disappear quickly. However, unstable foam still can be obtained if too much foam produced at certain formed crystals even the crystal formation kinetics is not so slow.

Chapter 8 combines what we have learnt in the previous chapters to try and create solid foams by forming a silica gel inside the foam matrix. Combining the results of rheology measurements, averaged bubble size measurements and the

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correlation behavior, we show that the foam aging can be arrested with higher gel strength and faster gelation time, indicating that the gel strength and gelation kinetics are two important factors to control the foam stability.

Chapter 2 Background

2.1 Phase behavior in miscibility gap

The definition of a miscibility gap from the science dictionary is that the region of temperature and composition in which two kinds of liquids form two layers or phases when brought together. A miscibility gap in the liquid state exists in a considerable number of largely different systems such as organic liquids [1], metal-metal/oxide systems [2, 3], polymer mixtures [4-8], glasses [9], or most common ingredients to daily experience in cooking, water and oil. The list of materials being immiscible in the liquid state is endless.

The materials in the miscibility region have a wide range of applications. For example, immiscible organic liquids are widely used in cosmetic and food industry, metallic systems are often used as switches, electrical contacts and bearing in car engines [3], immiscible glasses are mostly used as shock-resistant ceramics, low-thermal expansion glasses and so on [9].

The phase separation processes in the miscibility gap have a strong effect on the

final microstructure. Therefore, studying the phase behavior in the miscibility gap can lead to a better understanding and control of the microstructure.

2.1.1 Thermodynamics of liquid-liquid phase separation

According to the theory of thermodynamics, the system can spontaneously occur only when the change of Gibbs free energy is less than 0, the liquid-liquid phase separation obeys this criterion too. In the following we will use the law of regular solution to discuss the thermodynamic process of liquid-liquid phase separation.

When components A and B exist independently, the free energy of the system is given by Equation 2.1 as

$$G_{(A+B)}^L = x_A G_A^L + x_B G_B^L \quad (2.1)$$

Where x_A , x_B are the molar fractions of A and B respectively; G_A^L , G_B^L are the molar free energies of A and B; $G_{(A+B)}^L$ is the molar free energy of the whole system when A and B are not mixed.

The molar free energy of mixing A and B, at constant temperature T and pressure P, can be written as

$$G^L = G_{(A+B)}^L + \Delta G_{mix} \quad (2.2)$$

where ΔG_{mix} is the molar mixing free energy.

According to the Helmholtz-Gibbs Equation, the relationship between molar mixing free energy ΔG_{mix} and molar mixing enthalpy ΔH_{mix} and molar mixing entropy ΔS_{mix} as

$$\Delta G_{mix} = \Delta H_{mix} - T \Delta S_{mix} \quad (2.3)$$

For a regular solution, ΔH_{mix} can be expressed as

$$\Delta H_{mix} = \Omega x_A x_B \quad (2.4)$$

Where Ω is a coefficient related to the change of free energy and coordination number when components A and B mixed. x_A and x_B are the molar fraction of A and B, and satisfy the relationship $x_A + x_B = 1$. From statistical thermodynamics, we know that the mixing entropy of the solution can be expressed as

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$$\Delta S_{mix} = -R(x_A \ln x_A + x_B \ln x_B) \quad (2.5)$$

Where R is the gas constant. x_A and x_B are smaller than 1, so ΔS_{mix} is always positive.

The mixing free energy ΔG_{mix} is given by Equations (1.3), (1.4) and (1.5) as

$$\Delta G_{mix} = \Omega x_A x_B + RT(x_A \ln x_A + x_B \ln x_B) \quad (2.6)$$

The second term on the right of Equation (1.6) is negative, so a value of mixing free energy higher or lower than 0 depends on the first term. There are two conditions:

(1) For exothermic solutions, the mixing enthalpy $\Delta H_{mix} \leq 0$ at all temperatures and all compositions mixed results in the decrease of the free energy ($\Delta G_{mix} < 0$). The system can occur spontaneously.

(2) For the endothermic solutions, the mixing enthalpy $\Delta H_{mix} > 0$, and whether the system can occur spontaneously depends on the temperature and composition of the system. When the temperature is high, $T\Delta S_{mix}$ is higher than ΔH_{mix} for all the compositions and ΔG_{mix} is still lower than 0 as shown in Figure 2.1(a). Therefore, the system still can occur spontaneously. When the temperature is low, for some compositions $T\Delta S_{mix}$ is higher than ΔH_{mix} and for some compositions $T\Delta S_{mix}$ is lower

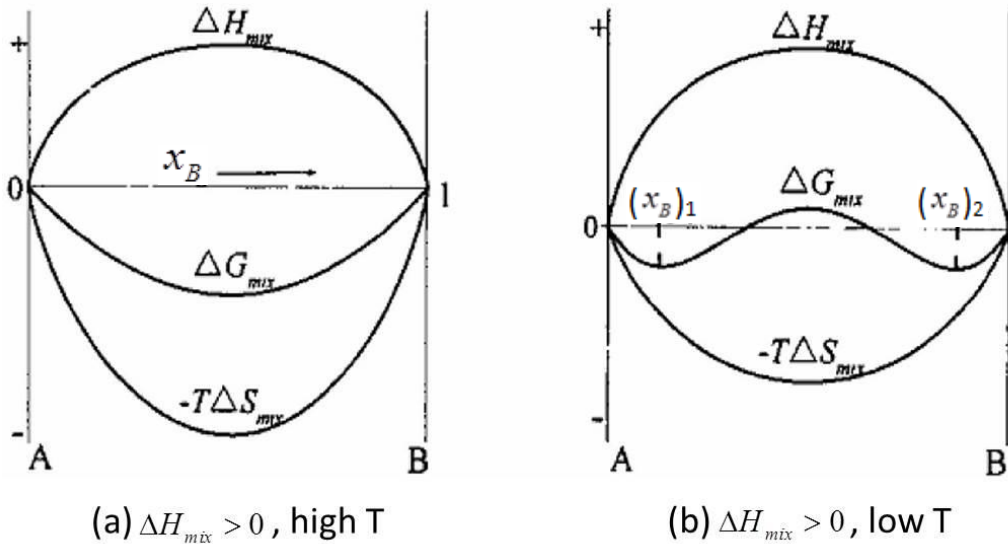


Figure 2.1 The curves of mixing Gibbs-free energy (ΔG_{mix}) at different temperatures when the mixing enthalpy $\Delta H > 0$, A and B represent two components, x_B represents the molar fraction of component B, ΔS_{mix} is the molar mixing entropy and T is the temperature. (a) at high temperature, (b) at low temperature.

than ΔH_{mix} , so ΔG_{mix} is not always lower than 0 at all the compositions as shown in Figure 2.1(b). In other words, the system cannot occur spontaneously at all the compositions.

2.1.2 Kinetics of liquid-liquid phase separation: Nucleation growth and spinodal decomposition

Figure 2.2(a) gives the curve of ΔG_{mix} plotted versus x_B at temperature T_1 . The points A and B represent the points where the straight dashed red line touch A and B is tangential to the curve and called the binodal points. All the binodal points at all the temperatures make the binodal curve, which can be obtained from the Equation

$$\left(\frac{\partial \Delta G_m}{\partial x_B} \right)_T = 0$$

Put into Equation (1.6) this gives

$$\begin{aligned} \Omega(x_A - x_B) + RT \ln \frac{x_B}{x_A} &= 0 \\ T &= \frac{\Omega(1 - 2x_B)}{R \ln \left(\frac{1 - x_B}{x_B} \right)} \end{aligned} \quad (2.7)$$

This is the Equation of the binodal curve in a liquid-liquid immiscible gap as shown in Figure 2.2(b).

The points P and Q are the points of inflection, where the curvature of the curve ΔG_{mix} changes sign, and are called the spinodal points. All the spinodal points at all the temperature range assemble the spinodal curve, which can be obtained from the Equation

$$\left(\frac{\partial^2 \Delta G_m}{\partial x_B^2} \right)_T = 0$$

Used with Equation (2.6) this gives

$$\begin{aligned} -2\Omega + RT \left(\frac{1}{x_A} + \frac{1}{x_B} \right) &= 0 \\ T &= \frac{2\Omega}{R} x_B (1 - x_B) \end{aligned} \quad (2.8)$$

This is the Equation of the spinodal curve in a liquid-liquid immiscible gap as shown in Figure 2.2(b).

From Figure 2.2 we can see that the spinodal curve separates the liquid-liquid

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miscibility gap into another two regions:

(1) Metastable region: The region between binodal curve and spinodal curve, where the phase separation pattern is called nucleation growth (NG).

(2) Unstable region: The region surrounded by the spinodal curve, where the phase separation pattern is called spinodal decomposition (SD).

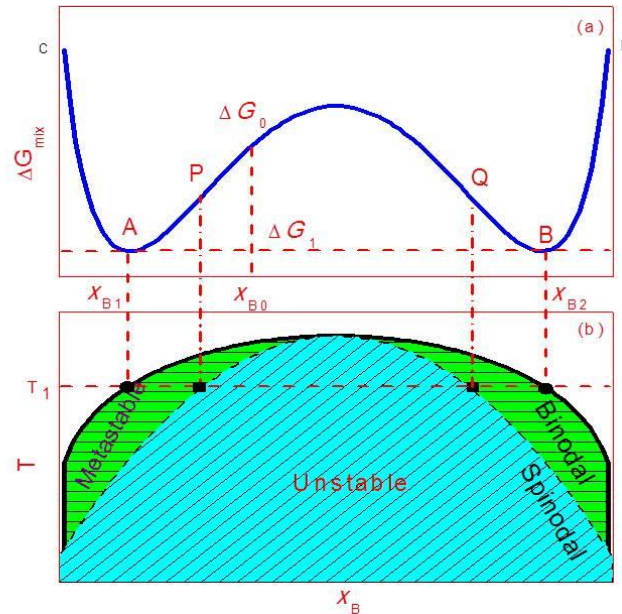


Figure 2.2 Schematic diagram of ΔG_{mix} versus X_B at temperature T_1 (a) and the formed binodal and spinodal curves (b).

NG type phase separation is associated with metastability, which means that the existence of an energy barrier, small fluctuations in compositions can lead to the increase of the free energy. However, it can decrease for larger fluctuations if the mixture separates into two phases of compositions corresponding to the two points A and B in Figure 2.2(a). In this condition, domains of a minimum size, of the so-called critical nucleation radius, are necessary. The concentration profile of NG is illustrated in Figure 2.3(a) [10], this kind of phase separation mechanism results in domain size increasing with time and the domains tend to be spherical in nature.

As shown in Figure 2.2(b), SD type phase separation is associated with instability, which takes place in a completely different way compared with NG type. Small fluctuations in composition between the point P and Q as shown in Figure 2.2(a) can lead to the lowest free energy. The concentration profile of SD is illustrated in Figure 2.3(b), a continuous growth of the amplitude of a concentration fluctuation

without change the wavelength, starting from the infinitesimal values and to the final state of the two equilibrium phases. The initial phase separation structure is interconnected. However, it must be pointed out that with time both kinds of domains (NG and SD) may coalesce and form larger and larger spherical structures in the late stages of phase separation.

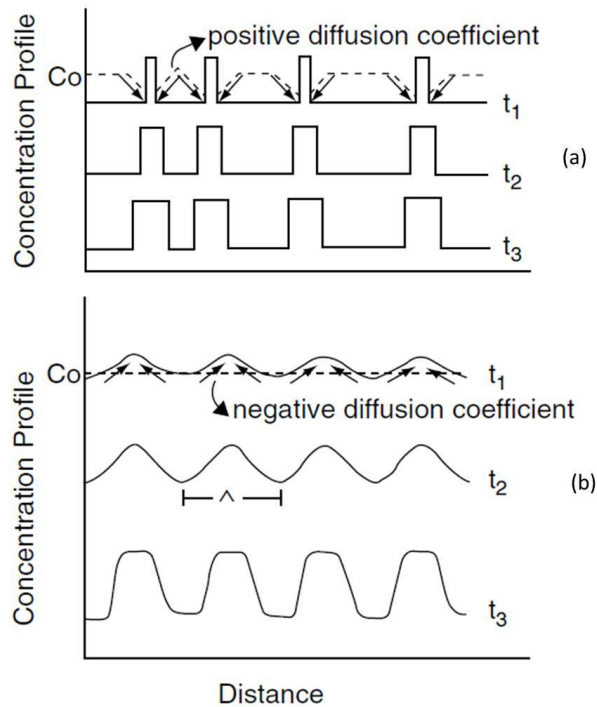


Figure 2.3 Schematic drawing of the concentration profiles during phase separation [10] via (a) nucleation and (b) spinodal decomposition.

2.1.3 Schematic phase diagram type of the systems with miscibility gap

For the variety of systems with a miscibility gap, normally there are two types phase diagram as shown in Figure 2.4, the solid line is binodal line and the dash one is the spinodal line [11]. (a) is the first type with a lower critical solution temperature (LCST) above which there are two phases with increasing T that a certain range of concentrations increase in width and below which there is a single phase for all the compositions. (b) is the second type with an upper critical solution temperature (UCST) below which there are two phases with decreasing T that a certain range of concentrations increase in width and above which there is a single phase for all the concentrations. Normally, many polymer systems have LCSTs, and most solutions of

small molecules have UCSTs. However, more complicated type of behavior with more than one UCST or LCST or neither type of critical solution temperature are also observed for polymers.

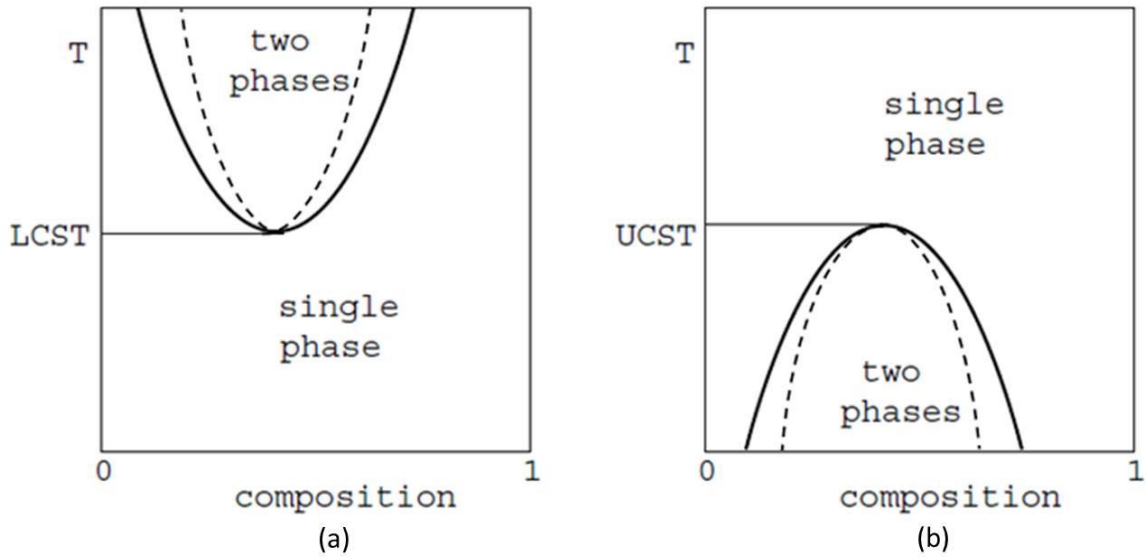


Figure 2.4 Schematic phase diagrams for mixtures showing binodals and spinodals with (a) lower and (b) upper critical solution temperature.

2.1.4 Marangoni force

Young, Ratke et al [12-15] showed that in the liquid-liquid miscibility gap if there is an interfacial tension gradient between the second phase droplets formed through NG or SD and the matrix phase, the droplets would be pushed to the lower interfacial energy region by the Marangoni force [15], which results from the interfacial tension gradient. The resulting terminal velocity of the droplets is given by

$$v_m \approx \frac{-2r}{3(3\mu_d + 2\mu_m)} \cdot \frac{\partial \sigma}{\partial T} \cdot \frac{\partial T}{\partial x} \quad (2.9)$$

Where r is the radius of the droplet, μ_d and μ_m are the viscosities of the droplet and the liquid matrix, σ is the interfacial energy, T is the temperature, and x is the distance.

2.2 Colloidal gels

Colloids are particles that are small enough to be influenced by thermal fluctuations and not dominated by gravity. This means that they typically have a size in the range from around 1nm to 1 μ m. Colloidal particles are important in many fields of science and technology, in particular to change the rheological properties of fluids [16-21]. Often, the dispersed colloidal particles are insoluble in water, but stabilized to form aqueous dispersions through electrostatic repulsion, which should be stronger than the Van der Waals attraction.

However, if the suspension is destabilized the particles aggregate and can form a gel. The basic definition of a gel from Britannica encyclopedia: coherent mass consisting of a liquid in which particles are either dispersed or arranged in a fine network throughout the mass. In rheological terms the gel point can be defined as the point where the Storage modulus (G') becomes higher than the Loss modulus (G'') indicating that the fluid has transitioned from fluid like behavior to solid elastic behavior [22]. However, the resulting gels can be very different, they can be jellylike or elastic, or quite solid and rigid (like silica gels) [23].

Previous experiments and theoretical predictions have shown that the gelation of any particle system with short-range attraction is a direct consequence of liquid-gas phase separation [24-27]. The typical phase diagram of particle gelation with short range attraction (for example due depletion because to the addition of polymer) is given in Figure 2.5, where you can see the red binodal line and black dashed spinodal line as in the systems with miscibility gap. The x-axis is the packing fraction and the y-axis is temperature, which is inversely related to the attraction strength. The scenario of an arrested phase separation is observed if a quench is performed at a temperature below the temperature T_g^{sp} . On the other hand, if the temperature is higher than T_g^{sp} in the two phase region, the system would undergo a standard phase separation into a gas and liquid phase [28].

Gels have a variety of applications and can be produced in many systems. In this dissertation, we are working with charged colloids by adding salt to screen the repulsive electrostatic force between them to make gel. This is the reason why we only talk about colloidal gels.

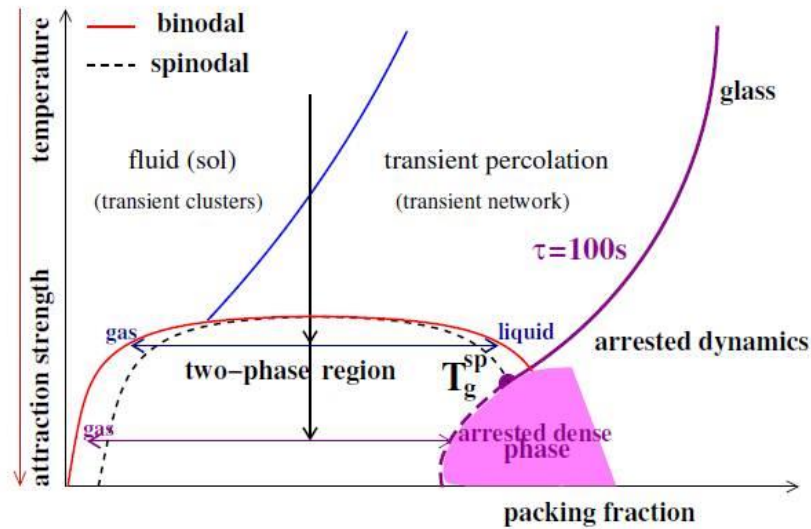


Figure 2.5 Schematic picture of the interrupted phase separation or arrested spinodal scenario [29].

2.2.1 DLVO theory

As discussed above, the repulsive electrostatic and the attractive van der Waal forces play an important role in the stability of colloidal particle dispersions. In this setting, the interaction between these two forces can be qualitatively explained using the theory developed by Derjaguin, Landau, Verwey and Overbeek (DLVO)[30].

A major advance in colloidal science occurred during the 1940s when two groups of scientists-Boris Derjaguin and the renowned physicist Lev Landau in the Soviet Union and Evert Verwey and Theo Overbeek in the Netherlands-independently published a quantitative theoretical analysis of the problem of colloidal stability. The theory they proposed became known by the initial letters of their names: DLVO, which assumes that the more long-ranged interparticles interactions mainly control colloidal stability. Two types of force are considered. A long range van der Waals force ($U_A(r)$) and a repulsive double-layer force ($U_C(r)$) [31, 32]. The total interaction between the charged particles is thus given by a sum of the Van der Waals attraction and the Coulombic repulsion:

$$U_{DLVO} = U_{VDW} + U_{EL} \quad (2.10)$$

The fast aggregation (the aggregation process is solely limited by mutual diffusion or Brownian motion) of colloidal systems is governed by an attractive

interaction potential and the slow aggregation (the aggregation process is limited by some remaining repulsive electrostatic forces) is controlled by a thermally activated energy barrier crossing. The aggregation of particles is faster at higher salt concentrations or for weakly charged particles, while it is slower at low salt concentrations or for highly charged particles [31, 33]. The transition from an attractive potential to a barrier controlled aggregation is called the critical coagulation concentration (CCC). The DLVO theory has successfully predicted how the CCC decreases with an increased ion valence, consistent with the Schulze-Hardy rule. Since the 1940s, the theory has been widely used to explain different phenomena found in colloid science. It has worked reasonably well for low electrolyte concentrations, where electrostatics dominates [34-36].

The DLVO theory for the stability of lyophobic colloidal suspensions is based on the hard sphere-like colloidal particles interacting with the point-like ions through the Coulomb potential. It showed that the primary minimum interaction potential between colloidal particles is arising from the mutual van der Waals attraction, which is not accessible at low electrolyte concentrations because of a large energy barrier. When the electrolyte concentration is higher than the critical coagulation concentration (CCC), the barrier height of the energy drops down to zero, which leads to the aggregation of colloids and precipitation. However, the DLVO theory predicts that the CCC should be the same for all monovalent electrolytes, which is apparently not the case [37-41]. The total interaction between the particles should include the non-DLVO force, such as the dispersion force and so on:

$$U = U_{VDW} + U_{EL} + U_{DIS} + \dots \quad (2.11)$$

We will describe the specific salt effects more in section 2.4.

2.2.2 Gel structure

Once the colloids are no longer stable in solution they start to aggregate. Depending on their concentration they form different types of structures. In many cases the aggregation process leads to the formation of a gel, so a large solid network that spans macroscopic space. However, at very low volume fractions of colloidal particles, the aggregation can be so slow that the clusters sediment before they can form a spaces panning gel [42, 43]. Classical light scattering studies of the

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aggregation of colloidal particles show that the structure of the aggregates can be characterized in the frame of fractal geometry using the equation:

$$S(q) \sim q^{-D_f} \quad (2.12)$$

Where $S(q)$ is the structure factor, q the scattering vector, and D_f is the fractal dimension [44-46]. This method is what the researchers often use to get the structure of gels.

Lin et al [47-50] have shown that using a combination of dynamic and static light scattering. Colloidal aggregation exhibits two universal limits: diffusion limited colloid aggregation (DLCA) which is characterized by a complete destabilization of the colloidal suspension with aggregation taking place upon every collision and reaction limited colloid aggregation (RLCA) for which some remaining electrostatic forces allow only a small fraction of collisions to result in aggregation. The structure of the aggregates in DLCA is rather open and a fractal dimension of $D_f \sim 1.8$ has been found both in experiments and computer simulations [50]. For comparison, the lower sticking probability in RLCA results in denser aggregates with $D_f \sim 2.1$, which has also been confirmed in experiments and computer simulations [49, 51-53].

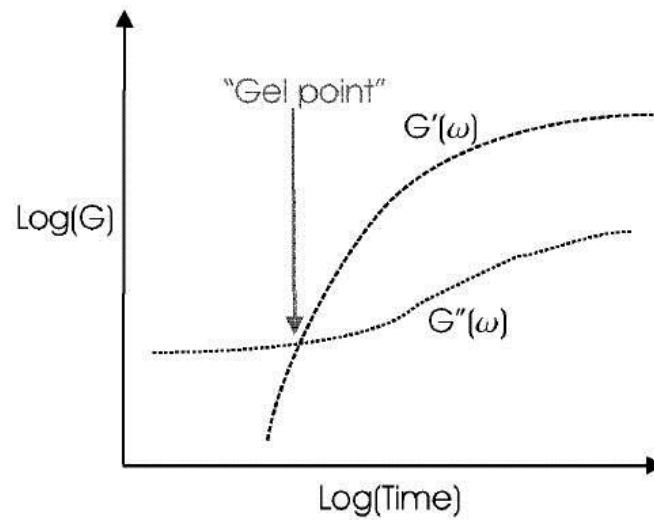


Figure 2.6 A schematic illustration of the storage modulus (G') and the loss modulus (G'') evolution with time during gel formation [54].

The aggregate structures are linked to the mechanical properties of the gels. Small amplitude oscillations are often performed to monitor the gel formation in colloidal dispersions as illustrated in Figure 2.6, where the storage and loss moduli are

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shown as a function of time measured at a certain frequency and amplitude. The storage modulus (G') in viscoelastic solids measures the stored energy, representing the elastic portion; the loss modulus (G'') measures the energy dissipated as heat, representing the viscous portion. As the definition given in the previous part, the gel point shown in Figure 2.6 is the point where storage modulus is equal to the loss modulus indicated by the black arrow. The mechanical properties of colloidal gels are important in many technological areas. The fabrication of products such as paper, paint, pharmaceuticals, composites, or ceramics is often based on colloidal processing.

2.3 Foam

Aqueous foams are formed by the dispersion of gas bubbles in a water phase [55, 56]. In order to generate the foam, energy is needed to create the interface between the liquid and gas. The interfaces cost energy, which is why without suitable stabilizers foams are completely unstable and disappear very quickly. In order to prolong their stability various stabilizers are used, the stabilizers adsorb onto the gas/liquid interfaces. In this section I will summarize the basic properties of foams, in particular how they age and how their ageing can be slowed down or controlled. However, I will start by a short section describing surfactants which is what I have used to stabilize the gas/water interfaces.

2.3.1 Surfactants

Surfactant molecules have two parts one that is water soluble (oil insoluble) and another that is water insoluble (oil soluble). This gives rise to their unique properties and makes them adsorb onto interfaces and to modify the surface properties. In aqueous foams the surfactant molecules adsorb on the surfaces of the bubbles, with the water soluble hydrophilic head groups in the water phase and water insoluble hydrophobic tails extend into the gas phase.

Surfactants adsorb onto interfaces, and because of the hydrophobic parts they have a limited solubility in water. As more and more surfactant is added into solution at some point the surfactants no longer stay as monomers but start to aggregate, to form micelles (although other assemblies are also possible). The concentration at

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which micelles start to form is called the critical micellar concentration (CMC), at this point the surface tension also saturates to almost a plateau. In some surfactant systems there is no CMC, but as the concentration increases at some point the surfactants precipitate out of solution. This concentration also depends on the temperature and is called the “Krafft boundary” [57].

2.3.2 Foam structure

The physical properties of foam depend strongly on the liquid fraction and the bubble size. The liquid fraction is defined by the liquid contained in a foam, $\Phi_1 = V_1 / V_{\text{foam}}$, the ratio of the volume of liquid to the total volume of the foam. At high liquid fractions, above random close packing of 36 % (critical liquid fraction ϕ_C), they are not called foams, but bubbly liquids. Below this liquid fraction the bubbles become deformed and films are formed between bubbles. Typically the foams are called wet down to a liquid fraction of around 10% and foams below this are dry foams.

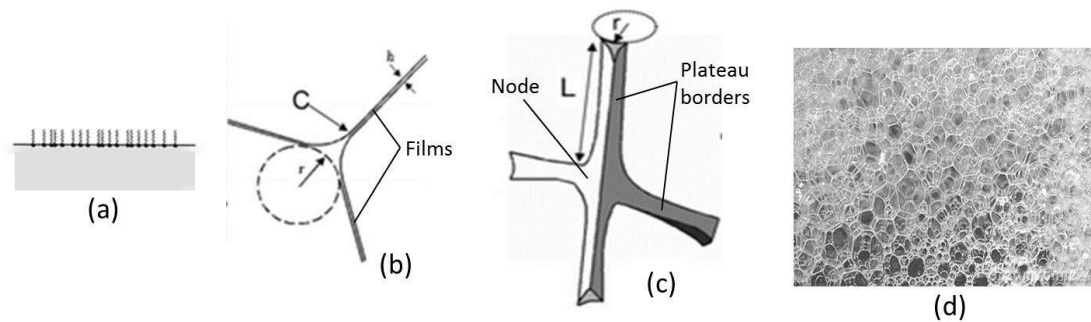


Figure 2.7 (a) Gas-liquid interface. (b) Cross section of a Plateau border with three films attached to it at point C [58], (c) Four Plateau borders (PBs) attached by a node, L is the length of PB and r is the radius of PB [58], (d) Bulk foams.

The bubbles in foams self-organize to minimize the surface energy. Foam structure is complicated as they have specific structural features at a range of length-scales. Starting at the smallest length-scales (nanometers) the surfactants are arranged at the gas/water interfaces to stabilize the foam as shown in Figure 2.7. Where two bubbles meet a film is formed, and their thickness can vary from tens of nanometers up to microns depending on the bubble size and the liquid fraction (b). Where three films join together is called a Plateau border (PB) (b, c) and the junctions

between the PBs are nodes (c). The liquid skeleton of channels inside the foam is then composed of films, PBs and nodes. At even larger length-scales above that of individual bubbles (d) the macroscopic properties of the foam are determined. The properties of the foams is why are they are widely used, but understanding the microscopic origin of the properties is complicated as the properties are determined by those in all the length-scales below.

2.3.3 Foam aging

All foams are thermodynamically unstable. After the generation of foam, the liquid drains, and the bubbles grow with time. Eventually the foam disappears. The three destabilization mechanisms in foam are: drainage, coalescence, and coarsening as schematically illustrated in Figure 2.8.

✧ *Drainage*

Drainage is the flow of liquid out of the foam and it results in drier foams. Gravity driven drainage occurs because of the density difference between gas and water leading to the flow of liquid out to the bottom of the foam. The liquid flows through the network of PBs and nodes, which can be quite narrow. This is why drainage depends strongly on the bubble size and the liquid fraction which determine the size of the channels. Drainage reduces the liquid fraction and leads to the drier foams, however in freely draining foam the foam is not homogeneous and it is the driest at the top (Figure 2.8.a) [55, 58-60].

✧ *Coalescence*

Coalescence (Figure 2.8.b) of the bubbles is due to the rupture of the film, between two bubbles. It is also responsible for the collapse of foam, as the bubbles at the top coalesce with the atmosphere above leading to the complete disappearance of the foam [61].

✧ *Coarsening*

The last destabilization mechanism is coarsening (Figure 2.8.c), which is driven by the Laplace pressure as given by the Laplace-Young equation [62]:

$$\Delta P = \frac{2\gamma}{R} \quad (2.13)$$

where R is the bubble's principle radius of curvature.

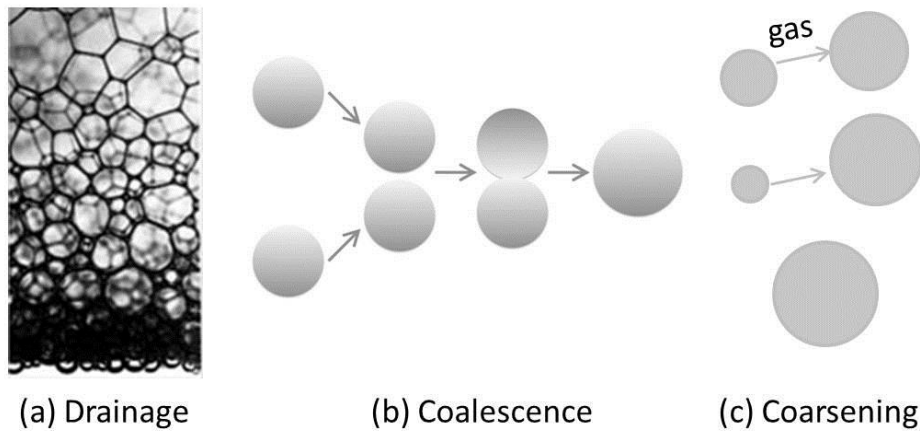


Figure 2.8 Schematic drawing of the three main foam destabilization mechanisms. (a) is drainage of the liquid due to gravity, (b) Coalescence of two bubbles, (c) Coarsening of the bubbles due to the Laplace pressure.

The gas pressure inside small bubbles is larger than inside large ones due to the curvature of the bubble surface. As a consequence, the gas diffuses through the aqueous films from the small towards the large bubbles leading to the disappearance of the smaller bubbles [63]. In this way, the bubbles disappear one after another and the remaining average bubble size increased.

2.3.4 Slowing down the ageing of foam

As discussed above, foams are thermodynamically unstable, although some surfactants are very efficient in slowing down the ageing mechanisms. In order to obtain very long lived (or ultrastable) foams, we need to find ways to radically slow down or even stop the mechanisms that destabilize the foams.

The simplest way to slow down drainage is to increase the fluid viscosity. For instance, adding some glycerol in the liquid phase leads to an increase of the bulk viscosity which leads to a decrease of the drainage rate [64]. However, this will never arrest the drainage. It will just be slowed down. In order to arrest drainage, the continuous phase has to be either solidified (to have a yield stress) or larger particles need to be trapped inside the channels to stop the channels from becoming smaller and therefore to stop the drainage. It has been shown that drainage can be arrested

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using a colloidal gel (made of Laponite), as the yield stress of the gel becomes higher than the gravitational stresses driving the drainage of the foam [65].

In coarsening, the diffusion of gas through the liquid phase is the key step in the process. Therefore using a gas which is poorly soluble or insoluble in the liquid will slow down the gas transport through the liquid phase. Therefore, foam stability is higher in the presence of fluorinated gases than nitrogen or air because their solubility is much lower in water. However, this again does not stop the coarsening completely.

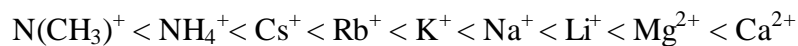
In order to stop coarsening, theoretical and numerical studies on the dissolution of a single bubble have shown that either interfacial elasticity can arrest the foam coarsening when the Gibbs stability criteria is satisfied:

$$E_d > \sigma/2 \quad (2.14)$$

Or the foam coarsening can be arrested through making the bulk elastic enough [66].

2.4 Hofmeister series

All salts are not equal, the first person to classify them according to their ability to salt out or salt in proteins was Franz Hofmeister after who the series of salts is named. According to their ability to precipitate proteins, the order of cations is usually given as follows:



The sequence indicates that the negatively charged proteins remain stable in the presence of high concentration of electrolyte containing the ions on the right side, while they already precipitate at low concentration of electrolyte containing the ions on the left side. Although the first studies of Hofmeister effect was more than 100 years ago [67-69], the reasons behind the ordering in the Hofmeister series are still under debate. In a colloidal system, over more than a half century the aggregation behavior of colloidal particles has been explained quite well with the DLVO theory.

However, as has been discussed in 2.2.1 the CCC predicted by the theory is the same for all the monovalent electrolytes, which is not correct. It can't explain the ion specific effects on the particle aggregation within the Hofmeister series, since it assumes that the ions have no difference except in their valence. In order to solve this

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problem, one of the approaches is based on Collins's concept of matching water affinities [70]. Depending on how the ions interact with water, they can be divided into two main groups: Kosmotropes and chaotropes as given in Figure 2.9. Kosmotropes have a large hydration shell around the ion and experience a repulsive dispersion potential with the surface. In contrast, chaotropes have a poor hydration shell around the ion and experience an attractive dispersion potential [71].

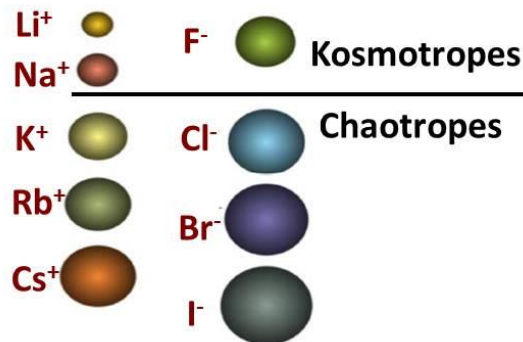


Figure 2.9 The Groups of IA alkali cations and VIIA halide anions are divided into kosmotrope (strongly hydrated) and chaotropes (weakly hydrated) according to their size [70]. The ions are drawn approximately to scale of their bare radii.

2.4.1 Ions at interface

Although the properties of bulk electrolyte solutions can be described by the theory of Debye and Hückel (DH) [72], the surface properties of electrolytes remain a puzzle. The mystery first appeared when the surface tension of various electrolytes was measured by Heydweiller [73] and it was observed that it is larger than the interfacial tension of pure water. Recently theory and experiments have given new insight into this problem. By using only one adjustable parameter—the hydrated radius of sodium cation, $a_h=2.5 \text{ \AA}$, Levin *et al.* [74] presented a new theory which can explicitly calculate the surface tension, the ionic density profiles, and the electrostatic potential difference across the solution-air interface. Predictions of the theory are found to be in excellent agreement with the experiments. Schelero *et al.* [75-78] investigated salt effects on the film thickness and stability of wetting films. They found that with increasing the ion size (decreasing charge density), both cations and anions show a stronger tendency to adsorb at the interface. The results demonstrate that the effect of the hydration shell of ions dominates over electrostatics on their adsorption at the air-water interface.

Except the air-water interface, the ions are absorbed on the surfaces of the colloidal particles screening the electrostatic interactions and leading to the aggregation of the colloidal particles [38-40, 79-81]. Oncsik *et al.* showed that the differences in the aggregation rates in the presence of different types of salts could be rationalized by taking into account the changing surface charge with the varying ion adsorption [82], poorly hydrated counterions adsorb strong on the surface of hydrophobic latex particles and well hydrated counterions adsorb weakly or not at all.

2.4.2 Interactions between colloidal particles in the presence of electrolyte

The interactions between colloidal particles in aqueous electrolytes solution are relevant to fields ranging from molecular biology and bioengineering to the colloidal-based technologies. As we discussed above, for more than half century, their interactions are explained by the famous DLVO theory [83, 84], which is a very successful theory can reproduce many phenomena. However, specific ion effects are not taken into account in this theory.

Over the past 20 years, there has been a growing realization the importance of ionic polarizability (the effective rigidity of the electronic charge distribution), which play a significantly role in the ion specificity [85-88]. Ninham *et al.* [37, 89, 90] developed a more analytical approach to ion specificity published a series papers over the past decade and a half. They proved that the proper inclusion of quantum mechanical non-electrostatic dispersion interactions missing from the classical theories of electrolytes can explain ion specific effect at surfaces and in colloidal suspensions. The London-Lifshitz theory predicts that the dispersion interaction between a surface and an ion decays with the third power of separation and is proportional to the ionic polarizability [91]. The chaotropic ions (K^+ , Cs^+) have an attractive dispersion potential with the micelle surface and the kosmotropic ions (Li^+ , Na^+) have a repulsive dispersion potential [71]. Force measurements between silica surfaces in electrolyte solutions have given results consistent with the above theory. Taking ions at the same concentration, more chaotropic ions adsorbed onto the silica surfaces leading to a smaller force between the silica surfaces compared with the kosmotropic ions. Moreover, as the ion concentration is increased more cations adsorb to the negatively charged silica surface and neutralize the surface charge, leading to screening the electrostatic repulsion to reveal the Van der Waals attraction. However,

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the concentration needed to neutralize the surface is not the same for different cations, and it decreases as the cation radius increase. At even higher salt concentrations, repulsion reemerges due to the surface charge reversal by excess adsorbed cations [92]. Oncsik et al [82] also show that the ions of SCN^- adsorption on positively charges particles leads to charge reversal. Therefore, we can see that the ions with same valence but different radius have different ability to aggregate particles.

Chapter 3 Materials and methods

3.1 Materials

3.1.1 Phase separation

Succinonitrile (SCN, $\geq 99.9\%$) was purchased from J&K and used without further purification. Milli-Q water (18.2 M Ω cm) was used to prepare the samples. Iron(Fe, $\geq 99.99\%$) and tin(Sn, $\geq 99.999\%$) were purchased from Alfa Aesar. Argon (Ar) was used to eject the melted alloy to form ribbons. The mixture of HNO₃ and alcohol was used to etch the samples.

3.1.2 Gels

Silica particles (Ludox TMA from Sigma Aldrich (TMA in the following)) with a particle diameter of 27 nm (from SAXS measurements) and a stock concentration of 34 wt% were used. The pH of the stock solution measured was 7.0. Sodium chloride (NaCl, $\geq 99.5\%$), potassium chloride (KCl, $\geq 99.0\%$), lithium chloride (LiCl, $\geq 99\%$),

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cesium chloride (CsCl , $\geq 99.9\%$) and magnesium chloride (MgCl_2 , $\geq 99.9\%$) were all from Sigma Aldrich and were used without further purification.

In the light transmission experiments, same silica particles were bought from the above company, but the pH is around 4, so the pH was changed to 7 by the addition of NaOH.

Milli-Q water (18.2 M Ω cm) was used for the preparation of all the samples.

3.1.3 Foam

Sodium dodecyl sulfate (SDS, $\geq 99.0\%$) was purchased from Sigma Aldrich and used without further purification. Sodium chloride (NaCl) and potassium chloride (KCl) were the same as in gel. Milli-Q water (18.2 M Ω cm) and D₂O were used for the preparation of aqueous solutions. Air was used as gas for most of the experiments and perfluorohexane C₆F₁₄ was added for the SANS experiments to slow down foam coarsening. Stock solutions of 1 M NaCl, 1 M KCl and 555 mM SDS were used in the sample preparations. Due to the hydrolysis of the SDS the surfactant stock solution was used within a week of preparation.

3.1.4 Gel foam

Sodium dodecyl sulfate (SDS) and sodium chloride (NaCl) were the same as in the foam. Silica particles were brought from the same company Sigma Aldrich as in the gel and have the same diameter with pH around 4. In all the related experiments, we change the pH of the silica to 8 by using NaOH to make the particles less charged and for the gel to form faster. Perfluorohexane C₆F₁₄ was used as gas to slow down the foam aging. Stock solutions of 4 M NaCl and 555 mM SDS were used in the sample preparations. The stock SDS solution was used within a week of preparation to avoid the hydrolysis of SDS.

3.2 Methods

3.2.1 Sample preparation in miscibility gap and calculation

3.2.1.1 SCN-H₂O system sample preparation

SCN was added to the water solution and heated to 353 K for 20 min, then the samples were immediately injected into the sandwiched cells with a dimension of 25 × 10 × 0.5 mm and sealed. The cell's covers are made of glass and its height was controlled by the Teflon film spacers. During the experiment, a round copper block was used for producing an isothermal field and its temperature was controlled by the 3504 Eurotherm. The isothermal field was used for the micro phase separation of nucleation growth (NG) and spinodal decomposition (SD) and observed by the optical microscope. Two copper blocks with 10 or 12 mm distance were used for producing a uni-directional thermal gradient and their temperature was controlled by the flow inside the copper blocks. The uni-directional thermal gradient was used for the macro phase separation of NG and SD simultaneously (the samples were put side by side or separated) and observed by a Samsung camera. The samples were immiscible at room temperature, and they were put in copper block at 353 K for 5 min before put in the copper block for observation.

3.2.1.2 Fe-Sn ribbons preparation

The Fe-Sn alloys were melted by radio-frequency (RF) induction heating and overheated to about 100 K above its liquidus temperature for several minutes under an argon atmosphere in a 13 mm ID × 15 mm OD × 160 mm fused silica tube. The overheated samples were ejected by Ar atmosphere with an overpressure of 50 kPa through a nozzle ($\phi=0.7$ mm) at the bottom of the silica tube onto a Cu single roller. The wheel speed was set as 3 or 10 m/s.

Then the Fe-Sn ribbons were mounted in epoxy, sectioned, polished, and etched with a mixture of 3 mL HNO₃ + 100 mL alcohol. The solidification microstructures were examined by Zeiss MAT optical microscope and TESCAN VEGA3 LMH scanning electron microscopy (SEM). The chemical compositions of the identified constituent phases were determined with an energy dispersive spectrometer (EDS) fitted in SEM.

3.2.1.3 Calculation of the spinodal curve and volume fraction

According to the theories of the thermodynamics, the spinodal curve is calculated under the condition, $\partial^2\Delta G/\partial^2x=0$, for given temperatures, in which ΔG is the difference in Gibbs free energy during phase transformation, and x is concentration.

On the basis of the thermodynamic theories, ΔG can be expressed as [93]

$$\Delta G = RT \sum_i x_i \ln x_i + \sum_i \sum_{j>i} x_i x_j \sum_{k=0}^n {}^k L_{i,j} (x_i - x_j)^k \quad (3.1)$$

where R is the gas constant, T the temperature, x_i and x_j denote the concentrations of pure substances i and j , ${}^k L_{i,j}$ is the k th binary interaction parameter between i and j and may dependent on the temperature as $A+BT$, in which A and B are model parameters.

For SCN-H₂O system, ${}^k L_{i,j}$ s are given as follows ($k = 0, 1, 2, 3$) [94]

$$\begin{aligned} {}^0 L_{SCN,H_2O} &= 19240 - 44.85T \\ {}^1 L_{SCN,H_2O} &= -9871 + 25.32T \\ {}^2 L_{SCN,H_2O} &= 9412 - 25.52T \\ {}^3 L_{SCN,H_2O} &= 19181 - 60.85T \end{aligned} \quad (3.2)$$

For Fe-Sn system, ${}^k L_{i,j}$ s are given as follows ($k = 0$) [95]

$${}^0 L_{Fe,Sn} = 6676 + 12.818T \quad (3.3)$$

The spinodal curves of the SCN-H₂O and Fe-Sn systems are calculated on the basis of the above equations.

3.2.1.4 Calculation of the volume fraction

The density of SCN is 0.985 g/cm³, which is close to the density of water 1 g/cm³. So the volume fraction is close to the mass fraction in the phase diagram. The schematic phase diagram in the miscible gap is shown in Figure 3.1. When the temperature is quenched to T , a sample with composition C separates to two phases L_1 and L_2 , the corresponding concentration were C_1 and C_2 . We use the lever rule to

calculate the volume fraction, the volume fraction of L_1 is $f_{L_1} = \frac{C_2 - C}{C_2 - C_1}$ and

$f_{L_2} = 1 - f_{L_1}$. T_M is the bottom temperature of the miscibility gap.

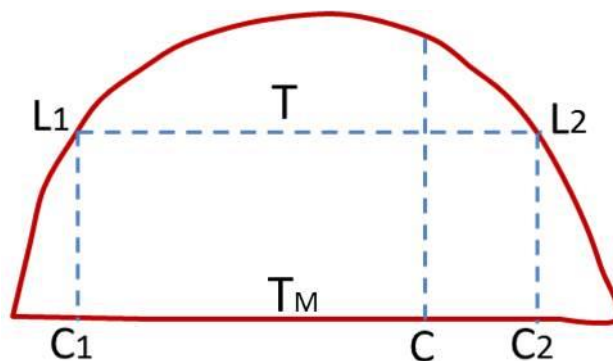


Figure 3.1 Schematic phase diagram in the miscible gap.

3.2.2 Gel sample preparation and measurements

3.2.2.1 Gel sample preparation and rheology measurement

Silica stock was added to salt solutions ranging from 0-500 mM in concentration and immediately agitated with a vortex mixer for 10 s to ensure homogeneous mixing. Samples were then sealed to avoid solvent evaporation and stored for observation - save for those samples prepared for SAXS and rheological experiments. These were immediately transferred into SAXS capillaries (see below) and into folded paper containers respectively, both of which were sealed and stored until the measurements. The paper containers allowed transfer of the samples into the rheometer with minimal perturbation.

After the gels go from liquid to solid, there are several two ways to measure how their mechanical properties evolve. One way is to measure G' and G'' at different time after gelation by using small amplitude oscillations (fixed frequency of 10 Hz and strain 1 %), another way is to measure G' and G'' at fixed time by using the strain sweep measurement (at constant strain rate amplitudes $5s^{-1}$, where the strain is from 0.05 to 25). The former is to obtain the mechanical properties evolution with time without destroying the structure of gel and the latter is to acquire the mechanical properties evolution with strain at breaking the gel structure. From these

measurements, we can know how the gel ages with time its yield strain.

3.2.2.2 SAXS measurements

The SAXS measurements were performed at the European Synchrotron Radiation Facility (ESRF, Grenoble, France) on the bending magnet beamline BM02 (D2AM), at a photon energy of 7 keV. The experimental setup is described in detail in reference [96]. The data were acquired using a CCD Peltier-cooled camera (SCX90-1300, from Princeton Instruments Inc., New Jersey, USA) with a resolution of 1340×1300 pixels. Data preprocessing (dark current subtraction, flat field correction, radial regrouping and normalization) was performed using the *bm2img* software developed at the beamline.

The samples were contained in cylindrical glass capillaries (Mark-Rörchen) 1 mm in diameter and the exposure times were between 2 and 10 seconds, depending on the concentration. The samples which phase separate were measured in the lower solid-like phase.

3.2.2.3 Modeling SAXS data

The intensity scattered by the spherical silica colloids can always be written as:

$$I(q) = \Delta\rho^2 \times n \times S(q) \times P(q) \quad (3.4)$$

where $S(q)$ is the effective structure factor, $P(q)$ is the form factor of individual colloids which is a constant characteristic of the system, $\Delta\rho$ is the electronic contrast of the colloids and n is the colloidal density.

The form factor, $P(q)$, in the case of spherical silica colloids is [97]:

$$P(q) = |F(q,R)|^2 = \left| 3 \times \frac{\sin(qR) - qR \times \cos(qR)}{(qR)^3} \right|^2 \quad (3.5)$$

where $F(q,R)$ is the scattering amplitude of a sphere of radius R .

Experimentally, the form factor (in fact $\Delta\rho^2 \times n \times P(q)$) can be evaluated in two ways: i) from the scattered intensity $I(q)$ of dilute solutions with high salt concentration (where the electrostatic interaction is screened, and the structure factor can be considered equal to 4); ii) from adjusting the scattering intensity $I(q)$ at high q -values from various individual curves; a method allowing to estimate the uncertainty on R and the effective values of $\Delta\rho^2 \times n$.

The effective structure factor is then obtained for each image as:

$$S(q) = \frac{I(q)}{\Delta\rho^2 \times n \times P(q)} \quad (3.6)$$

During the formation of gels, $S(q)$ becomes time-dependent (since $I(q)$ is also time-dependent due to the clustering of the colloids) and is composed of two different contributions: i) the contribution of the effective interactions between individual colloids inside the clusters; ii) the contribution of the cluster dimension. The first contribution arises at intermediate q -values while the second is at low q -values. In the case of mass fractal gels (as expected at the lowest volume fractions), the latter is characterized by an increase in forward scattering corresponding to the dependence of the signal as q^{-D_f} where D_f is the fractal dimension [44, 45]. However, our experiments probe mainly the local colloidal environment due to the q -range accessible (the lowest q -value is around $4 \times 10^{-3} \text{ \AA}^{-1}$). In addition most of our experiments are at relatively high silica volume fractions where the experimental determination of the fractal dimension from the $S(q)$ is not direct [98]. As a consequence, we use a simple model, where the contribution of the cluster inner structure is taken as a constant baseline, B , to which a power law is added, resulting in $Aq^{-\alpha} + B$. This has been applied for $q < 0.01 \text{ \AA}^{-1}$ on the data once the $S(q)$ have stopped evolving to obtain α . We use the power exponent α to compare the results at different volume fractions.

3.2.2.4 Light transmission observation for gels

Gel samples were prepared the same way as in 3.2.5. After the gel samples were prepared, they were transfer to a black box, light source was provided by the white light. Images were taken by a UEye camera every 5 minutes. Before starting to observe, a black cloth was covered on the black box to avoid environment light to influence the experiments.

3.2.3 Foam sample preparation and stability studies

3.2.3.1 Preparing KDS

KDS was obtained from SDS by an ion exchange in KCl solution [99]. SDS powder was dissolved in KCl solution (1M) at 50 °C up to a ratio of the components

of KCl:SDS = 2:1. Then the solution was allowed to stand at 50 °C for 2 h and at room temperature for next 12 h [99]. The sediment was filtered out using a Shott filter, washed with Milli-Q water and acetone and dried in air until the mass remained constant. The product yield was about 95%.

3.2.3.2 Determination of the dissolution temperature and kinetics of crystal formation

The samples were crystallized by cooling them below the dissolution temperature. The temperature was slowly increased by 1 °C every 30 minutes. Once the crystals started to dissolve this was slowed down to 0.5 °C every 30 minutes. The dissolution temperature was defined as the temperature when the crystals became invisible to the eyes. Then the samples were placed in a water bath heated 1 °C higher than the measured dissolution temperature above until no crystals can be observed. The temperature was then set to the target temperature at which the sample was observed and the time at which crystals started appearing was noted as the crystallization time.

3.2.3.3 Making foam

All the foams were prepared at room temperature ($T=21 \pm 2$ °C), unless otherwise stated in the text. The foams were prepared using a setup consisting of two disposable syringes connected by a constriction. The volume of a syringe is 20 mL and the diameter of the constriction is 2 mm. The syringes are filled with air (with some C_6F_{14} for the SANS experiment) and foaming solution. Salt solution and water start in one syringe, and the SDS solution in another. This ensures that they come into contact only as the foam generation process begins. Different ratios of liquid to gas were used to make the foams, most often 1:4 or 1:8, and the total volume of foam made was varied. The foam is formed by pushing the liquid and gas forward and backward through the constriction 40 times.

3.2.3.4 Foam stability studies

After making the foam, the samples were transferred into glass vials. Images were taken by a UEye camera every 5 minutes at room temperature and at varying intervals when heated (according to the foam disappearance rate). Some of the samples were photographed under a microscope to observe the bubble surfaces more

closely. For the heated samples, the temperature was set above the previously measured precipitation temperature, using the microscope to observe the micro evolution of the foam bubbles and a UEye camera to obtain the foam's macro evolution.

3.2.3.5 Small angle neutron scattering experiments

The experiments were carried out at the Orphée reactor in Saclay on the PAXY spectrometer. Three different configurations were used with wavelengths of $\lambda = 15 \text{ \AA}$ and $\lambda = 4 \text{ \AA}$ and sample to detector distances of 6.75 m and 1.250 m. This gives an accessible scattering vector q-range from 2×10^{-3} to $5 \times 10^{-1} \text{ \AA}^{-1}$. Samples were enclosed in quartz cells of 1 mm inner thickness with pure D₂O as solvent. All the measurements were performed at atmospheric pressure and room temperature. The scattered intensities were corrected for the detector background by cadmium scattering, for the parasitic intensity scattered by quartz cell and empty beam by subtraction and normalized to the water scattered intensity. Standard procedures for data reduction [100] were done using the *Pasinet* software [101]. Absolute values of the scattering intensity, $I(Q)$ in cm^{-1} , were obtained from the direct determination of the number of neutrons in the incident beam and the detector cell solid angle [102]. The scattering intensity of the solute was obtained by subtraction of the intensity of the solvent (measured independently) to the one of the solution. In the following, this final intensity will be noted $I(q)$.

At high q ($> 0.2 \text{ \AA}^{-1}$) the intensity saturates to a constant value for both samples due to the incoherent scattering. The intensity of the sample with KCl is higher, because the foam prepared with potassium is more stable and there is more sample. The foam made with NaCl the foam partially collapsed during the experiment.

3.2.3.6 Calculating the enthalpies of dissolution of NaDS and KDS

The equilibria between crystals and micelles are set by kinetic constants, which depend on the concentrations of the constituents. These kinetic constants can be linked to the change in Gibbs free energy as $\Delta G^0 = -RT \ln K = \Delta H^0 - T \Delta S$ and a Van't Hoff plot will allow us to estimate the enthalpies of dissolution from

$$\ln K = -\frac{\Delta H}{RT} + \frac{\Delta S}{R} \quad (3.7)$$

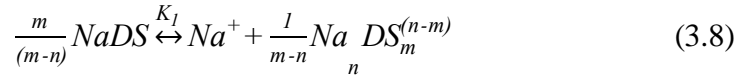
Chapter 3 Materials and Methods

In order to calculate this we need to take several approximations. We assume that the concentration of monomers is negligible (reasonable as we are working with 69 mM DS^- and the CMC of SDS is below 1 mM at the salt concentrations studied [103]). We also assume that the micellar size is sufficiently peaked that we consider only one size of micelle, which does not depend on the salt concentration. We also assume that the counter ion binding does not depend on the bulk salt concentration, and we assume them to be the same and constant value of 0.8 for both salts (the degree of binding has been shown to depend little on temperature [104]).

The case with SDS with the added KCl is much more complicated due to the presence of both Na^+ and K^+ . This is why for both salts we only consider the range of high added salt concentrations (from 0.5 to 1 M). This means that the added salt concentration is much higher than that of the SDS and for the analysis with KCl we can neglect the concentration of sodium ions. The absolute values of ΔH change if we change the range, however we always find ΔH_{SDS} lower than ΔH_{KDS} . This is why we only discuss the difference between the ΔH and not the absolute values.

Dissolution of NaDS

Where n is the number of Na^+ associated with a NaDS micelle and m is the number of monomers per micelle (aggregation number). The melting process can be written as:



Below the melting temperature all of the SDS is in the micelles, so the number of micelles is C_{SDS}/m and $[DS^-] \approx 0$ and the concentration of sodium ions can be written as $[Na^+] = c_{Na} - n[Na_n DS_m] \approx c_{Na} - \beta c_{SDS}$, where for Na^+ the total concentration of sodium includes the counter ions from the SDS molecules as well as the added salt and β is the degree of counter ion binding onto the micelles.

We can describe the reaction coefficient in terms of the known concentrations as: $K_2 = (C_{Na} - \beta C_{SDS}) \cdot \left(\frac{C_{SDS}}{m}\right)^{\frac{1}{m-n}}$. In Figure 3.2 we show the plot of $\ln K_2$ as a function of $1/T$. Assuming a constant enthalpy and entropy, which is not unreasonable considering the linearity of the data, we can get the enthalpy of dissociation of SDS as 75 kJ/mol.

Dissolution of KDS

Thus corresponding equation for melting (with constant K_4) can be exactly analogously to those of SDS. The reaction constant of melting can be simply written as

$$K_4 = (c_K - \beta c_{DS}) \left(\frac{C_{KDS}}{m} \right)^{\frac{1}{m-n}}$$

In Figure 3.2 we also show a plot of $\ln K_4$ as a function of $1/T$. This allows us to extract the enthalpy of dissolution of KDS as 88 kJ/mol.

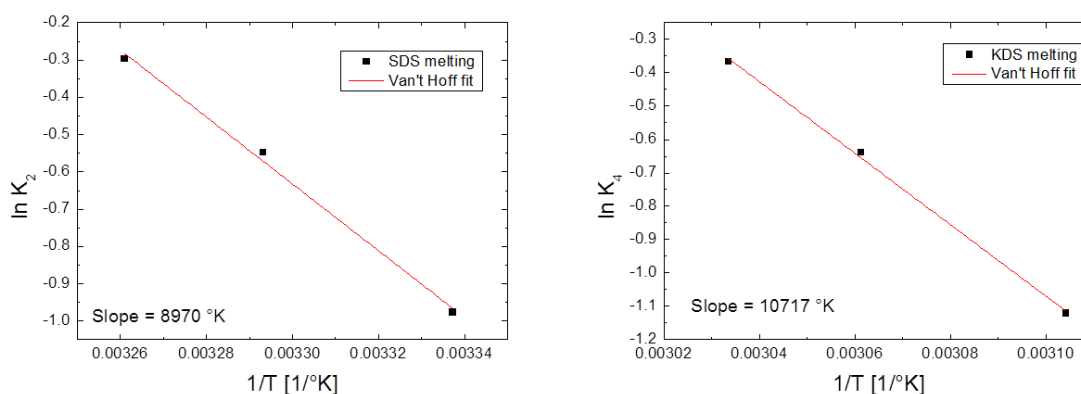


Figure 3.2 The Van't Hoff representations of the SDS and KDS melting temperatures. The lines are linear fits and the slopes are used to calculate the enthalpies of dissolution.

3.2.4 Foam aging with gel phase

3.2.4.1 The way to change pH of the TMA solution

2M NaOH solution was prepared first. Then a certain volume of TMA solution was taken from the bulk solution and put in the glass vial. The solution was stirred using a magnetic stirrer and NaOH solution was added little by little while the pH of the solution was measured. The addition was stopped when the pH of the solution reached 8, at which point the amount of NaOH solution used was noted. For the following solutions the same amount of NaOH was added to the same quantity of TMA solution without measuring the pH again. We considered the pH obtained is 8. However, each time when change the volume of TMA solution, the process to measure how much NaOH solution needed to get pH=8 was repeated again.

3.2.4.2 Making gel foam

All the foams were prepared at room temperature ($T=21 \pm 2$ °C) and generated by the foam machine connected with two syringes at velocity 50mm/s and 20 times. The volume of a syringe is 60 mL and the diameter of the constriction is 2 mm. The syringes are filled with air saturated with C_6F_{14} and foaming solution. Salt solution and water are put in one syringe, and the SDS solution and TMA solution in another. This ensures that they come into contact only as the foam generation process begins. The ratio of liquid to gas was 1:6 and the total volume of liquid was 7 mL.

3.2.4.3 Gel foam studies

After making the gel foam, the samples were transferred into petri dishes, which were fixed with clips and set vertically. A rectangular prism was put in the center of the cell to take high resolution photographs of the surface of the gel foam. Images were taken by a UEye camera every 5 minutes at room temperature.

3.2.4.4 Rheology studies in the bulk gel phase

In order to compare the gel phase evolved in the gel foam, bulk gel rheology was measured using a rheometer. SDS solution, TMA solution, salt solution and water were mixed without making foam and transferred into the double gap of rheometer immediately. We waited for 1 hour and started to measure the storage (G') and loss moduli (G'') at a fixed frequency of 1 Hz and strain 1 %. The measurements continued for three hours, stopped and waited for 20 min, then started again to measure G' and G'' at fixed frequency of 1 Hz and varied strain from 0.01 to 500 %.

Chapter 4 Phase separation mechanisms studied in miscibility gap

4.1 Introduction

In nature, a phase transition proceeds spontaneously if the total free energy of a system decreases, or proceeds along the direction to a low chemical potential. This leads to two manners of phase separation in the system with a miscibility gap: nucleation-growth (NG in the following) and spinodal decomposition (SD in the following) [105, 106]. The miscibility gap, exists in a considerable number of different systems such as fluid mixtures [107-110], polymer mixtures [7, 8], glasses and ceramics [111, 112], and metallic systems [113-115], so the NG and SD processes occur frequently in daily life. For this reason, the understanding of the mechanisms on the phase separation via the two manners is essential in the areas of condensed matter physics, materials science, and biological sciences.

From the point of view of variation in the free energy, the NG-type phase separation is a metastable process and tiny perturbations leads to an increase in free energy. The free energy can only be decreased in the case if nuclei are formed with a composition very different from the matrix. While the SD-type one is an unstable

process. Small perturbations will cause the free energy to decrease and therefore it proceeds spontaneously. From the point of view of the morphology evolution, the new phase formed in NG process is well separated droplet. Whereas in SD process the new phase forms in two stages: in the early stage, long-wavelength delocalized concentration fluctuations grow exponentially and interconnected domains or network like structures are produced. Then in the later stage, the interconnected domains coagulate and evolve into droplets. The characteristic droplets radius r grows with time as $r \sim t^m$, where $m = 1/3$ in the early, purely diffusive stage, and $m = 1$ at a later time, when the surface tension effects become dominate [116, 117]. In the later stage, the growth of the new phase droplets via the SD manner is like that of nucleation [118-120]. This is the reason why the researchers in the field of condensed matter physics usually believed that there is no significant difference between NG and SD [121]. However, due to the difference in the early dynamic processes of the two manners and their volume fraction of the minority phase, the pattern evolutions may be changed drastically if some external conditions are imposed.

In this study, NG and SD type phase separation were realized in a transparent system, SCN-H₂O, which has a miscibility gap. The reason to select the transparent system is that their phase separation process can be observed in-situ. Otherwise, for the alloy system, their phase separation process only can be inferred from their final structure. Temperature and isothermal field were imposed on the samples with these two types phase separation. It was found that the pattern formations via these two manners are quite different. The evidences obtained in the present work show that the NG and SD type manners will result in distinct morphology evolutions which could have potential applications in designing specific structural materials.

4.2 Results and discussion

4.2.1 Phase separation of SCN-H₂O system in a uni-directional temperature field

Phase diagram of SCN-H₂O system is shown in Figure 4.1. NG and SD type phase separation can be obtained according to the phase diagram. In this experiment, SCN-70wt%H₂O and SCN-50wt%H₂O were chosen to realize the process of NG and SD in the uni-directional temperature field. The macroscopic NG and SD type phase

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separation processes were investigated simultaneously in the temperature field at low temperature (left side) $T_L=297.5$ K and high temperature (right side) $T_H=330.5$ K. The photographs as they evolve in time were shown in Figure 4.2. Photographs of NG process with SCN-70wt%H₂O solution was given in (a) and SD process with SCN-50wt%H₂O solution was given in (b).

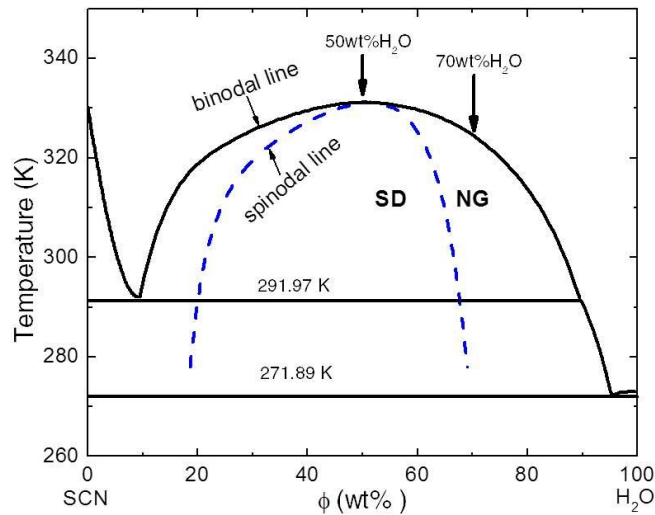


Figure 4.1 Phase diagram of SCN-H₂O system [115]. Metastable and unstable regions were divided in the miscibility gap. In the former, the phase separation type was NG (between the binodal and spinodal line in the immiscible gap), whereas in the latter the phase separation type was SD (below the spinodal line).

As shown in Figure 4.2, the phase separation of NG and SD processes both started at the low temperature side, this is because the sample at low temperature side will go into the miscibility gap first. However, the macroscopic morphology evolution of the two types of phase separation was distinct.

The NG type, SCN-rich phase which has a small volume fraction and defined as the minority phase, nucleated as droplets in the matrix after the temperature is quenched below the binodal line. In Figure 4.2(a) at 4 s, most of the solution was still miscible, then at 10 s it can be seen that there were many droplets formed and pushed to the high temperature side by the Marangoni force [122, 123], which was caused by the interfacial tension gradient between a spherical droplet and a liquid matrix [15]. After the droplets formed, they can surpass the interaction interface front as they migrated to the high temperature side like at 20 s. This was much more obvious at 30 s and the size of the droplets became larger during the migration. One can note that

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there were still many droplets and no apparent aggregation was observed.

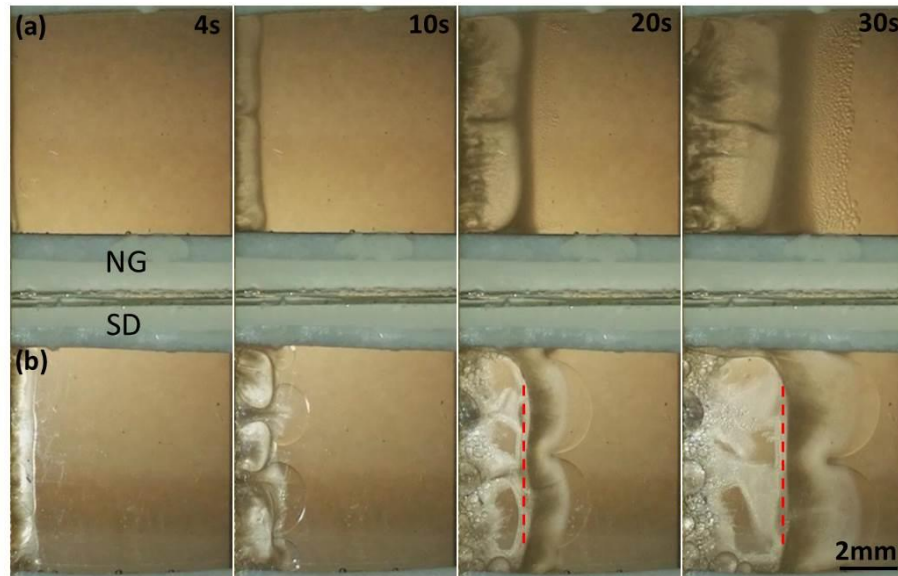


Figure 4.2 Macroscopic morphology evolution of NG with SCN-70wt% H₂O solution (a), and SD with SCN-50wt% H₂O solution (b) with time. The low temperature (left side) was $T_L=297.5$ K and high temperature (right side) $T_H=330.5$ K. The red dash line in (b) was the interfacial layer between the matrix phase and the minority rich phase.

Nevertheless, the SD type, the morphology evolution was totally different. At the time of 4 s (the time $t=0$ is when SD type phase separation started) as shown in Figure 4.2(b) phase separation had occurred, this is because the spinodal temperature for SCN-50wt% H₂O is higher than the binodal temperature for SCN-70wt% H₂O. After the SD type phase separation started, big size aggregations formed very soon as seen clearly in Figure 4.2(b) at 10 s. Then from the macroscopic perspective, there was one large aggregate formed which continued to grow as it migrated to the high temperature side pushed by Marangoni force, but there were many small droplets inside it. They formed one large aggregate in order to decrease the interfacial energy when the migration process proceeds. The newly produced droplets continued to merge into the large aggregate, which is why it continued to grow.

During this process, one obvious interfacial layer formed marked as the red dash line like at 20 s. The interfacial layer was not straight due to contact with the edges of the sample. In fact, the interfacial layer was the left side of the large aggregate and migrated to the high temperature side together with it. The front of the large aggregate was cellular as a result of the instability of it.

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In order to have a better understanding of the difference between the two types of phase separation we take a closer look at the samples. Figure 4.3 gives the microscopic evolution of NG type phase separation for SCN-70wt% H_2O at different times observed by the microscope under the uni-directional temperature field. The left side (low temperature) was 297.5 K and right side (high temperature) was 323.5 K.

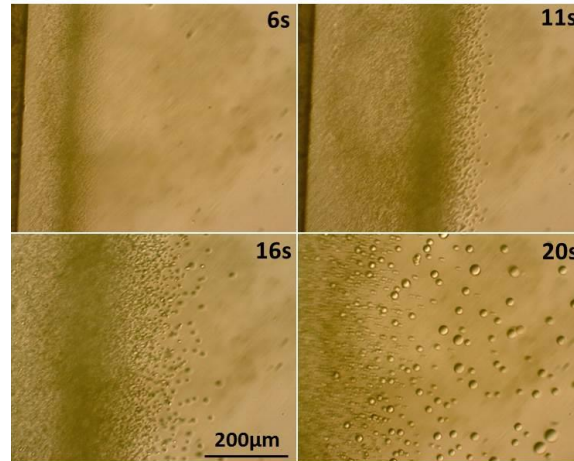


Figure 4.3 Photographs of the phase separation of NG for SCN-70wt% H_2O evolution in time observed by microscope under the uni-directional temperature field. The low temperature (left side) was $T_L=297.5$ K and high temperature (right side) $T_H=323.5$ K.

The microscopic phase separation was similar like in the macroscopic process. The SCN-rich phase nucleated as small droplets in the matrix when the temperature below the binodal temperature and the droplets migrated to the high temperature side pushed by the Marangoni force. In the beginning, the droplets were too small to be seen clearly. This is because the lens we selected is small and the purpose is to compare the microscopic phenomenon with the macroscopic one. The droplets can be seen clearly as they evolve during 20 s. One can note that the small droplets grow larger and larger along with their migration and the velocity of bigger droplets was faster than the smaller one, which can be seen in Figure 4.3 at 20 s that the droplets with larger radius at the right side of the photograph.

For comparison, the evolution of SD type phase separation for SCN-50wt% H_2O at different times observed with the microscope under the uni-directional temperature field was shown in Figure 4.4. The low temperature (left side) was 293 K and high temperature (right side) was 333 K. The microscopic phase separation was similar as in the macroscopic process as well. In the microscopic process, the aggregated of droplets can be seen clearly. For the SD process, the initial transition of network-like

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structure to the spherical droplets was fast, especially under the temperature gradient, so in the beginning of Figure 4.4 we only saw the small droplets instead of the network-like structure. The small droplets are pushed by the Marangoni force and they aggregate very fast like in the macroscopic process. One can note that at 6 s the big size aggregates side by side have the trend to connect together. Then at 10 s they connected to form one large aggregate and an obvious interfacial layer produced like at 20 s in the macroscopic process. The small droplets on the left side of the layer continue to merge into the large aggregation as the blue arrow pointed in Figure 4.4 at 10 s.

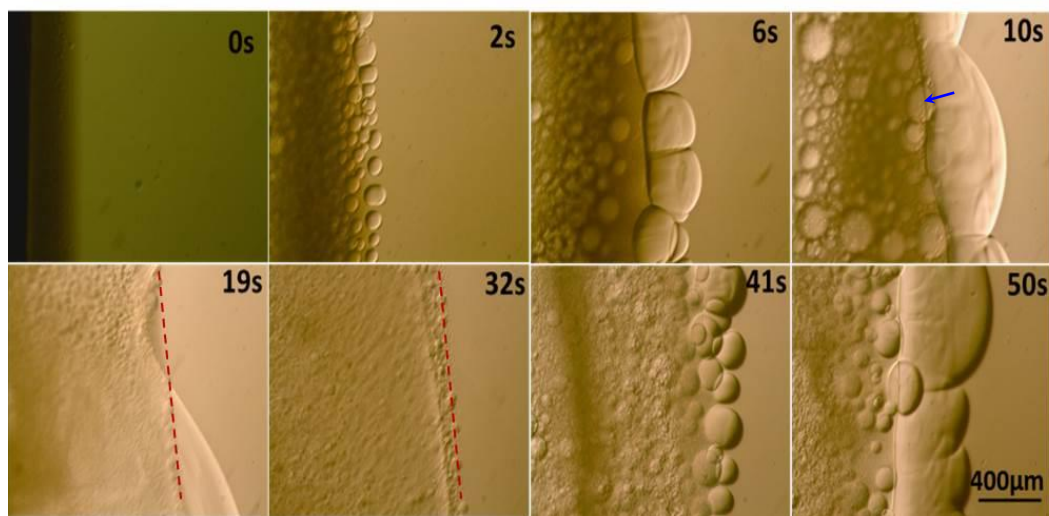


Figure 4.4 Images of microscopic phase separation of SD for SCN-50wt% H_2O evolved as time observed by the microscope under the uni-directional temperature field. The low temperature (left side) was $T_L=293$ K and high temperature (right side) $T_H=333$ K. The red dash line was the reaction interface front.

At 10 s, the layer is not formed in Figure 4.2 but it is already formed in Figure 4.4. Therefore, the speed to form the layer was faster in the microscopic than in the macroscopic process. One reason was that the observed scale in microscopic process was smaller compared with the macroscopic one. The second reason was that the left side temperature was lower and the right side temperature was higher in the microscopic process. When we did the experiment, there was another difference between microscopic and macroscopic, the distance between low and high temperature side was 12 mm in microscopic and 10 mm in macroscopic respectively.

Not like the NG type, the microscopic evolution of SD type phase separation was

different as in the macroscopic process where only one interfacial layer formed. For the microscopic process of SD type, the way to form the first layer during 10 s was similar like in the macroscopic process. Nevertheless, as the phase separation continued, when the velocity of reaction interface front was higher than the migration of the aggregation front, the aggregation behavior of the minority phase would repeat the process from 0 to 10 s and form another interfacial layer as shown in 50 s. The red dash line was the reaction interface front, which partially surpassed the big aggregate front at 19 s and totally surpassed it at 32 s. Then the formation process of the second interfacial layer was like the first one. We didn't see this in the macroscopic process. May be because the sample is longer and the temperature interval between the low and high side is larger in the microscopic process than in the macroscopic one. For this experiment, the right side temperature was higher than the spinodal temperature, so the second interfacial layer with the big aggregate would disappear as they migrated to the position where the temperature was higher than the spinodal temperature.

The radius of the drop is hard to measure during the migration when the temperature gradient exists. In order to avoid this deficiency, next the NG and SD types were performed at the temperature 1 K lower than binodal and spinodal value under the condition with isothermal field.

4.2.2 Phase separation of SCN-H₂O system at isothermal field

Figure 4.5 was the microscopic evolution of the phase separation process at isothermal field observed by the microscope. Photographs of SCN-70wt%H₂O solution with NG type at T=323 K evolved as a function of time was shown in (a). From the phase diagram of Figure 4.1, it can be known that the SCN-rich phase was minority phase and nucleated as small droplets after the phase separation started. Then the small droplets grow bigger and bigger with time, which is a typical characteristic of the nucleation growth. All the droplets are separated from their neighbors and they grow independently by pure diffusion without coalescence. Photographs of SCN-50wt%H₂O solution with SD type at T=330 K evolved in time was shown in (b). The difference to the NG type is that the network-like structure formed when the temperature quenched below the spinodal line for SD type as shown in 3 s. The network-like structure is typical of the initial state of the spinodal

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decomposition growth and cannot be seen clearly under the condition of exerting the temperature field. Then the network-like structure coarsens and the shape becomes spherical (as shown at 24 s), which is similar to that of nucleation. This process was much faster in the uni-directional temperature since the droplets would collide and merge with each other.

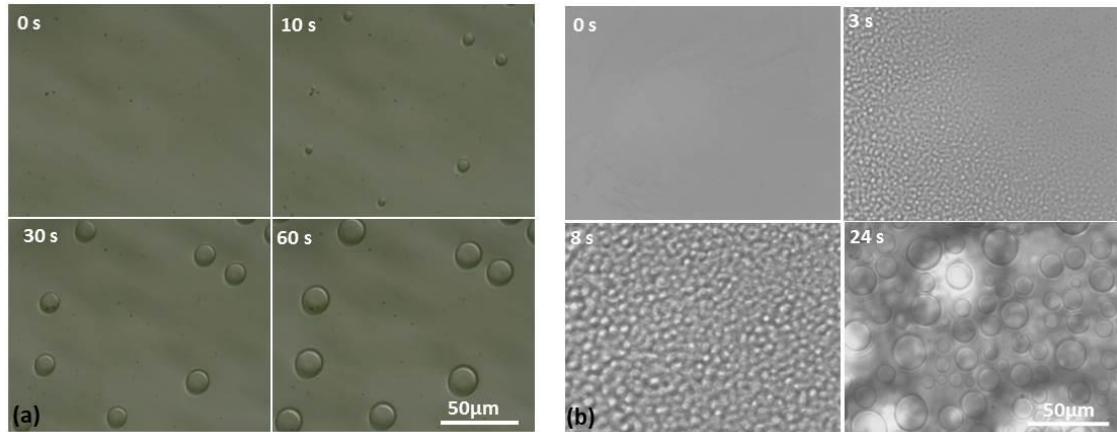


Figure 4.5 Microscopic evolution of the NG type phase separation at T=323 K with SCN-70wt% H₂O solution (a), and SD type at T=330 K with SCN-50wt% H₂O solution.

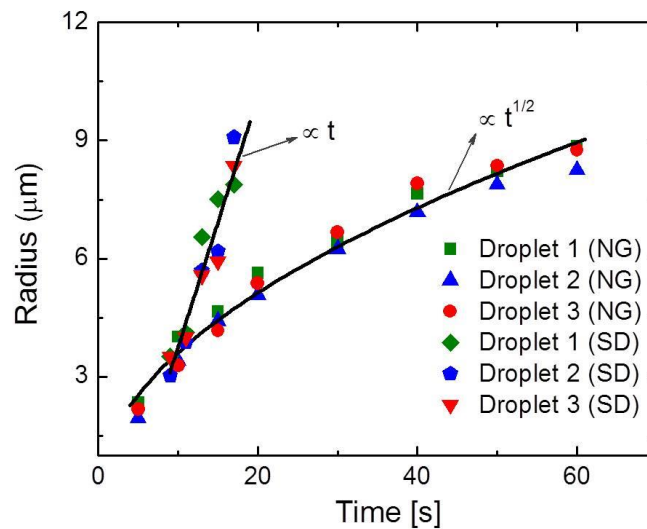


Figure 4.6 Radius increased with time for both NG and SD type phase separation, three droplets were chosen for each type measurement.

The relationship between the radius of droplets and time at isothermal field was shown in Figure 4.6 for both NG and SD type phase separation. Three droplets for each type were chosen for the measurements. We considered the time 0 s as we saw

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the spherical droplets or network-like structure appear by our eyes, this would have some errors compared to the real case. For SD type, the measurement started after the network-like structure transition to the spherical droplets. It can be seen that the growth of the droplets via SD type was faster than the NG type and the relationships of $R_{SD} t = 0.636t - 2.612$ and $R_{NG}(t) = 1.123t^{1/2}$ were obtained, respectively. The parabolic law $R_{NG}(t) \sim t^{1/2}$ is a typical characteristic of pure diffusive growth process for NG case [124]. On the contrary, the linear law $R_{SD}(t) \sim t$ is the typical characteristic of the later stage of the spinodal decomposition when the surface tension effects become dominant [125-127], the constant -2.612 comes from the time 0 we selected is not the real time 0. Therefore, we can see that the data in our experiment agrees well with the theory of NG and SD type phase separation. Moreover, it should be noted that when extend the fitted linear line of SD to the X-axis, the radius of the minority phase for SD is negative at $t=0$. This is because that the morphology of SD in the beginning is network like, however, the radius of the minority phase is measured after its shape transformed from network like to spherical. This means that it's reasonable the radius of the minority phase is negative when extend the fitted linear line of SD to the X-axis at small t .

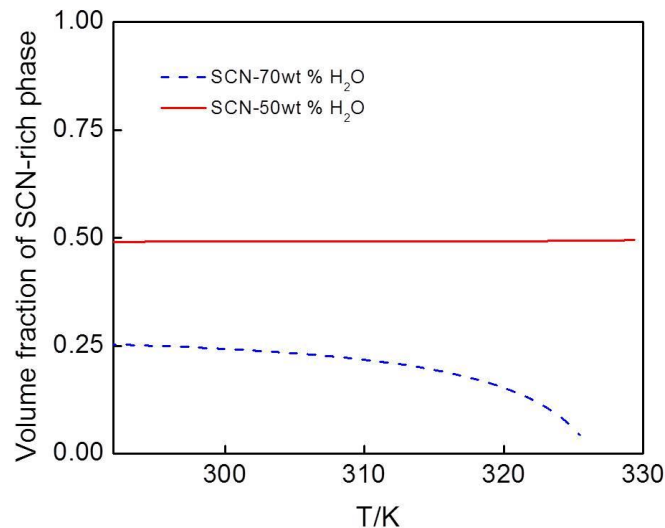


Figure 4.7 Volume fraction of the SCN-rich phase as a function of temperature for SCN-50wt% H_2O (red solid line) and SCN-70wt% H_2O (blue dash line).

The volume fraction of SCN-rich phase (the calculation method given in section 3.2.1.4) for samples SCN-50wt% H_2O (SD type) and SCN-70wt% H_2O (NG type) evolution with temperature was shown in Figure 4.7. In both cases, the minority phases were SCN-rich phase (f_{SCN}). The red solid line was SCN-50wt% H_2O and the

blue dashed line was SCN-70wt% H_2O . For SCN-50wt% H_2O , f_{SCN} was a little bit smaller than 0.5 and constant for all the temperature, whereas for SCN-70wt% H_2O , it can be seen that f_{SCN} near 0 when the temperature near the binodal temperature (around 325 K) and increased to the maximum of 0.25 when the temperature decreased to reach the bottom of the miscibility gap (around 290 K). The different volume fractions of the minority phases can affect the aggregate behavior during the phase separation process.

4.2.3 Growth rate and volume fraction of minority phase to the effect of the microstructure

From Figure 4.2, it can be seen that the migration velocity and aggregation rate of the minority phase in NG type are slower than in SD type after the phase separation started. The migration of the minority phase droplets in the liquid matrix is induced mainly by Marangoni motion and the velocity is given by [12, 128]

$$v_m \approx \frac{-2r}{3(3\mu_d + 2\mu_m)} \cdot \frac{\partial \sigma}{\partial T} \cdot \frac{\partial T}{\partial x} \quad (4.1)$$

where r is the radius of the droplet, μ_d and μ_m are the viscosities of the droplet and the liquid matrix, σ is the interfacial energy, T is the temperature, and x is the distance. Under the current experimental conditions, the two samples are put in the same temperature field at the same time. This means that the temperature regimes are nearly the same for both the NG and SD type phase separations, which results in almost the same interfacial tension gradients and the viscosities. In this case, v_m is mainly decided by and is proportional to r . Thus, the droplet radius plays a key role in the migration.

The relationship between the radius of the minority phase and time under the condition with isothermal field was shown in Figure 4.6, it can be seen that the radius of the minority phase is proportional to t for SD type phase separation after transition to the spherical droplets and proportional to $t^{1/2}$ for NG type. This suggests that the growth kinetics of the minority phase in SD is faster than in NG. As can be seen in Figure 4.6, the droplets formed via the SD have a larger size than via the NG if the phase separation starts at the same time. This makes the migration of the droplets during the SD faster than during the NG process. Meanwhile, the higher growth rate of the minority phase has higher possibility to aggregate. However, we should keep in

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mind that when the temperature gradient exists the growth rate of the minority phase should be faster due to coalescence resulting from collision and merging.

The aggregation rate is also related to the volume fraction of the minority phase. From Figure 4.7, one can note that the minority phase of NG and SD type phase separation are both SCN-rich. With decreased temperature, the volume fraction of the SCN-rich phase in SCN-70wt% H₂O increases to the maximum of 0.25 from near 0 when the temperature reaches the bottom of the miscibility gap. However, the SCN-rich phase in SCN-50wt% H₂O nearly stays constant at 0.5. This difference leads to hard aggregation of the minority phase in SCN-70wt% H₂O system for NG case, which can be seen under both the condition with and without thermal gradient. Without the thermal gradient, the coarsening of the droplets in SD type proceeds soon after transition from the interconnected network, so that it needs a shorter time to form a certain size droplets in SD process than NG process. It is stronger with the thermal gradient due to collision and merging of the small droplets [129-131]. The high volume fraction promotes the coarsening to increase the droplet size, leading to higher migration velocities and fast aggregation of the minority phase.

4.2.4 The probability of produced multi-layer structure

For the SD type phase separation, one obvious interfacial layer formed in Figure 4.2(b) as marked by the red dashed line. In this case, a two-layer structure formed, one is the matrix phase in the left side of the interfacial layer and another is the minority-rich phase on the right side. In fact, if one see carefully in Figure 4.2(a), there has two-layer structure formed as well with matrix and minority-rich phase, even the interfacial layer is not obvious as in the SD type. The difference is that in the NG type the minority rich phase is distributed with the small droplets and in the SD type is the big aggregate of the minority phase. This means that even both NG and SD type phase separation can form the layer structure, their final microstructures are not the same.

As we have discussed in the previous section for the microscopic evolution of SD type in Figure 4.4, the difference in the macroscopic process is that there is another interfacial layer formed at around 50s. In this case, a four-layer structure is formed. The first and the third layer were matrix phase (the phase left after the

minority phase migrated) and the second and the fourth layer were the big aggregate of the minority phase. The evolving process of the second layer interface is exactly the same as the first layer interface formation process. In our case, finally the second layer interface and the big aggregate will melt and disappear. This is because the temperature at the high temperature side is higher than the spinodal value.

Considering that if the sample is long enough and can be moved and solidified during its migration process, and the temperature controlled appropriately to keep the temperature of the reaction interface front always lower than the spinodal value. Then the aggregation process can be repeated and a multi-layer structure can be formed with matrix and the big aggregate of the minority phase alternately.

According to the analysis above, multi-layer structure also can be formed in the NG process. The mainly difference is that in the multi-layer structure, the minority rich phase in SD process is the big aggregation and in NG process is the distribution of the small droplets.

4.2.5 The phase separation pattern to the effect of the solidified structure

The system of Fe-Sn alloy who has a miscibility gap. Next we will see what the phase separation pattern to the influence of the solidified structure of Fe-Sn system. The ribbons of Fe-Sn alloy [132] were prepared by ejecting the melted sample onto a Cu single roller at certain wheel speed. The phase diagram of Fe-Sn alloy is given in Figure 4.8(a), the red dashed line is the spinodal line. The solidification microstructure of a ribbon at a wheel speed 10 m/s of Fe-68wt%Sn alloy is shown in Figure 4.8(b), which experiences SD type phase separation. The dark phase in (b) is Sn-rich phase and the light one is Fe-rich phase. The fibers of Fe-rich phase formed in the upper side of the ribbon, this is the result of the aggregation of the minority phase (Fe-rich), which is similar like the aggregation process of SD type in SCN-H₂O system. In the bottom of the ribbon, the typical initial fine network like structure of SD type was preserved and (b') was the enlargement of the area selected in (b). Such structure can be preserved in the bottom of the sample since the cooling rate near the wheel side is high and the initial SD morphology does not have time to coarsen before solidifying totally.

From (b'), we can see that the influence of cooling rate to the final solidified

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morphology is very important. The network like structure was small in the bottom of (b') and much larger in the upper part. This is because the cooling rate near the wheel side was the maximum and decreased toward the upper part of the ribbon. Like shown in (b) the fibers of Fe-rich phase formed in the upper part of the ribbon, which has smaller cooling rate, the Fe-rich phase has enough time to aggregate to form the fiber. It should be noted that the structure shown in the upper part of (b) is a rudiment of the layer structure since the cooling rate is high and the different small parts cannot aggregate into the long layer. For comparison, the solidification microstructure via NG type phase separation of Fe-58wt%Sn alloy at 3m/s is presented in Figure 4.8(c). In this concentration, the minority phase is Sn-rich phase. As given in (c) that the Sn-rich droplets nucleated and distributed homogeneously in the matrix and there is no evidence to form fiber or layer structure.

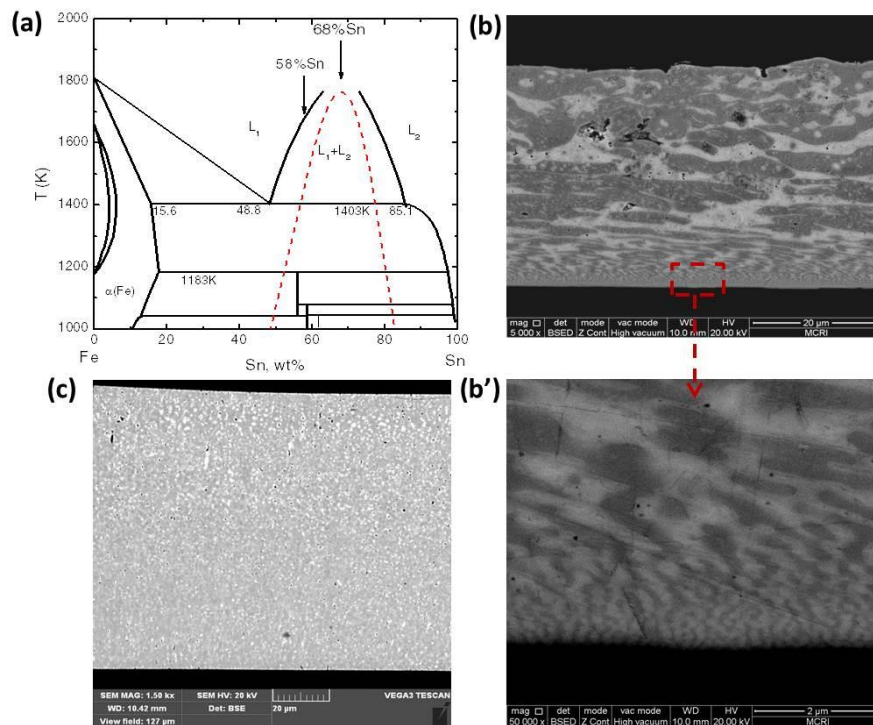


Figure 4.8 (a) Phase diagram of Fe-Sn system. (b) SEM image of the SD-type solidification microstructure in Fe-68wt%Sn alloy at 10 m/s. (b') Enlargement of area in (b) selected to show the worm-like structure. (c) The NG-type solidification microstructure in Fe-58wt%Sn alloy at 3 m/s. In the images, the dark phase is Fe-rich phase and the light one is Sn-rich phase.

In fact, for the alloy system with a miscibility gap, normally the temperature interval is more than 1000 K, the cooling rate is extremely fast when the melted

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samples are quenched to room temperature. Like in the Fe-Sn ribbon, the cooling rate is so fast that the initial phase separation morphology in the immiscibility gap can be reserved. However, a perfect layer structure needs good a design of the thermal gradient and the cooling rate.

Although the late stage evolution of the minority phase in SD type is similar like in NG type under the isothermal field, both are the spherical droplets as shown in Figure 4.5. This is the reason why researchers in the field of condensed matter physics usually believed that there is no significant difference between NG and SD during the phase separation process [121]. However, if the morphology can be solidified in the early stage of the phase separation process, the two processes should have a difference. Figure 4.8 (b) and (c) are the Fe-Sn ribbon of SD and NG type. It can be seen clearly that the network like structure in the early stage of SD type and the spherical droplets in NG type phase separation are preserved. This proved that the different initial phase separation pattern of NG and SD can lead to different morphologies. Even in the late stage of SD, the formed morphology under the thermal gradient can have big difference because of the different growth kinetics and volume fraction of the minority phase in NG and SD, like the formed layer structure in SCN-H₂O system. Therefore, we can see that these two processes of phase separation can lead to different morphologies.

4.3 Conclusions

In this study, SCN-50wt%H₂O and SCN-70wt%H₂O solution were used to realize SD and NG type phase separations. Under the thermal gradient, macroscopic observations show that the aggregation rate of the minority phase with SD type is faster than NG type and two layer structures can be formed for both cases. Nevertheless, the difference is that with SD type the second layer is the large aggregates of the minority phase and with NG it's the distribution of the minority phase. For the microscopic observations, NG type is similar as in the macroscopic case, but SD type can produce four layer structures and the formation process of two latter layers is the repetition of the two former layers.

Under the isothermal field, the relationship of droplet's radius and time shows that the growth rate of the minority phase with SD type is faster than with NG type. Compared with NG type, SD type has a higher volume fraction of the minority phase

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and it is easier to coagulate to form the big aggregates. This suggests that the kinetics properties and the volume fraction of the minority phase play key role in the change in the morphology evolution.

The results of Fe-Sn ribbons show that due to the initial distinct structure characteristic of these two types of phase separation, different morphologies can be obtained. In addition, multilayer structures can be produced if the thermal gradient and the cooling rate can be well designed. However, although the late stage evolution of minority phase in SD type is similar like in NG type, the formed multilayer structures with minority rich phase are still not same, big aggregates and distribution of minority phase respectively.

Thus, we can conclude that NG and SD type phase separation can produce different morphologies. According to our findings, the materials can be designed by selecting appropriate parameters to suit the specific material purposes.

Chapter 5 Influence of salt type on gelation kinetics (NaCl or KCl)

5.1 Introduction

Gels are important in many applications, such as in materials science, food science, biological cells and so on [133-136]. Though gelation has been described in several reviews [137-139] many aspects of this process are still not fully understood. To make a gel, the building blocks identified above must aggregate. Aggregation can be induced in a number of ways. For colloidal particles, for example, depletion interactions arising from a polymer in solution can lead to gels that are the result of an arrested phase separation[140, 141]. In many food systems, gels are the result of the protein denaturation that precedes aggregation [142, 143]. In this case, the loss of stability comes from the interactions between protein domains that are not exposed in the native form[143].

As in most complex fluids, the repulsive electrostatic and the attractive van der Waal forces play an important role in the stability of colloidal and nano-particle dispersions. In this setting, the interaction between these two forces can be

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qualitatively explained using the theory developed by Derjaguin, Landau, Verwey and Overbeek (DLVO) [30]. In DLVO theory the addition of counter ions to a dispersion lowers the repulsive potential between particles by screening their surface charge and at some critical ion concentration aggregation ensues. Whilst DLVO is one of the few analytical models that can be derived for this problem it has serious limitations. One such limitation is that salt ions of the same valence are considered equivalent and therefore affect the inter-particle potential in the same manner; a consideration that does not reflect reality where systems are sensitive to both a given ion's valence *and* its chemical nature.

An example of the latter are the “salting in” and “salting out” effects observed in protein solutions. Here, counter ions of the same valence may either stabilize (salting in) or de-stabilize (salting out) the system depending on their elemental nature [70]. There is, however, some systematic behavior and the ions can be ordered in a sequence according to the effects they have on solubility in the so-called Hofmeister series. It has been found that this series tallies with the respective water affinities of the ions [70] and recent work has related the size of an ion's hydration shell to its position in the series. [144]. Further, it has been shown that it is possible to predict the critical coagulation concentration with different salts when the specific adsorption of the ions on the surface of the colloids, is accounted for. Specifically, chaotropic ions, i.e. those that can easily lose their hydration shell, tend to be adsorbed on the colloidal surface while kosmotropic ones are not [41, 145] decreasing and increasing stability respectively.

Whilst there is an obvious connection with the hydration phenomena described above and an ion's capacity to coagulate colloidal systems [41], there have been less studies on how such phenomena influence the kinetics and the structure of the gels. Colloidal silica has been extensively studied, mainly in the presence of NaCl. The fractal nature of the gels has been shown to form through a reaction limited cluster aggregation process (RLCA) [45, 146-148]. The peculiar influence of salt on the coagulation concentration of silica was demonstrated almost 50 years ago [149], when this influence was shown to depend strongly on the pH of the silica stock solution. Silica gels have been shown to form much more quickly in the presence of chaotropic ions (such as NH_4^+ or K^+) rather than kosmotropic ones, such as Na^+ [82, 150-152]. The changes in the critical coagulation concentrations of silica particles with a range

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of salts was recently shown to correlate very well with the change in the surface charge arising from differences in ionic adsorption [82]. The gel times have been measured by eye-inspection, turbidity measurements or rheology all of which focus on larger length-scales. However, there has not been, to our knowledge, a comparison between the aggregation kinetics at the microscopic and macroscopic scales.

With this aim in mind, in this Chapter, we have used time resolved small angle X-ray scattering (SAXS) for two different types and a range of concentrations of salt, and for several particle densities. In doing so, we are able to define a *microscopic* transition time in addition to the macroscopic one defined by traditional eye inspection. In this way, the chain of events leading to gelation at the microscopic and macroscopic length-scales can be compared. Moreover, the question of the mechanical properties of the different gels and their relations to the nature of the salt and the time elapsed from preparation is addressed.

The work in this Chapter has finished and the results have been published: *Zhang, Li, et al. "Varying the counter ion changes the kinetics, but not the final structure of colloidal gels." Journal of colloid and interface science 463 (2016): 137-144.*

5.2 Results and discussion

5.2.1 Gel General observations and phase diagrams

Figure 5.1(a) shows the photographs of different types of samples observed by adding salt to silica dispersions: translucent, turbid, two-phase and solid-like, as defined by their macroscopic features. Specifically, the translucent and the turbid samples were fully fluid, the two-phase samples were formed of a fluid phase (eventually transparent) sitting on top of a solid-like phase (always turbid) and samples classed as solid-like were composed of a single phase that supports its own weight when turned upside down. In the following, both solid-like and two-phase samples are called gels. The range of salt concentration (c_S) is from 0-500 mM and silica from 0-12 vol%. Phase diagrams of samples 2 days after preparation with NaCl and KCl are shown in Figure 5.1(b) and (c). The region of gels (shaded in grey) is much larger with KCl than with NaCl. Compared with NaCl, less KCl salt at the same silica concentration is required to make gels and similarly less silica is needed at the

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same salt concentration.

Gels are out of equilibrium structures. This implies that their properties can evolve with time as the system ages. It is therefore of interest to understand if the phase diagrams discussed above undergo further evolution with time. To probe the long time evolution of the gels, we stored the samples for 6 months after which we

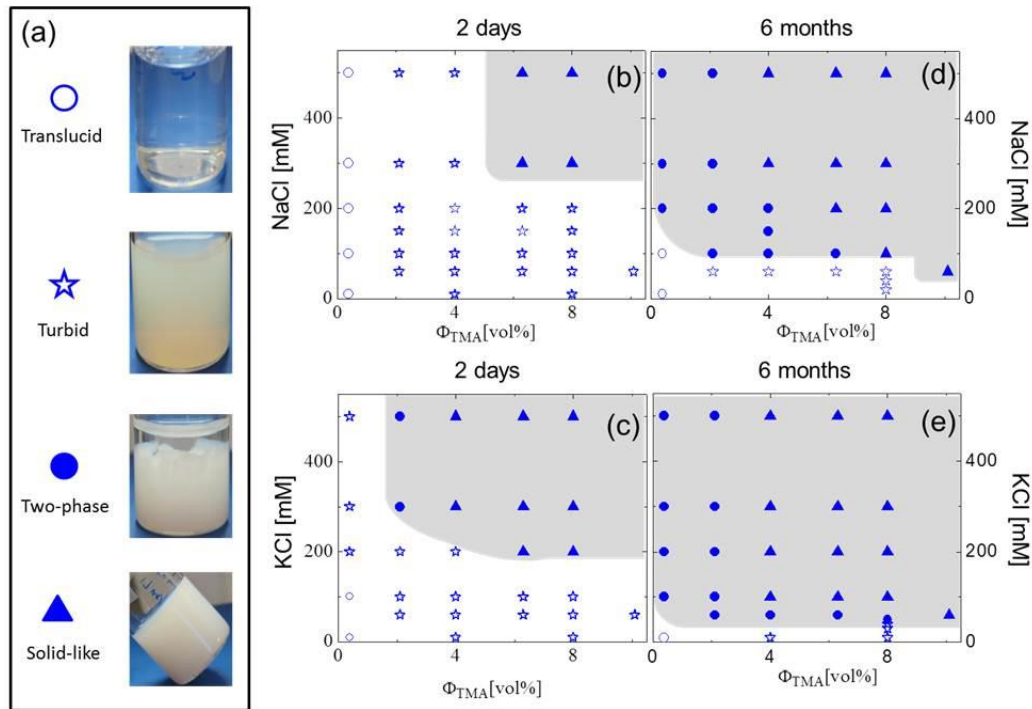


Figure 5.1(a) Photographs of the different types of samples encountered: translucid, turbid, two-phase and solid-like with the symbols used to denote them in the phase diagrams. Phase diagrams obtained from visual observation with different TMA volume fractions and salt concentrations 2 days and 6 months after preparation for NaCl (b and d respectively) and for KCl (c and e respectively). The highlighted zone corresponds to two-phase and solid-like samples.

re-constructed the phase diagrams as shown in Figure 5.1(d) and (e). It's evident that after this period there is greater similarity between the NaCl and KCl samples. Most of the samples prepared with both salts in the range of silica concentrations studied have become two-phase or solid-like. The two-phase samples are formed at the lower salt concentrations or at the lowest silica concentrations while the solid-like samples are formed at higher salt and silica concentrations. Some differences remain however, slightly higher concentrations of NaCl are required to form the solid-like samples compared with KCl. For the samples prepared with KCl, 60 mM is required to form

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the two-phase or solid-like samples whereas 100 mM is needed when NaCl is employed. However, this difference could disappear after an even longer waiting time. Nevertheless, these results indicate that the macroscopic character of the samples produced from both salts is similar after the gels have been allowed to age significantly.

5.2.2 Gel structure

In order to probe the intimate structure of the evolved gels we used SAXS to extract their final structure factors, determined when the $S(q)$ measured cease to change with time, called $S_f(q)$. This time varies from sample to sample, ranging from several hours to months and for the lowest concentrations of TMA the experimental time is shorter than this and we do not have the corresponding data. Figure 5.2(a) shows the $S_f(q)$ as a function of q for 5 different concentrations of TMA

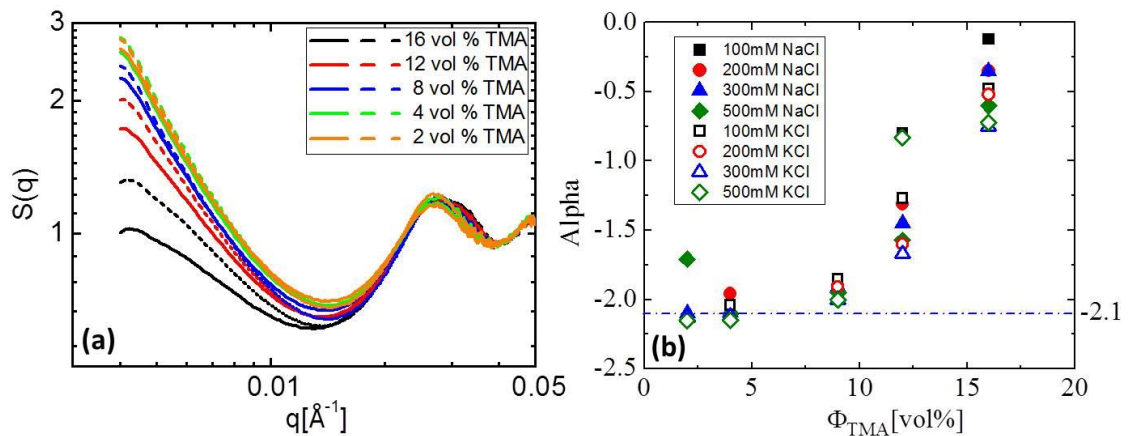


Figure 5.2(a) Structure factor $S(q)$ changed with q at different volume fractions of TMA ($\Phi_{\text{TMA}}=2\% - 16\%$) with 300 mM salt, NaCl with solid lines and KCl with dashed lines. (b) The variation of α with the volume fraction of TMA.

with 300mM NaCl (solid line) and KCl (dash line). Above 0.02 \AA^{-1} , all the structure factors are similar indicating that the ordering is hardly influenced by the concentration of particles or type of salt used, although the first interaction peak moves slightly to higher q for the highest volume fractions, indicating a closer contract of the particles. However at lower q values, which mean larger length scales, they become very different. The intensity at low q increases as the volume fraction of silica decreases.

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At low q we have fitted the $S_f(q)$ with a power law of the type $Aq^{-\alpha} + B$, as shown by the red line in Figure 5.3(a). In this way we assume that the contribution of the local $S(q)$ is a constant, which is not strictly true and for a fuller analysis a model combining the local amorphous structure with a fractal cluster structure should be developed. However, the fits allow us to compare all the data conveniently, so the corresponding α are shown in Figure 5.2(b). In fractal systems the power law exponent is equal to the fractal dimension. At the lowest silica we find $\alpha \approx 2.1$, a typical value for the fractal dimension of gels formed by reaction limited cluster aggregation (RLCA) [53]. Therefore, in the q -range probed the gels at 2-4 vol% have a fractal nature, with a fractal dimension of 2.1, which compares well with previous experiments on colloidal silica gels [51, 52]. It also seems that the aggregation, even at the highest salt concentrations, is dominated by a significant electrostatic barrier as the aggregation is still reaction limited.

As the volume fraction of particles increases the low q behavior of the $S_f(q)$ starts to change; the slope decreases and the depth of the first minimum deepens. At this point we can no longer equate the α with fractal dimension, however comparing the values is useful as it allows us to see that the change in shape occurs for both salts at all salt concentrations. The values of α become much more scattered at higher ϕ_{TMA} , and the values for the samples with NaCl are always slightly lower than those with KCl. However these effects are minor compared with the effect of increasing ϕ_{TMA} . The shape of the $S_f(q)$ in the q -range studied is no longer that of a fractal assembly, but starts to resemble that of more compact solids. The change in shape is qualitatively similar to the results of off-lattice simulations on diffusion limited cluster aggregation at higher volume fraction [153]. We can conclude that the final structure factor is influenced much more strongly by the particle volume fraction than salt type or concentration.

We have also seen in Figure 5.1 that the phase diagrams with NaCl and with KCl are very different after two days, but they become increasingly similar with time. In addition, the final local structure in the samples depends predominately on the volume fraction of particles, and is hardly influenced by the concentration or the type of salt added. This seems to suggest that the main difference between NaCl and KCl lies in the kinetics.

5.2.3 Kinetics

In order to further analyse this situation we define both a macroscopic gelation time, τ_M and a microscopic one, τ_X . The latter is linked to structural arrest in X-ray experiments. τ_M is linked to the mechanical properties of the gel and denotes the time at which the yield stress σ_y of the sample becomes higher than the gravitational stresses σ_g . In our samples this means $\sigma_y > \sigma_g \approx 10^2$ Pa. For the solid-like samples τ_M is taken as the time at which the sample supports its own weight after being turned upside down. For two-phase samples it was taken as the time at which part of the sample became solid-like. The sedimenting phase, which eventually becomes solid-like, is denser than the supernatant. This means that the volume fraction of TMA in it is higher than in the sample initially and the τ_M measured for these samples should be taken with some caution.

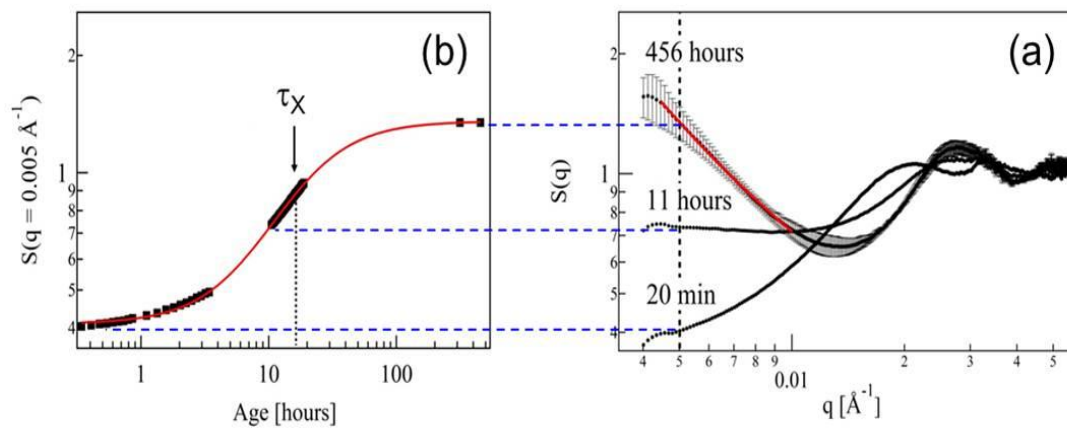


Figure 5.3(a) The structure factor $S(q)$ for a sample with 12 vol% TMA, 200 mM NaCl, at 20 min, 11 hours and 456 hours after preparation. For clarity, the error bars are only shown for one curve: they are mainly due to the systematic uncertainty in evaluating the form factor. The solid red line is a power-law fit (see text). (b) Time evolution of the structure factor $S(q=0.005 \text{ \AA}^{-1})$ for the same sample (dots) and fit with the sigmoidal function.

The kinetics at the local scale is followed with the measurements of $S(q)$ in time. We can see the evolution of $S(q)$ after sample preparation in Figure 5.3(a) for a sample composed of 12 vol% TMA and 200 mM NaCl. At short times the $S(q)$ is typical of a fluid sample. With time, the low- q structure factor increases indicating structuration at larger length-scales, and possibly the formation of a gel.

In order to quantify the timescales of change, we characterized the time

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evolution of the samples by plotting the structure factor at a fixed scattering vector ($q_0=0.005 \text{ \AA}^{-1}$) as a function of sample age: $S(q_0, t)$ and fit with the sigmoidal function

$$S(q_0, t) = 0.5 \times (a + b) + 0.5 \times (b - a) \times \tanh \frac{\log(t) - \log(\tau_x)}{c} \quad (5.1)$$

where a is baseline, b is plateau, c is the width of transition. The sigmoidal function is mathematical function having an ‘‘S’’ shape (sigmoidal curve).

The evolution of $S(q_0)$ is shown in Figure 3(b). From such figures we extract τ_x defined as the time where inflection of the curve is observed and τ_x is the characteristic time linked to the arrest of the structural evolution at $q_0 = 0.005 \text{ \AA}^{-1}$ (corresponding to 1256 \AA , about 5 particle diameters). We note that the choice of q_0 is arbitrary and a different choice will change the curves obtained. Therefore we must keep in mind that we are comparing structural evolution at a single length-scale.

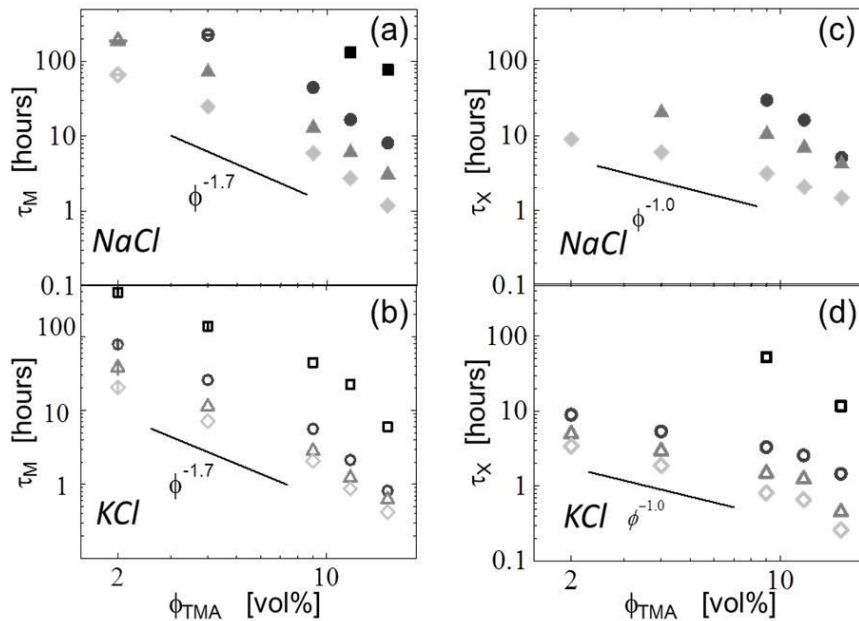


Figure 5.4 Transition times obtained from visual observations at different TMA volume fractions and salt concentrations 100 mM (\square), 200 mM (\circ), 300 mM (Δ), 500 mM (\diamond) for (a) NaCl and (b) KCl. Samples in the two-phase region are indicated with horizontal (NaCl) or vertical (KCl) lines inside the symbols. The microscopic transition times (τ_x) are shown in Figures 5.4 (c) for NaCl and (d) for KCl.

The characteristic times of gelation obtained from the macroscopic observations (τ_M) for different salt concentrations and TMA volume fractions are shown in Figure 5.4(a) and (b) where τ_M decreases with both increasing ϕ_{TMA} and c_S . Increasing the

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concentration of salt shifts τ_M to shorter times, but keeps the ϕ_{TMA} dependency constant, i.e. all the curves can be scaled. The τ_M using KCl are much smaller, in some cases 5 times so, than with NaCl. However, the dependence on ϕ_{TMA} is the same with both salts.

The gel time (from light scattering experiments) has been shown to be independent of salt concentration and to depend on the particle volume fraction with a power law of -1.6 for colloidal polymer gels with a fractal dimension of 2.1 [154]. Recently van der Linden et al [155] measured the τ_M of silica particle gels (Ludox HS – diameter 17 nm) with the addition of LiCl, NaCl and KCl. They showed that the volume fraction, ϕ , dependence was in agreement with $\phi^{-1.7}$ as predicted by a DLVO type model with an added hydration potential. Our data follows the same power law dependence rather well for the lowest volume fractions of TMA. For $\phi_{\text{TMA}} > 10$ vol%, the behavior deviates from the power law. The theoretical prediction associated with the $\phi_{\text{TMA}}^{-1.7}$ implies a fractal dimension of 2.1 for all concentrations [152], experimentally we observe a fractal behavior only for $\phi_{\text{TMA}} \leq 10$ vol%. The changes in the structural properties at high volume fraction of TMA can explain why at the highest concentrations τ_M decreases more strongly than the theorized $\phi_{\text{TMA}}^{-1.7}$ slope.

After this complete study of the macroscopic behavior, we turn our attention to the timescales of local structural evolution, which have not been previously studied. The values of τ_X measured are plotted for both salts in Figure 5.4 (c,d). The τ_X values found are smaller than τ_M apart from the highest ϕ_{TMA} where the two times become comparable. The values of τ_X also decrease as ϕ_{TMA} is increased. Nonetheless the τ_X dependency with ϕ_{TMA} does not follow the power law scaling of -1.7 observed macroscopically, even if there is no reason why a local structural transition should evolve in the same way as the macroscopic yield stress.

Instead of $\phi_{\text{TMA}}^{-1.7}$, the ϕ dependence in microscopic gelation time is $\phi_{\text{TMA}}^{-1.0}$ as shown in Figure 5.4 (c) and (d). This is an indication that we are at the early stage of the aggregation when the first clusters start to form by Brownian diffusion and aggregation. The behavior at this stage, also known as perikinetic aggregation, was pioneered by Smoluchowski coagulation (or population balance) equation [156]. In this case the cluster size distribution evolves as

$$\frac{N_k}{N_0} = \frac{(t/t_{0.5})^{k-1}}{(1+t/t_{0.5})^{k+1}} = f(t/t_{0.5}) \quad (5.2)$$

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where N_k is the number of clusters of size k and N_0 the initial number of monomers. This population density evolves in time following a single time-scale, the half-life, that following Smoluchowski takes the form

$$t_{0.5} = \frac{1}{K_S W} = \frac{3\eta}{4K_B T \rho_0 W} \propto \frac{1}{\phi} \quad (5.3)$$

where k_S is the Smoluchowski rate of aggregation as defined by diffusion. The term W is the Fuchs stability ratio that takes into account the form of the inter-particle potential which in turn depends on salt concentration. For the same salt concentration, $t_{0.5}$ will scale as the inverse of the packing fraction as is observed in the data in Figures 5.4 (c, d).

Interestingly, if we estimate the time at which the $S(q_0)$ stops evolving (time to reach the plateau values in Figure 5.3 b) and compare it with τ_M we can see that for most of the samples the gel becomes stress-bearing much before the structure has been fixed at the scale of a few colloidal particles. This may suggest that particle rearrangements take place at the microscopic scale, even if the gel is macroscopically arrested. This might imply that the mechanical properties are still evolving, as we shall see in the section 5.2.4.

5.2.4 Scaling

Now that we have seen the ϕ_{TMA} dependence on both timescales, those data are compared to better understand the effect of the salt concentration and type on the gel formed. It has previously been shown that for a fixed particle volume fraction the evolution of the structure and the mechanical properties of gels formed with different concentrations of NaCl can be completely scaled onto a master curve by introducing an appropriate gel time for normalization [154, 157, 158]. It was shown that changing the concentration of NaCl only changes the kinetics of gelation and alters neither the structure nor the strength of the gel formed thereafter.

Similarly, we now show that it is possible to scale both τ_M and τ_X . One can see in Figures 5.4 that the ϕ_{TMA} dependence is the same for all of the salt concentrations and both salts. This means that we can use simple multiplicative constants to collapse all the data, these constants are defined as β_M and β_X (the data with 500 mM of added KCl have been chosen as a reference). Our rescaled data is shown in Figure 5.5,

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where we see a complete collapse of the data for both salts. Therefore we show that a single constant works for a range of particle volume fractions. The values of β are summarized in Table 1. One can note that in most cases, the values obtained for β_M and β_X are the same, so in the following we will refer to the scaling factors β used either for microscopic or macroscopic scaling.

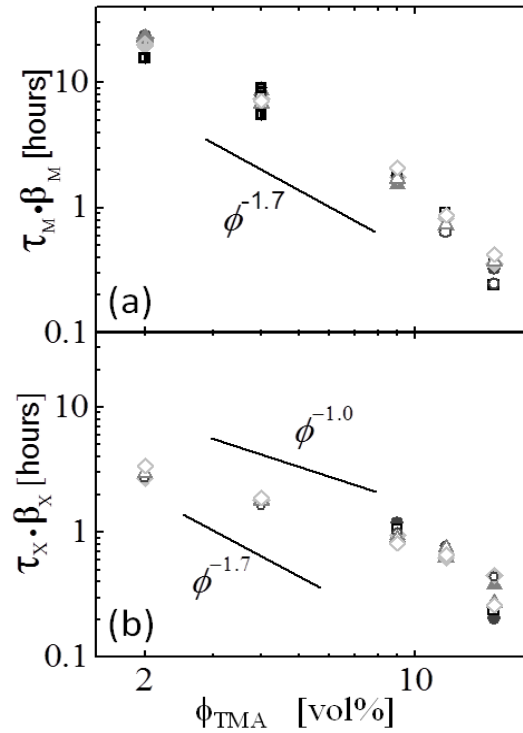


Figure 5.5 The normalized transition times from the macroscopic observations $\beta_M \tau_M$ (a) and from the SAXS experiments $\beta_X \tau_X$ (b).

	NaCl/mM				KCl/mM			
	100	200	300	500	100	200	300	500
β_M	0.005	0.04	0.12	0.3	0.04	0.3	0.6	1.00
β_X		0.04	0.09	0.3	0.02	0.3	0.6	1.00

Table 1 The scale factors β used to collapse the values of τ_M and τ_X onto master curves for the different salt concentrations and types.

The scaling of τ_X (extracted from $S(q_0, t)$) indicates that at a given length-scale the structural evolution is equivalent if the normalized time βt is used. Figure 5.6

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shows the full $S(q)$ for 9 vol% TMA and 500 mM KCl and NaCl at $\beta t = 3$ hours. We find that the curves coincide very well over the range of q values once again using the scaling factor β . In the inset we show that the choice of β is appropriate over the full evolution of the structure, as normalizing the time with β leads to a collapse of the two $S(q_0)$. This means that variation of the structural evolution with the two salt types can be fully captured by a single scaling factor.

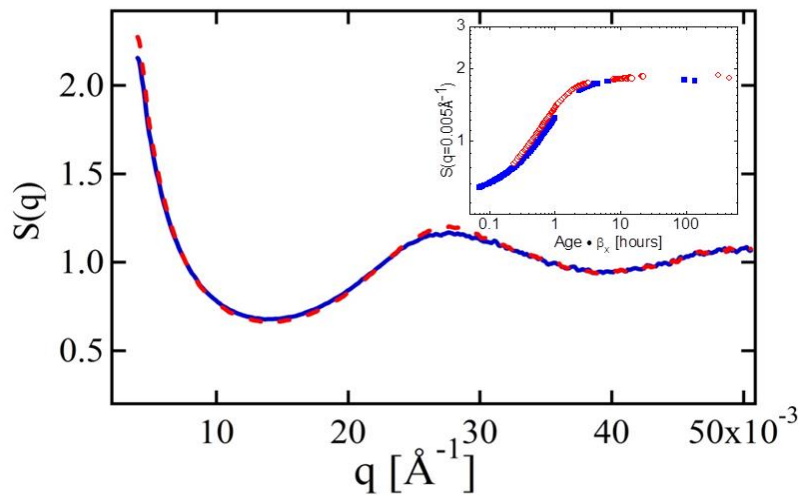


Figure 5.6 Structure factor $S(q)$ for the samples of 9vol% TMA and 500 mM salt with KCl at 3 hours (dashed line) and NaCl at 10 hours (solid line). The inset is shows $S(q=0.005 \text{\AA}^{-1})$ where the time is scaled with β_x for the same sample NaCl (empty symbols) KCl (filled symbols).

The τ_M are linked to the mechanical properties of the gels, and we have seen that, similarly with the structural variation, the time to reach a given yield stress can be normalized by a scaling factor. This has led us to measure the storage and loss moduli of a gel after 1, 4 and 100 days at fixed frequency 10 Hz and strain 1 % with $\phi_{\text{TMA}} = 9$ vol% $c_S = 500$ mM for both salts. The kinetic dependencies of the moduli during the gel-formation in the presence of both NaCl (filled symbols) and KCl (open symbols) are presented in the inset in Figure 5.7. One can see that for both samples G' and G'' continue to increase with gel aging even after the macroscopic transition time is elapsed. In addition it is clear that at a given time the values of G' and G'' are much higher for gels formed with KCl compared to those with NaCl, at early times the elastic modulus of a gel with KCl is more than 10 times higher than with NaCl. This

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is in agreement with previous studies where the counter ion type has been shown to affect gel stiffness [151, 159]. However, the difference is decreased as the gel ages.

However we know that the structure of the gels evolves towards a final state that mainly depends on ϕ_{TMA} . It has already been shown that for a single salt the mechanical properties can be scaled at fixed particle volume fractions [157, 158]. We plot the G' and G'' as a function of βt for both salts in Figure 5.7. We obtain a master curve with both the samples containing NaCl and KCl, once more confirming that the effect of counter ions on the mechanical properties is a kinetic one. We want to stress that this scaling is obtained using a parameter that is determined from a completely independent set of scattering experiments. Therefore, our analysis of the kinetics seems to be rather robust.

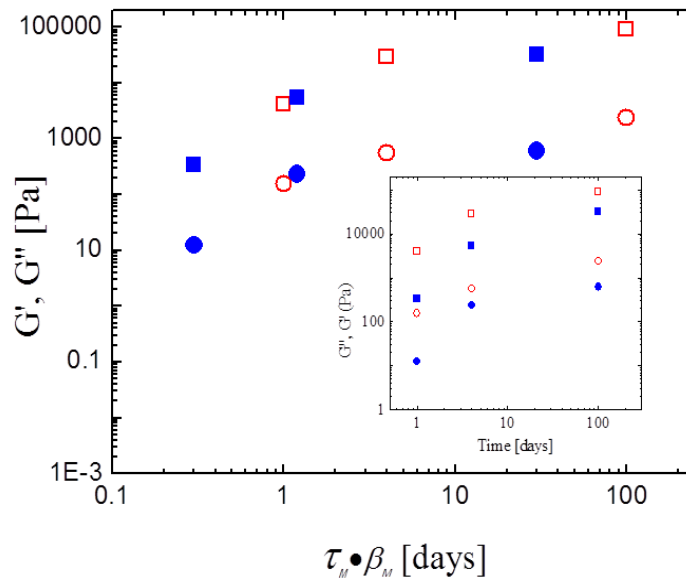


Figure 5.7 Storage (squares) and loss (circles) moduli as a function of time for the sample with $\phi_{\text{TMA}} = 9 \text{ vol}\%$ $c_S = 500\text{mM}$ NaCl (filled symbols) and KCl (empty symbols). The frequency is 10 Hz and the strain 1 %. The inset shows the raw data and in the main figure the time has been scaled by β_M .

This study shows that for a fixed particle volume fraction changing the type of salt can only influence the kinetics of gelation and not the properties of the gel when fully formed. This means that for different types of salts and salt concentrations, it is only a matter of time to obtain a given property in the gel sample. Therefore, depending at which time a certain physical property is required (e.g. a given yield stress), the appropriate salt type and concentration can be selected to achieve it.

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Moreover, we have also shown that the scaling factors are exactly the same for the two time sets (macroscopic and microscopic, see Table 1), despite being linked to structure and mechanical properties at very different length-scales. This confirms the universal nature of gelation over the length and time-scales.

In order to understand the meaning of the normalization times further, we return to the half-life $t_{0.5}$. Here, salt effects are accommodated in the value of W (the Fuchs stability ratio), which is confirmed by the ability to scale all the points (independently of the packing fraction). Figure 5.8 shows that β vary linearly with c_s ,

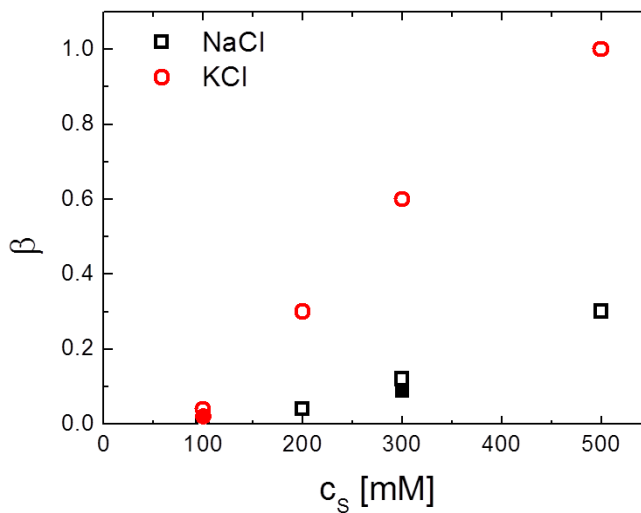


Figure 5.8 Normalization constants, β , as a function of salt concentration for NaCl (circles) and KCl (squares). The filled symbols are shown for the two values of τ_x where the β are slightly different between the τ_x and the τ_M .

which implies that W decreases as c_s^{-1} . This decay is close to a previous investigation on larger particles by light scattering [160], but rather different from what was found with fluorinated polymer colloids at lower salt concentrations [158]. Recently Oncsik *et al.* showed that the differences in the aggregation rates in the presence of different types of salts could be rationalized by taking into account the changing surface charge with the varying ion adsorption [82]. We have measured the zeta potential of our particles at 0.5 vol% in the presence of different concentrations of NaCl (blue square) or KCl (red circle) as shown in Figure 5.9. The zeta potential is a key indicator of the stability of colloidal dispersions. The magnitude of the zeta potential shows that the degree of electrostatic repulsion between adjacent, similarly charged particles in a dispersion. It can be seen that for both salts as the salt concentration increased the zeta

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potential increased too, and the zeta potential with KCl is always higher than with NaCl. This suggests that more KCl is adsorbed on the particle surfaces, and it seems that the differences in W could be the direct result.

A complete description of the microscopic mechanisms leading to the changing kinetics of gelation is still missing, but adding our results to the other recent observations of the strongly changing particle-particle interactions with ion type [92, 161, 162] should provide further testing ground for the predictions of the current theories [41].

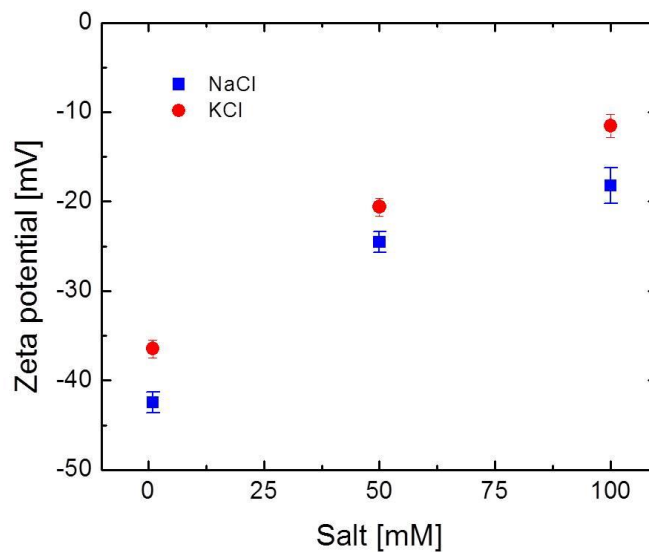


Figure 5.9 Zeta potential evolution with salt concentration in the presence of 0.5 vol% TMA, the red circles are with KCl and blue squares with NaCl.

5.2.5 Gel rheology at a given time

From Figure 5.7, we know that at a given time the values of G' and G'' are much higher for gel samples formed with KCl compared to those with NaCl. However, they can be scaled onto a master curve by using the scaling factor β , which means that the structures produced from both salts are the same after the gels have been allowed to age significantly. It should be noticed that the strain used during the measurement in Figure 5.7 is very small (1 % fixed) in order not to destroy the structure of the gels. Nevertheless, it is worth to see what the structure response of gels formed with both salts when the strain is gradually increased to destroy their structure.

Chapter 5 Influence of salt type on gelation kinetics (NaCl or KCl)

Storage modulus (G') and loss modulus (G'') of the gels were measured with the sample $\phi_{\text{TMA}} = 9 \text{ vol\%}$ in the presence of $c_S = 300 \text{ mM}$ NaCl (blue circle) or KCl (red square) 1 week after preparation as shown in Figure 5.10, where the strain rate is kept constant at 5 s^{-1} and the strain is from 0.05 to 25. For both salts, the solid symbol is corresponding to G' and the open one is corresponding to G'' .

It can be seen that for both samples G' and G'' are constant when the strain is small, this is because in the range of small strain the structure of the gels have not been destroyed. Then as the strain continues to increase, G' gradually decreases and G'' gradually increases after a certain point, where the structure of the gels start to be destroyed. From Figure 5.10, one can note that there is a point at which the values of G' is equal to G'' . When the strain is exceeds than that point, the value of G' is lower than G'' , indicating the sample became from solid to liquid state. With NaCl the value of strain at that point is 12.5 and with KCl is 10. The result shows that for NaCl it needs higher strain to break the gel structure from solid to liquid state. It also can be seen that the strain needed is higher with NaCl than KCl when G' is began to decrease. Therefore the gels formed with KCl are stronger at a certain point in time, although they at long times they end up the same.

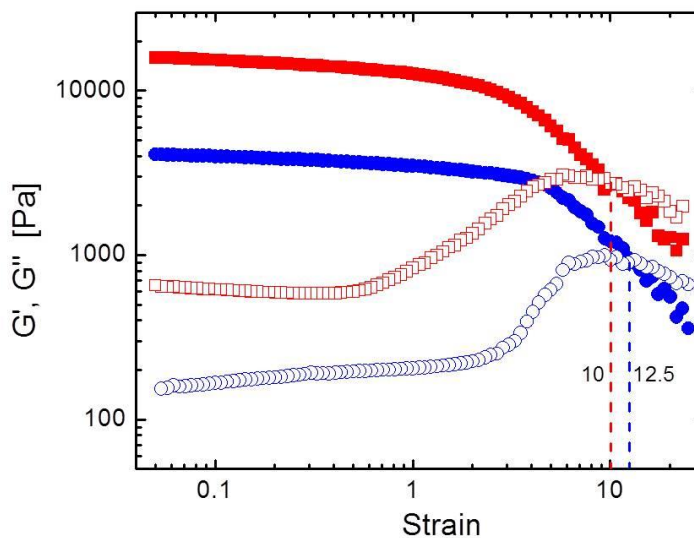


Figure 5.10 Storage modulus(solids) and Loss modulus(opens) evolved as strain with the sample $\phi_{\text{TMA}} = 9 \text{ vol\%}$ $c_S = 300 \text{ mM}$ at strain rate 5 for KCl (red square) and NaCl (blue circle) after 1 week preparation. The strain of $G'=G''$ with KCl is 10 and NaCl is 12.5.

5.3 Conclusions

In this Chapter the salt-specific effects on the gelation process were investigated through adding NaCl or KCl to a suspension of colloidal silica. Macroscopic observations showed that the solidification with KCl is much faster than with NaCl. This was in agreement with results obtained from SAXS experiments where the evolution of the microstructure of the samples was followed and the characteristic timescale of local structural arrest extracted. Both the macroscopic observations and the local structure can be scaled onto a single master curve suggesting that the counter ion type changes the timescale of gelation but not the equilibrium structure. This equivalence of the structures over several length-scales is further confirmed by the collapse of the storage and loss moduli when normalized with a scaling factor.

Further, the simple possibility to scale all our results suggests that the final gel characteristics depend only on the volume fraction of TMA particles, at least when salts such as NaCl or KCl are used. Mastering the properties of a gel is a very important due to the range of applications in which they are found. This work highlights that comparing properties of gels at times shortly after their formation can be misleading if their long term characteristics are sought after.

The effect of salt in Soft Matter is extremely subtle. The Hofmeister series for the precipitation and the “salting in” and “salting out” effects have been known for more than a hundred years but their physical origin still remains elusive. In this work, we have explored the effect of this observation on gelation. Indeed the two salts explored here, result in different gelation times but the final gels are very similar in structure and mechanical properties. This observation suggests that one could speedup gelation without changing the structural properties of the final gel by simply choosing the correct salt in the Hofmeister series.

Chapter 6 Influence of different salts on the gelation kinetics

6.1 Introduction

In Chapter 5, the salts used for investigating ion specific effects on the gelation process were NaCl and KCl. The results show that the counter ion type only changes the timescales of gelation but not the equilibrium structure. It would be interesting to see if the equivalence between the two salts can be extended to other monovalent salts and even to divalent ones.

In this section, in addition to NaCl and KCl, the monovalent salts LiCl, CsCl and a divalent salt MgCl₂ are selected to study the ion effect on the gelation process by adding salt to the suspension of silica particles. In Chapter 5, the betas we obtained are from scaling of the macroscopic and microscopic timescales. We are wondering that if there is an easier way to get the information of betas.

As an example, Figure 6.1 is the results of light transmission with samples 9 vol% TMA and 500 mM NaCl (open square) and KCl (open triangle). (a) is the normalized transmitted light intensity with time using the formula $\frac{I(t) - I(\infty)}{I(0) - I(\infty)}$, where I(t) is the

Chapter 6 Influence of different salts on the gelation kinetics

transmitted light intensity in time, $I(\infty)$ is the transmitted light intensity after it stops evolving and $I(0)$ is the transmitted intensity at time $t=0$. It can be seen that the normalized intensity decreases with time for both salts. However, the decrease is faster with KCl than with NaCl. The transmission decreases as the particle size increases. In our case it means that I is linked to the aggregation of TMA. This means that the aggregation rate of silica particles in the presence of KCl is faster than with NaCl. We already knew this from the SAXS experiments shown in the previous chapter. All of the different measurements performed in Chapter 5 could be scaled onto master curves using appropriate normalization constants. It would then seem reasonable that the transmitted intensity could be too.

If indeed it can, it would be a simple way to get the information of relative timescales of gelation with different kinds of salts.

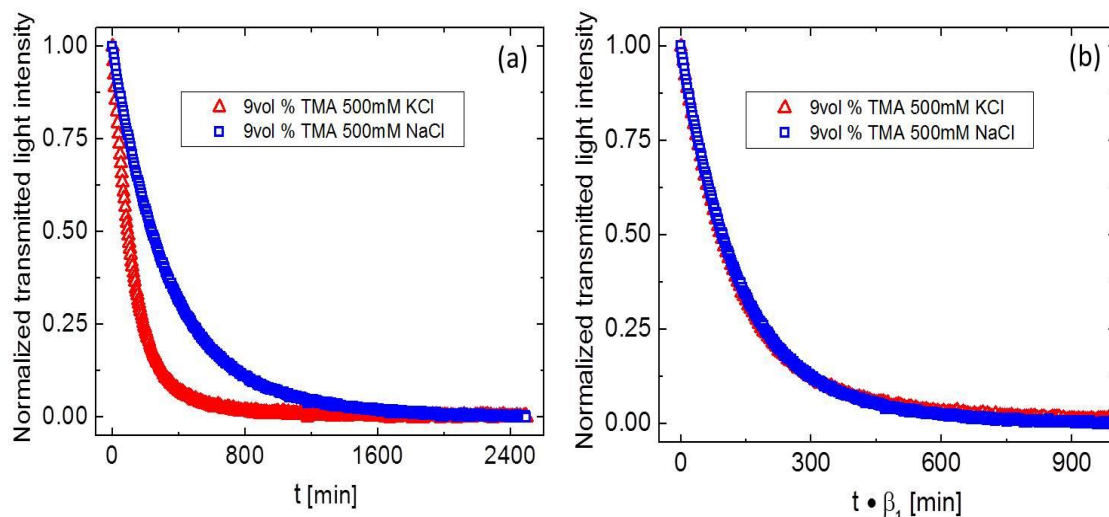


Figure 6.1 Normalized transmitted light intensity evolved in time (a) and scaled time (b) with 9 vol% TMA and 500 mM NaCl (open square) and KCl (open triangle).

The good news is that the normalized transmission light intensity can be scaled as shown in (b) and the two curves coincide very well. The scaling factor, called β_1 is 0.4, which compared with 0.3 obtained in Chapter 5 can be considered very good within the experimental error.

Therefore, in this Chapter, we will use the light transmission method to investigate the ion specific effects on the gelation process by adding salts $MgCl_2$, $LiCl$, $NaCl$, KCl , $CsCl$ in the suspension of silica particles separately.

6.2 Results and discussion

6.2.1 General observation of gel samples

Four different kinds of monovalent and one bivalent salt are used in the light transmission experiments. The range of TMA concentration is from 4 vol% to 16 vol% and salt is from 100 mM to 500 mM. In this part, we take the middle concentration 9 vol% TMA and 300 mM salt as an example. The photographs of the samples at 0, 3 and 6 hours are shown in Figure 6.2. One can see that just after the samples prepared at 0 hour, the color of the sample with CsCl is most dark, the rest of other salts are lighter. With time increased to 3 hours, all of the samples became darker. Up to 6 hours, we can't see much difference by eyes of the color changes except salt LiCl.

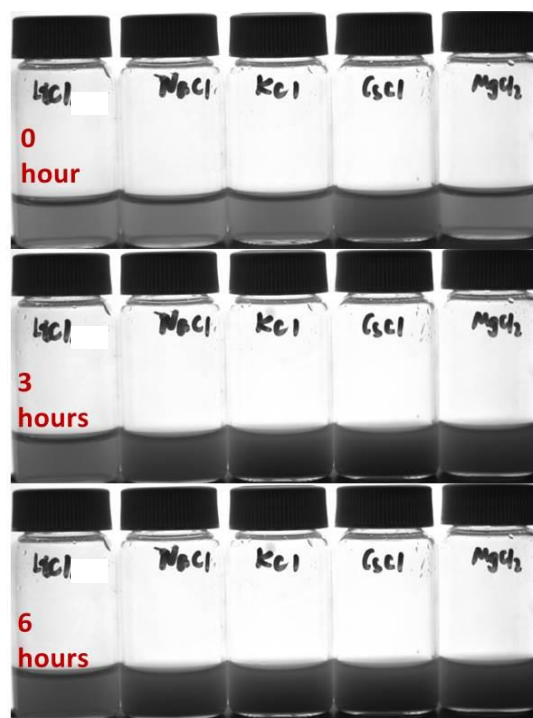


Figure 6.2 Photographs of samples with 9 vol% TMA and 300mM salt at 0, 3 and 6 hours. From left to right, the salts are in order of LiCl, NaCl, KCl, CsCl and MgCl₂.

The software Image J is used to extract the information of transmitted light intensity with time. Figure 6.3 gives the normalized transmitted light intensity evolution in time. As the gelation proceeds, the transmission decreased for all salts. This is because of the aggregation of silica particles. The more aggregation proceeds

the less light is transmitted through the sample. The rate of aggregation is the fastest with CsCl and slows down according to the order of salt $\text{CsCl} > \text{KCl} > \text{LiCl} > \text{MgCl}_2 > \text{NaCl}$.

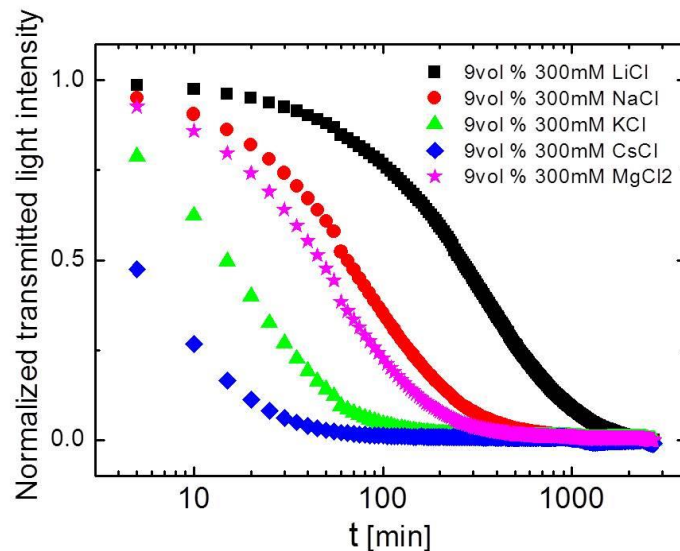


Figure 6.3 Normalized transmitted light intensity as time in the presence of 9 vol% TMA and 300 mM LiCl (square), NaCl (circle), KCl (triangle), CsCl (diamond) and MgCl_2 (star).

6.2.2 The scaling behavior

From Figure 6.1, we know that the curves of normalized transmitted light intensity with time can be scaled onto the same curve in the presence of salt NaCl and KCl. Now we are trying to know if the curves with all the salts used can be scaled, Figure 6.4 shows the curves with all the salts after scaling in the presence of 9 vol% TMA and 300 mM salt, β_I is the time scaling factor. In order to keep the same way to get β_I , here the curve with 9 vol% TMA and 500 mM KCl was fixed as reference, whose value was considered as 1, then we shift the curves with other kinds of salt onto it. The scaling factors β_I are given in Table 1 following the salt order: LiCl (0.042) < NaCl (0.15) < MgCl_2 (0.24) < KCl (0.67) < CsCl (2.1). Together with the normalized transmitted light intensity in Figure 6.3, we know that the aggregation rate was faster with larger value of β_I . One can see that all the curves coincide extremely well. It suggests that the evolution with different kinds of salts can be scaled at fixed silica and salt concentration.

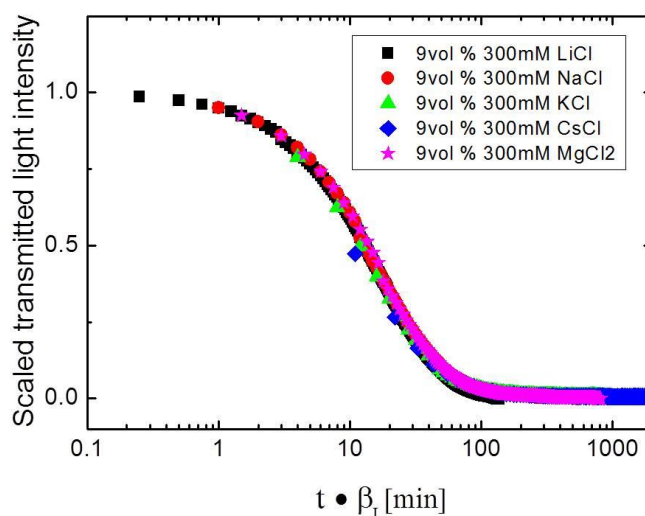


Figure 6.4 Scaled transmitted light intensity with scaled time for the sample of 9 vol% TMA and 300 mM LiCl (square), NaCl (circle), KCl (triangle), CsCl (diamond) and MgCl₂ (star).

We repeated the experiment with other TMA and salt concentrations, and the β_I are shown in Table 6.1. The ways to obtain β_I are the same, the curve with 500 mM KCl is fixed as reference 1 for each TMA concentration, see the red color part in Table 6.1. Then we shift the curves with other different concentrations of salts onto it. Errors are given for each value of β_I . The empty region in Table 6.1 is because the experimental time of the samples is not long enough and the transmitted intensity has not reached its plateau. The values in blue mean that the tail of normalized transmitted light intensity is not quite flat, so the blue values may not be accurate as $I(\infty)$ is overestimated.

From Table 6.1, it can be seen that at fixed salt concentration, the β_I are increased following the salt order: LiCl < NaCl < MgCl₂ < KCl < CsCl and their values are almost the same within the errors in the range of TMA concentrations for each kind of salt. As the salt concentration is increased the β_I increase except the samples with 500 mM CsCl. From the results of Chapter 5, we know that the type of counterion only changes the kinetics of gelation but not the final gel characteristics, which depend only on the volume fraction of TMA particles. In Chapter 5, there are only two kinds of monovalent salt used. In this Chapter, we can use the light transmission method to scale the normalized transmitted light intensity to obtain β_I as in Chapter 5, but with more monovalent salts and even the bivalent salt used. The results may suggest that we can extend the conclusions in Chapter 5 to more monovalent salts and even to the

Chapter 6 Influence of different salts on the gelation kinetics

bivalent salt. These may as well indicate that the scaling behavior of specific ion effect on the aggregation of colloidal particles is universal.

TMA/vol% Salt/mM	LiCl	NaCl	KCl	CsCl	MgCl ₂	
4 100			0.065 ± 0.005	0.4 ± 0.03	0.05 ± 0.002	4 500 KCl 1
9 100			0.043 ± 0.003	0.36 ± 0.01	0.035 ± 0.002	9 500 KCl 1
12 100		0.0115 ± 0.0005	0.08 ± 0.005	0.65 ± 0.02	0.05 ± 0.002	12 500 KCl 1
16 100		0.018 ± 0.001	0.1 ± 0.005	0.5 ± 0.03	0.057 ± 0.002	16 500 KCl 1
4 200		0.055 ± 0.002	0.35 ± 0.01	2.00 ± 0.1	0.14 ± 0.01	4 500 KCl 1
9 200		0.049 ± 0.03	0.29 ± 0.01	1.5 ± 0.1	0.11 ± 0.01	9 500 KCl 1
12 200	0.021 ± 0.001	0.07 ± 0.01	0.37 ± 0.3	1.5 ± 0.1	0.13 ± 0.01	12 500 KCl 1
16 200	0.035 ± 0.002	0.1 ± 0.01	0.5 ± 0.01	1.7 ± 0.1	0.17 ± 0.01	16 500 KCl 1
4 300	0.042 ± 0.002	0.13 ± 0.01	0.56 ± 0.03	1.8 ± 0.1	0.25 ± 0.01	4 500 KCl 1
9 300	0.042 ± 0.002	0.15 ± 0.01	0.67 ± 0.03	2.1 ± 0.1	0.24 ± 0.01	9 500 KCl 1
12 300	0.07 ± 0.005	0.19 ± 0.01	0.7 ± 0.03	1.8 ± 0.1	0.23 ± 0.01	12 500 KCl 1
16 300	0.095 ± 0.005	0.25 ± 0.02	0.8 ± 0.03	1.6 ± 0.1	0.27 ± 0.03	16 500 KCl 1
4 500	0.16 ± 0.01	0.36 ± 0.02	1	1.6 ± 0.2	0.75 ± 0.05	4 500 KCl 1
9 500	0.15 ± 0.01	0.42 ± 0.03	1	1.5 ± 0.5	0.58 ± 0.02	9 500 KCl 1
12 500	0.25 ± 0.02	0.5 ± 0.03	1	1.3 ± 0.5	0.57 ± 0.03	12 500 KCl 1
16 500	0.27 ± 0.02	0.5 ± 0.03	1	1.4 ± 1.0	0.5 ± 0.03	16 500 KCl 1

Table 6.1 Scaling factors β_1 are obtained by taking 500 mM KCl (red color) as reference for each volume fraction of silica particles. The range of TMA is from 4 vol% to 16 vol% and salt concentration is from 100 mM to 500 mM. The values in blue indicate that the experimental time is not long enough to get the flat tail in the transmission, so the value maybe not accurate. In the empty region the gelation time of the samples is longer than the experimental time.

The scaling factor β_1 reflects the aggregation rates of silica particles, which means that the aggregation rates increased following the above salt order and as the salt concentration increased except for the sample with 500 mM CsCl. When observing the values of β_1 with CsCl, one can see that there is a peak at 300mM as the concentration of CsCl increased. This implies that at 300 mM the aggregation rate of silica particles is fastest. Then if we continue to increase the concentration of CsCl the aggregation rate decreased. It seems that this behavior is contradictory to other salts.

However, many studies have shown that a strong adsorption of the counter ion onto the particle surface, which can lead to its charge reversal [82, 92]. Moreover, the recent research shows that the ion specific effects in the aggregation process are mainly because of the variation in ion adsorption changing the surface charge [82]. In our case, the aggregation of silica particles is the fastest in the presence of CsCl, which suggests that the interaction of Cs^+ is the strongest with the surface. At some point, when the adsorption is enough the surface charge will reverse and the aggregation rate will decrease as at 500 mM CsCl. The good thing is that even the surface charge is reversal the gelation process still can be scaled.

6.2.3 Half-time of the transmitted intensity

Another way to look at the transmitted data is to compare the time it takes for the intensity to decrease by half, and this time is defined as τ_{half} . This time could be linked to the aggregation similarly to τ_x , but at a larger length-scales. Figure 6.5 gives the relationship between τ_{half} and the volume fraction ϕ of TMA with all the monovalent salts used. (a) is with LiCl, (b) with NaCl, (c) with KCl and (d) with CsCl, the range of salt concentration used is from 100 mM to 500 mM and ϕ_{TMA} is from 4 vol% to 16 vol%.

All the data decreased as the volume fraction of silica particles increased and the salt concentration increased. From (a) to (d), the τ_{half} with LiCl is the largest and CsCl is the smallest at a fixed salt and silica concentration. The volume fraction dependence of power law -1.7 is plotted in each graph in Figure 6.5. Rather surprisingly, we can be seen that the τ_{half} of first three kinds of salt follow the $\phi^{-1.7}$ dependence very well. It means that the transmission probes length-scales are sufficiently large, which linked to the gel structure but not to the initial small aggregation like τ_x in Chapter 5.

However, for the salt of CsCl as given in Figure 6.5(d), the overall trend of the data follows the same linear relationship, but there have deviation at some points. The data are very close for different concentrations of CsCl except 100 mM at the range of TMA volume fraction. This is because that the aggregation of silica particles with CsCl is very fast. The transmitted light intensity decreased by half is accomplished in less than 10 minutes for most of the samples. Before taken the photos, it will spend 2

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or 3 minutes for sample preparation. For the sample with slower gelation time, the sample preparation time can be neglected compared with τ_{half} . However, for the sample with CsCl, its value is comparable with τ_{half} . Therefore, for this kind of salt the time τ_{half} we got may not be accurate.

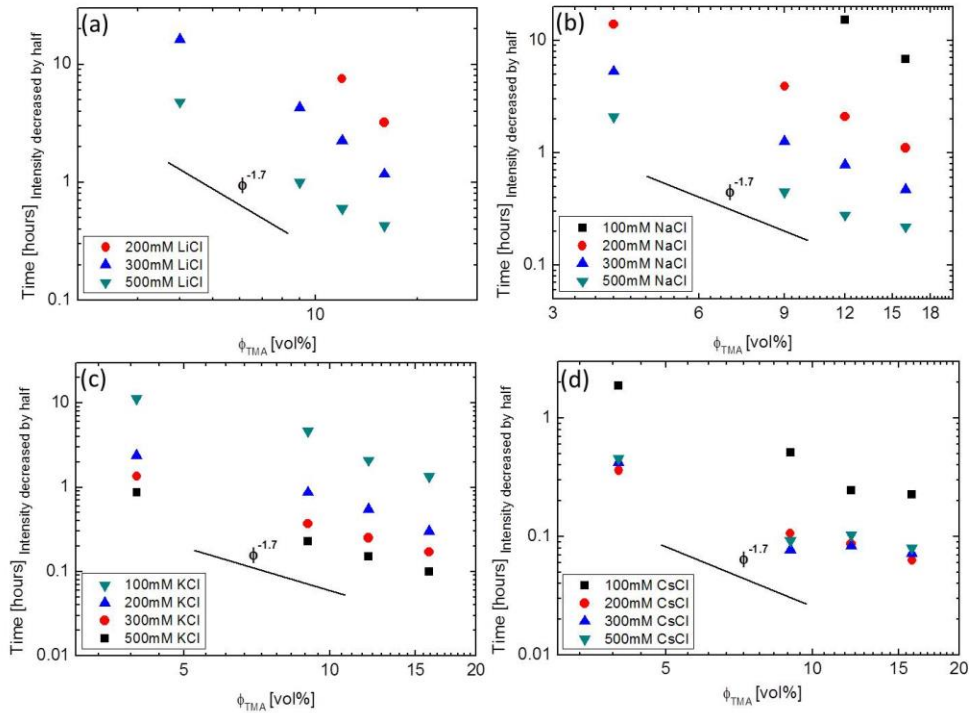


Figure 6.5 The time of normalized transmission light intensity decreased by half with monovalent salt (a) LiCl, (b) NaCl, (c) KCl and (d) CsCl. The range of salt concentration is from 100 mM to 500 mM and ϕ_{TMA} is from 4 vol% to 16 vol%.

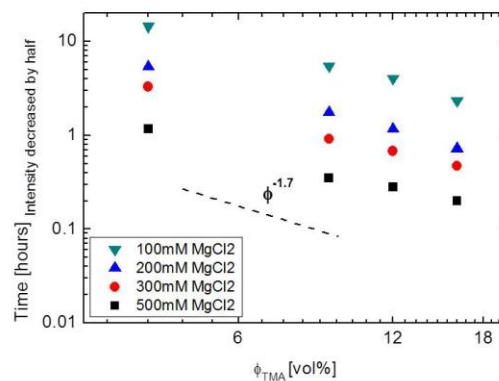


Figure 6.6 The time of normalized transmission light intensity decreased by half with divalent salt MgCl_2 . The range of salt concentration is from 100 to 500 mM and ϕ_{TMA} is from 4 vol% to 18 vol%.

The time of normalized transmission light intensity decreased by half with divalent salt $MgCl_2$ is shown in Figure 6.6. The line $\phi^{-1.7}$ is also plotted in the graph and all data are agreed well with the $\phi^{-1.7}$ dependence although the salt is bivalent. Moreover, the relationship between the data and ϕ_{TMA} and the salt concentration have the same trend as the monovalent salt. The results suggest that the ions with different valence have the same mechanism on the effects of gelation process.

From Figure 6.5 and 6.6 we can see that the volume fraction variation leads to a power law -1.7 for the τ_{half} for both monovalent and bivalent salts at all concentrations used (only the CsCl shows some deviation). Because τ_{half} is just one point of the full intensity curves we have collapsed in 6.2.2, they should be scalable onto a master curve as well using the β_I we already obtained in Table 6.1. The scaled data is given in Figure 6.7, where we can see the good collapse for all salts even there are some scattered points, which are attributed to the salt with CsCl. The advantage to look at τ_{half} is to see ϕ dependence, which we can't obtain from the intensity $I(t)$.

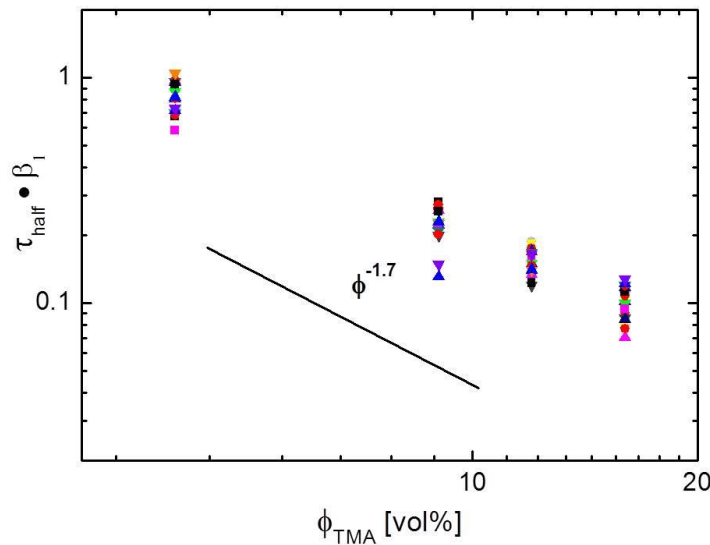


Figure 6.7 The normalized time of transmitted light intensity decreased by half for the different salt concentrations and types with the volume fraction of silica particles.

6.2.4 Stability of the gel system

Figure 6.8 shows the relationship of $1/\beta_I$ and normalized salt concentration. Mg^{2+} is the bivalent ion, so we need to normalize it by multiplying by 2 when comparing the results with monovalent salt. As discussed above, the scaling factors β_I

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are almost the same at all volume fractions of TMA particles for a given salt concentration. Therefore, the data in Figure 6.8 with 4, 9, 12, 16 vol% TMA are almost the same. With the first three kinds of salt, all data decrease as the salt concentration increased. However, with KCl and CsCl, the data seem to stop decreasing at the higher concentrations and even increase a little with CsCl.

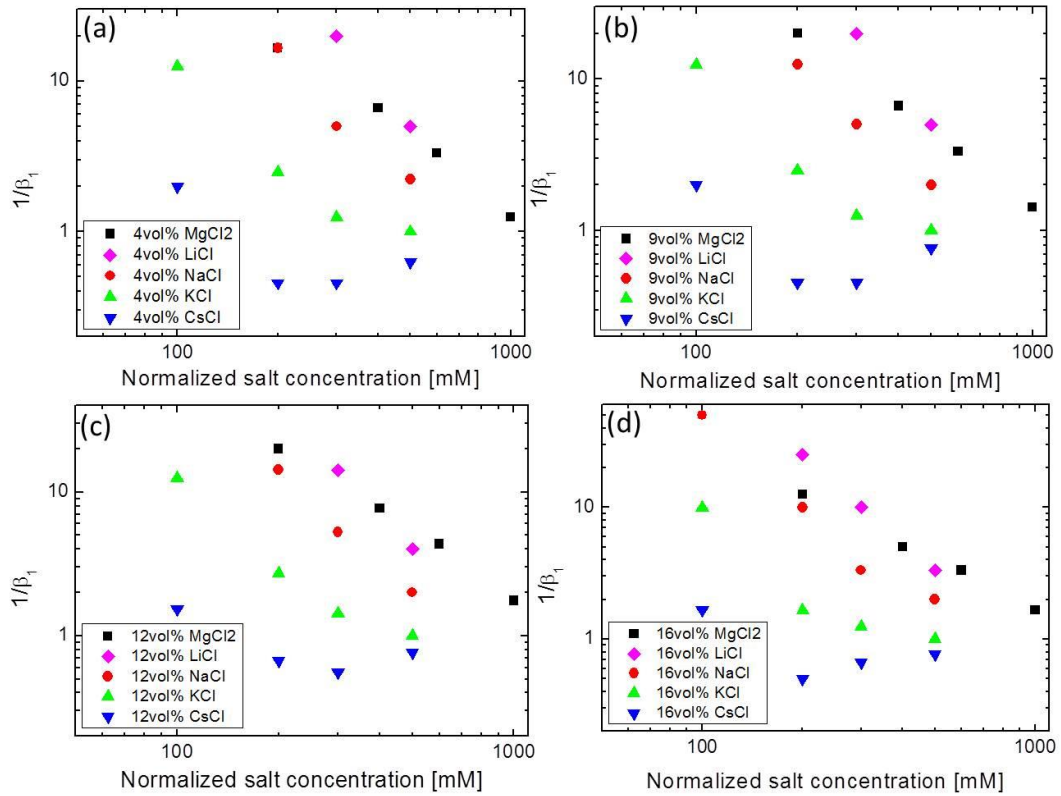


Figure 6.8 The inverse of scaling factor, $1/\beta_1$, as a function of normalized salt concentration for MgCl₂ (square), LiCl (diamond), NaCl (circle), KCl (up triangular), and CsCl (down triangular) in the presence of 4 vol% TMA (a), 9 vol% TMA (b), 12 vol % TMA(c) and 16 vol % TMA(c).

From Chapter 5, we showed that $1/\beta_1$ is proportional to the Fuchs stability ratio W , which is linked to the interparticle potential. The interactions are different and the height of the potential barrier is the lowest with CsCl, probably because the charge of the TMA is lower. As discussed in 6.2.2 that the specific ion effects on the aggregation process is due to the ion adsorption onto the surface charge. At higher salt concentrations, excess absorbed the counterions can lead to the surface charge reversal [92]. This can explain why the W with CsCl at higher salt concentration is a little bit increased. We could imagine that with further increase in the salt concentration, the other salts may have the same trend.

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From top to bottom, the ability of salt to assemble silica particles follows the order: $\text{MgCl}_2 < \text{LiCl} < \text{NaCl} < \text{KCl} < \text{CsCl}$, which is also the Hofmeister series for the cations. However, the data of Mg^+ and Cs^+ seem to cross over at some point when the salt concentration is low. Within the experimental error, we can see that from the perspective of ion specific effects on the gelation process, both monovalent and divalent ions they are followed the Hofmeister series. Although the physical origin behind the Hofmeister series still remains elusive, our study gives the new insight on the ion specific effects in the gelation process.

6.3 Conclusions

Ion specific effects on the gelation process were investigated via adding LiCl, NaCl, KCl, CsCl or MgCl_2 to a suspension of colloidal silica. Light transmission was used to observe the gelation process. The results show that the transmitted light intensity can be scaled at different concentrations and types of salt. The volume fraction dependence of τ_{half} follows the power law -1.7 for both monovalent and bivalent salts at all concentrations selected. The influence of the salt type on the kinetics is similar to changing the quantity of salt as we saw also in the previous Chapter. This might lead one to speculate that the properties of all the silica gels are the same whatever the salt type, although to show this conclusively would require some further experiments.

Moreover, in this Chapter, the ability of ions to assemble the silica particles was investigated. They are following the Hofmeister series no matter monovalent salt or bivalent one.

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Chapter 7 Mix salt and surfactant to make ultrastable and stimulable foam

7.1 Introduction

Foams are found in a wide variety of applications in industry and personal life, such as firefighting, enhanced oil recovery, mineral flotation, food processing and personal care products. In some of these applications good foam stability is extremely important. All foams are thermodynamically unstable and are destined to disappear [163]. In order to prolong their life, various types of stabilizing agents are used, such as surfactants, polymers, proteins or particles [56]. These stabilizing agents adsorb onto the surfaces of the bubbles and slow down the different mechanisms by which foams age: drainage, coalescence and coarsening.

In some cases foams that are stable for very long periods of time are required, so called *ultrastable* foams, in which the processes of coarsening and drainage should be arrested. Previous studies have shown that the ultrastable liquid foam can be made using the dispersions of lamella liquid crystals [164], hydrophilic particles [65], mixed surfactant [165] and so on. Ultrastable foams have many applications in

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industry such as shown above in firefighting, enhanced oil recovery, mineral flotation. However, in other cases, good foam stability is initially required but at a given moment it should become unstable and disappear. Therefore, the destruction of foam is often required in practical applications. The foams should be stimuable. The foam stability can be tuned by the external stimuli parameters such as pH, magnetic fields, temperature and so on [166-171].

In this Chapter, we add NaCl or KCl to SDS to make ultrastable and temperature stimuable foam. We show that foam stability is controlled by the formation of crystals on the surface of the bubbles and in the aqueous phase. The time it takes for the crystals to form is the key factor to obtain stable foams. These ultrastable foams can be destroyed by heating above the Krafft boundary (below which precipitates form).

The work in this Chapter has finished and the results have been published: *Zhang, Li, et al. "Precipitating Sodium Dodecyl Sulfate to Create Ultrastable and Stimuable Foams." *Angewandte Chemie* 127.33 (2015): 9669-9672.*

7.2 Results and discussion

7.2.1 Foamability and foam stability with fixed SDS at room temperature

Foams were prepared using 69 mM SDS with added NaCl or KCl. Photographs of these foams as they evolve in time are shown in Figure 7.1. Samples in (a) and (b) were made with 250 mM and 500 mM of NaCl, while samples in Figures 7.1 (c), (d) and (e) were with KCl. The solutions with NaCl foam very well, all of the gas is incorporated in the foam. The foam with 250 mM NaCl disappears within 2 hours (even more quickly than foam with no added salt) as shown in 7.1 (a). With 500 mM NaCl given in Figure 7.1 (b), most of the foam collapses quickly but the remaining foam continues to evolve slowly: the bubble size increases while the height of the foam remains constant over several hours.

The instability of the foam with 250 mM added NaCl could be expected. The screening of the electrostatic repulsion between the two interfaces dominates over the effect of the increased surface concentration of surfactant and the films become

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unstable. The stability of the foam with 500 mM NaCl after an initial phase of foam collapse is surprising.

The behavior with KCl is very different as seen in Figures 7.1 (c) and (d). The foams produced are very similar with the two KCl concentrations. Not all of the air can be incorporated into the foam and even when the amount of liquid used is increased. We can only make around 8 mL of foam with an initial liquid fraction of around 50 %. We have not been able to make dry foams, only bubbly liquids. In a matter of seconds the bubbles have creamed to the top of the sample, and as they become close packed (liquid fraction around 30 – 40 %) the drainage slows down dramatically, but continues over several hours before arresting. The coarsening in these samples arrests as well. This leads to *ultrastable* foams, and as shown in Figure 7.1 (e), the foam is still intact after 6 months.

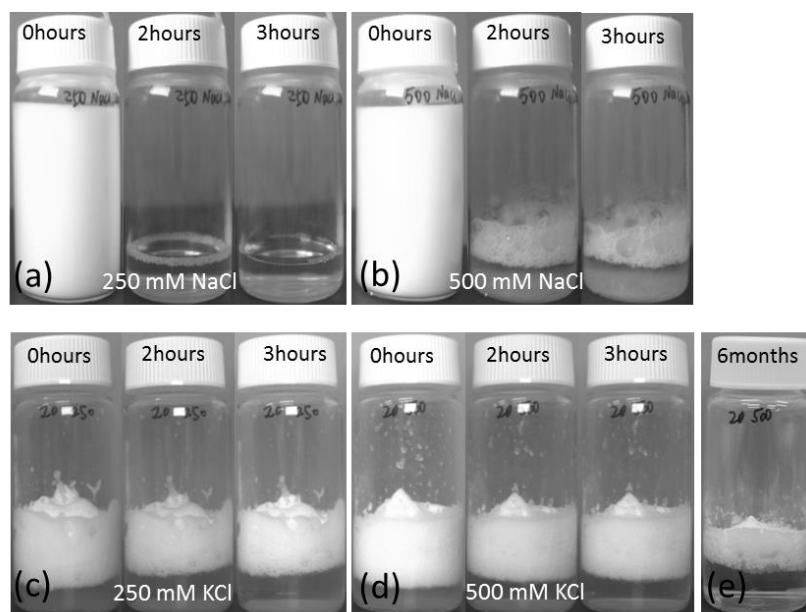


Figure 7.1 Photographs of foam samples made with 69 mM SDS and (a) 250 mM NaCl; (b) 500 mM NaCl; (c) 250 mM KCl; (d) 500 mM KCl, (e) sample (d) 6 months later.

We have also prepared foams from KDS with added KCl (69 mM with 500mM salt). These are much less convenient to work than their SDS homologues as the KDS solution needs to be heated up above the Krafft boundary (around 50 °C) to prepare the foams. However their appearance and stability are very similar to those from SDS with added KCl. In this Chapter we will mainly talk about the foam prepared with SDS.

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In order to understand these differences we take a closer look at the samples. We can see some precipitate at the bottom of the flask in Figure 7.1 (b), but nothing with KCl in Figure 7.1 (d). We made optical microscopy experiments on bulk samples (without foaming). In both samples the precipitates are composed of crystals. The crystalline domains formed with NaCl as given in Figure 7.2(a) are plate-like structures of tens of micrometers in size while the objects with KCl are smaller as shown in Figure 7.2(b).

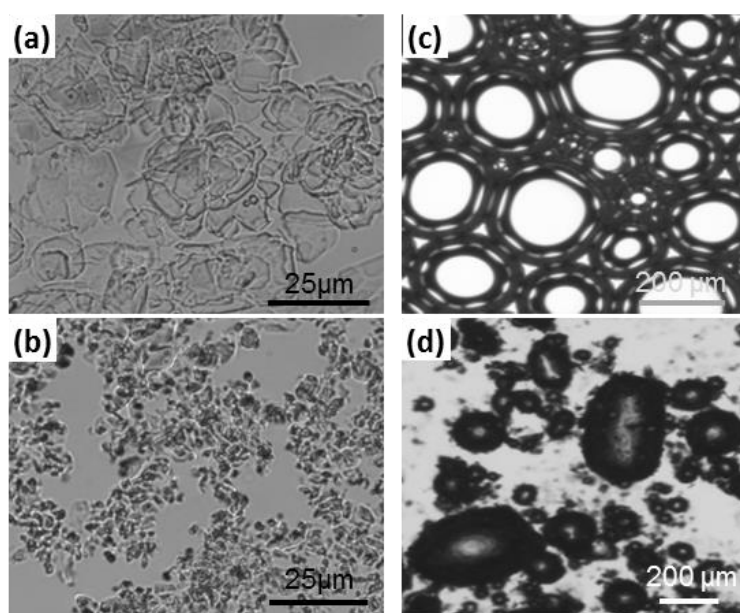


Figure 7.2 Microscope images of solution with 69 mM SDS and 500 mM NaCl (a) and KCl (b) taken a day after mixing. Images of bubbles immediately after preparation prepared with the same concentrations, NaCl (c) and KCl (d).

C_S / mM	$T_{\text{NaCl}} / ^\circ\text{C}$	$T_{\text{KCl}} / ^\circ\text{C}$
100	18.5 ± 0.5	40.5 ± 0.5
250	22.5 ± 0.5	45.5 ± 0.5
500	26.5 ± 0.5	51.0 ± 0.5
750	30.5 ± 0.5	53.5 ± 0.5
1000	33.5 ± 0.5	56.5 ± 0.5

Table 7.1 Temperature at which the crystals are no longer visible in the presence of 69 mM SDS with 250 or 500 mM salt.

The samples were heated to measure the temperature at which the crystals are no longer visible by eye (Table 7.1). From these values the enthalpies of dissolution, ΔH ,

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can be estimated using the Van't Hoff equation. We find $\Delta H_{\text{SDS}} = 75 \text{ kJmol}^{-1}$ and $\Delta H_{\text{KDS}} = 88 \text{ kJmol}^{-1}$. Like previously reported by Smith *et al.* [172], the enthalpy for the melting of SDS is slightly lower than KDS. However assuming that the energy gain of sodium is 84 kJmol^{-1} more than for potassium [144], the interaction energies are weaker in KDS than in SDS.

Figures 7.2(c) and (d) show photographs of bubbles taken under the microscope immediately after the generation of foaming the samples. The foam with NaCl (Figure 7.2c) looks exactly like normal surfactant foam: it is rather wet and the bubbles have a diameter of around $200 \text{ }\mu\text{m}$. The sample with KCl looks nothing like a surfactant foam (Figure 7.2d): the bubbles are much smaller (mostly below $100 \text{ }\mu\text{m}$ in diameter) and the larger bubbles are not spherical but ellipsoidal.

The presence of elliptical bubbles is surprising as the optimal shape for an air bubble is spherical. A non-spherical shape indicates that the interfaces are solid-like [173]. Therefore coarsening of bubbles is arrested making the foam stable (addition of KCl).

From Figure 7.2 (a) and (b) we know that the precipitates of solution with 69 mM SDS and 500 mM NaCl or KCl without foam are composed of crystals. In the foam with 500 mM NaCl, the solution collected at the bottom of the vial is slightly turbid. This implies that not all crystals are inside the foam. The solution that drains out of the foams prepared with KCl is transparent, despite a non-foamed solution being turbid. This means that the crystals can get trapped and collect in the Plateau borders, to stabilize the foam against drainage [174, 175]. In Figure 7.2(d), the solid-like bubble surfaces in the presence of KCl show this.

The stability of the foams with KCl can therefore be explained by the formation of the crystals on the bubble interfaces and in the interstices between the bubbles. However the relative instability of the foam with NaCl is still not entirely clear.

7.2.2 Influence of changing SDS concentration on foam generation and stability

Photographs of foam prepared with 100 mM KCl at various SDS concentrations (35 , 69 , 139 and 277 mM) are shown in Figure 7.3. The foam immediately after preparation is shown in (a), one hour after preparation in (b) and 7 hours later in (c).

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The graph (7.3.d) shows the evolution of the foam height for these samples in time. The height of generated foam, which we will term *foamability* increased with increased SDS concentration. Not all of the gas incorporated into the foam samples except the sample with 277 mM SDS.

For the samples with 35, 69 and 139 mM SDS, the produced foams are loosely packed as one can see in (a), there are many big bubbles in the foam. However, after one hour, it seems that most of the bubbles have disappeared (7.3.d the foam height changed little after one hour) and the foams can be stable at least for several months. Furthermore, in Figure d, it looks that there is an optimum concentration of SDS to make the maximum of stable foam near 139 mM.

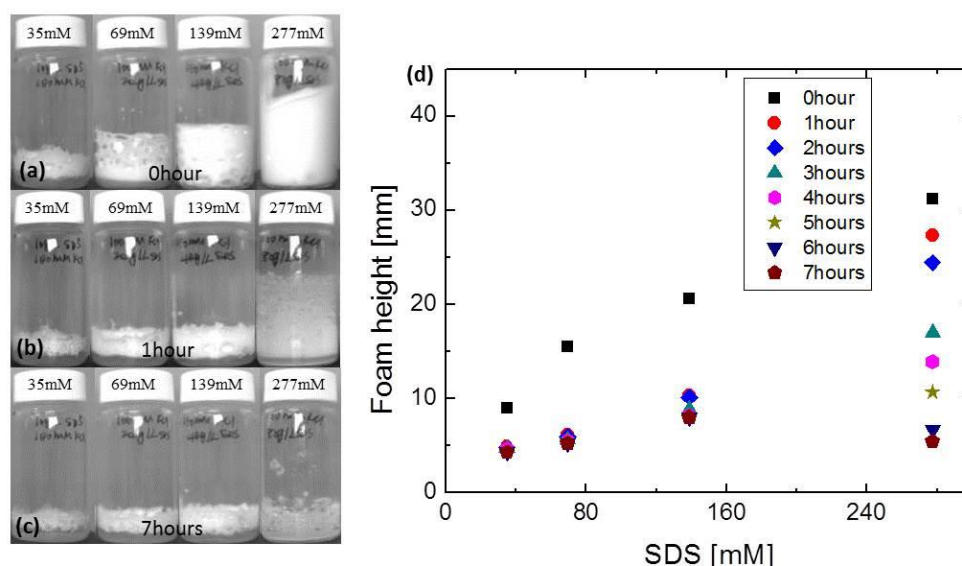


Figure 7.3 Photographs of foam samples made with 100 mM KCl and 35, 69, 139, 277 mM SDS.

(a) Foam after prepared. (b) Foam after prepared 1 hour. (c) Foam after prepared 7 hours. (d) Measurement of foam height with SDS concentrations at different hours.

Then for the sample with 277 mM SDS, the foamability is the best (the largest volume of foam is produced) and the produced foam is the most homogeneous with a small bubble size. However, the foam is unstable. As one can see, after one hour, due to the drainage and coarsening, the foam has changed a lot. In fact, it's much more like a dry network structure than a foam. There are no discernable bubbles left and the structure is connected by the white crystals and it's very brittle. The network like structure is unstable and collapses to the bottom with time as shown by the foam height change in (d).

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Photographs of foam prepared with 250 mM KCl at various SDS concentrations (35, 69, 139 and 277 mM) are shown in Figure 7.4. The foam immediately after preparation is shown in (a), 3 hours after preparation in (b) and 7 hours later in (c). The graph (7.3.d) shows the evolution of the foam height for these samples in time. One can see that the foamability increased with increased SDS concentration. For most of the samples not all of the gas could be incorporated into the foam.

For the foams produced with 35, 69, 139 and 277 mM SDS, they quickly drain after preparation, after which the drainage slows down dramatically before completely arresting. The coarsening of the foam samples arrest as well. However, for the foam with 412 mM SDS, if you observe it carefully, you can see that the foam is unlike the foams to the left of it. This foam is like the foam produced with 277 mM SDS and 100 mM KCl. Their aging process are very similar, but the difference is that the foam with 250 mM KCl needs longer time to become a dry looking network like structure with crystalline collection in the Plateau borders, which also needs longer time to collapse.

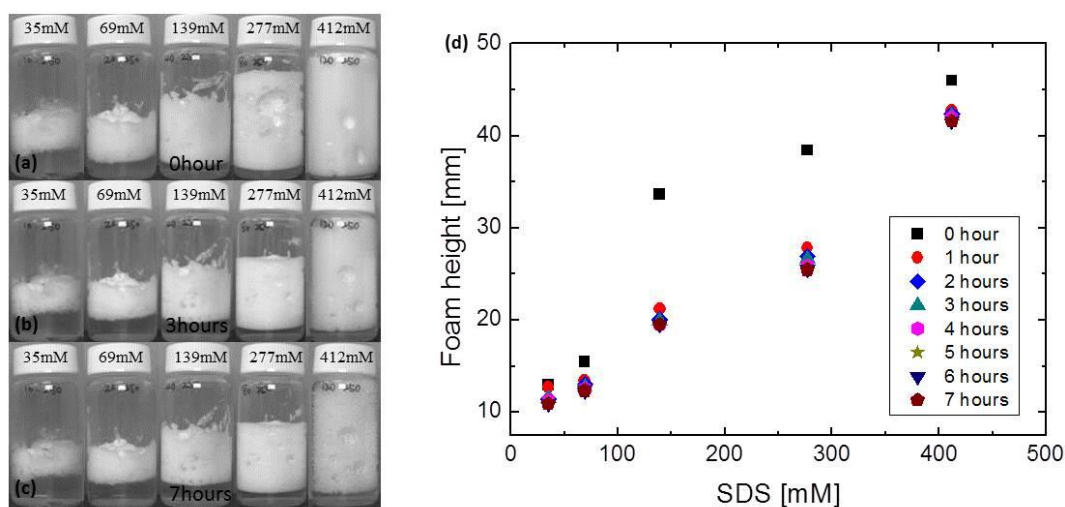


Figure 7.4 Photographs of foam samples made with 250 mM KCl and 35, 69, 139, 277, 412 mM SDS. (a) Foam after prepared. (b) Foam after prepared 3 hours. (c) Foam after prepared 7 hours.

(d) Measurement of foam height with SDS concentrations at different hours.

Indeed, at 7 hours it can be seen that the network like structure has already started to form. For the other foams, they can stable at least for several months. The foam height after arresting has linear relationship with the SDS concentration. It is increased with the increased SDS concentration as seen in (d). Moreover, from (d) one

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can note that the foam behavior changes at the concentration of 139 mM SDS. Compared with 35 and 69 mM SDS, the foamability raises suddenly and the foam height falls strongly after one hour, which means that at higher SDS concentration the foamability is increased. Although the foam will collapse to a certain point after preparation the foam is still stable.

A third concentration of KCl was explored at 500 mM. Photographs of foam prepared with 500 mM KCl at various SDS concentrations (35, 69, 139 and 277 mM) are shown in Figure 7.5. The foam immediately after preparation is shown in (a), 3 hours after preparation in (b) and 7 hours later in (c). The graph (7.3.d) shows the evolution of the foam height for these samples in time. One can see that the foamability increased with increased SDS concentration. Not all of the gas incorporated into the foam samples.

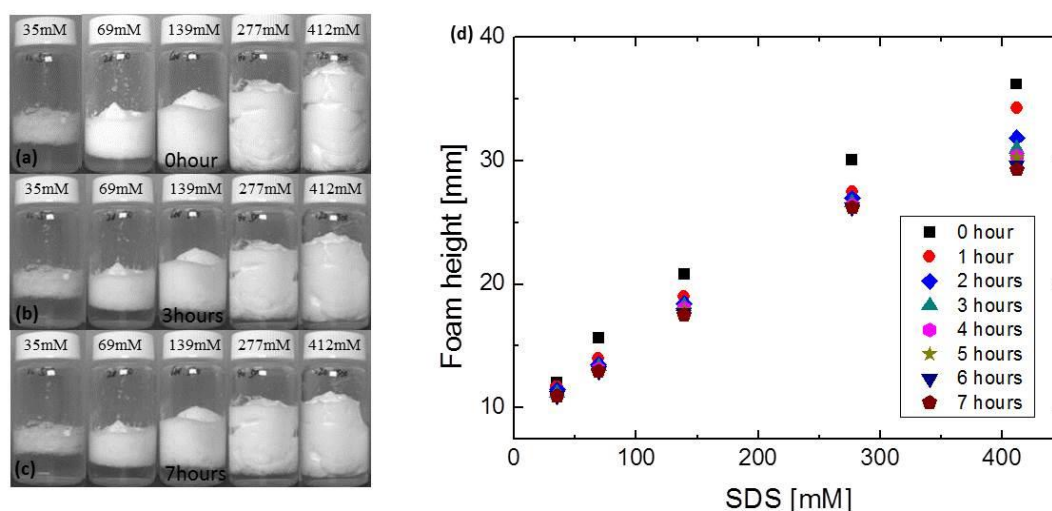


Figure 7.5 Photographs of foam samples made with 500mM KCl and 35, 69, 139, 277, 412 mM SDS. (a) Foam after prepared. (b) Foam after prepared 3 hour. (c) Foam after prepared 7 hours. (d) Measurement of foam height with SDS concentrations at different hours.

The initial liquid fractions of these foams from left to right are around 20 %, 51 %, 43 %, 39 % and 34 %. One can note that the liquid fraction is decreased with the increased SDS concentration except for the sample with 35 mM SDS. This is correct because more foam can be made at higher SDS concentration but the total liquid volume is fixed. Then in a matter a seconds the bubbles have creamed to the top of the samples, as the foam become close packed (liquid fraction from left to right around 13 %, 45 %, 40 %, 33 % and 31 %) the drainage and coarsening slow down

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dramatically, but continues over several hours before arrests. One hour later, the foams height is almost unchanged except the one with 412 mM SDS as seen in (d), which needs longer time to age. After the foams arrest, the foam height is increased with the increased SDS concentration. The relationship between them is approximate linear. When the salt concentration is higher than SDS, maybe the amount of produced crystals is proportional to the SDS concentration. That is why the foam crystals can stabilise it proportionally as well. All the foam samples obtained with 500 mM KCl and the given SDS concentrations are ultrastable, they can be stable more than 6 months at room temperature.

Figures 7.3, 7.4 and 7.5 show that for the foam samples at fixed salt concentration foamability is increased as the surfactant concentration increased and most of the foams are ultrastable. However, for the sample with 277 mM SDS in Figure 7.3 and with 412 mM SDS in Figure 7.4, the formed foams are unstable and the foam ageing is not like the normal foam. The foam ages to the network-like structure first and then collapse to unstable the foam. When compared with the ultrastable foams, one can see that for this kind of foam samples the surfactant concentration used is much higher than the salt concentration used.

The foamability is much better at fixed salt concentration with higher surfactant concentration, which means that much more foam can be produced. However, the total quantity of crystal is constant so that for each bubble there might not be enough crystals to stabilize it. We'll get back to the reasons behind what's going on after having looked at the kinetics of crystal formation.

7.2.3 Kinetics of crystals formation

In order to explain the instability of the NaCl foams, we have measured the time after which the crystals become visible to the eye when the samples are cooled down from a homogeneous state. In order to keep the same condition for the samples, each time we heated the samples 1°C higher than the dissolution temperature measured in 7.2.1 to get a homogeneous solution. Then we cooled to the target temperature and recorded the time at which crystals appeared. The times are shown in Figure 7.6 (a). The crystallization time (t_c) is increased as ΔT is decreased. ΔT is the temperature difference between the dissolution temperature and the target temperature. In all the

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ΔT range, t_c with NaCl is higher than with KCl. It takes at least twice as long for each ΔT . This means that the crystallization kinetics is considerably slower with NaCl than with KCl.

Figure 7.6 (b), (c), (d) and (e) are the foam samples prepared with 69 mM SDS and 500 mM salt at different ΔT and different times. (b) and (c) are with KCl, when $\Delta T=20\text{ }^\circ\text{C}$, t_c is smaller than 1min and the foam aging is rapidly arrested and the bubbles remain very small. Ultrastable foam can be obtained in this condition. When $\Delta T=8\text{ }^\circ\text{C}$, t_c increases to around 3 minutes, the foam ageing is eventually arrested as the crystals form, however the resulting material is more like a crystal network-like structure than an aqueous foam and it is very brittle, like the foam formed with 277 mM SDS in Figure 7.3 and 412 mM SDS in Figure 7.4, will collapse finally. (d) and (e) are with NaCl, at $\Delta T=8\text{ }^\circ\text{C}$ and $5\text{ }^\circ\text{C}$, t_c increases to around 5 min and 10 min respectively. Under this condition, the foam has enough time to evolve and it will partially collapse before the ageing can arrest, like in (d) and (e). t_c with $\Delta T=8\text{ }^\circ\text{C}$ is smaller compared with $\Delta T=5\text{ }^\circ\text{C}$, so there is more foam left with $\Delta T=8\text{ }^\circ\text{C}$.

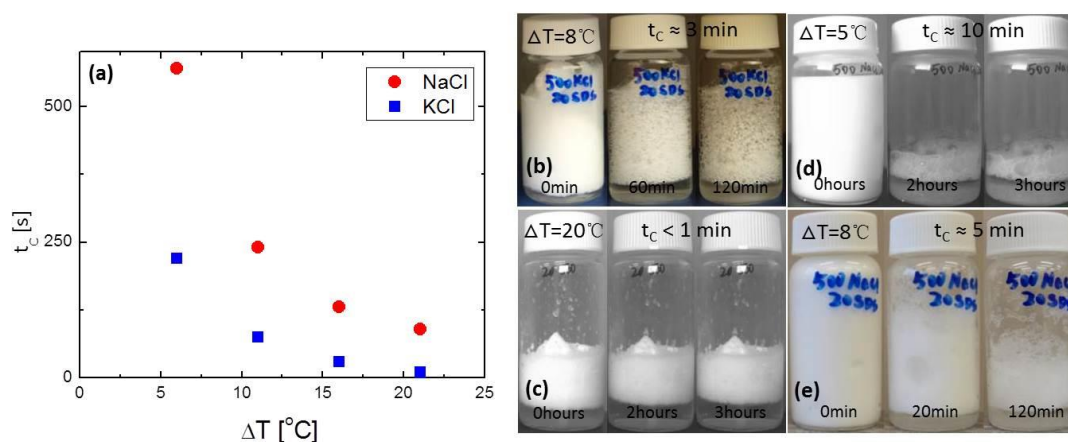


Figure 7.6(a) Time for the precipitate to become visible by the naked eye after cooling. (b) Photographs of foam at different times with $\Delta T=8\text{ }^\circ\text{C}$ and $t_c \approx 3\text{ min}$. (c) Photographs of foam at different times with $\Delta T=20\text{ }^\circ\text{C}$ and $t_c < 1\text{ min}$. (d) Photographs of foam at different times with $\Delta T=5\text{ }^\circ\text{C}$ and $t_c \approx 3\text{ min}$. (e) Photographs of foam at different times with $\Delta T=8\text{ }^\circ\text{C}$ and $t_c \approx 5\text{ min}$. Figures b and c are with 500 mM KCl and d and e with 500 mM NaCl. 69 mM SDS was used for all the samples.

The investigated kinetics of crystal formation given in Figure 7.6 can explain the instability of the NaCl foams. For the samples shown in Figure 7.1, it takes tens of

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minutes for the crystals to appear in the sample with NaCl, but with KCl they appear within seconds of mixing. Therefore in the sample with NaCl the foam has ample time to evolve (coarsen, coalesce and drain) before the crystals form and can start stabilizing the foams. Similarly making foams with low concentrations of added KCl (with SDS or KDS) leads to relatively unstable foams, as the crystallization process is slower than the destabilization process.

However, there is another situation that can exist as shown in Figure 7.6 (b), the formed foam with KCl is unstable (a crystal network-like structure and collapse) although the crystallization time is not very long. When compare the samples (b) and (c), one can note that the difference between them is foamability (b is higher than c). This indicates that unstable foam will obtain if much more foam produced but there are not enough crystals to stabilize it even the crystal formation kinetics is not so slow. From foam formed with 277 mM SDS in Figure 7.3 and 412 mM SDS in Figure 7.4, we can get the same conclusion. However, for this part, the detailed mechanisms about how the network-like structure formed need more experiments.

This means that whether the foam is stabilized depends on the link between the kinetics of crystal formation and the foam ageing times, as well as how much foam is produced at certain formed crystals. If crystallization is too slow the foam has time to evolve and it will partially collapse or totally disappear before the ageing can arrest. Or if too much foam is produced the formed crystals are not enough to stabilize it. The stability of the foams from both SDS and KDS with added KCl suggest that it is not the presence of a mixture of counter ions that is determinant in the stabilization process (Na^+ and K^+). The requirement seems to be for the presence of potassium and dodecyl sulfate in sufficient concentration and at a temperature below the Krafft boundary. Of course the Krafft boundary should depend strongly on the solution and it is sensitive to the type and concentration of ions present, i.e. DS^- and Cl^- , with Na^+ and/or K^+ .

7.2.4 Structure of crystallites inside the foam

We have carried out SANS measurements on the foams prepared with 69 mM SDS and 500 mM NaCl or KCl. The foam made with NaCl partially collapsed during the experiment. The medium and high q data from the foam with NaCl were

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multiplied by a factor 4 in the data treatment, to compensate for the disappearance of scattering material during the measurement. The scattered intensity as a function of q for the two samples is shown in Figure 7.7 (a) where we can see that at low q the intensity decreases as q^{-4} . Such decay is typical of sharp interfaces, such as the surfaces of the bubbles and the crystallites.

We can also distinguish two peaks arising from the crystal structure in Figure 7.7(b). For the sample with NaCl, the first peak is at $q^* = 0.16 \text{ \AA}^{-1}$ and the second one at 0.32 \AA^{-1} , so twice the first one. The sample with KCl has peaks at 0.19 \AA^{-1} and 0.38 \AA^{-1} . The structure of SDS crystals has been previously measured, they have been shown to have a lamellar structure where the inter-planar distance, d , depends on the degree of chain tilt and hydration [176]. We measure $d = 39 \text{ \AA}$ ($2\pi/q^*$) for the SDS crystals (precipitated with NaCl). This is exactly what has been measured when SDS is crystallized from water, it forms monoclinic weakly hydrated ($\text{SDS} \cdot 1/8 \text{ H}_2\text{O}$) crystals with $d = 38.9 \text{ \AA}$ [176]. The crystals formed with KCl also have a lamellar structure, however the spacing is smaller than with SDS at $d = 33 \text{ \AA}$. Due to the large difference in the crystallization temperatures, the crystals should be almost exclusively of KDS. This means that the KDS crystals are more tightly spaced than SDS, suggesting that the KDS crystalline unit cell is more strongly tilted.

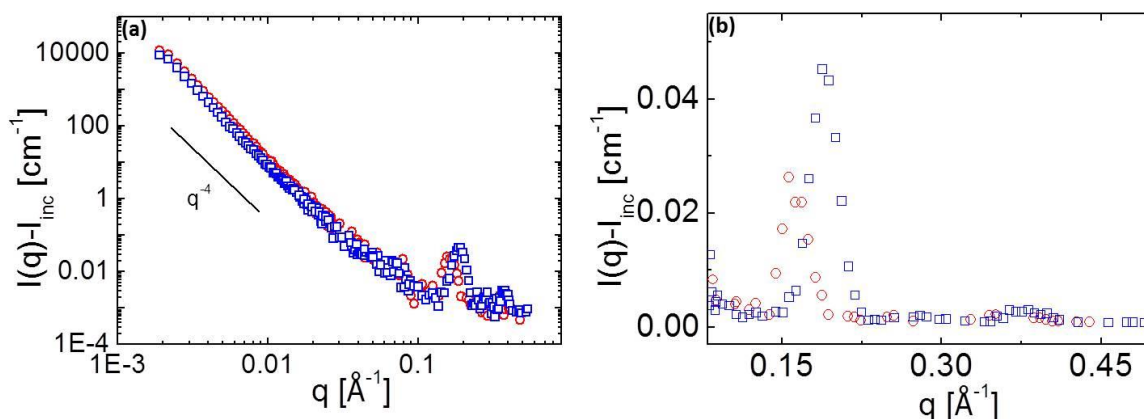


Figure 7.7 (a) The scattered intensity as a function of the wave vector for a foam prepared with 69 mM SDS and 500 mM NaCl (red circles) and 500 mM KCl (blue squares). In (b) the high q data is shown in a linear scale.

7.2.5 Stimulating the foam by temperature

The photograph of Figure 7.1(e) shows that foam prepared with 69 mM SDS and 50 mM KCl can be stable for at least 6 months at room temperature. We have shown that the incredible stability of the foam arises from the presence of crystallized KDS both at the surfaces of the bubbles and in the interstices between the bubbles. In order to break it we heat it to 51 °C to melt the crystals. The images are shown in Figure 7.8. The bubbles shown in Figure 7.8(a) have rugged surfaces and some precipitates are also found in the surrounding fluid. Very quickly the surface of the bubbles starts to melt, as seen in the photograph taken after 13 s. The bubbles start coarsening and coalescing, before disappearing in a few minutes.

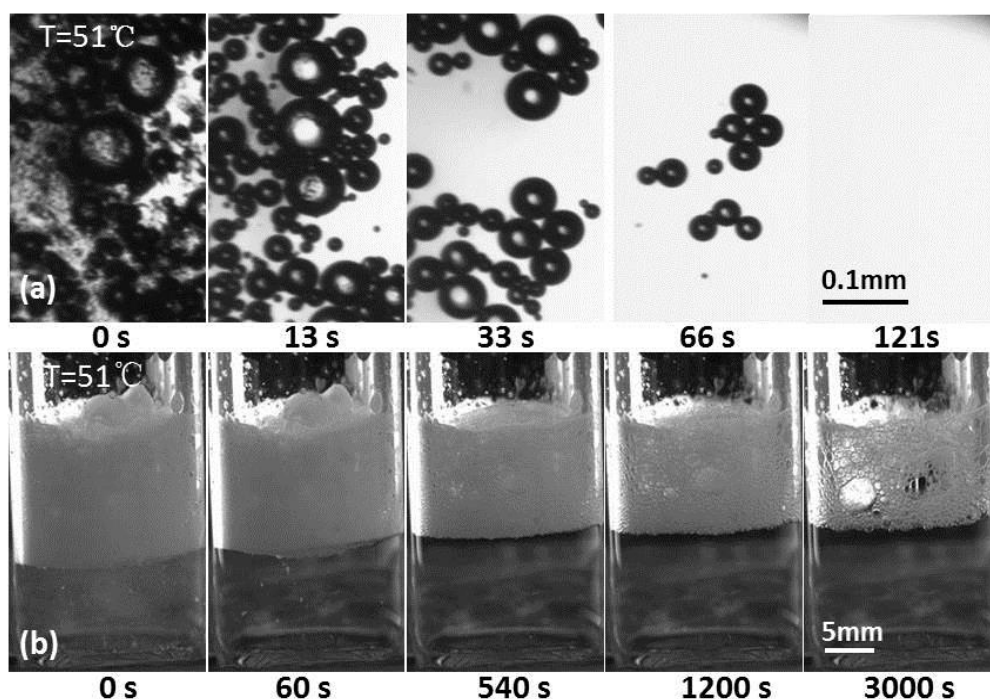


Figure 7.8 Bubbles (a) and foams (b) prepared with 69 mM SDS and 500 mM KCl heated suddenly to 51 °C.

We can see the same effect on bulk foam in Figure 7.8(b). Within one minute the drained solution has become transparent. The foam starts to age as the crystals disappear from the foam, although this probably takes some time as foam is a very poor heat conductor. After 1 minute some liquid has drained, and after around 10 minutes the bubble size starts to change considerably. The melting of the crystals (bulk and interfacial) transforms the foam into common wet foam, which disappears

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within a few hours.

The produced foams are temperature stimuable. It is also possible to stop the foam ageing before all the foam has disappeared to reform a stable foam again. We have prepared a sample of foam with 69 mM SDS and 500 mM KCl as shown in Figure 7.9, which is ultrastable at room temperature as already known in the previous part. The foam has been left to age for an hour at room temperature after preparation, then suddenly put in the water bath with the temperature of 51 °C, which is higher than the dissolution temperature of crystals formed at the surfaces of the bubbles and in the interstices between the bubbles.

The drained solution in 51 s in the photograph has become transparent. The foam starts to age as the crystals melt from the foam as shown in the photograph at 88 s, some of the foam has disappeared. The foam is left to destabilise for 2 minutes after which it is plunged into a water bath at room temperature. The crystals start to reform and the ageing of the foam is slowed down (at 143 s). As the crystals reform we find many of them in the drained solution at the bottom of the foam sample (the solution is turbid). These crystals will eventually reform and sediment to the bottom of the sample (at 70 min). The ageing of the reformed foam sample will arrest after several hours, and it is still very stable at room temperature (we have given 4 days, but it can remain stable longer than 4 days).

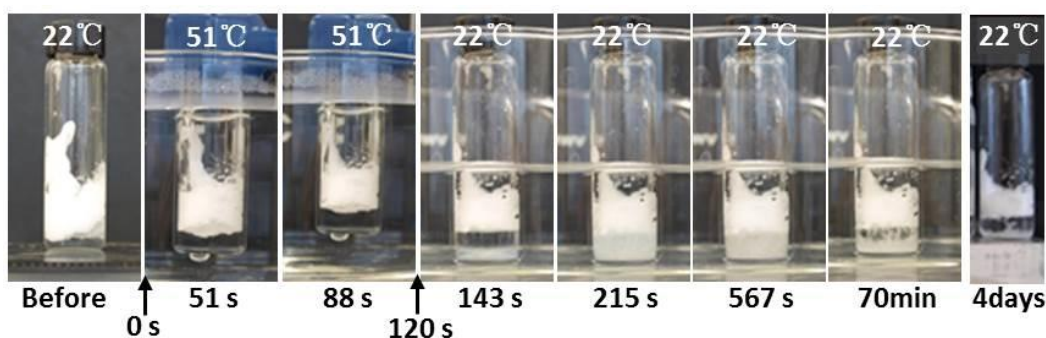


Figure 7.9 Foam prepared with 69 mM SDS and 500 mM KCl at room temperature and waited for 1 hour. Then the foam was placed in a water bath at 51 °C and taken out after 120 s and placed in another water bath at room temperature ($T = 22$ °C). The foam sample also was given after 4 days at room temperature.

We show that the process can be stopped and started, however the resulting foam is different as the concentration of crystals changes due to the drainage of the

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surfactant solution.

7.3 Conclusions

The addition of salt at a high concentration can be used to make ultrastable foams from SDS. Stable foams are made below the Krafft temperature. However whether the foams are stable or not also depends on the kinetics of crystal formation. This can be tuned via the preparation temperature by changing the type and concentration of added salt. If crystallization is too slow, the foam has time to disappear. If the crystals have time to form on the surfaces of the bubbles the foams are stable over months or until they are heated to melt the crystals at which point they start to age and disappear quickly. Nevertheless, there is one exception, unstable foam still can be obtained if too much foam produced at certain formed crystals even the crystal formation kinetics is not so slow, like the concentration of surfactant is much higher than salt in our case. This can be controlled by selecting appropriate sample's concentration.

We have shown how the crystallization of surfactant can be used to our advantage in creating ultrastable or/and stimuable foams. We have also seen that the addition of KCl is much more efficient than NaCl. However the detailed mechanisms including the importance of the presence of two types of counter ions in the foams with KCl, or the role of the crystal structure on foam stability still require further experiments and/or simulations.

These results are important as they provide a simple way of making very stable foams. They could be used in applications where the self-life of a product should be measured in months or years without degradation of the quality of the foam. Thanks to their sensitivity to temperature they could even be used as simple temperature sensors to indicate prolonged heating during a transport phase. However their main quality is their simplicity, superstability and stimulability become affordable for more applications.

Chapter 8 Foam aging modified by the gel phase

8.1 Introduction

Solid foams are found in a wide variety of materials, and this makes understanding the process of making solid foam so important. It is one of the simple methods to prepare very light porous ceramic materials, which have various applications in areas such as tissue engineering, thermal or acoustic insulation, heterogeneous catalysis, and chromatography due to their low mass density and high surface area [177-181]. So it's important to know how to control their properties such as mechanical, thermal or acoustic and so on. To do this we need to understand the evolution of the microstructure of the foam.

Solid foam is made from the precursor of wet foam, in which the continuous phase needs to be either solidified or gellified. Solid silica foams are produced by drying the silica-loaded wet foams for production of porous materials [182, 183]. If the continuous phase becomes a gel, as the gelation process proceeds, the viscosity of the gel phase will first increase and it will acquire a certain elasticity. From Chapter 5 and 6, we know that a gel can be formed by adding salt to the suspension of silica

particles. Therefore, in this Chapter, salt was added to the suspension of silica particles to produce the gel phase, which was used as the continuous phase of the foam to slow down and even arrest the foam ageing. We use a mixture of N_2 with traces of C_6F_{14} (perfluorohexane) to slow down the coarsening and SDS is used as surfactant to generate the foam.

8.2 Results and discussion

8.2.1 The evolution of bubbles in the gel foam

A range of samples was investigated with different TMA and salt concentrations: 9 vol% TMA and 500 mM NaCl; 12 vol% TMA and 300 mM NaCl; 12 vol% TMA and 500 mM NaCl; 16 vol% TMA and 300 mM NaCl; 16 vol% TMA and 200 mM NaCl. All the samples also had 10 g/L SDS, which means that when considering the ionic strength of the solutions we should also take into account the 69 mM of Na^+ . The reason to select these concentrations is because the macroscopic gelation times measured range in a few hours, which is a typical aging time of foams (they will coarsen and drain, but will not disappear within this time, hence giving us the possibility to arrest the foam ageing before they are gone). In addition, the sample 300 mM NaCl 10 g/L SDS without particles used as reference. The photographs of foam at 1 and 3 hours are given in Figure 8.1 for each concentration with the bulk liquid volume fraction ϕ_l and the averaged bubble radius R .

All the foams are prepared with the same initial liquid fraction Φ_l of 14.3 %. After generation the foam ages. Looking at the liquid fractions we can see that they drain to around 7 % within one hour after which the drainage slows down and the liquid fraction changes little in the next 2 hours. The bubbles also coarsen, and the average bubble size increases for all the samples. In all the samples the Φ_l and the average radius are different. If you look at the photographs carefully, you can find that the shapes of the bubbles have differences as well. Some of them are not spherical anymore, and not because of the foam becoming very dry. For example, the bubbles for sample in (c) and (e) at 3 hours.

Before running this experiment, we measured the macroscopic gelation times for the samples without SDS (this was done exactly like in Chapter 5 to get the τ_M). From

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(a) to (e) the gelation times are 65 min, 131 min, 30 min, 271 min and 55 min. The gelation time of the samples in (c) and (e) are faster than other samples. Therefore, we could expect that the ageing of the foam in these two samples is the most influenced by the bulk gel phase.

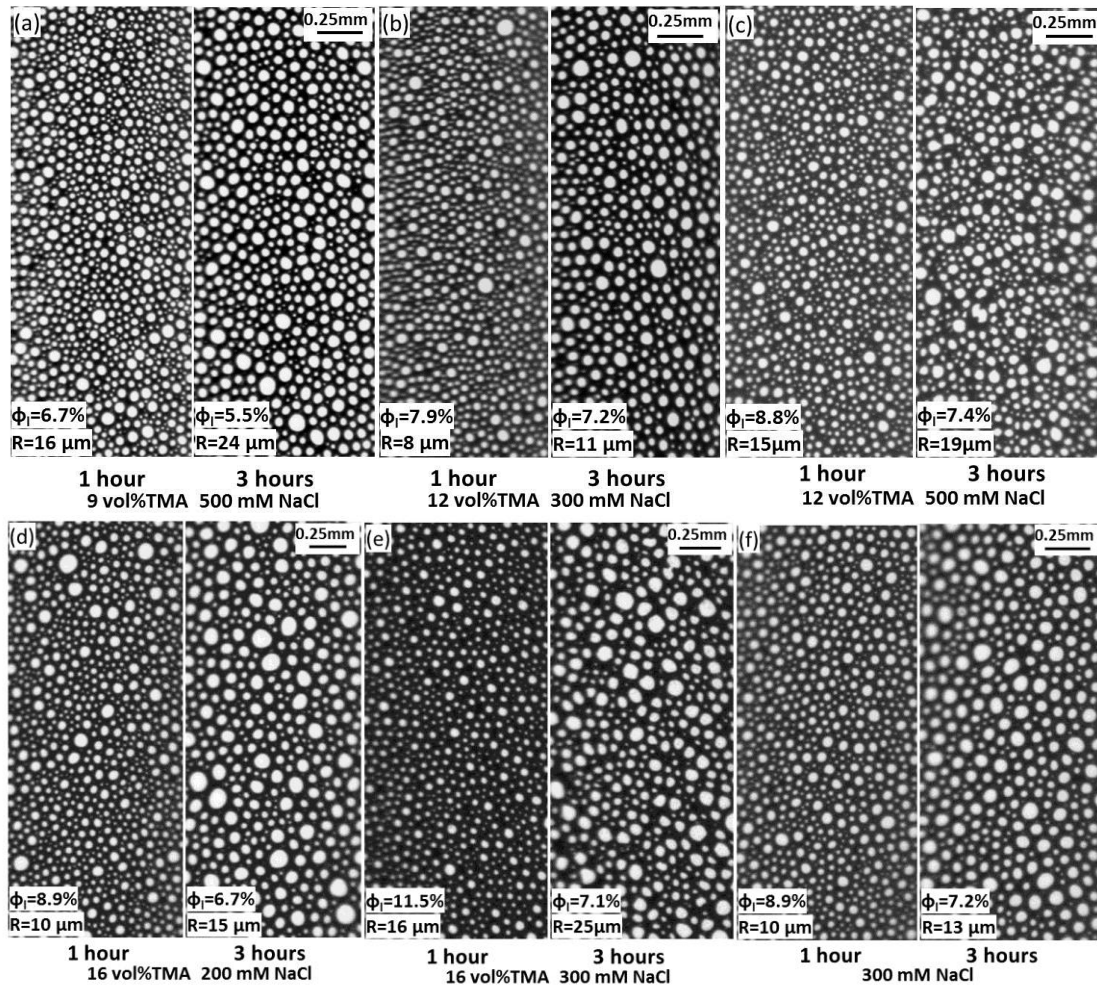


Figure 8.1 Photographs of bubbles at 1 hour and 3.0 hours in the presence of 9 vol% TMA 500 mM NaCl (a), 12 vol% TMA 300 mM NaCl (b), 12 vol% TMA 500 mM NaCl (c), 16 vol% TMA 200 mM NaCl (d), 16 vol% TMA 300 mM NaCl (e), and 300 mM NaCl (f). For all the concentrations, SDS was used at 10 g/L.

We will now look at the distribution of bubble radii in the first 6 hours, and these are shown in Figure 8.2. The samples are the same as those in Figure 8.1. In the first 2 hours, one can see that the peaks of the curves decrease and shift to a higher radius as the foam ages for all the samples. Then for the next several hours, in (a), (b), (d) and (f), the peaks of the curves continue to decrease but very slowly as they shift to the higher radii as well. For these samples the foam aging is slowed down. However, for

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comparison in (c) and (e), the peaks of the curves are unchanged after 3 hours, which indicates that the foam aging of these two samples is arrested.

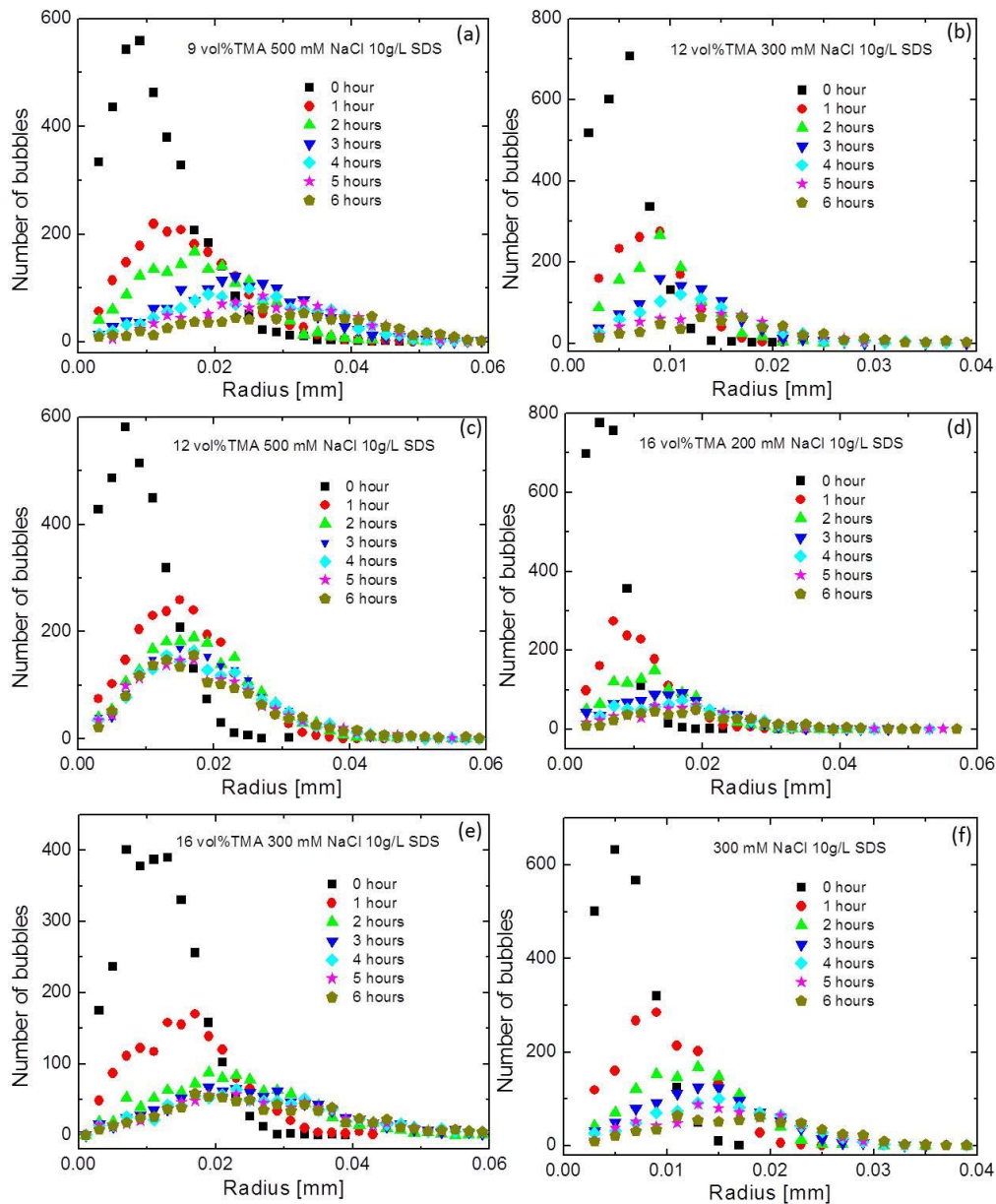


Figure 8.2 The distribution of numbers of bubbles as a function of radius in the first 6 hours. (a) with 9 vol%TMA 500 mM NaCl, (b) with 12 vol%TMA 300 mM NaCl, (c) with 12 vol%TMA 500 mM NaCl, (d) with 16 vol%TMA 300 mM NaCl, (e) with 16 vol%TMA 200 mM NaCl, and (f) with 300 mM NaCl. For all the concentrations, SDS used was 10 g/L. 0 hour (square), 1 hour (circle), 2 hours (UpTriangular), 3 hours (down triangular), 4 hours (diamond), 5 hours (star), and 6 hours (pentagon).

In fact, from Figure 8.2, it can be seen that the change of bubble distribution is

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only fast in the first 1 hour, this is consistent with the result of liquid fraction obtained in Figure 8.1. After that the foam aging is slowed down or arrested depending on the the different salt and TMA concentrations used.

As foam ages, the shapes of the bubbles are not spherical anymore. So in our case, we only calculate the radius of the bubbles in the first 7 hours by using the equation $S=\pi r^2$ and consider that they are still spherical. The normalized radii as a function of time are given in Figure 8.3(a). Here the radius taken is as the average radius. Because the graph is in log-log scale, the data at $t=0$ is not shown. One can note that in the first 7 hours, the radii of the bubbles evolves as a power law for the samples with 9 vol% TMA 500 mM NaCl, 12 vol% TMA 300 mM NaCl, 16 vol% TMA 200 mM NaCl and the reference sample 300 mM NaCl and they have the similar slopes, which are slightly smaller than 0.5. However, the samples with concentration of 12 vol% TMA 500 mM NaCl and 16 vol% TMA 300 mM NaCl stopped to increase at $t=4$ hours. In the linear part, the slope of former is lower than 0.3 and the latter is higher than 0.3.

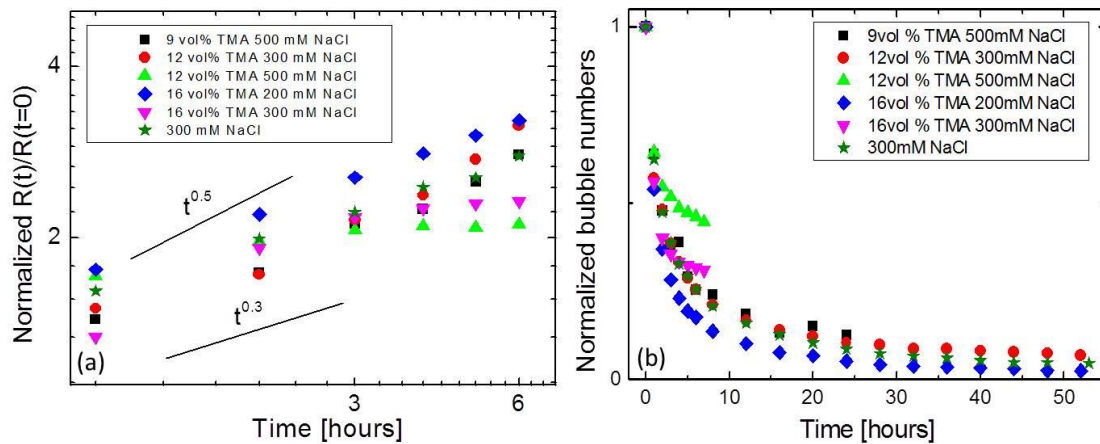


Figure 8.3 Normalized bubble radius (a) and normalized bubble numbers (b) with time for the concentration 9 vol%TMA 500 mM NaCl (square), 12 vol%TMA 300 mM NaCl (circle), 12 vol%TMA 500 mM NaCl (up triangular), 16 vol%TMA 200 mM NaCl (diamond), 16 vol%TMA 300 mM NaCl (down triangular), and 300 mM NaCl (star). The linear lines $t^{0.3}$ and $t^{0.5}$ are shown in (a).

When you look at the power law showing the relationship between the average bubble radius and time, it is funny that the power law is not going as 0.5 as the standard surfactant foams that coarsen and age normally. However, for our samples the continuous phases of foams are gel phases, it is interesting to see that the power

laws of them are close to 0.5 or 0.3. Moreover, it can be seen from the data that the growth of the bubbles can be stopped for the samples same as in Figure 8.1 (c) and (e), then for the rest of them their growth rate of the bubbles are similar like the reference sample without gel phase. This is a proof to show that the ageing of the foam can be influenced by the bulk gel phase.

The normalized number of bubbles as a function of time are given in Figure 8.3 (b). One can see that all the data decrease with time. The data dropped slowest for the sample with concentration 12 vol% TMA 500 mM NaCl and fastest one is 16 vol% TMA 200 mM NaCl, other samples are between them. Moreover, it can be seen from Figure 8.3 (b) that the time taken for the number of bubbles to reduce to half of its original value is much slower for sample 12 vol% TMA 500 mM NaCl (about 4 hours) than sample 16 vol% TMA 200 mM NaCl (about 1 hour).

8.2.2 The mechanical properties of the bulk gel phase

In order to understand why the ageing of the foam is influenced as it is, we did measurements of the bulk rheological properties. The measurement process was as follows: the samples are transferred into the Double Gap immediately after preparation and we wait for 1 hour for the gel to form, and then start the measurement

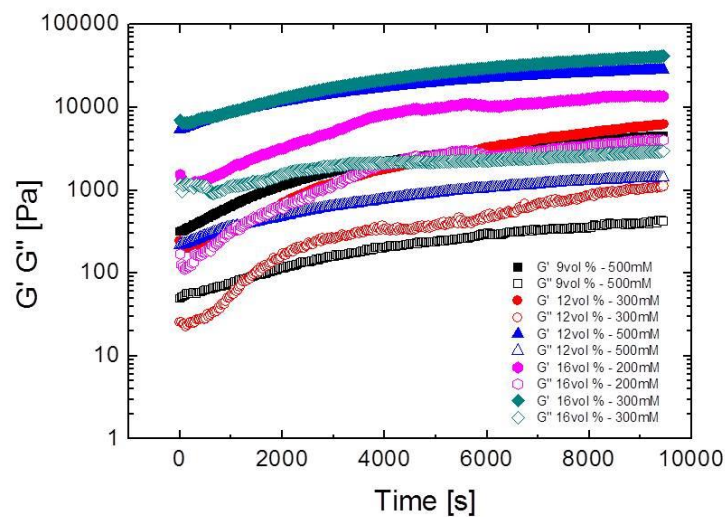


Figure 8.4 Storage modulus (G') and Loss modulus (G'') as a function of time with 9 vol% TMA 500 mM NaCl (square), 12 vol% TMA 300 mM NaCl (circle), 12 vol% TMA 500 mM NaCl (up triangular), 16 vol% TMA 200 mM NaCl (pentagon), and 16 vol% TMA 300 mM NaCl (diamond). The solid symbols corresponding to G' and open symbols G'' .

with 1 % strain and 1 Hz frequency for 2.5 hours, so at the end of the measurement the sample age is 3.5 hours. Storage modulus (G') and loss modulus (G'') evolution with time are shown in Figure 8.4. For all the concentrations, like the mechanical properties measured in Chapter 5, G' are higher than G'' and both moduli increase with time. G' and G'' also varied with the concentration used.

8.2.3 The effect of gel strength on foam aging

It is known that an elastic modulus of the fluid forming the foam can strongly change the ageing process of the foam. The drainage and coarsening can be slowed down and even arrested. We could imagine that if the coarsening process is slowed down a lot by the elastic modulus of the gel, the radius of the bubbles should depend on the G' of the gel at a given time. Therefore, we have plotted R as a function of G' . The relationship of R and G' for all the concentrations in the first 3 hours is obtained from the previous part as shown in Figure 8.5, (a) is the normalized radius and (b) is the average bubble radius. There are many factors that influence the growth of the bubble size, for example the silica and the salt concentrations. As seen in Figure 8.5(b), it is complicated to say something about the relationship between R and G' . Therefore, in the following we discuss the relationship between the normalized R and G' in Figure 8.5(a), as this seems more reasonable.

The three points for each symbol from left to right show the values of R and G' (of the bulk phase not the foam) at 1 hour, 2 hours and 3 hours respectively. Keeping in mind the data in Figure 8.3(a), we know that the growth of the bubbles continued in the first 7 hours for the samples with lower concentrations of TMA and NaCl and stopped after 4 hours for the two concentrations with high TMA and/or NaCl (12:500 and 16:300). Therefore, we can see that the silica gels can be sufficiently strong to arrest the growth of the bubbles leading to stable foam. Simulations of the conditions of arrest have been carried out by Fyrillas [184] *et al.* However, their results are difficult to compare with our experimental values.

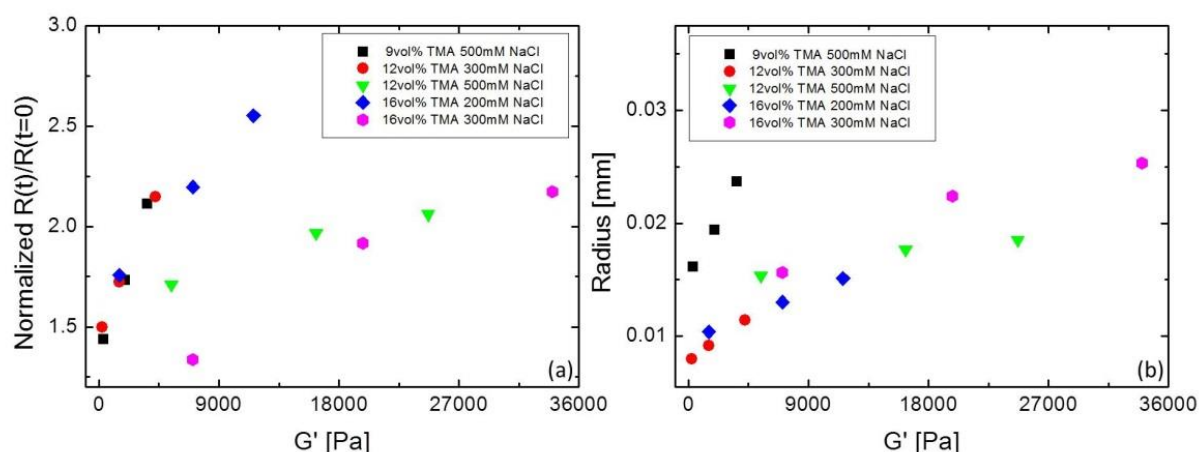


Figure 8.5(a) Normalized radius with storage modulus G' for the concentration 9 vol%TMA 500 mM NaCl (square), 12 vol%TMA 300 mM NaCl (circle), 16 vol%TMA 200 mM NaCl (diamond), 12 vol%TMA 500 mM NaCl (down triangular), and 16 vol%TMA 300 mM NaCl (hexagon). (b) is the average radius corresponding to the normalized one. The three points from left to right for each symbol represent 1 hour, 2 hours and 3 hours. The growth of the bubbles will arrest after 4 hours for the samples with green triangles and purple hexagons.

From Figure 8.3 (a), we know that the bubble's radius does not always continue to grow. The samples with purple and green symbols will stop their growth at 4 hours. Nevertheless, as shown in Figure 8.5(a), the slopes between R and G' are not the same for these two samples. In other words, the values of G' are different for them to arrest the foam aging. Therefore, we can conclude that there should be a critical point of the gel strength to stable the foam. That is to say, if G' is less than the critical point, the radius of the bubbles continues to grow and the foam is unstable; if it is above the critical value, they arrest. Because of the evaporation of the samples in the rheometer, we only obtained the gel strength in the first 3 hours. In order to ascertain whether the reasoning is correct we should do more detailed measurements of foam rheology.

As discussed above, it is known that the gel strength is an important factor to influence the foam stability, with higher gel strength comes higher stability of the foam. However, if we compare the data with purple and green symbols, blue and black or red symbols in Figure 8.5(a), you can find that the former have larger G' and bubble size. It seemed that this is contradictory to the gel strength analysis above. Nevertheless, if you see the two sets of data listed carefully, you can see the salt concentrations are different. The former has lower salt concentration than the latter.

We can say that the foam aging is influenced much more strongly by the salt concentration than the particle volume fraction. This can be shown in Figure 8.3, although the gel phase exists in the sample 16 vol% TMA 200 mM NaCl, the evolution of its bubble size and numbers are still faster than the reference sample, which has the salt concentration of 300 mM. Moreover, we already know from Chapter 5 that with higher salt the gelation process is faster.

Therefore, we can conclude that the gel strength and gelation kinetics are two important factors to modify the foam aging.

8.2.4 Correlation behavior

In the previous section, we know that the gel strength and gelation kinetics are important factors to slow down or arrest the foam aging. In this case, the movement of the bubbles for the samples with higher gel strength and salt concentration should be slower than others. The correlation behavior can compare the movement at certain time to the previous time. Therefore we use the software Image J to obtain the correlation map and the correlation coefficient R between two images. Correlation map is a map showing the difference between the local areas. Correlation coefficient reflects how much the two images related. Higher R means more closely related. The time interval between two images is 5 minutes. First 20 images of the samples with the concentration 16 vol% TMA 200 mM NaCl and 16 vol% TMA 300 mM NaCl are selected to do the measurement (in 95 min). By doing this, the next image is considered as the target and the previous one considered as the source. The correlation sequence is from target to the source.

As an example, Figure 8.6 shows the correlation map with correlation coefficient R (a) is 0.215 and (b) is 0.937. The color of the correlation map is darker with small R and lighter with large R . R is small means the bubbles in the next image have strong movement based on the previous image; otherwise, the movement of the bubbles is not so obvious in the next image.

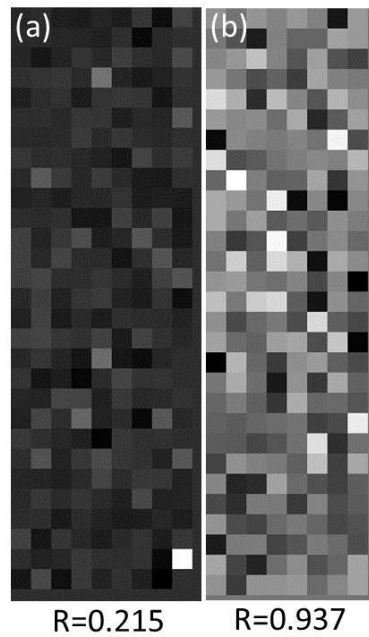


Figure 8.6 Correlation map with the correlation coefficient (a) $R=0.215$ and (b) $R=0.937$.

The correlation coefficient R for the 20 images is given in Figure 8.7. In the x axis, 1 represents the correlation coefficient between image 2 and image 1, 2 represents the correlation coefficient between image 3 and image 2 and so on until 19 represents the correlation coefficient between image 20 and image 19.

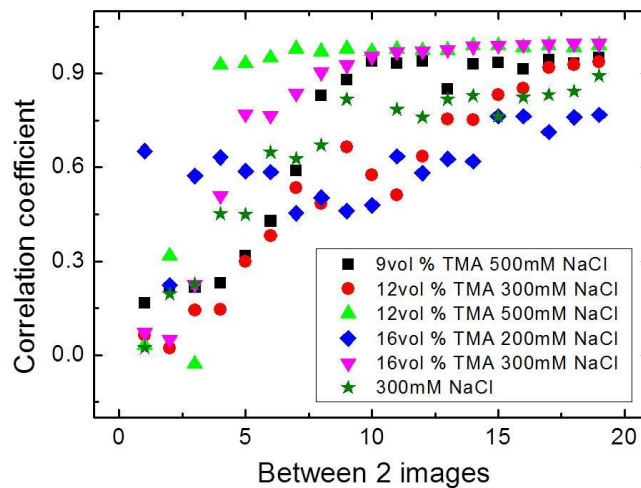


Figure 8.7 Correlation coefficient between 2 images with the concentration 9 vol% TMA 500 mM NaCl (square), 12 vol% TMA 300 mM NaCl (circle), 12 vol% TMA 500 mM NaCl (uptriangle), 16 vol% TMA 200 mM NaCl (diamond), 16 vol% TMA 300 mM NaCl (downtriangle) and 300 mM NaCl (star).

From Figure 8.7, it can be seen that as foam ages, all the correlation coefficients increase except in the sample of 16 vol% TMA 200 mM NaCl in the first several hours. From all of concentrations selected, 12 vol% TMA 500 mM NaCl is the one where R increased almost 1 ($R=1$ represents the 2 images are same, higher R corresponds to smaller movement of the bubbles) most quickly and the next one is 16 vol% TMA 300 mM NaCl. This indicates that the foam aging in these two samples can be arrested. Then for the rest of the samples, the foam aging is slowed down but not arrested during the measurement time. This is again to manifest that the samples with higher gel strength and salt concentration have stronger ability to arrest the foam aging.

8.2.5 Small angle Neutron Scattering measurements

In Chapter 5 we have studied the aggregation behavior of particles in the bulk gel phase, it will be interesting to see how the particles evolve in the continuous phase of foam. From the foam stability studies in Chapter 7, we know that the foams made with NaCl are unstable in the room temperature. Therefore, in order to prolong the foam aging we only select KCl as salt and C_6F_{14} as gas. The TMA concentrations used are 3.4 and 13 wt%, the salt are 100, 250 and 500 mM KCl, as well as 5 g/L SDS. For each concentration, two samples are prepared: one to make foam and another one without making foam (just mixed together). We note that the TMA used here was bought from the same company as in Chapter 5, but the pH is around 4 and the samples did not gel. We did not know this until we had finished the experiments. However, it is still worth to have a look at the results.

Figures 8.8 and 8.9 show the scattering intensity after subtraction of the incoherent background with q for the samples of 3.4 or 13 wt% TMA with 100/250/500 mM KCl in the presence of 5 g/L SDS. The solvent used is a mixture of 44 H_2O and 56 D_2O . In this case, the scattering from the silica particles is matched (although only almost as we will see later). On the left are the samples with foam and on the right with liquid (we expected them to gel, but in fact they did not). In the foam samples of (a), (c) and (e), the crystal peaks can be observed. This is because the mixture of KCl and SDS can produce KDS crystals as studied in Chapter 7 at room temperature. However, in the liquid samples of (b), (d) and (f), there are no crystal peaks. This is due to the way to take the liquid samples. We took them from the

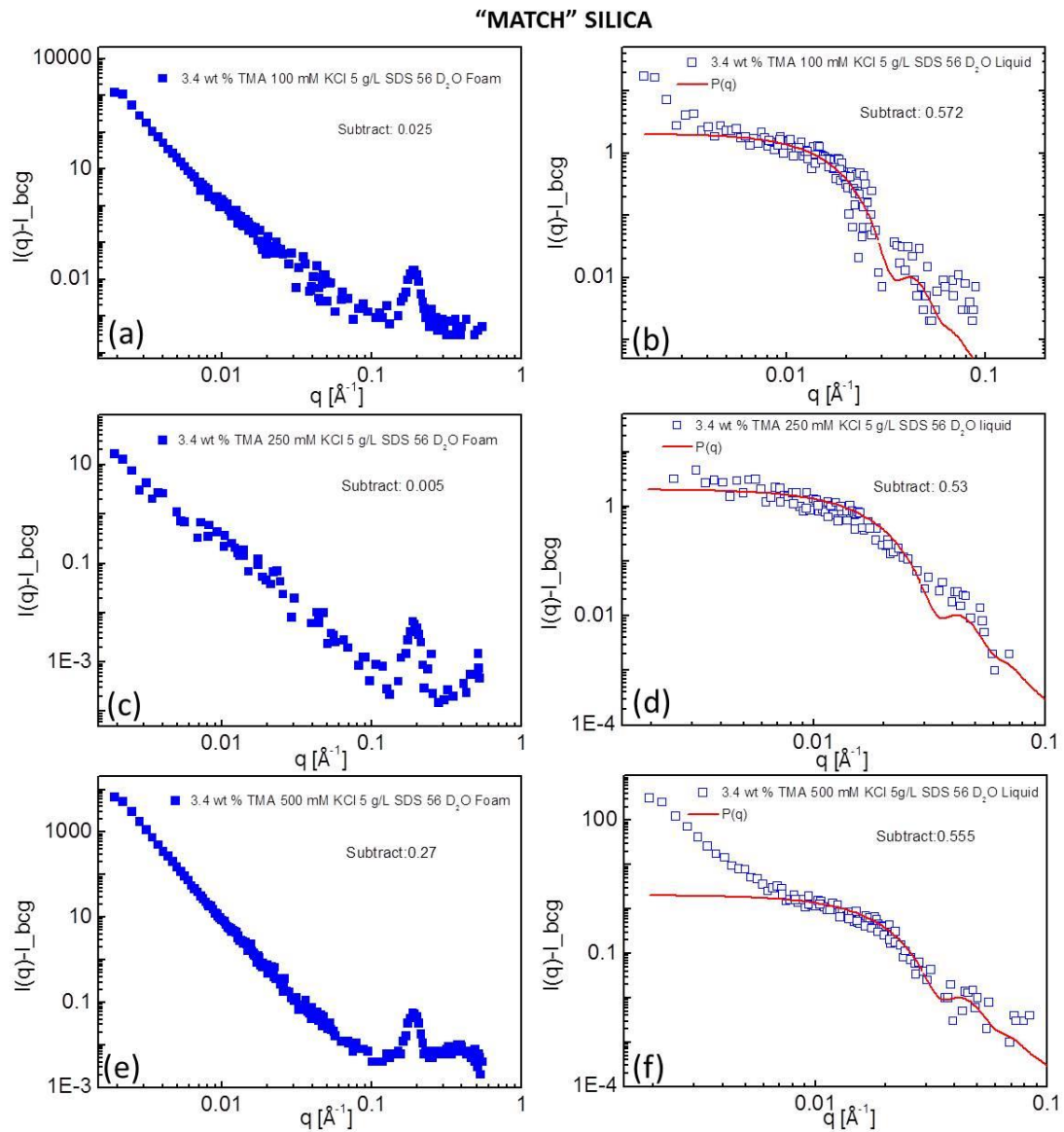


Figure 8.8 Scattering intensity $I(q)$ after subtraction the incoherent background I_{bcg} as a function of q for the samples with 3.4 wt% TMA at various salt concentrations in the presence of 5 g/L SDS. The samples on the left side are foam and right side are liquid. (a) and (b) with 100 mM KCl, (c) and (d) with 250 mM KCl, and (e) and (f) with 500 mM KCl. The solvent is the mixture of H_2O and D_2O (44:56). The red line is the form factor of silica particles. Solid square symbol represents the foam sample and open square one represents the liquid sample.

bottom and the crystals are on the top. It is difficult to say something from the figures, but we can estimate the liquid fraction in the foam from the incoherent scattering. This is linked to the flat background measured at high q . We take the intensity of foam and divide it by the liquid one. In the figures the red line is a calculated form factor of

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silica particles. When we match silica, in the liquid samples with 13 wt% TMA, from the shape of the curves it seems that we still can see the silica particles slightly. In these samples the measured intensity is very low, we did not have enough statistics.

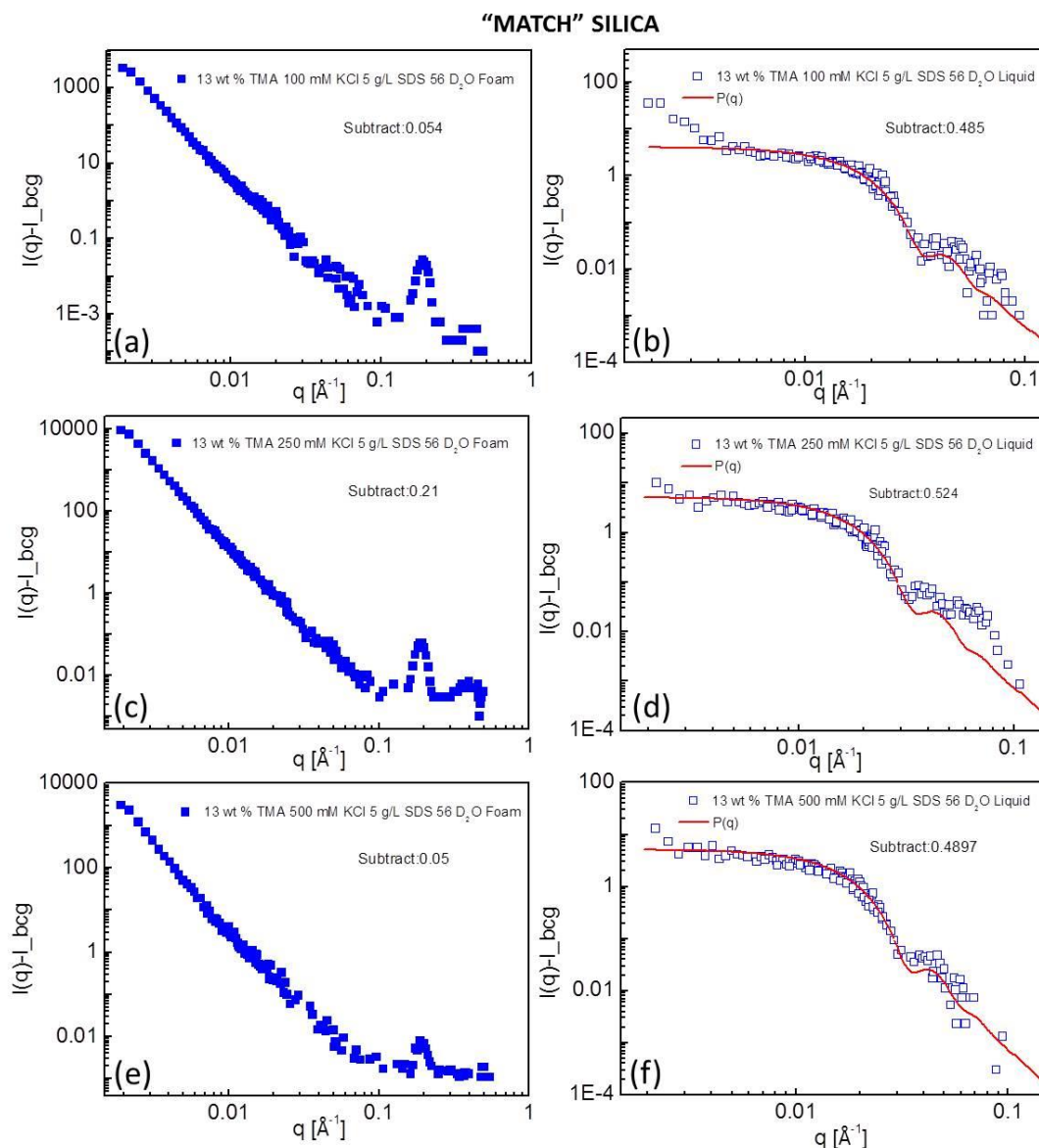


Figure 8.9 Scattering intensity $I(q)$ after subtraction the incoherent background I_{bcg} as a function of q for the samples with 13 wt% TMA at various salt concentrations in the presence of 5 g/L SDS. The samples on the left side are foams and right side are liquids. (a) and (b) with 100 mM KCl, (c) and (d) with 250 mM KCl, and (e) and (f) with 500 mM KCl. The solvent is the mixture of H₂O and D₂O (44:56). The red line is the form factor of silica particles. Solid square symbol represents the foam sample and open square one represents the liquid sample.

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The measured values of foam liquid fraction from the data in Figures 8.8 and 8.9 are shown in Table 1. One can see that with 3.4 wt% TMA Φ_l is increased with salt concentration except for 250 mM KCl when the scattering form silica particles is matched. Although the errors in these measurements are rather important due to the insufficient measurement times for some of the samples, the tendency seems logical. We know that the foams are more stable with the higher concentrations of salts. However, with 13 wt% TMA the maximum Φ_l is with 250 mM KCl, which is a little strange. But it is not easy to explain why it is like this.

	Silica/wt%	KCl/mM	100	250	500
Match "Silica"	3.4		4.3%	0.9%	48.6%
Match "air"	3.4		0.2%	2.1%	12.6%
Match "Silica"	13		11.1%	40.1%	10.2%
Match "air"	13		4.4%	23.8%	8.7%

Table 1 Volume fraction of the samples calculated from Figure 8 to 11.

Figures 8.10 and 8.11 are the same concentration as in Figures 8.8 and 8.9. The difference is that the solvents used are a mixture of 92 H₂O and 8 D₂O. In this condition, air is matched. In (a), (c) and (e) for all the foam samples, we can see the crystal peaks as when we match the silica particles, but not in the liquid samples in (b), (d) and (f). Moreover, we can see the nice shape of the scattering curves coincides exactly with the form factor $P(q)$ of silica particles. This means that the silica particles can be seen inside the foams as well as the gels. However, it seems that the silica particles have not started aggregating and the increase in the scattered intensity at low q is mainly because of the gas/liquid interfaces.

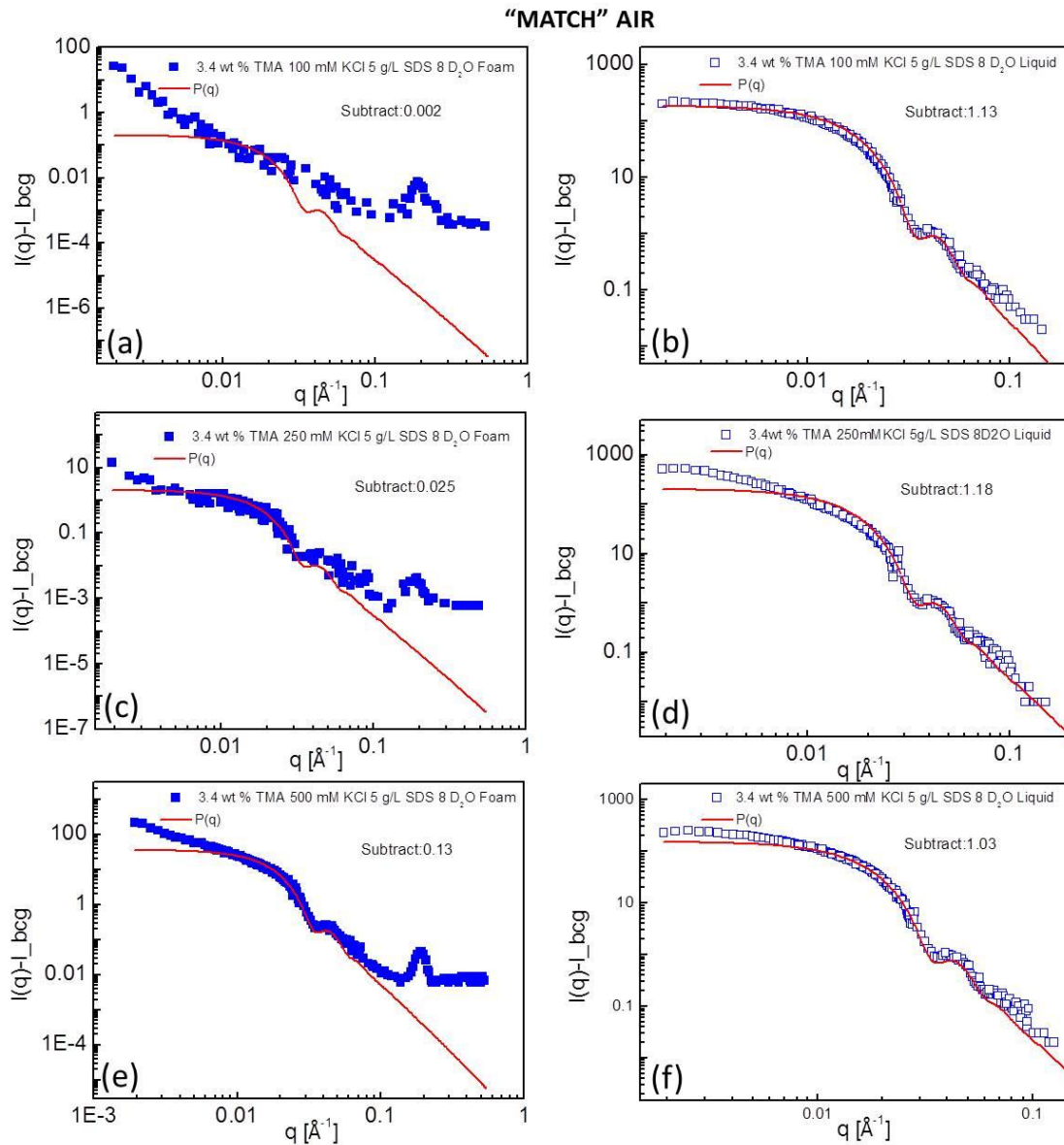


Figure 8.10 Scattering intensity $I(q)$ after subtraction the incoherent background I_{bcg} as a function of q for the samples with 3.4 wt% TMA at various salt concentrations in the presence of 5 g/L SDS. The samples on the left side are foams and right side are liquids. (a) and (b) with 100 mM KCl, (c) and (d) with 250 mM KCl, and (e) and (f) with 500 mM KCl. The solvent is the mixture of H_2O and D_2O (92:8). The red line is the form factor of silica particles. Solid square symbol represents the foam sample and open square one represents the liquid sample.

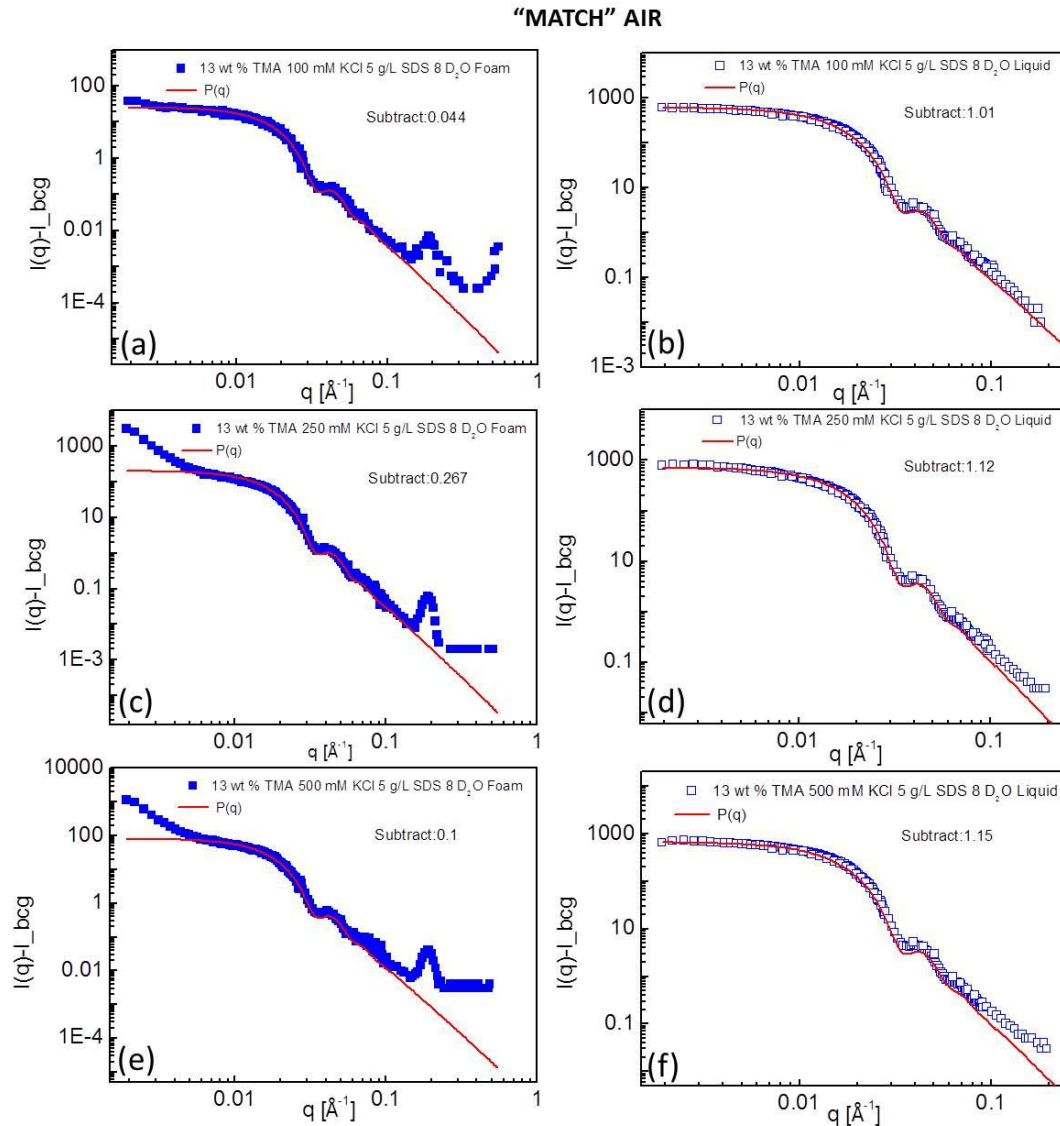


Figure 8.11 Scattering intensity $I(q)$ after subtraction the incoherent background I_{bcg} as a function of q for the samples with 13 wt% TMA at various salt concentrations in the presence of 5 g/L SDS. The samples on the left side are foams and right side are liquids. (a) and (b) with 100 mM KCl, (c) and (d) with 250 mM KCl, and (e) and (f) with 500 mM KCl. The solvent is the mixture of H₂O and D₂O (92:8). The red line is the form factor of silica particles. Solid square symbol represents the foam sample and open square one represents the liquid sample.

In order try to understand more about the behavior of silica particles in the foam sample, we show an apparent structure factor $S(q)$ with concentration 13 wt% TMA 250 mM KCl 5 g/L SDS when air is matched is given in Figure 8.12. We have divided the scattered intensity by the calculated $P(q)$ of the silica particles at the given concentration. One can see that $S(q)$ is increased with decreasing q , but we are not sure the scattering is from the surface of silica particles or the crystals. Anyway, it's interesting to see the silica particles in foam sample. This part needs more experiments.

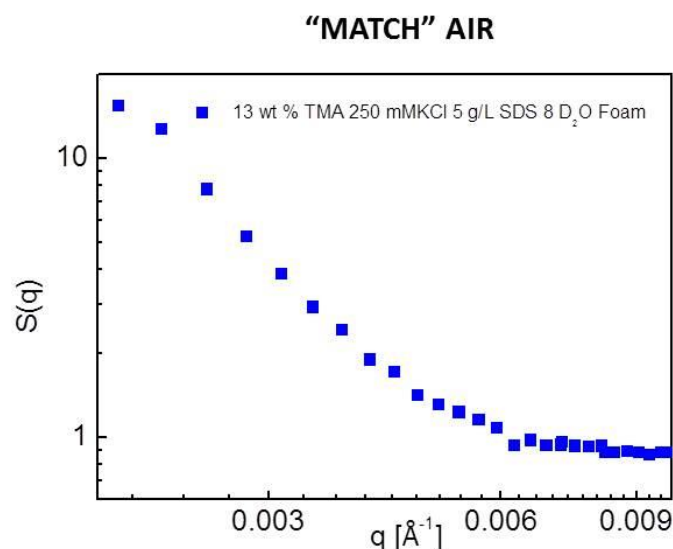


Figure 8.12 Structure factor $S(q)$ evolved as q for the foam sample with the concentration of 13 wt% TMA 250 mM KCl and 5 g/L SDS when air is matched. The solvent is the mixture of H_2O and D_2O (92:8).

8.3 Conclusions

In this Chapter the modification of the foam aging by the gel phase was investigated by mixing NaCl or KCl, silica particles, SDS and C_6F_{14} to produce gel foam. A reference sample was selected without particles. The results of liquid fraction show that the drainage of foam is fast in the first one hour and then it slowed in the next hours. This is consistent with the distribution of bubble sizes, the changement of which is only fast in the first hour. After that, the peaks of the distribution curves slowly shift to the higher radius except the samples with 12 vol% TMA and 500 mM NaCl and 16 vol% TMA and 300 mM NaCl, for these the curves are stopped to shift after 3 hours. When look at the normalized radius with time, one can find that the radii of them stopped to increase at around 4 hours. These suggest that foam aging is

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arrested with these two samples.

The rheological properties of bulk gel phases are measured, the relationship between R and G' imply that gel strength and gelation kinetics are two important factors to slow down or arrest the foam aging. For the samples of 12 vol% TMA with 500 mM NaCl and 16 vol% TMA with 300 mM NaCl they have high gel strength and smallest gelation time. That is the reason why they can arrest the foam aging. For rest of them they only can slow down of it. The correlation behavior is another proof to manifest that the gel strength and gelation kinetics are two important factors to modify the foam aging.

These results are useful as they provide a simply way to make solid foam. Foam aging can be tuned by changing the concentration of salt and particles in the sample.

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The dissertation is focused on the pattern of phase separation in the miscibility gap, ion specific effects on the aggregation of colloidal particles and surfactant, and gel phase influences to the foam stability.

We have observed the macroscopic and microscopic phase separation processes at various conditions using a microscope and scanning electron microscopy (SEM). The structure and the mechanical properties of gels are investigated by small angle X-ray scattering (SAXS) and rheology methods. Small angle neutron scattering (SANS) measurements are performed to determine the structure of crystallites inside the foam. The detailed conclusions are summarized as below:

1. In the miscibility gap, SD and NG type phase separations have been investigated. The results show that layer structures can be formed for both types under the thermal gradient but their morphologies are not the same. This is due to their distinct kinetic characteristics and the volume fraction of the minority phase. For SD type, it has a higher growth rate and volume fraction of minority phase leading to fast aggregation. As shown in the microscopic evolution of SD type, when the parameters are controlled appropriately, multilayer structures can be obtained. This is feasible for NG type as well. However, the difference is that for the former the minority phase

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rich layer is composed of the big aggregates of the minority phase and for the latter is the distribution of minority phase as spherical droplets.

Further, the initial structure characteristics of these two types of phase separation are not the same. According to this, different morphologies can be obtained such as the Fe-Sn ribbon. Our studies show that NG and SD type phase separations both in the early and late stage can produce different morphologies.

2. NaCl or KCl is added to a suspension of colloidal silica to investigate the salt-specific effects on the gelation process. Macroscopic observations and microscopic structure from SAXS experiments showed that the solidification with KCl is much faster than with NaCl. It's found that the macroscopic observations and the local structure can be scaled onto a single master curve, indicating that the counter ion type changes the timescale of gelation but not the equilibrium structure. The collapse of the storage and loss moduli when normalized with a scaling factor is further confirmation of the equivalence of the structure over several length-scales. The results also indicate that one could speedup gelation without changing the structural properties of the final gel by simply choosing the correct salt in the Hofmeister series.

When salts such as NaCl or KCl used it's possible to scale all results, suggesting that the final gel characteristics depend only on the volume fraction of TMA particles. The rheology measurements as a function of strain show that the strain needed to destroy the gel structure is higher with NaCl than with KCl, implying that the gel structure with NaCl is more flexible than with KCl even its storage modulus is less strong, when they are compared at a given time. Of course at long times they seem to tend to the same.

3. The light transmission method is used to observe the gelation process by adding different kinds of salt to the dispersion of silica particles. The normalized transmitted light intensities can be normalized by a scaling factor for all concentrations and types of salt selected, as well as the time (τ_{half}) when the transmitted light intensity decreased by half. This suggests that at least the scaling behavior with NaCl or KCl in Chapter 5 can be extended to more monovalent salts and even to divalent ones.

The ability of ions to assemble the silica particles has been investigated as well.

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It is found that they are following the Hofmeister series no matter monovalent salt or bivalent one.

4. The addition of salt at a high concentration to SDS has been studied. It's shown that ultrastable foams are made below the Krafft temperature. However whether the foams are stable or not also depends on the kinetics of crystal formation. If crystallization is too slow, the foam has time to disappear. If the crystals have time to form on the surfaces of the bubbles the foams are stable over months or until they are heated to melt the crystals at which point they start to age and disappear quickly. Nevertheless, there is one exception, unstable foam still can be obtained if too much foam is produced at a certain quantity of formed crystals even the crystal formation kinetics is not so slow. Such that the concentration of surfactant is much higher than salt. This can be controlled by selecting appropriate sample concentrations. Moreover, the type of salt with KCl is much more efficient than NaCl in creating ultrastable or/and stimulative foams.

5. The foam aging modification by the gel phase is investigated by mixing salt, silica particles and surfactant solution to produce gelling foam. The results of averaged bubble size and rheology measurements suggest that the gel strength is the important factor to restrict the growth of the bubbles, which are smaller when the gel strengths are higher. Comparing the bubble size data of sample 16 vol% TMA and 300 mM NaCl with 12 vol% TMA and 500 mM NaCl or sample with 16 vol% TMA and 200 mM NaCl with a reference sample, we found that gelation kinetics is another factor to influence the evolution of bubbles. The aging of foam with lower salt concentration is faster than with higher one.

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Appendix Résumé substantiel de la thèse

De nombreux produits et procédés industriels communs sont composés de plusieurs phases qui sont incompatibles. Selon les procédés, les systèmes peuvent être appelés à rester séparés, tels que des mousses et des émulsions (mélanges de gaz et de fluides liquides ou 2) lorsque les dispersions sont stabilisées par l'utilisation de molécules ou de particules actives aux interfaces. De tels systèmes comprennent également des suspensions de particules (telles que des peintures, du papier, des sols, des argiles, etc.), qui sont souvent stabilisées par des charges de surface. Cependant, dans d'autres cas, les mélanges ne sont pas stabilisés et la séparation de phase se produit à travers mûrissement. Le procédé de séparation de phase peut être importante car elle détermine la structure du matériau final. Par exemple, les alliages métalliques à microstructure spéciale sont fabriqués par refroidissement à partir d'une température supérieure à la température de fusion est similaire à de nombreux systèmes polymères. Pendant ce temps, les particules peuvent agréger comme phase solide sort.

Il existe un large éventail de systèmes qui présentent une séparation de phase et ma thèse a porté sur l'étude des différents types de tels systèmes. J'ai étudié la séparation de phase d'un système transparent dans l'intervalle de miscibilité en Chine, mais en

Appendix Résumé substantiel de la thèse

09,2013 comme je l'ai eu l'occasion de passer un an et demi en France dans le cadre de mes études je me suis concentré sur des systèmes légèrement différents. Mon projet est d'étudier les effets spécifiques d'ions sur l'agrégation des systèmes de la matière molle. Par conséquent, dans ma thèse, le chapitre 4 est mon travail en Chine et au chapitre 5, 6, 7 et 8 sont le travail en France.

Mon travail en Chine est concentré sur l'étude de la séparation de phase dans l'intervalle de miscibilité. Lorsque la température est trempé dans l'intervalle de miscibilité un procédé de séparation de phase a eu lieu. Ce qui est soit une croissance de nucléation (NG) ou de la décomposition spinodale (SD). L'étude du motif de séparation de phase dans l'intervalle de miscibilité est significative d'un point de vue pratique pour fournir une nouvelle approche pour créer des microstructures régulières spécialisés. Cela donne à penser qu'il est nécessaire d'étudier l'évolution de la microstructure sous certaines conditions et la cinétique de formation de la phase minoritaire. Dans cette thèse, un système transparent avec un écart de miscibilité est utilisé pour étudier le vieillissement de la microstructure pour SD et le type NG avec le gradient thermique et le taux de croissance de la phase minoritaire avec le champ isotherme.

En France, je travaillais sur la fabrication d'une mousse stable grâce à la formation d'un gel à l'intérieur de la mousse. L'ajout de sel à la dispersion de particules colloïdales peut conduire à l'agrégation due à un dépistage de la force électrostatique répulsive entre les particules et faire des gels, qui ont de nombreuses applications telles que la nourriture et la science des matériaux. Il est important de savoir comment le gel âgés avec le temps, ce qui a déjà été largement étudiés. Toutefois, des études antérieures ont tendance à observer le temps de gélification macroscopique et en utilisant le même sel à diverses concentrations en comparant les propriétés du gel. Dans ce mémoire, nous observons tout d'abord le temps de gélification au microscope, puis de comparer les propriétés du gel en présence de différents types de sels.

L'obtention de mousses stables est une question importante dans la vue de leur grande variété d'applications. Il existe de nombreuses façons de faire des mousses stables jusqu'à maintenant. Toutefois, bon nombre d'entre eux sont compliqués. Dans ce mémoire, en ajoutant des concentrations élevées de sel (NaCl ou KCl) à l'agent tensioactif SDS, la mousse ultrastable peut être effectuée et la mousse est sensible à la température. En outre, les mousses solides ont également de nombreuses applications

en raison de leur densité de faible masse et des propriétés de grande surface. Cela indique qu'il est important de savoir comment le vieillissement des bulles pendant les changements de mousse que la phase continue va d'un liquide à un solide (gel). Dans ce mémoire, la phase de gel est utilisée pour modifier la stabilité de la mousse.

Le chapitre 2 donne un aperçu des différents concepts qui sont utilisés dans le reste du manuscrit. Le chapitre 3 décrit les méthodes expérimentales et les matériaux utilisés.

Mécanismes de séparation de phase étudiés dans l'intervalle de miscibilité

Le chapitre 4 présente SD et NG séparation de phase de type dans l'intervalle de miscibilité. Sous le gradient de température, des structures de couches peuvent être formées avec les deux types mais leurs morphologies ne sont pas les mêmes que ceux indiqués sur la figure 1. Ceci est dû aux caractéristiques cinétiques et la fraction volumique de la phase minoritaire. Pour le type SD, il a un débit et le volume de croissance plus grande fraction de la phase minoritaire conduisant à l'agrégation rapide. Si les paramètres sont contrôlés de façon appropriée, la structure multicouche peut être formée aussi.

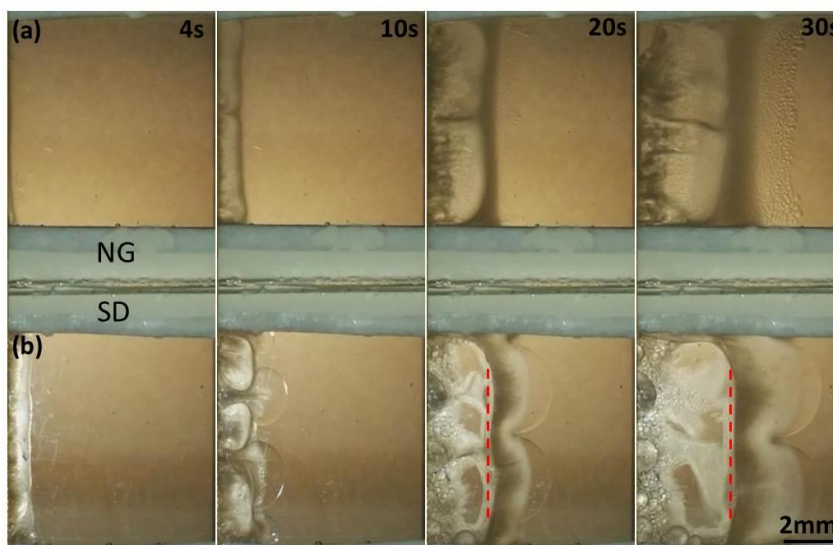


Figure 1 Evolution acroscopique de la morphologie de NG avec une solution SCN-70% en poids H_2O (a) et SD avec une solution SCN-50% en poids H_2O (b) avec le temps. La basse température (côté gauche) était $T_L = 297,5$ K et une température élevée (côté droit) $T_H = 330,5$ K. La ligne pointillée rouge (b) est la couche interfaciale entre la phase de matrice et la phase riche en minorité.

Effet spécifiques des ions sur la formation des gels colloïdaux: Le chapitre 5 décrit le processus de gélification en présence de sel NaCl ou KCl pour étudier les

effets spécifiques de sel sur le processus de gélification. Les observations macroscopiques et microscopiques à partir d'expériences structure de SAXS a montré que la solidification de KCl est beaucoup plus rapide qu'avec NaCl. Cependant, comme on le voit sur la figure 2, les observations macroscopiques et la structure locale peuvent être mises à l'échelle sur une courbe ma fresse unique, ce qui indique que le type de compteur d'ions modifie l'échelle de temps de gélification, mais non la structure d'équilibre. L'effondrement du stockage et de la perte des modules lorsque normalisé avec un facteur d'échelle est une nouvelle confirmation de l'équivalence de la structure sur plusieurs échelles de longueur. Le chapitre 6 poursuit l'étude a commencé au chapitre 5 et explore la cinétique de formation de gel en utilisant une large gamme de sels, mais en limitant les expériences de transmission de la lumière. Les intensités lumineuses transmises peuvent être mises à l'échelle sur la courbe ma fresse unique, montrant que (au moins à la longueur des échelles sondée utilisant la transmission de la lumière), le processus de gélification ne diffère que par la cinétique même avec une plus large gamme de sels.

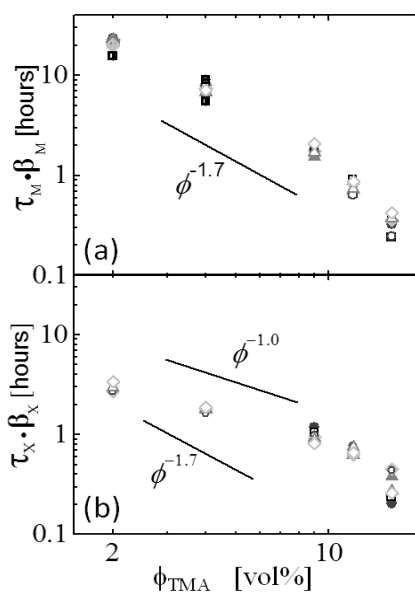


Figure 2 Les temps de transitions normalisés à partir des observations macroscopiques $\beta_M \tau_M$ (a) et à partir des expériences SAXS $\beta_X \tau_X$ (b).

Effets spécifiques d'ions sur la stabilité de la mousse: Le chapitre 7 montre que les mousses peuvent être faites ultrastable en dessous de la température de Krafft en ajoutant des une concentration élevée en sel de NaCl ou KCl à SDS. Les mousses sont stables ou non, dépendant de la cinétique de formation des cristaux comme

indiqué sur la figure 3. Si la cristallisation est trop lente, la mousse a le temps de disparaître.

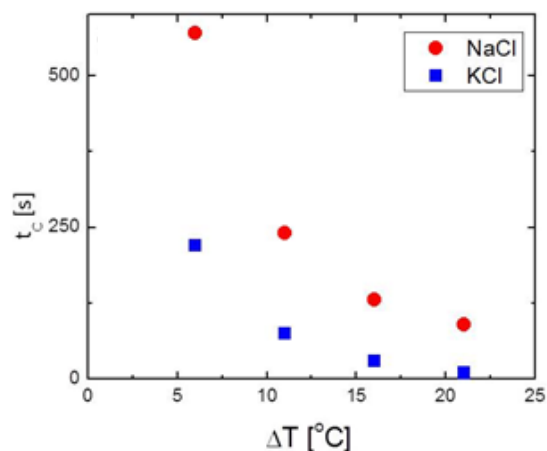


Figure 3. Temps à la quelle la précipité deviens visible à l'oeil nu en froidssant.

Si les cristaux ont le temps de se former sur les surfaces des bulles des mousses stables au cours des mois ou jusqu'à ce qu'ils sont chauffés pour faire fondre les cristaux à quel point ils commencent à l'âge et disparaissent rapidement. Avec du NaCl le temps de cristallisation est plus lent que par NaCl, par conséquent, la mousse fabriquée est moins stable avec du NaCl, comme le montre la Figure 4

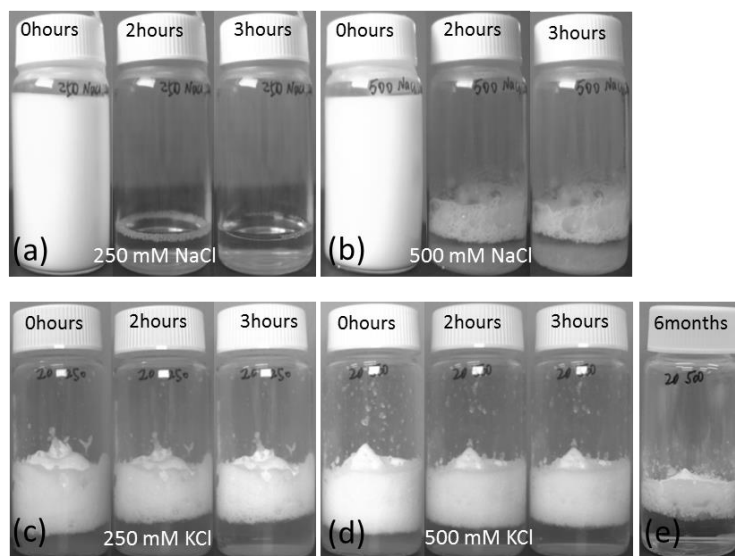


Figure 4 photographies des échantillons de mousse à base de SDS à 69 mM et (a) 250 mM de NaCl; (B) 500 mM NaCl; (C) 250 mM KCl; (D) KCl 500 mM, (e) l'échantillon (d) 6 mois plus tard

Mousse vieillissement accordé par la phase de gel: Dans le chapitre 8, le vieillissement de la mousse est modifiée par la phase de gel pour produire gélifiant

Appendix Résumé substantiel de la thèse

mousse. Les résultats de la taille des bulles et la rhéologie mesures moyennées suggèrent que la résistance du gel et de la cinétique de gélification sont deux facteurs importants pour influencer sur l'évolution des bulles, qui sont plus petites lorsque les résistances de gel sont plus élevées. Comme on le voit sur la figure 5, les échantillons avec mM de NaCl, 16% en volume de TMA 300 mM de NaCl et 12% en volume TMA-500 présentent une résistance de gel élevée et plus rapide cinétique de gélification, leur vieillissement de la mousse peut être arrêté

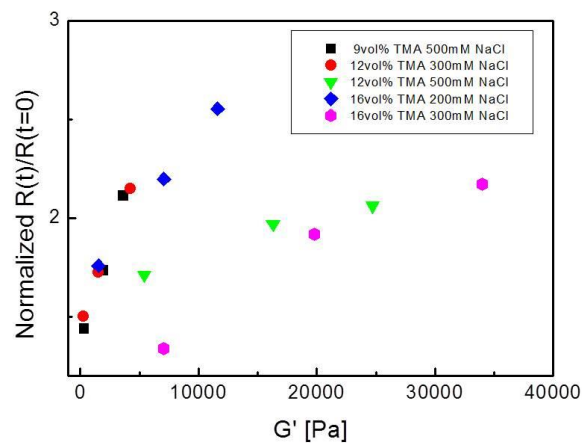


Figure 5 Rayon normalisé avec module de stockage G' pour la concentration 9% en volume TMA 500 mM de NaCl (place), 12% en volume TMA 300 mM de NaCl (cercle), 16% en volume TMA 200 mM de NaCl (de diamant), 12% en volume TMA 500 mM de NaCl (triangle vers le bas) et 16% en volume de TMA 300 mM de NaCl (hexagone).

Titre : L'étude de la séparation de phase dans une zone de miscibilité et des effets spécifiques des ions sur l'agrégation des colloïdes et des mousses

Mots clés: Nucléation, décomposition spinodale, sel, gel, mousse, colloïde, démixtion, diffusion aux petits angles

Résumé : Le procédé de séparation de phase est importante car elle détermine la structure des matériaux finaux. Il existe de nombreux systèmes qui ont plus d'une phase tels que des mousses et des gels. Les mousses sont des dispersions aqueuses de bulles de gaz dans une phase aqueuse et gels apparaissent lorsque certains microscopique unité de base commence à se rassembler formant un grand réseau solide qui enjambe l'espace macroscopique. Ils ont de nombreuses applications dans l'industrie et la vie quotidienne. Dans cette thèse, tout d'abord, je me concentre sur l'étude de différents types de séparation de phase. Deuxièmement, j'étudie les effets spécifiques d'ions sur l'agrégation des particules colloïdales et tensioactif, le but est de faire des mousses stables. Dans la lacune de miscibilité il existe deux types de séparation de phase: la croissance nucléation et la décomposition spinodale, ils ont différents mécanismes et de la cinétique de croissance. Par conséquent, mon premier projet est d'étudier le

processus d'évolution d'eux et de leurs effets sur la structure finale du matériau. Les gels peuvent être préparés par l'ajout de sel à la dispersion de particules colloïdales, ils ont un grand nombre d'applications telles que dans les aliments et la science des matériaux. Dans cette thèse, nous utilisons différents types de sels de comparer les propriétés de gel à partir de deux aspects macroscopiques et microscopiques. Obtenir des mousses stables est significatif dans la vue de leur beaucoup d'applications, mais les moyens de les faire sont pour la plupart compliqué. Dans cette thèse, nous pouvons obtenir des mousses stables par l'intermédiaire de deux façons. On est tout simplement en ajoutant des sels de solutions de tensioactifs, à travers lequel nous pouvons faire la mousse ultra-stable. Une autre façon est d'utiliser la phase de gel, nous avons étudié en tant que phase continue dans les mousses à arrêter le vieillissement de la mousse.

Title : The study of phase separation in the miscibility gap and ion specific effects on the aggregation of soft matter systems

Keywords : Nucleation, Spinodal decomposition, Salt, Gel, Foam, Colloid, Demixing, Scattering

Abstract : Phase separation process is important as it determines the structure of the final materials. There are many systems that have more than one phase such as foams and gels. Aqueous foams are dispersions of gas bubbles in a water phase and gels appear when some basic microscopic unit starts to aggregate forming a large solid network that spans macroscopic space. They have many applications in industry and daily life. In the present thesis, firstly, I focus on studying different types of phase separation. Secondly, I studied the ion specific effects on the aggregation of colloidal particles and surfactant, the purpose is to make stable foams. In the miscibility gap there are two types of phase separation: Nucleation growth and spinodal decomposition, they have different growth mechanisms and kinetics. Therefore, my first

project is to investigate the evolution process of them and their effects to the final structure of material. Gels can be made by adding salt to the dispersion of colloidal particles, they have a large number of applications such as in food and material science. In this dissertation, we use different types of salts to compare gel properties from both macroscopic and microscopic aspects. Obtaining stable foams is significant in the view of their plenty of applications, but the ways to make them are mostly complicated. In this thesis, we can obtain stable foams via two ways. One is simply by adding salts to surfactant solutions, through which we can make ultrastable foam. Another way is using the gel phase we have studied as the continuous phase in foams to arrest the foam aging.

