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## École Doctorale de Physique et Chimie-Physique

Nanomatériaux pour les Systèmes Sous Sollicitations Extrêmes NS3E, UMR 3208 ISL-CNRS-UNISTRA

## THÈSE présentée par :

 Florent PESSINAsoutenue le : 05 octobre 2016

# pour obtenir le grade de : Docteur de l'université de Strasbourg Discipline/ Spécialité : Chimie Physique-Chimie 

## Toward Particle Size Reduction by Spray Flash Evaporation the case of organic energetic crystals and cocrystals

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## $\infty * \infty$

«Qui a dit que la science désenchante le monde? Assurément un ignorant, car toutes les peurs se nourrissent de l'ignorance et des ignorances entretenues.»

Pascal Pic, Darwin et l'évolution expliqués à nos petits-enfants (2009).
"SCIENCE: A way of finding things out and then making them work. Science explains what is happening around us the whole time. So does RELIGION, but science is better because it comes up with more understandable excuses when it is wrong."

Terry Pratchett, Wings (1990, 2007), 147.
since we are living in a so-called modern age where PR and economic interests seems to have won against science.

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Extended Abstract

The development of nano-technology took off with the invention of the Scanning Tunneling Microscopy (STM) and the Atomic Force Microscopy (AFM) in the early 80's at the IBM Zurich Research Laboratory (Binnig et al. 1986, 1983, 1982). By providing accurate and advanced characterizations on nanoparticles, those two crucial microscopy techniques allowed a control of the physicochemical properties of materials down to the atomic scale. Since then, the outstanding properties of new nano-materials led the research in energetic material to embrace this trend. The nano-structuration of classical explosives, such as 2,4,6-trinitrotoluene (TNT) or 1,3,5-trinitroper-hydro-1,3,5-triazine (RDX), can enhance their safety but also their reactive properties (critical diameter, tunable detonation velocity etc.).

Organic energetic materials release their intrinsic energy under an external stimulus such as a strong mechanical impulse, a great heat or an electrostatic discharge. This initiation is facilitated by the formation of hot-spots coming from the presence of impurities, open pores, entrapped gases or other inhomogeneities within the explosive matrix. Therefore, void free crystals have been an extensive research subject, but the mastering of crystallisation can be enhanced by the formation of particles smaller than the critical size of a hot spot. Moreover, achieving a controlled crystallisation enables further tailoring of the nanoparticles and thus of the physicochemical properties.

The continuous formation of nanosized energetic material is a long-standing challenge. From wet productions methods to dry crystallisation processes, Spray Flash Evaporation (SFE) is a major technique for continuously producing energetic materials at submicron or nano scale. It relies on the superheating of a solvent sprayed into vacuum and thus flashing. The versatility of the SFE internally developed (Doctoral Thesis Risse 2012; Risse et al. 2012) and patented ("Method for producing cocrystals by means of flash evaporation" 2016; "Préparation de nanoparticules par évaporation flash" 2013) allows the continuous engineering of nano-crystals and nano-cocrystals for oxides (Klaumünzer et al. 2015), medical and energetic applications (Spitzer et al. 2014).

This present research project aims to understand and control the crystallisation occurring in the SFE process, in order to reduce further the particle size of energetic crystals. 1,3,5-trinitroperhydro-1,3,5-triazine (RDX) is chosen as a reference material for its wide use for civilian and military applications. Cocrystals -two or more molecules that form a unique crystalline structureare also relevant in energetic materials in order to decrease the sensitivity
without losing reactivity; for instance a low sensitive compound could be cocrystallised with another one having a high sensitivity and a high reactivity. Therefore, the cocrystal CL-20:HMX 2:1 was studied as proof-of-concept but also to overcome the limited in situ characterizations. Crystallisation depends on the supersaturation; in SFE, the supersaturation is a function of time and space as it is linked to the size distribution and velocity of droplets. Since those measurement was first out of reach, supersaturation was raised with an anti-solvent and the enhancement of the SFE with a dual nozzle system. Later, a Phase Doppler Analysis (PDA) was used to elucidate the question of supersaturation.

Another route to control the crystallisation is the addition of chemical agent. PolyVinylPyrrolidone (PVP) and PolyEthylene Clycol (PEG) were used to alter the two steps of the crystallisation, namely the nucleation and the growth. PEC 400 triggers the early nucleation of RDX with low nucleation rate leading to bigger particles up to $5 \mu \mathrm{~m}$. PVP 40K acts as a nucleation and growth inhibitor, forming RDX spherical particles with a mean size of 160 nm . Additionally, the synthesized RDX samples were less sensitive, especially toward electrostatic discharge.

During this work, many standard analytical methods have been found to be impossible or difficult to apply on energetic material, due to their sensitivity toward heat, or toward vacuum, or their organic nature; the nano scale and so the high specific surface area worsen those phenomena. The relevancy of the sensitivity tests is also questionable when reaching the nano scale.

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## Résumé étendu français

## Réduction de la taille des particules par Spray Flash Evaporation : le cas des cristaux et cocristaux organiques énergétiques.

Le développement des nanotechnologies a réellement décollé avec l'invention des microscopies par effet tunnel (STM) et à force atomique (AFM), au début des années 80 à l'Institut de Recherche IBM de Zurich (Binnig et al. 1986, 1983, 1982). Ces deux techniques permettent l'analyse directe de nanostructures jusqu'à l'échelle atomique, et sont donc devenues indispensables pour contrôler finement les propriétés physicochimiques des matériaux. Depuis quelques décennies, les nouveaux nanomatériaux ont pris leur essor dans notre société grâce à des propriétés remarquables pour de nombreuses application, et aux couts de production maîtrisés. Le développement des nanotechnologies a aussi permis la création et l'amélioration de technologies connexes. Contrairement à la révolution numérique, les secteurs scientifique et industriel des matériaux énergétiques sont restés bien longtemps en marge de cette vague technologique, et ne s'engagent que depuis peu dans l'exploration des propriétés de nanostructures énergétiques. Parmi les attentes, la nanostructuration d'explosifs classiques comme le 2,4,6-trinitrotoluene (TNT) ou le 1,3,5-trinitroperhydro-1,3,5triazine (RDX) peut améliorer leur sensibilité et donc faciliter leur manipulation, mais aussi nombre de leurs propriétés réactives (diamètre critique, vitesse de détonation, homogénéité...).

Les explosifs étudiés ici sont les matériaux énergétiques organiques; ils libèrent leur énergie intrinsèque suite à un stimulus tel une sollicitation mécanique importante, une forte chaleur ou une décharge électrostatique. Cette initiation est facilitée par la formation de points chauds, hot-spot, qui proviennent d'impuretés, de cavités et autres défauts dans la matrice cristalline. Ainsi, la production de cristaux à haute pureté et haute cristallinité fut un champ de recherche privilégié pendant des décennies, mais la maîtrise de la cristallisation peut être poussée encore plus loin par la formation de particules plus petites
que la taille critique d'un point chaud. De plus, atteindre une cristallisation contrôlée permet de façonner avec précision les nanoparticules et donc d'ajuster leurs propriétés physicochimiques.

L'étude des nanomatériaux énergétiques organiques commence par leur formation; le retard pris par la communauté pyrotechnique en nanotechnologie s'explique en partie par la difficulté de produire des nanoparticules d'explosifs. Ainsi la cristallisation en continu de matériaux énergétiques à une échelle au moins submicronique est un défi de longue date. Parmi les méthodes de production de la voie humide à la voie sèche, le procédé Spray Flash Evaporation (SFE) est une technique émergente majeure pour la production continue d'explosifs nanométriques ou de compositions énergétiques nanostructurées. Cette méthode se base sur la surchauffe d'un solvant pulvérisé dans un vide primaire/moyen, provoquant alors une évaporation quasi instantanée, flash. La polyvalence du SFE, développé en interne (Thèse de Doctorat Risse 2012) et breveté ("Method for producing cocrystals by means of flash evaporation" 2016; "Préparation de nanoparticules par évaporation flash" 2013), permet la formation d'oxydes (Klaumünzer et al. 2015) ainsi que de nanocristaux et co-cristaux pour des applications énergétiques et médicales (Spitzer et al. 2014).

Le présent projet de recherche vise à comprendre et contrôler la cristallisation au sein du procédé SFE, afin de réduire la taille des cristaux énergétiques. Le 1,3,5-trinitroperhydro-1,3,5-triazine (RDX) a été choisi comme matériau énergétique de référence du fait de son utilisation large pour des applications civiles et militaires. La cristallisation dépend du degré de sursaturation; dans le SFE, la sursaturation est fonction du temps et de l'espace car liée à la distribution en taille des gouttes et à leur vitesse. La caractérisation in situ des gouttes requiert l'utilisation de techniques avancées d'interférométrie optique acquises à la fin du projet. Pour palier cette absence, la sursaturation a été augmentée par l'ajout d'un anti-solvant et la mise en place d'un système d'injection à double buses. Finalement, un appareil d'interférométrie optique, Phase Doppler Analysis (PDA), est utilisé pour déterminer les tailles et vitesses des gouttes.

Pour déterminer la persistance des gouttes, le co-cristal CL-20:HMX 2:1 sera employé avec le système d'injection à double buses. L'utilisation de co-cristaux (deux molécules ou plus dans un même réseau cristallin unique) pour étudier la cristallisation au sein du SFE est d'autant plus pertinente que la formation de co-cristaux énergétiques est une autre stratégie actuellement explorée pour réduire la sensibilité de l'explosif sans sacrifier sa réactivité.

La cristallisation au sein du SFE peut aussi être maîtrisée par l'ajout d'agents polymériques. Le PolyVinylPyrrolidone (PVP) et le PolyEthylene Gilycol (PEG) ont été employés pour modifier les conditions de cristallisation donc les étapes de nucléation et de croissance. Le PEG 400 provoque la nucléation anticipée du RDX
amenant à la formation de particules de 500 nm à $5 \mu \mathrm{~m}$. La PVP 40k s'adsorbe en surface et agit comme agent inhibiteur de nucléation et de croissance : le RDX cristallise en nanoparticules sphériques avec une taille moyenne de 160 nm . Les échantillons de RDX synthétisés ainsi sont également moins sensibles, tout spécialement à la décharge électrostatique.

Lors de ce travail de recherche, de nombreuses méthodes de caractérisation ont été testées et bien peu se sont avérées être applicables de manière fiable sur les nanomatériaux énergétiques. En effet, ces derniers -des cristaux moléculairessont sensibles à la chaleur et au vide; cette sensibilité est encore exacerbée pour les nanomatériaux du fait de leur grande surface spécifique. De plus, la pertinence des tests de sensibilité à cette échelle est critiquable.

## Cristaux et cocristaux organiques énergétiques

Les matériaux énergétiques regroupent tous types de matériaux (composite, polymère, organiques...) qui peuvent libérer rapidement de l'énergie par une violente réaction d'oxydo-réduction. Un stimulus externe comme un choc, un frottement ou une décharge électrostatique peut initier localement la réaction de décomposition; cette dernière se propage à travers le matériau via le front de réaction. La vitesse de ce front de réaction dépend du matériau et du mode de décomposition.

On distingue trois modes de décomposition : la combustion (mm/s - m/s), la déflagration ( $\mathrm{m} / \mathrm{s}-\mathrm{km} / \mathrm{s}$ ) et la détonation ( $>\mathrm{km} / \mathrm{s}$ ). La combustion requiert un apport extérieur d'oxygène alors que la déflagration est auto-entretenue. Lors d'une détonation, la réaction se propage par une onde de choc supersonique. Par la suite, on peut classer les matériaux énergétiques selon leur mode normal de décomposition et leurs autres propriétés pyrotechniques. Les poudres propulsives brûlent de manière contrôlée avec une importante génération de gaz afin de produire la poussée nécessaire aux engins autopropulsés. Les explosifs détonent et sont également classés selon leurs sensibilités et puissances: les explosifs primaires, très sensibles, servent à l'initiation par onde de choc des explosifs secondaires, tels que le RDX ou le 2,4,6-trinitrotoluene (TNT). On retrouve parfois des matériaux comme le nitrate d'ammonium et le perchlorate d'ammonium classés comme explosifs tertiaires du fait de leur grande stabilité. D'un point de vue chimique, les explosifs organiques sont des cristaux moléculaires dont la cohésion est assurée par des forces faibles (Van der Waals : $\pi$ stacking, liaison hydrogène ...).

Un co-cristal est un cristal comprenant plusieurs molécules électriquement neutres au sein de la même maille cristalline, avec un ratio stæchiométrique défini. La définition est toujours en débat (Sun 2013) mais les hydrates et
solvates sont généralement exclus. Bolton et al. (2012) furent les premiers à rapporter la formation et la caractérisation du co-cristal CL-20:HMX avec un ratio molaire de 2:1.

## Procédés et Intérêt de la nanocristallisation

Ces matériaux hautement explosifs peuvent être accidentellement initiés, engendrant malheureusement nombre de victimes et ce bien trop souvent comme nous le rappellent les lettres de l'Inspecteur de l'armement pour les Poudres et Explosifs. Outre cet aspect, la désensibilisation du matériaux entraîne fréquemment des traitements supplémentaires (enrobage, mises en forme...) voire une perte de performances. Des inclusions, des défauts cristallins ou un habitus cristallin trop rugueux sont différents paramètres physico-chimiques pouvant fragiliser et sensibiliser le matériau; une cristallisation contrôlée à une échelle nanométrique permet d'éviter ce type de défauts micrométriques et de réduire le nombre d'étapes aboutissant au produit fini.

De nombreux procédés de recristallisation existent et ont été appliqués aux matériaux organiques énergétiques. Les méthodes par voie liquide permettent d'atteindre des tailles nanométriques et des morphologies contrôlées, deux caractéristiques intéressantes qui sont par la suite perdues lors du séchage : les processus de séchage les plus performants tels que le séchage supercritique réduisent la dégradation des cristaux mais fonctionnent par lot et non en continu. Les méthodes en voie sèche les plus abouties actuellement sont le Spray drying (Broadhead et al. 1992; Stein 1973) et le Rapid Expansion of Supercritical Solutions (RESS) (Krukonis 1984 ; Matson et al. 1987a,b) : le premier fonctionne en continu mais ne permet pas d'atteindre l'échelle nano ni le submicron, alors que le second permet d'atteindre de telles tailles mais opère séquentiellement. De plus le RESS est un procédé industriel coûteux du fait de l'utilisation de fluides supercritiques (faible solubilité, pression importante) rarement utilisés dans l'industrie (Sheth et al. 2012).

Le procédé Spray Flash Evaporation (SFE) permet la production en continu et en voie sèche de particules nanométriques ou submicrométriques ou de composites nanostructurés. Il se situe entre le RESS et le Spray drying en terme de pression et de température. Inventé (Doctoral Thesis RISSE 2012; RISSE et al. 2012) et breveté ("Method for producing cocrystals by means of flash evaporation" 2016; "Préparation de nanoparticules par évaporation flash" 2013) au sein du laboratoire NS3E, le SFE a été précédemment optimisé grâce à la thèse de Risse (2012) ; cependant seuls cinq paramètres ont été étudiés, chacun dans une certaine mesure. Il apparaît nécessaire qu'afin de contrôler et de réduire encore la taille des particules cristallisées par SFE, une bonne compréhension
de la cristallisation au sein du SFE doit être acquise soit directement par une métrologie en ligne, soit par des variations induites dans la cristallisation.

## Spray Flash Evaporation : principe et cristallisation



Figure 0.1 - Schéma du procédé de Spray Flash Evaporation (SFE)

Le procédé SFE consiste à pressuriser et surchauffer un solvant comprenant un ou plusieurs composés organiques dissous, puis à pulvériser cette solution dans une enceinte sous vide. Le SFE repose alors sur le principe thermodynamique de flash évaporation : lorsqu'un liquide possède une énergie interne importante (ici d'origine thermique) et est soumis à un déséquilibre thermodynamique important (notamment lorsque la température du liquide est bien supérieure à sa température d'ébullition une fois sous vide), cette énergie est convertie en chaleur latente. Les gouttes se désintègrent et s'évaporent quasi instantanément.

La cristallisation est gouvernée par le degré de sursaturation dans chaque gouttelette; la conjonction de nombreux phénomènes thermodynamiques mène à une taille nanométrique. La fission des gouttelettes diminue le volume de chaque réacteur, le niveau de surchauffe du liquide influence la solubilité du(des) composé(s) dans le solvant mais aussi la méta-stabilité des gouttes avant le flash... A cela s'ajoute une composante temporelle essentielle où on peut distinguer deux plans d'évolution en fonction du temps: le moment de l'évaporation flash avec le taux d'évaporation d'un côté, et de l'autre le début de la nucléation primaire avec le taux de nucléation (Figure 0.2).


Figure 0.2 - Illustration schématique des phénomènes d'évaporation et cristallisation en jeu dans le SFE. La limite de 500 nm correspond à la limite actuelle de détection possible par mesure directe en ligne en anémo-granulométrie Phase Doppler

## Compréhension du SFE

Peu de techniques sont à même de mesurer des aérosols à haute vitesse et de l'ordre du micron. L'interférométrie Phase Doppler est une méthode de mesure optique avancée qui, couplée à la vélocimétrie LASER, permet la mesure in situ, simultanée et en temps réel de la taille et de la vitesse d'objets quasi sphériques et microniques. Elle a été pour la première fois adaptée à la technologie SFE: la mesure des tailles dans l'espace du cône de pulvérisation permettra le calcul de la sursaturation. Dans un premier lieu, il s'agit de caractériser le phénomène de flash évaporation : les Figures 0.3 et 0.4 montrent les premiers résultats obtenus avec un appareil optimisé et calibré sur l'acétone. Il est remarquable d'observer trois distributions modales centrées en $2.1,2.8$ et $3.8 \mu \mathrm{~m}$ à toutes les températures; comme attendu, la taille moyenne chute vers la limite de détection proche du micron lorsque la température augmente. En revanche, l'étude montre alors que le phénomène de flash évaporation est transitoire et commence dès $100^{\circ} \mathrm{C}$ et semble ne pas être unique à $160^{\circ} \mathrm{C}$ du fait de la présence persistante de deux distributions à 2.1 et $2.8 \mu \mathrm{~m}$.


Figure 0.3 - Distribution en taille des gouttes pulvérisées à 100, 140 et $160^{\circ} \mathrm{C}$.

## Définition d'une particule

La première année de recherche fut menée sur l'étude des paramètres du SFE influençant la taille et la morphologie des cristaux. Ces derniers ont été observés en suivant une méthode développée précédemment au sein du laboratoire : il s'agit de compresser la poudre obtenue et de lisser la surface par micro coupe pour imager par Microscopie à Force Atomique (AFM). L'AFM n'apporte aucune énergie à l'échantillon, contrairement à la Microscopie Électronique à Balayage (MEB) dont le faisceau d'électrons dégrade le matériau énergétique. La méthode par AFM souffrait en revanche d'une analyse des images longues et fastidieuses, ce qui fut tout d'abord amélioré. Une méthode semi automatique a été mise en place avec le logiciel Gıwyddion et la technique Watershed. Elle est composée des étapes suivantes:

Processus de localisation des grains La surface est inversée - les particules deviennent des creux - puis de l'eau virtuelle est déposée en chaque point. Ces gouttes d’eau glissent le long des pentes et la répétition de cette pluie virtuelle forme ainsi des lacs dans les minimum locaux. Ces lacs, ces ensembles virtuels, délimitent alors la position des grains.

(a) $100^{\circ} \mathrm{C}$

(b) $140^{\circ} \mathrm{C}$

(c) $160{ }^{\circ} \mathrm{C}$

Figure 0.4 - Régression des profils de distribution en taille des gouttes pulvérisées à 100,140 et $160^{\circ} \mathrm{C}$.

Segmentation Précédemment si deux lacs se touchaient lors d'une pluie virtuelle, ils étaient fusionnés. Dans l'étape de segmentation, deux lacs adjacents seront notés comme différents et une bordure sera définie. La qualité des frontière entre les grains s'améliore avec des gouttes plus fines, mais le temps de calcul augmente fortement avec la diminution de la taille de goutte.

Inspection visuelles et corrections mineures Le logiciel permet l'affichage en surbrillance, le marquage et l'édition manuelle des grains ainsi que plusieurs améliorations du contraste pour permettre une vérification visuelle efficace et une correction des défauts. Les autres canaux de données tels que la phase ou l'amplitude peuvent aider à déterminer la validité d'une frontière de grain.

Distribution en taille et régression Le logiciel permet l'affichage de la distribution en taille des particules mais, grâce à l'export des données, une régression des profils de distributions peut être appliquée par un logiciel tiers. Ici le diamètre est défini comme celui d'un disque d'aire équivalent à la particule mesurée. La distribution en taille semble suivre une loi log normale et non une loi Gaussienne ce qui signifie que les particules sont générées par l'effet de nombreux effets aléatoires et multiplicatifs comme le sont souvent les aérosols (Limpert et al. 2001).


Figure 0.5 - Analyse Watershed illustrée sur une simulation de sphères de 200 nm .

Une étude de la méthode a été entreprise pour déterminer sa fiabilité et sa robustesse. Deux facteurs prépondérants sur la taille de particules ont été dégagés:

L'effet de la pression La presse utilisée pour la compression des matériaux énergétiques consiste en un levier supporté par un piston hydraulique ; à l'extrémité du levier, des masses sont accrochées, puis le piston est actionné pour descendre doucement le levier et donc former le comprimé dans des conditions adiabatiques. La pression appliquée est calculée en fonction du poids employé; les valeurs utilisées sont affichées en Figure 0.1.

| Poids $(\mathrm{kg})$ | Pression (MPa) |
| :---: | :---: |
| 2 | 12 |
| 5 | 26 |
| 10 | 50 |
| 20 | 97 |
| 30 | 140 |
| 45 | 210 |
| 70 | 330 |
| 97 | 460 |

Table 0.1 - Poids utilisé et pression correspondante calculée : l'effet de levier suit la loi $P=6 \cdot \frac{M}{A}+31$ où $A=\frac{\pi}{4} \cdot \varnothing^{2}$ avec $M$ la masse du poids.

L'effet de la pression peut s'observer en Figure 0.6, où la même face de comprimé a été analysée par AFM et aucune micro coupe n'a été réalisée. Dans la Figure 0.6a une chute brutale de la taille de particule est clairement observable dès $S I 140 \mathrm{~kg}$ puis la valeur se stabilise autour de 90 nm : ce changement est aussi visible en Figure 0.6b. Dans les Figures 0.6c et 0.6d, les particules sont difficilement identifiables.

Les résultats provenant de comprimés micro coupés en Figure 0.7 montrent là encore que la pression joue un rôle crucial sur la taille de particule mesurée par AFM. La réduction de taille est progressive avec l'augmentation de la pression. Au delà de $97 \mathrm{MPa}(20 \mathrm{~kg})$, les comprimés sont bien trop cohésifs pour pouvoir être usinés par micro coupe ; leur grande dureté du fait d'un comportement quasi vitreux les rend cassants sous la lame.

Le RDX micronique (M5 Eurenco) utilisé pour la recristallisation a également été analysé selon cette méthode; les comprimés obtenus sont friables à un tel point qu'aucune micro coupe n'a pu être effectuée. Cependant, alors que la taille moyenne reste de l'ordre du micron, à la pression maximale de 97 MPa


Figure 0.6 - Effet de la pression, sans micro coupe, $5 \mu m \times 5 \mu m$ pour $1024 p x \times 1024 p x$, contraste amélioré.
une chute de la taille moyenne est observée de la même manière que le RDX recristallisé par SFE. Ainsi il apparaît clairement que le nano RDX est broyé à des contraintes plus faibles et donc plus facilement : cet effet de casse ou de désagrégation doit être étudié plus en profondeur car les explosifs sont utilisés notamment en charges pressées.

Effet de la micro coupe D'après les résultats en Figures 0.7a et 0.6a, la micro coupe réduit la taille moyenne et l'effet de la pression précédemment mis en évidence est accentué. Cet effet s'explique par la dureté accrue des comprimés avec la pression : la force de micro coupe doit être plus élevée donc l'effet de broyage en surface est accru.


Figure 0.7 - Effet de la pression, avec une micro coupe, $5 \mu \mathrm{~m} \times 5 \mu \mathrm{~m}$ pour $1024 p x \times 1024 p x$, contraste amélioré.

| Pression (MPa) | Brut | Avec micro coupe |
| :---: | :---: | :---: |
| 12 |  | 280 |
| 26 | 180 |  |
| 50 | 170 | 230 |
| 97 | 235 | 140 |
| 140 | 100 |  |
| 210 | 80 |  |
| 330 | 110 |  |
| 460 | 90 |  |

TABLE 0.2 - Diamètre moyen en nm selon la pression appliquée et le pré traitement par microtome ; par MEB, la taille moyenne est de 500 nm .

## Découplage des phénomènes au sein du SFE et contrôle des tailles

La cristallisation se déroule principalement en deux étapes successives: la nucléation et la croissance cristalline, qui peuvent être contrôlés par l'ajout d'additifs. La PolyVinylPyrrolidone (PVP) est un additif polymérique notamment utilisé dans l'industrie comme émulsifiant et stabilisant, et est enregistré comme l'additif alimentaire E1201. Il est également utilisé comme inhibiteur de croissance et promoteur de nucléation grâce à sa propriété d'adsorption autour de cristaux organiques (Ozakı et al. 2013; Patel et al. 2015 ; Posteraro et al. 2015). De même, le PolyEthylène Cilycol (PEG) est un additif polymérique utilisé comme promoteur de croissance ou comme enrobant et est enregistré comme l'additif alimentaire E1521. L'effet stérique du PEG est principalement utilisé pour déclencher et permettre la croissance de cristaux de protéines (Внат et al. 1992).

Du PVP 40k sous forme solide et du PEG 400 sous forme liquide ont été utilisés avec succès pour la cristallisation du RDX par SFE. Outre l'extension de la polyvalence du SFE en permettant la cristallisation de composés organiques avec additif polymérique sous forme solide ou liquide, la taille moyenne et la morphologie de particules ont été contrôlés. Le RDX produit avec ajout de PVP a été réduit jusqu'à 160 nm avec une morphologie sphérique; de plus la stabilité dans le temps des tailles et morphologies ainsi que les sensibilités sont améliorées par la présence de PVP. Cette diminution de taille s'explique par la nucléation retardée par la PVP au delà du moment flash du solvant. L'ajout de PEG induit une nucléation très tôt dans des volumes de goutte plus important ainsi qu'un taux de nucléation faible. Les cristaux croissent jusqu'à des tailles micrométriques comparables à celles du RDX commercial mais avec des sensibilités grandement réduites notamment pour la décharge électrostatique.

## Innovations du SFE comme outil de recherche

Au cours de ce projet, de nombreuses améliorations et changements ont été apportés au procédé SFE et ses appareils. Parmi les innovations majeures, se trouve être l'utilisation de plusieurs buses pour étudier la cristallisation par SFE.

L'hexane est un antisolvant parfait du RDX et est thermodynamiquement compatible avec le SFE. Le mélange acétone-hexane présente aussi un azéotrope permettant une température d'évaporation plus basse que les deux solvants purs: la force motrice du SFE réside dans le degré de surchauffe du fluide, ainsi une température d'ébullition plus faible permet d'atteindre plus rapidement


Figure 0.8 - Illustration du principe de cristallisation in situ via multi-buses
un degré de surchauffe élevé. Tous ces avantages sont étudiés en mono buse selon divers ratio solvants/anti solvants; l'abaissement du point d'ébullition et l'augmentation de la sursaturation réduisent effectivement la taille des cristaux de RDX. Dans la continuité, un système multi-buses a été mis en œuvre pour la première fois sur le SFE afin d'augmenter brutalement le degré de sursaturation, quelques instants après le début du spray alors que les gouttes sont dans un état méta-stable. Ce système a été protégé dans l'extension d'un brevet à l'internationale ("Method for producing cocrystals by means of flash evaporation" 2016). Les avantages de passer d'un système de mono buse à plusieurs buses sont nombreux. Ainsi pour des applications industrielles du SFE, l'ajout d'un anti solvent présente l'immense désavantage de réduire la solubilité du composé et donc de réduire la productivité du procédé : le multi-buse permet alors de conserver la haute solubilité du produit dans son solvant de prédilection, mais agir sur le nuage de gouttelettes permet également plus de flexibilité et autorise les réactions chimiques in situ.

De part la pulvérisation de l'anti solvent par une seconde buse, se pose alors la question de savoir dans quel état l'anti solvent arrive : est il gazeux ou liquide sur le nuage de gouttes de la première buse? La cocristallisation est alors étudiée en multi-buses avec des débits contrôlés et des solvants différents. Ce système multi-buse, à débit contrôlé par débitmètres de précision à effet Coriolis avec vanne intégrée, découple alors l'éternel triptyque suivant : solubilité, débit


Figure 0.9 - Diagramme ternaire d'un cocrystal 1 :1 AB
des buses et ratio du cocristal. La co-cristallisation à partir de deux réservoirs et buses différents a été réalisée avec succès pour la première fois au sein du SFE. En revanche, des études complémentaires sont à mener afin de déterminer les diagrammes de solubilité du cocrystal dans l'acétone-héxane.

Toutes ces études préliminaires ont posés les bases d'une étude complète et précise de la cristallisation par SFE et ont débloqué de nouvelles voies de recherche telles que les réactions in situ.

## Liste des publications et communications

## Communications

- Europyro 2015, $41^{\mathrm{e}}$ International Pyrotechnic Seminar (Toulouse).
- $4^{\text {e }}$ ISL Budding Science Colloquium (Saint Louis, 2015).
- European Congress and Exhibition on Advanced Materials and Processes EUROMAT 2015, B1.3 Section Nanocrystallisation (Varsovie).
- Material Weekend Warsaw; un atelier de travail pour doctorant alliant présentations orales et cours.
- Exposant stand DGA à l'Eurosatory 2016, Defence and Security International Exhibition ( 572 exposants de 56 pays, 213 délégations officielles de 94 pays)
- $5^{e}$ ISL Budding Science Colloquium (Saint Louis, 2016).
- Junior EUROMAT 2016 (Lausanne).
- 6e NANOstructures and nanomaterials SElf-Assembly (NanoSEA) (Ciardini Naxos (ME), Italie 2016).
- 1 poster: $3^{e}$ ISL Budding Science Colloquium (2014).


## Publications

- Blas, Lucia, Martin Klaumünzer, Florent Pessina, Silke Braun, and Denis Spitzer. "Nanostructuring of Pure and Composite-Based K6 Formulations with Low Sensitivities." Propellants, Explosives, Pyrotechnics 40, no. 6 (2015) : 938-44.
- Florent Pessina, Fabien Schnell, and Denis Spitzer. "Tunable Continuous Production of RDX from Microns to Nanoscale Using Polymeric Additives." Chemical Engineering Journal 291 (May 1, 2016) : 12-19. doi :10.1016/j.cej.2016.01.083.
- Martin Klaumünzer, Florent Pessina, and Denis Spitzer. "Indicating Inconsistency of Desensitizing High Explosives against Impact through Recrystallisation at the Nanoscale." Journal of Energetic Materials, July 1, 2016, $1-10$. doi :10.1080/07370652.2016.1199610.
- Denis Spitzer, Vincent Pichot, Florent Pessina, Fabien Schnell, Martin Klaumünzer, and Lucia Blas. "Continuous and Reactive Nanocrystallization : New Concepts and Processes for Dual-Use Advances." Comptes Rendus Chimie, July 2016. doi :10.1016/j.crci.2016.06.009.
- Florent Pessina and Denis Spitzer. "The longstanding challenge of the nano crystallization of 1,3,5-trinitroperhydro-1,3,5-triazine (RDX)" Beilstein Journal of Nanotechnology Under Review.


## Formations scientifiques suivies

- Sensibilisation à la pyrotechnie 3PSC17C, Centre de Formation de la Défense (Bourges 2013)
- Advanced Functional Materials and Characterization, CNRS-EWHA Winter School (Strasbourg 2014)
- Nano-OptoMechanics, School in Physics (Strasbourg 2014)


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## Chapter 1

## Explosives and Characterization

### 1.1 Overview

The term "energetic material" encompasses any type of material (composite, polymer, organic...) which can rapidly release energy by a violent reductionoxidation reaction. A stimulus like shock, friction, heat or electrostatic discharge triggers the local reaction; then it propagates through the material creating a reaction front. That decomposition usually produces large amount of gas and heat, and three modes of decompositions can be identified mainly from the velocity of the redox reaction front.

The combustion is the slowest mode of decomposition ( $\mathrm{mm} / \mathrm{s}-\mathrm{m} / \mathrm{s}$ ), and is characterized by the complete oxidation of all intermediate products. The combustion requires so large amounts of oxygen, that oxygen is mainly provided by the environment. Faster than the combustion, the deflagration ( $\mathrm{m} / \mathrm{s}-\mathrm{km} / \mathrm{s}$ ) occurs when the released heat propagates beyond the reaction front and so facilitates the redox reaction. Deflagration can be considered as a form of burning, but in contrast to pure combustion, the phenomena is self-propagating and does not require an external source of oxygen. Supersonic explosions created by high explosives are known as detonations which travel via supersonic shock waves ( $>\mathrm{km} / \mathrm{s}$ ); that wave, and not the thermal front of reaction, propagates the reaction. Transition from one mode to another can happen intentionally or not; without compaction or enough ignition energy, the material may only burn (1,3,5-trinitroperhydro-1,3,5-triazine (RDX) in the C4 composition burns at $2 \mathrm{~cm} / \mathrm{s}$ whereas it detonates at $8.75 \mathrm{~km} / \mathrm{s}$ ), or when accidentally confined, a propellant detonates.

Therefore, depending on their decomposition mode and their pyrotechnic properties, energetic materials can be sorted in three classes: propellants, primary explosives (or initiating explosives) and secondary explosives (or base
charge). Materials such as Ammonium Nitrate (AN) or Ammonium Perchlorate (AP) are sometimes classified as tertiary explosives, which are even less sensitive and energetic. From a chemical point of view, explosives are intrinsic energetic materials in which usually nitro or nitramine groups react with the closest carbon available inside the same molecule; on the contrary, thermites are a physical mix of an oxidizer (e.g.: $\mathrm{Fe}_{3} \mathrm{O}_{4}$ ) and a reducing agent (e.g.: Al) (Comet et al. 2016).

Used in gunpowder, solid-fuel rockets and mining industry, propellants are deflagrating explosives with the specificity of producing high amount of gases, usually to get a thrust. Primary explosives detonates through the influence of a moderate external stimulus; less sensitive detonative ones are called secondary explosives. The initiation of secondary explosives generally requires the shock wave energy from a primary explosive: such succession of explosive event is called explosive train involved in detonators for instance. All explosives having a higher sensitivity than pentaerythritol tetranitrate (PETN) can be considered as primary, and the less sensitive ones as secondary explosives. The sensitivity to impact and friction of PETN is $3 \mathrm{~J}-4 \mathrm{~J}$ and 60 N , respectively. The notion of sensitivity for energetic materials is discussed in Section 1.3.2.

### 1.2 Organic Secondary Explosives

This work was focused on a very few organic explosives, in order to carefully study the crystallisation parameters independently from the chemical compound. The first one, RDX, is widely used in civilian and military applications, and serves as a reference energetic material in scientific studies. Both octahydro-1,3,5,7-tetra-nitro-1,3,5,7-tetrazocine (HMX) and 2,4,6,8,10,12-hexanitro-2,4,6,8,10,12-hexaazaisowurtzitane (CL-20) are studied here due to their ability to cocrystallise; a cocrystal is simply a multicomponent molecular crystal, owning a unique crystalline structure with each compound included in the unit cell. The following short overview presents their structural characteristics and their physical and pyrotechnical properties.

### 1.2.1 1,3,5-trinitroperhydro-1,3,5-triazine (RDX)

The 1,3,5-trinitroperhydro-1,3,5-triazine is also found under the following denominations cyclo-1,3,5-trimethylene-2,4,6-trinitramine, 1,3,5-trinitrohexahydro--s-triazine, cyclotrimethylenetrinitramine, hexahydro-1,3,5-trinitro-s-triazine, trimethylenetrinitramine, T 4, cyclonite, hexogene, and RDX. The most common and widely accepted one is the acronym RDX whose origin is surprisingly not known for sure; probably from its first secret code "Research Department

(a) Molecule of RDX with thermal ellipsoids drawn at $50 \%$ probability level (Hakey et al. 2008)

(b) Crystallographic cell of $\alpha-\mathrm{RDX}$

Figure 1.1 - RDX visual representations. H atoms have been omitted for clarity.

Explosive". RDX is probably the most important high-brisance explosive from the Second World War to nowadays.
$\alpha-\mathrm{RDX}$ is the stable form of RDX for all temperatures at 1 atm ; however, at high pressures, several polymorphs of RDX exist and have been recently discovered : $\gamma$-RDX is stable above 3.8 GPa between room temperature and $225^{\circ} \mathrm{C}$, and above that temperature $\beta$-RDX lies from $2.5 \mathrm{C}, \mathrm{Pa}-7 \mathrm{C}, \mathrm{Pa}$ (Hakey et al. 2008). A $\delta$ form has been reported but not resolved (Ciezak et al. 2007), and the dense $\varepsilon-R D X$ formed at 3.6 G . Pa can be recovered at 1 atm at $150 \mathrm{~K}-220 \mathrm{~K}$ (Millar et al. 2010).

RDX is soluble in acetone, dimethylsulfoxide (DMSO), DiMethylFormamide (DMF), N-Methyl-2-pyrrolidone (NMP) etc. (Sitzmann et al. 1973), sparingly soluble in ether and ethanol, almost insoluble in water (16, 35-52 and $123 \mathrm{mg} / \mathrm{L}$ at 5,20 and $40^{\circ} \mathrm{C}$ (Boyer et al. 2007)) and totally insoluble in n-hexane (PANT et al. 2013). Cyclohexanone, nitrobenzene and glycol are solvents at elevated temperatures (Sitzmann et al. 1973).

The RDX used in this work is provided by Eurenco, labelled as M5 and used as is, without further purification; the mean particle size is $6.8 \mu \mathrm{~m}$.


Figure 1.2 - HMX visual representations. H atoms have been omitted for clarity.

### 1.2.2 Octahydro-1,3,5,7-tetranitro-1,3,5,7-tetrazocine (HMX)

The octahydro-1,3,5,7-tetranitro-1,3,5,7-tetrazocine is also found under the following denominations cyclotetramethylene tetranitramine, homocyclonit(e), octogen but is commonly named HMX. HMX was first discovered as a by-product of RDX by the Bachmann process (Bachmann et al. 1949). Therefore, like RDX, the HMX acronym may refers to High Melting eXplosive, Her Majesty's eXplosive, High-velocity Military eXplosive, or High-Molecular-weight RDX. Due the high density of its stable $\beta$ phase, its high melting point and its detonation performances, the HMX is a prime secondary explosive. HMX exhibits three distinct polymorphic forms $-\alpha\left(105^{\circ} \mathrm{C}-160^{\circ} \mathrm{C}\right), \beta$ and $\delta\left(160^{\circ} \mathrm{C}-\mathrm{m} . \mathrm{p}\right.$. $)$ - and a $\gamma$ hydrated form metastable existing at all temperatures at 1 atm .

HMX solubilities are even worst when compared to RDX; HMX is soluble in DMSO but not in DMF nor NMP, and is slightly soluble in acetone ( $2.8 \mathrm{wt} \%$ at Standard Ambient Temperature and Pressure as a temperature of 298.15 K and an absolute pressure of 100 kPa (1 bar) (SATP)).

### 1.2.3 2,4,6,8,10,12-hexanitro-2,4,6,8,10,12-hexaazaisowurtzitane (CL-20)


(a) Molecule of CL-20 with thermal ellipsoids drawn at $50 \%$ probability level at 20 K (Meents et al. 2008)

(b) Crystallographic cell of $\varepsilon$-CL-20

Figure 1.3 - CL-20 visual representations. H atoms have been omitted for clarity.
2,4,6,8,10,12-Hexanitro-2,4,6,8,10,12-hexaazaisowurtzitane is also found under the following denominations hexanitrohexaazaisowurtzitan(e), 2,4,6,8,10,12-(hexa-nitro-hexaaza)-tetracyclododecane, HNIW or CL-20. CL-20 is the most widely used acronym and comes from the Naval Air Weapons Station (NAWS) China Lake facility where it was first produced by Nielsen (1997). CL-20 can be considered as a potent explosive due to its high density and high detonation velocities, but the difficult detection of the decomposition gas and the high oxygen balance place the CL-20 as a remarkable propellant too.

CL-20 exhibits also a high degree of polymorphism: four forms $(\alpha, \beta, \gamma, \varepsilon)$ have been observed at SATP conditions (Foltz et al. 1994; Russell et al. 1993) and two $(\delta, \zeta)$ under pressure. The $\zeta-C L-20$ comes from the $\gamma \rightarrow \zeta$ transition at 0.7 GPa . The stability of different phases can be sorted as $\varepsilon>\gamma>\alpha>\beta$ and is schematically described in Figure 1.4a p. 36. However, the hydration of CL-20 plays an important role at intermediate pressures and temperatures in the stability of the $\alpha$ form as described in Figure 1.4b p. 36.

The solubility of $\varepsilon$-CL-20 is good at SATP in acetone ( $100 \mathrm{wt} \%$ ), ethyl acetate ( $45 \mathrm{wt} \%$ ) and tetrahydrofuran (THF) but slight in aromatic or organochloride
solvents (von Holtz et al. 1994). The $\varepsilon-C L-20$ is the phase of interest due the highest density ( $\left.\rho_{\varepsilon}=2.04>\rho_{\beta}=1.98>\rho_{\alpha}=1.97>\rho_{\nu}=1.92 \mathrm{~g} / \mathrm{cm}^{3}\right)$ and the highest detonation velocity ( $v_{\varepsilon}=9660>v_{\beta}=9380 \mathrm{~m} / \mathrm{s}$ (Dumas 2003)).


Figure 1.4 - CL-20 polymorphism adapted from Foltz et al. (1994).

### 1.2.4 Cocrystal CL-20:HMX 2:1

Bolton et al. (2012) first reported the crystallisation and characterization of the cocrystal CL-20:HMX with a molar ratio of 2:1. An impact sensitivity as low as $\beta-\mathrm{HMX}$ was measured while a higher detonation velocity than $\beta-\mathrm{HMX}$ was predicted. Those results are representative of the advantage of crystallisation as a solid state engineering strategy for improved energetic material. This approach is well know for pharmaceutical compounds (Fleischman et al. 2003; Schultheiss et al. 2011; Vishweshwar et al. 2006) and is also emergent for optic (Sun et al. 2006; Yan et al. 2011) and semiconductors (Sato et al. 2012).

### 1.3 Analytical Methods

### 1.3.1 Classic Material Characterization Methods

X-Ray Difraction (XRD) The periodicity of a crystal can be investigated by using a X-ray beam. In X-Ray Difraction (XRD), the incident beam penetrates through the matter within several hundreds of microns; the photons interact

| Characteristics | $\alpha-R D X$ | $\beta$-HMX | ع-CL-20 |
| :---: | :---: | :---: | :---: |
| Colour | colourless | colourless | colourless |
| Molecular formula | $\mathrm{C}_{3} \mathrm{H}_{6} \mathrm{~N}_{6} \mathrm{O}_{6}$ | $\mathrm{C}_{4} \mathrm{H}_{8} \mathrm{~N}_{8} \mathrm{O}_{8}$ | $\mathrm{C}_{6} \mathrm{H}_{6} \mathrm{~N}_{12} \mathrm{O}_{12}$ |
| Molecular weight | 222.1 | 296.2 | 438.19 |
| Space Group | Pbca | P2/lc | P2//c |
| CCDC IDs | $\begin{gathered} \hline \text { CTMTNA, 03, } \\ 08-12 \end{gathered}$ | NA | $\begin{gathered} \hline \text { PUBMUU 02, } 05, \\ 12-22 \end{gathered}$ |
| COD IDs | $\begin{gathered} 5000148, \\ 2019354-9, \\ 2219089 \end{gathered}$ | 4110146 | 2300020-4 |
| Stability range at 1 atm | RT to 222.1 | RT to $102-150^{\circ} \mathrm{C}$ | RT to $56.5^{\circ} \mathrm{C}$ |
| Energy of formation | $+401.8 \mathrm{~kJ} / \mathrm{kg}$ | +353.6 kJ/kg | +1005.3 kJ/kg |
| Enthalpy of formation | $+301.4 \mathrm{~kJ} / \mathrm{kg}$ | +253.3 kJ/kg | +920.5 kJ/kg |
| Oxygen balance | -21.6\% | -21.6\% | -10.95\% |
| Nitrogen content | 37.84\% | 37.83\% | 38.3\% |
| Volume of explosion gases | 903 l/kg | 902 l/kg | NA |
| Heat of explosion ( $\mathrm{H}_{2} \mathrm{O}$ liq.) | $5647 \mathrm{~kJ} / \mathrm{kg}$ | $5249 \mathrm{~kJ} / \mathrm{kg}$ | $6314 \mathrm{~kJ} / \mathrm{kg}$ |
| Heat of explosion ( $\mathrm{H}_{2} \mathrm{O}$ gas) | 5297 kJ/kg | $5599 \mathrm{~kJ} / \mathrm{kg}$ | $6084 \mathrm{~kJ} / \mathrm{kg}$ |
| Heat of detonation ( $\mathrm{H}_{2} \mathrm{O}$ liq.) | $6322 \mathrm{~kJ} / \mathrm{kg}$ | $6197 \mathrm{~kJ} / \mathrm{kg}$ | $N A$ |
| Specific energy | $1375 \mathrm{~kJ} / \mathrm{kg}$ | $1367 \mathrm{~kJ} / \mathrm{kg}$ | $1323 \mathrm{~kJ} / \mathrm{kg}$ |
| Density | $1.82 \mathrm{~g} / \mathrm{cm} 3$ | $1.91 \mathrm{~g} / \mathrm{cm} 3$ | $2.04 \mathrm{~g} / \mathrm{cm} 3$ |
| Melting point | $204{ }^{\circ} \mathrm{C}$ | $280{ }^{\circ} \mathrm{C}$ | $\begin{gathered} >195^{\circ} \mathrm{C} \\ \text { (decomposition) } \end{gathered}$ |
| Detonation velocity, confined | $8750 \mathrm{~m} / \mathrm{s} \text { at } 1.76$ g/cm3 | $9100 \mathrm{~m} / \mathrm{s}$ at 1.9 $\mathrm{g} / \mathrm{cm}^{3}$ | $\begin{aligned} & 9660 \mathrm{~m} / \mathrm{s} \text { (Dumas } \\ & \text { 2003) } \end{aligned}$ |
| Impact sensitivity | 7.4 N.m | 7.4 N.m | 4 N.m |
| Friction sensitivity | 120 N | 120 N | 48 N |

Table 1.1 - Characteristics of the most common crystalline forms of RDX (Krause 2005; Meyer et al. 2008; Miller et al. 2001), HMX (Krause 2005; Meyer et al. 2008; Miller et al. 2001) and CL-20 (Krause 2005; Meents et al. 2008; Meyer et al. 2008; Nair et al. 2005)

(a) Layers of CL-20 in yellow and HMX in blue in the co-crystal from CL-20 and HMX (CL-20:HMX) 2:1

(b) Crystallographic cell of CL-20:HMX

Figure 1.5 - CL-20:HMX visual representations (Bolton et al. 2012). H atoms have been omitted for clarity.
with the electrons of the material which oscillate at the same frequency and scatter the electromagnetic waves. Waves scattered from different points in space travel different paths and consequently exhibit a phase shift, therefore causing destructive interferences. The detectable X-ray emissions in a crystalline sample come from the resonance of ordered atoms in the crystallographic cell at a specific angles. The Bragg's law determines those specific directions where the interferences are constructive: $2 d \sin \theta=n \lambda$ where $d$ is the spacing between diffracting planes, $\theta$ the incident angle, $n$ an integer, and $\lambda$ the wavelength of the incident beam. The rotation of both the emitter and detector allows the recording of the diffracted signal depending on the angle $\theta$ in a unique diffractogram. The powder diffraction pattern provides various information of the crystalline structure as summarized in Figure 1.6 p. 39.

Powder X-Ray Diffraction was obtained on a D8 Advance (Bruker), with a LynxEye detector and a copper source with no filtering of the second wavelength. Please note that hkl indexes mentioned in this work are made according to the standardization of the IUCr ; so previous publications mentioning abc indices are quoted here as cab. Figure 5.7 p. 155 and crystallographic studies have been made using the open-source software VESTA (Momma et al. 2011).


Figure 1.6 - Diagram highlighting the information available from the interpretation of an XRD pattern (Dinnebier 2001).

Scanning Electron Microscopy (SEM) allows the direct imaging of a sample at micron or nano scale with a focused beam of electrons. When interacting with the sample, both photons and electrons are emitted giving various information from the sample: X-rays for thickness and also qualitative and quantitative chemical information, secondary electrons for topology, Auger electrons for chemical information, catholuminescence for electrical information and primary backscattered electrons to determine the atomic number and the topography. Secondary electron detector and back-scattered detector are standard equipments for a Scanning Electron Microscopy (SEM). To avoid noisy interactions with gaseous molecules, the imaging occurs under vacuum. For conventional imaging in the SEM, the sample's surface must be electrically conductive and electrically grounded to prevent any accumulation of electrostatic charges.

Sizes measurements were made manually over at least one thousand particles per sample within the software Giwyddion (Nečas et al. 2012) then a log-normal fit was applied on the particles size distribution (PSD): geometrical mean and multiplicative standard deviation (dimensionless) (Limpert et al. 2001) are reported here and written as "mean(SD) unit". Gaussian fitting is in poor accordance; droplets size distributions of aerosols usually have a log-normal shape (Zender 2008) and colloids can be found also to follow a log-normal
distribution (Limpert et al. 2001).
Brunauer-Emmett-Teller theory (BET) Brunauer-Emmett-Teller theory (BET) theory explains the multilayer adsorption of gas molecules on solids. The BET apparatus measures the amount of gas adsorbed across a wide range of relative pressures at liquid nitrogen temperature ( 77 K ) and applies the BET theory to calculate the specific surface area, the pore size distribution and the pore volume. The adsorption and desorption isotherms also return some information about the type of porosity of the sample. Decreasing the molecular size of the adsorbed gas used - for instance from nitrogen to krypton- increases the precision but limits the measurement to lower surface area ( $\sim 1 \mathrm{~m}^{2} / \mathrm{g}$ for krypton).

Atomic Force Microscopy (AFM) The development of nano-technology started with the invention of the STM and quickly followed by the Atomic Force Microscopy (AFM) in the early 80's at the IBM Zurich Research Laboratory (Binnig et al. 1986, 1983, 1982). Specifically, AFM allows the visualization at the atomic scale of non-conductive samples by a vibrating cantilever with a tip at its end. When the tip is interacting with the surface of the sample (Van der Waals forces, dipole-dipole interactions, electrostatic forces, etc.), the amplitude of the cantilever oscillation decreases. Therefore, this change is used to detect the proximity of the surface: the altitude of the cantilever is regulated to keep a constant amplitude oscillation thus to give the topographic image of the sample surface. This mode of acquisition is called tapping mode and the phase of the cantilever oscillation is also recorded. Phase changes occur when heat is dissipated by the cantilever, allowing the detection of variation in hardness or adhesive properties.

Dynamic Light Scaterring (DLS) When a light source passes through a colloid, particles with a size smaller than the wavelength scatters the light in all direction. Just as in XRD, the diffraction comes from different positions in space and exhibits constructive or destructive interferences. Due to the Brownian motion, the optical path length is constantly changing in time, so the resulting noisy diffracted pattern changes in time and with the size of the particles. The intensity fluctuations from this motion, namely the computed intensity correlation function, is analysed to provide the diffusion coefficient of the particles. Then an hydrodynamic radius is calculated from the Stokes-Einstein equation

$$
\begin{equation*}
D=\frac{k_{B} T}{6 \pi \eta r} \tag{1.1}
\end{equation*}
$$

where $\eta$ is the dynamic viscosity, $r$ the radius of the assumed spherical particle, $k_{B}$ the Boltzmann's constant, and T the absolute temperature.


Figure 1.7 - DSC peak analysed from Höhne et al. (2003): (1) baseline (interpolated), (2) auxiliary lines, $T_{i}$ initial peak temperature, $T_{e}$ extrapolated peak onset temperature, $T_{p}$ peak maximum temperature, $T_{c}$ extrapolated peak offset temperature, $T_{f}$ final peak temperature.

Differential Scanning Calorimetry (DSC) Differential Scanning Calorimeters measure the change of the differential heat flow rate between the sample and the reference while regulating the temperature. A few milligrams of the sample are placed in a hermetically closed gold crucible. An identical empty pan is used as reference. The rate of heating heavily influences the peak shapes and resolutions; keeping a small rate is of interest to separate peaks, especially for energetic materials having the melting point close to their decomposition (e.g. RDX), but too small rate will result in broad peaks of small intensities overlapping each others. So the position of the peak maximum changes with the heating rate but also with the thermal conductance and the mass of the sample. Only the extrapolated peak onset temperature is relatively independent of experimental parameters (Höhne et al. 2003).

Differential Scanning Calorimetry (DSC) was performed with a Q-1000 DSC, from TA instruments, under $N_{2}$ flow of $50 \mathrm{ml} / \mathrm{min}$ at $2^{\circ} \mathrm{C} / \mathrm{min}$; the low thermal ramp is a compromise between peak separation and intensity. Extrapolated temperatures were obtained using the tangent technique as described by Höhne
et al. (2003) in Figure 1.7. The exothermic energy released by the decomposition is calculated from the integration of the heat flow over the temperature range of the peak.

Infrared (IR) Spectroscopy Bonded atoms in molecules are in motion between each other; each motion is periodic with a unique frequency and different modes of molecular vibration can be distinguished such as stretching and bending. When a molecule is hit by a radiation having the same energy of the transition energy of a vibration -the resonant frequency-, that radiation is absorbed. Since the related wavelengths are in the middle-infrared, between 10 et 4000 $\mathrm{cm}^{-1}$, the technique is named infrared spectroscopy (IR). The energy from the resonant frequency depends on the molecular potential energy surfaces, the masses of the atoms involved and the associated vibronic coupling, therefore allowing the identification of the chemical groups of the compounds and their interactions. However, the transition has to change the dipole moment of the molecule to be "IR active", unlike the stretching of C-C bond in ethane for instance. Furthermore, the greater the dipole is, the greater the absorbance intensity will be. The method used to measure infrared absorption and emission spectra is the Fourier Transform Infrared Spectroscopy (FTIR); the instrument uses a Michelson interferometer coupled with a Fourier transformation of the interferogram in order to obtain the final spectrum.

Nuclear Magnetic Resonance (NMR) Spectroscopy NMR occurs when the nucleus of certain atoms is placed in a static magnetic field and an additional oscillating magnetic field. Only some atoms can exhibit NMR: nuclei possessing a not null spin, more usually a spin of $1 / 2$ such as in ${ }^{1} \mathrm{H},{ }^{13} \mathrm{C},{ }^{19} \mathrm{~F}$ and ${ }^{31} \mathrm{P}$. Schematically, the transition between the two possible energy states of such nuclei is triggered when the frequency of the oscillating magnetic field matches that transition energy: such frequencies are typically in the radio frequency range for magnetic fields or around 20 T . NMR spectroscopy detects and records that magnetic resonant absorption.

### 1.3.2 Explosive Specific Characterization Techniques

The determination of the sensitivity of an explosive is the prime set of characterizations. Not surprisingly, pyrotechnic scientists put safety first, especially when it comes to explore new materials based on the most devastating explosives. Various methods of evaluation exist depending on the stimuli, the mass of the studied material and the application. At the small scale of a laboratory, only
three techniques are of interest based on the three main stimuli: impact, friction and electrostatic discharge.

(a) Julius Peters Bundesanstalt für Materialprüfung (BAM) FallHammer for impact test

(b) Julius Peters BAM Machine for friction test

(c) OZM Research Electrostatic Discharge (ESD) 2008 apparatus

Figure 1.8 - Apparatuses for testing the mechanical and electric sensitivity at small scale, in use at NS3E.


Figure 1.9 - Sample holder for BAM Fall-Hammer (Meyer et al. 2008).
Impact The small scale drop-hammer impact sensitivity test is described in the international guidelines of the UNECE (test code 3(a)(ii) (UN Manual of

Tests and Criteria 2016)) and in the French norm NFT 70-500. Historically the fall-hammer method was modified by the German BAM, in order to obtain better reproducible values (Meyer et al. 2008). A cylindrical spoon measures $40 \mathrm{~mm}^{3}$ of energetic material which is placed between two cylindrical pistons maintained by a ring (Figure 1.9 on the left). Those cylinders and rings are constituting the sample holder and are made of steel with controlled hardness, dimensions, surface roughness and flatness; they are renewed for each falling test procedure. If the sample is a powder or a paste, the upper cylinder is slightly pressed into the charged confinement device. The sample holder is set below a vertical rail guiding a free movable weight (Figure 1.8a p. 43). Two masses of 1 and 5 kg are available, falling from a height of 15 cm to 100 cm , allowing the measurements over a range of energy from 1.56 J to 50 J . The energy is simply calculated from the gravitational potential energy $e=m g h$.


Figure 1.10 - Schematic principle of the BAM friction sensitivity test.

Friction The small scale sensitivity BAM test is described in the international guidelines of the UNECE (test code 3(b)(i) (UN Manual of Tests and Criteria 2016)) and in the French norm NF T70-503. Again, a cylindrical spoon measures about $10 \mathrm{~mm}^{3}$ of energetic material which is placed on the surface of a roughened $25 \mathrm{~mm} \times 25 \mathrm{~mm} \times 5 \mathrm{~mm}$ porcelain plate. Then, on top of this plate is maintained a cylindrical porcelain peg ( 10 mm in diameter for a height of 15 mm ), having a roughened spherical end (Figure 1.10). This peg is fasten on a rod which can be moved up and down. The pressure applied on the sample by the peg is set by a weight at the end of the lever: the nine different weights and six different mounting positions on the arm allows a measurement range from 5 N to 360 N .

Electrostatic Discharge (ESD) The sensitivity towards electrostatic discharge is a recent technique: for instance, the electrostatic stimuli are not investigated in the Manual of Tests and Criteria on the transport of dangerous goods of the UNECE (UN Manual of Tests and Criteria 2016). OZM Research manufactures the ESD 2008A tester used in several European laboratories. The sample is placed inside a small sacrificial plastic ring on top of the ground electrode; the volume of material is $7 \mathrm{~mm}^{3}$. The electrostatic discharge is delivered from the top
by the main electrode; see Figure 1.11 on the left. The apparatus has several capacitors and also a potentiometer to change the tension; the energy delivered through the sample is simply $E=\frac{1}{2} C U^{2}$, where $U$ is the tension in Volt and $C$ the capacity in Farad.


Figure 1.11 - Schematic principle of the OZM ESD 2008A tester.

Data Interpretation and Evaluation To define the reaction of a small scale sensitivity such as those mentioned above, the operator should carefully watch for any smokes, odour, sparking, popping noises, scorch marks etc. An instrumented version of the BAM fallhammer called BIC records the overpressure and the lightening with four fibre optic detectors (Coffey et al. 1995). For instance, at the friction test, a simple odour is not significant enough to mark the event as a success full ignition, namely a Cio event.

The highest stimulus level at which a predetermined number of No-Go events are observed without any Go occurring is the Threshold Initiation Level (TIL) value. For small scale (several grams) of energetic material, the predetermined number is often 6, although 10 or 20 can be used to increase the accuracy of the TIL level for hundred of grams. However, the TIL value does not refer to a zero probability of reaction. Wild and Von Collani extensively studied the statistical description of the reactivity of energetic materials; they demonstrated that the Bruceton method, which is still in use in other notEuropean laboratories, is lacking of accuracy and is not scientifically justified. In addition, they clearly showed that their Weibull model can discriminate and explain the sensitivity differences between coarse and fine samples (Wild et al. 2002a,b).

### 1.4 Submicron and nano explosives

In the past years, the outstanding properties of new nano-materials led the research in energetic materials to embrace this trend. The nano-structuring of classical explosives should enhance their properties and safety. Even if the term "nano" strictly refers to an object with at least one dimension under 100 nm , in this work on energetic material, the term "nano" will refer to nano and submicron-sized particles for the sake of readability, just like n-RDX is an abbreviation for nano or submicron particles of RDX. However, mean particle sizes are always given when available.

### 1.4.1 Properties and Challenges

The development of new energetic materials led to new synthesized molecules such as 1,3,3-trinitroazetidine (TNAZ), CL-20, Octanitrocubane (ONC), 1,1-di-amino-2,2-dinitroethene (FOX-7), Ammonium DiNitramide (ADN) etc. Those newly available materials aim to achieve higher density, increase the processability and attain Insensitive Munitions (IM) characteristics; IM properties actually rely on the whole physic-chemistry of the system. Therefore, the development of powders with controlled particle sizes and morphologies and a well defined surface chemistry, is a whole new facet of the energetic materials largely unexplored at the submicron scale and below. Criteria that are advantageous for new energetic materials include the following:

- high decomposition temperature
- Low sensitivities
- no phase transitions under compression or depression
- no autocatalytic decomposition
- no voids from solvents or gas
- mechanical behaviour independent from temperature
- good ratio availability/cost
- easy processing

Compression of gaseous inclusions, cavities and voids, deformation, frictional heating, inter-crystalline shearing and spark discharges are initiation processes which can cause areas of an energetic material to warm up to several hundred Kelvin: these areas are called hot-spots and are deflagration or detonation origins if they reach a critical temperature. Tarver (Tarver et al. 1996) calculated for HMX the critical temperature of different sized hot-spots. For a $2 \mu \mathrm{~m}$ sized hot-spot he calculated a critical temperature of 985 K , whereas the critical temperature for a $0.2 \mu \mathrm{~m}$ sized hotspot already rises to 1162 K .

Risse (Doctoral Thesis 2012) measured a noticeable desensitization towards initiation by friction and electrostatic discharge for n-RDX crystallised by Spray Flash Evaporation (SFE), compared to the raw material (Table 1.2, p. 47). The noticeably lower sensitivity towards friction can be based on the self-lubricating effect, as small particles will tend to occupy small interstices instead of breaking. Sensitivity measurements were also performed on Hexolite, which showed a clear desensitization of the nano-structured explosive (Table 1.3, p. 47).

| RDX | Impact <br> $[J]$ | Friction <br> $[\mathrm{N}]$ | ESD <br> $[\mathrm{mJ}]$ |
| :---: | :---: | :---: | :---: |
| M5 (raw material) | $>3.52$ | 160 | 120 |
| nano-structured | $>3.52$ | $>360$ | 270 |

Table 1.2 - Sensitivity towards impact, friction and ESD of micron-sized and nanostructured RDX (Doctoral Thesis Risse 2012).

| Hexolite | Impact <br> $[J]$ | Friction <br> $[\mathrm{N}]$ | ESD <br> $[\mathrm{mJ}]$ |
| :---: | :---: | :---: | :---: |
| micro | 6 | 54 | 353,6 |
| nano | 25,06 | 72 | 436,6 |

Table 1.3 - Comparison of the sensitivity levels of micro Hexolite with those of a nano-sized Hexolite (Doctoral Thesis Risse 2012).

Using a sonocrystallisation process, Bayat and Zeynali (Bayat et al. 2011) succeeded in the preparation of $n-C L-20$ which was less sensitive towards friction, impact and electrostatic discharge (Table 1.4, p. 47).

| Particle size <br> $[\mu \mathrm{m}]$ | Impact <br> $[\mathrm{cm}]$ | Friction <br> $[\mathrm{kg}]$ | ESD <br> $[\mathrm{J}]$ |
| :---: | :---: | :---: | :---: |
| 15 | 25 | 6,4 | 45 |
| 0,095 | 55 | No reaction | 60 |

Table 1.4 - Comparison of the sensitivity levels of micro and nano CL-20 (Bayat et al. 2011).

Fathollahi et al. (2007) have studied the particle size effects on thermal decomposition on HMX: as the particle was getting smaller, temperature and the activation energy were decreasing.

However those trends are not always observed. Crystallised from Rapid Expansion of Supercritical Solutions (RESS), several nano RDX lots have been tested by (Stepanov et al. 2011); if both 500 nm and 200 nm RDX are less sensitive toward impact than milled $4 \mu \mathrm{~m}$ RDX, the 200 nm lot is substantially more sensitive than the 500 nm one. As it can be seen in Figure 1.12 p. 48 that minimum of sensitivity to impact is confirmed when coating the powders with a
binder; however that confirmation might reveal that the trend is more due to the intrinsic bulk properties of the particles instead of their surface.


Figure 1.12 - Sensitivities of RDX with various Particle Size Distribution (PSD) (Stepanov et al. 2011).

Beside safety, other improvements can emerge from the nano scale; critical diameter, tunable detonation velocity, delay before the detonation steady state etc. may be improved by the drastic grain size reduction. Energetic nanocomposites are also promising materials improved by a more intimate mixing. Liu Jie et al. (Liu et al. 2014) show that detonation velocities of PBX composition from their milled n-RDX and n-HMX are slightly better while being significantly safer. The burning rates of nitrocellulose was also improved by Zhang et al. (2014) due to the formation of submicron spheres. Recently, Comet et al. (2015) proved that energetic nanocomposites can easily replace the hazardous primary explosives to initiate a secondary explosive: $500 \mathrm{~nm} n-R D X$ from SFE were mixed with a nano thermite to initiate the detonation of PETN. The Flame Propagation Velocity (FPV) of composites made of $\mathrm{n}-\mathrm{WO}_{3} / \mathrm{n}-\mathrm{Al} / \mathrm{n}-\mathrm{RDX}$ can be tuned from $0.2 \mathrm{~km} / \mathrm{s}$ to $3.5 \mathrm{~km} / \mathrm{s}$ through their explosive content; in the same conditions, $\mathrm{n}-\mathrm{WO}_{3} / \mathrm{n}-\mathrm{Al}$ with $\mu$-RDX exhibit unstable regimes from $187 \mathrm{~m} / \mathrm{s}$ to $733 \mathrm{~m} / \mathrm{s}$, whereas the $\mathrm{n}-\mathrm{WO}_{3} / \mathrm{n}-\mathrm{Al} / \mathrm{n}-\mathrm{RDX}$ composite deflagrates at a constant velocity of $2529 \mathrm{~m} / \mathrm{s}$. Those results and other unpublished ones of our laboratory confirm the drastic reduction of the critical diameter with the decrease of particle size.

### 1.4.2 Challenges of the characterization of energetic materials

Some of the characterization techniques previously described in Section 1.3.1 p. 36 are difficult to apply on nano energetic material, due to their sensitivity toward heat, or toward vacuum, or their organic nature. Molecular solids are by their nature called soft matter, due to the type of bonds involved to create their crystalline structure: the dipole forces holding the molecules together are weaker than the covalent bonds in metals or the ionic bonds in ionic crystals.

XRD Solid organic explosives are molecular crystals: the crystallographic positions are occupied by the molecule and not just a single atom. XRD diffraction of molecular crystals produces much more reflections -up to thousands- for the very complex protein crystals. For instance in Figure 1.13, the XRD pattern of $\mathrm{CL}-20$ exhibits much more diffraction lines than the magnetite $F e_{2} \mathrm{O}_{3}$. Moreover,

(a) CL-20 diffraction pattern from Meents et
al. (Meents et al. 2008).

(b) magnetite diffration pattern from WH. Bragg (Bragg 1915).

Figure 1.13 - Examples of computer generated XRD patterns, both with the same broadening.
at the nano scale, the diffraction peaks are broadened. Line broadening in diffraction stems from instrumental and physical broadening; the latter is due to size effect and internal strain inside the lattice. Young and Desai (Young et al. 1989) described size broadening $\beta_{\text {size }}$ as a Gaussian contribution of the Scherrer's equation:

$$
\begin{equation*}
\beta_{\text {size }}=\frac{\lambda K D_{V}}{\cos (\theta)} \tag{1.2}
\end{equation*}
$$

where $K$ is the shape factor and $D_{V}$ the apparent volume weighted domain size. Stokes and Wilson (Stokes et al. 1944) defined the maximum strain definition as a dependency of the broadening:

$$
\begin{equation*}
\varepsilon=\frac{\beta_{\operatorname{strain}}}{4 \tan (\theta)} \tag{1.3}
\end{equation*}
$$

Therefore, the broadening from the material is simply:

$$
\begin{align*}
\beta_{\text {observed }}-\beta_{\text {instrumental }} & =\beta_{\text {strain }}+\beta_{\text {size }} \\
& =4 \varepsilon \tan (\theta)+\frac{\lambda K D_{V}}{\cos (\theta)}  \tag{1.4}\\
\Leftrightarrow \beta_{\text {strain }} \cos (\theta) & =4 \varepsilon \sin (\theta)+\lambda K D_{V}
\end{align*}
$$

Plotting $\beta \cos (\theta)$ as a function of $\sin (\theta)$ should give an affine function where the slope is directly related to the strain: they are known as Williamson-Hall plot. However, it requires to index and fit several reflection peak. Therefore, XRD patterns were also analysed by the Full Pattern Matching (FPM) method using the software Fullprof. The peaks shape was fitted with a Thompson-Cox-Hastings pseudo-Voigt convoluted with axial divergence asymmetry function (Finger et al. 1994). When compared to mathematical fitting features in data analysis software, the FPM technique as implemented in many XRD analysis software has the great advantage to take into account the specificity of XRD patterns, such as complex shape functions and the existence of the $K_{\alpha 2}$ radiation. Indexing many peaks by FPM gives a wider understanding of the material and increase the precision of the strain extracted of the Williamson-Hall plots. However, Williamson-Hall plot were found to be not always linear thus were not used afterwards. The assumptions leading to the Scherrer's equation and the final Equation (1.4) are not satisfied. That's why the accurate and complex Rietveld refinement method with size-broadening refinement for apparent crystallites morphology based on a spherical-harmonics representation (Balzar et al. 2005; Popa 1998; Popa et al. 2008) calibrated with $\mathrm{LaB}_{6}$ as implemented in Fullprof was used.

SEM Organic explosives are sensitive towards heat and their submicron-sized emphasizes even more that discrepancy due to a higher surface/volume ratio; under vacuum, that heat from the electron beam can not be transferred to the surrounding of the surface. The gold coating is accordingly increased to approximatively 10 nm to increment the heat transfer from the material to the sample holder. The energy from the beam can also be tuned to reduce the degradation of the sample. However, electrons has to interact with the sample surface in order to have enough contrast and so spatial resolution. Due to the low density of organic molecular crystals, the effective tension required is usually high, around 15 kV at working distances around 5 mm . The stabilization with gold deposit improves the imaging of n-RDX allowing magnifications up to 10.000x. Further magnifications alter the material and do not allow a complete and correct data acquisition.

The damages of the electron beam on sensitive organic samples can be avoided or diminished by working at higher pressures (up to 1 Torr-50 Torr


Figure 1.14 - High vacuum SEM imaging on a n-RDX pressed pellet coated with gold.
instead of $1 \times 10^{-5}$ Torr to $1 \times 10^{-7}$ Torr) with adjustable relative humidity up to $100 \%$. An Environmental Scanning Electron Microscopy (ESEM) FEG FEI XL30 was tested at the CLYM laboratory (Lyon, France) showing encouraging results about the increased stabilization at 2 Torr. As it can be seen in Figure 1.15, n-RDX without any coating exhibits at 2 Torr much more contrast compared to classical SEM with gold deposit.


Figure 1.15 - Comparison between high vacuum SEM imaging and at 2 Torr from ESEM on the same n-RDX sample

BET Prior to the measurement by gas injection, adsorbed water or organic gas have to be removed. This can be done by heating under vacuum or under a flow of dry, inert gas. The quality of the degassing influences directly the accuracy of the surface area calculated. As previously depicted, nano energetic materials are sensitive to heat and to vacuum, thus it can be expected to degrade them at the degassing step.

While using Krypton to gain in accuracy and access to smaller pores, BET results in Table 1.5 demonstrate the inaccuracy of BET measurements on n-RDX. At $100^{\circ} \mathrm{C}$ the mass loss is almost one magnitude higher which may indicate a good degassing, but the specific surface area is decreasing leading us to the conclusion that the powder is starting to be affected by sintering.

| degassing | mass loss | $S_{B E T}$ | extrapolated diameter |
| :---: | :---: | :---: | :---: |
| $\begin{gathered} \nearrow 2^{\circ} \mathrm{C} / \mathrm{min}- \\ 50^{\circ} \mathrm{C} 10 \mathrm{~min}- \\ \pi 1^{\circ} \mathrm{C} / \mathrm{min}- \\ 80^{\circ} \mathrm{C} 1 \mathrm{~h}- \end{gathered}$ | 0.1\% | 3.28 m/g | $1.0 \mu \mathrm{~m}$ |
| $\begin{gathered} \nearrow 2^{\circ} \mathrm{C} / \mathrm{min}- \\ 50^{\circ} \mathrm{C} 10 \mathrm{~min}- \\ \pi 1^{\circ} \mathrm{C} / \mathrm{min}- \\ 100^{\circ} \mathrm{C} 1 \mathrm{~h}- \end{gathered}$ | 0.8\% | 3.09 m/g | $1.1 \mu \mathrm{~m}$ |

Table 1.5 - BET measurements on n-RDX with Kr

DLS Depending on the anisotropy and polydispersity of the system, the data interpretation may exhibit an angular dependence. For instance, small spherical particles do not have any anisotropy hence no angular dependence; the ideal case of spherical particles is usually not effective and such samples will exhibit an angular dependence. An optimum angle of detection exists for each particle size distribution and particle morphology. For a polydisperse sample and at certain angles, the scattering intensity of some particles will completely overwhelm the weak scattering signal of other particles, thus making them invisible to the data analysis at this angle. Furthermore, even if most of the organic explosives are not soluble in water, nitro and nitramine groups trend to interact strongly; energetic colloids are not stable in water and aggregates easily with quick sedimentation. Experiments have been done using the Zetasizer from Malvern. Even if the addition of PolyVinylPyrrolidone (PVP) enhances the stabilization, no reproducible measurements could have been performed as it can be seen in Figure 1.16.

DSC When gaseous species are reactive towards the decomposing substance, it leads to the autocatalytic acceleration of the reaction rate. Therefore for energetic materials, the assumed constant pressure is not satisfied for closed crucibles; consistent kinetic analysis can be acquired only by effectively removing


Figure 1.16 - All Dynamic Light Scaterring (DLS) results acquired from n-RDX with $5 w t \%$ of PVP: even if this figure contains data with different experimental conditions such as duration of the ultrasonic bath or the dilution, none of the PSD could have been found reliable.
reactive gaseous products. Long et al. (Long et al. 2000) clearly demonstrated that the competition between liquid and gas phase decomposition decreases over time, the activation energy in both pierced and closed pan DSC experiments from $\sim 200 \mathrm{~kJ} / \mathrm{mol}$ to $\sim 140 \mathrm{~kJ} / \mathrm{mol}$, whereas open pan DSC and TGA experiments showed a constant value of $\sim 100 \mathrm{~kJ} / \mathrm{mol}$.

### 1.4.3 Specific health and safety hazards

A wide variety of nano materials is now being produced, including nanoparticles as well as nanofibers, nanowires, and nanosheets, and their range and types are continually expanding. The increase of the nanomaterial uses in every day products makes the human exposure inevitable, thus asking the question of nanotoxicology. To prevent the uncontrolled penetration of foreign substances, the human body has several barriers such as epithelial cells and mucus secretion. While the protective mucus of the lung trap micron-sized particles, nanoparticles are small enough to reach the deep lung and even further the air-blood barrier (Fröhlich et al. 2014). Epidemiological studies showed that exposure of humans to ultrafine particles $(<2.5 \mu \mathrm{~m})$ in the air increased pulmonary morbidity and
mortality. Nanoparticles can also be cleared from the bronchial epithelium and then absorbed in the gastrointestinal tract. However, particles morphology, metric-related characteristics and many other physicochemical properties largely influence their toxicity. For organic particles, the solubility of the compound in its environment is a major issue since unitary molecules can directly disturb the proteins activity. The report of Boyer et al. (2007) written for the SERDP and ESTCP -US Department of Defence's environmental research programs- provides a comprehensive overview of the toxicity of RDX and CL-20. The toxicity of CL-20 for soil invertebrate population is quite high with only 0.02 mg CL-20/kg of soil to damage it significantly, whereas 44 mg RDX/kg soil-660 mg RDX/kg soil is harmless. For fish and aquatic invertebrates, CL-20 may be more toxic than RDX; but CL-20 is substantially less toxic than RDX to plants and birds: as little as 5.8 mg RDX/kg soil caused adverse effects for some plant species, while 10 mg CL-20/kg soil had no effect. Unfortunately, no studies on the toxicity of CL-20 in mammalian species -including humans- have been published. In contrast, the US Environmental Protection Agency (EPA) has established a reference dose (RfD) of 0.003 mg RDX/kg body weight/day for oral exposure based on the results of toxicity studies on rats; RDX has also been classified as possible human carcinogen, based on liver tumours in mice exposed for 2 years to 7 mg RDX/kg body weight per day.

About the pyrotechnic safety, the articles from R.4462-1 to R.4462-36 of the Code du Travail (Labour Code) regulates the practices of any work involving the creation, study, experimentation, control, packaging, storage or destruction of energetic compounds or any object containing pyrotechnic parts. In addition to the Document Unique, a legal document listing all actual potential risks, the employer has to redact a safety study for each pyrotechnic activity, with a validity of five years: the content of this pyrotechnic safety study is regulated by the decree from the 7th of November 2013 (modified in July 2014). The accidental potential modes of degradation of the energetic material has to be identified and their effects on human life determined. A probability of accident is estimated and the area of effect is identified then segmented according to the lethality; additional countermeasures are established to reduce the exposure (probability) and the consequences of an accident. At NS3E, each laboratory room has been evaluated to confine the risk inside it. The quantity of energetic material is also limited according to its stability and equivalence to TNT; in many cases only five grams (TNT equivalent) is allowed to be handled per room. The number of simultaneous workers is also limited while studying energetic material, with usually a maximum of two persons. The compounds processed for the first time by SFE are classified in the most restrictive class until the sensitivity has been determined: therefore, only one gram is recovered with a
conductive strap to avoid electrostatic discharge. In France and for the DoD activities, the Inspecteur de l'armement pour les Poudres et Explosifs (IPE) has the authority to control and delegates experts on pyrotechnic safety: the IPE frequently writes open letters (http://www.defense.gouv.fr/dga/liens/ poudres-et-explosifs/lettre-de-l-ipe/lettre-de-l-ipe) to announce legislation changes, remind or dictate the good practices and list all recent pyrotechnic accidents from civilian or military uses.

### 1.5 Summary of the Chapter

The energetic material is a wide group which includes mixes of metals and oxides (thermites), amorphous materials (propellants) and organic or salt crystals (explosives). The present work focuses on a few organic secondary explosives: 1,3,5-trinitroperhydro-1,3,5-triazine (RDX), 2,4,6,8,10,12-hexanitro-2,4,6,8,10,12hexaazaisowurtzitane (CL-20) and octahydro-1,3,5,7-tetranitro-1,3,5,7-tetrazocine (HMX). The RDX is a compound of reference still extensively used for applications but also research studies; it has only one crystalline form at ambient pressure and is soluble in acetone, sparingly soluble in ether and ethanol but almost insoluble in water. Several analysis methods where tried because the degradation of the sample is often a source of limitations when dealing with energetic organic crystals. The Dynamic Light Scaterring (DLS) needs a stable suspensions without agglomeration nor Ostwald ripening. Under the electron flow in electronic microscopy, the energetic samples heat up and are decomposed. Environmental Scanning Electron Microscopy (ESEM) is a more suitable technology to investigate the particle size and shape, due to the low vacuum able to dissipate heat.

The measurement of the Particle Size Distribution (PSD) is crucial to anticipate the properties of the material and to understand their creation. In addition to the previously mentioned issues, each characterization method measures an unique size; on DLS a hydraulic diameter is determined where the particles' agglomeration and the layers of solvating are taken into account. Electron microscopy techniques provide a direct visualization of particles and are therefore favoured. Finding a suitable and accurate method to establish the Particle Size Distribution (PSD) was the first challenge of the project and is further described in the Chapter 3.

This trend to easily agglomerate, growth, decompose etc. comes from the intrinsic nature of secondary explosive: organic crystals are also called soft matter. Their crystallisation at a nano scale has been a long-standing issue over several decades, and the result depends on the chemical nature of the compound. Therefore, RDX has been extensively studied and crystallised by
almost all the known techniques from other applications in the field of chemical engineering. The following review on processes which led to reduced size of RDX is necessary to provide a global comprehension on the specificities of RDX crystallisation.

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## Chapter 2

## Production of Nano Explosives

The crystallisation of a compound or several ones is the phenomenon of transition between the liquid, gaseous or even solid state to the crystalline state where matter posses long range order and symmetry. Crystallisation can be used to adjust the physical properties and the morphology of a substance. Crystallisation involves the formation of nuclei and then their growth; when a solution is supersaturated, its thermodynamic equilibrium is reached through nucleation and growth. To favour smaller particle size, the trend is to increase nucleation rate, for instance through increasing supersaturation, to reduce crystal growth and avoid any aggregation. Most of the crystallisation techniques are based from solution but crystallisation processes from the melt and from the gaseous phase are also known (van der Heijden et al. 2005). Quite a few were tested on energetic materials; the following bibliography is meant to be a comprehensive review of the crystallisation of RDX and of similar energetic compounds at submicron or nano scale.

### 2.1 Wet production methods

### 2.1.1 Crystallisation from solution

The most commonly used technique is the crystallisation from solutions. Depending on the creation of supersaturation, distinctions are made between cooling, evaporation, vacuum cooling, drowning-out and reaction crystallisation. The study of the solubility of the compound is the key to determine which crystallisation process can be used: for instance if the solubility is not very temperature dependent, evaporation will be more effective than cooling (Figure 2.1 p. 62).

Fedoroff et al. (1966) indicates that the RDX solubility in acetone is divided by 4 by cooling from $60^{\circ} \mathrm{C}$ to $0^{\circ} \mathrm{C}$. PANT et al. (2013) used all standard techniques


Figure 2.1 - Solubility curves for different substances (Mersmann 2001).
available to recrystallize RDX into submicrometer crystals "in a beaker": the smallest size was obtained when the anti solvent were added to a highly supersaturated solution cooled down, while applying ultrasonication and stirring. Achieving a high level of supersaturation results in a higher nucleation rate, but aggregation rises at elevated rates; for this solvent/compound system, they produced smaller particles, and reduced the agglomeration by the sonication. Particles are finally obtained by drying. This method may be suitable for industry, however, the minimal size obtained is only 850 nm under tough condition, with a yield of $60 \%$ and rod shaped crystals.

Kumar et al. (2014) succeeded to produce finer RDX particles by quickly injecting a very small volume ( $100 \mu \mathrm{~L}$ ) of RDX dissolved in acetone into ultra pure water: the smallest mean particle size was $38 \pm 15 \mathrm{~nm}$ by SEM for the highest temperature $\left(70^{\circ} \mathrm{C}\right)$ and lowest concentration of RDX in acetone ( 5 mM ). It is worth to mention that DLS measurements were found to be not reliable when compared to SEM analysis, which can be explained by the lack of surfactant stabilizing the colloid. This technique was also applied on HMX (Kumar et al. 2015) with a particle size around 30 nm and the same conclusions were drawn out.

Bayat et al. (2015), through an optimization of the micro-emulsion process, crystallised 80 nm plate-like $\beta$-CL-20 particles. The severe agglomeration and plate-like morphology might be due to the freeze drying, then washing of the micro-emulsion. Gao et al. (2014b) recrystallized FOX-7 in ethyl alcohol within a submicrometric range: SEM pictures show an irregular plate-like morphology and therefore highlight the inconsistency of the unique mean particle size of 340 nm claimed. Particles exhibit also a certain degree of agglomeration which
can be probably explained again by the lake of a surfactant and the air-drying.
Luo et al. (2015) reached an impressive size of 30 nm of RDX. They used a surprising technique where RDX is dispersed in bacterial cellulose. The lowest particle size was obtained with $71 \%$ RDX/gelatine mix; however, increasing the content of RDX leads to an increment of the particle size and the maximum of RDX loading tested was $91 \%$ for a particle size of 50 nm . The sensitivity of that composite towards impact and friction is divided by two therefore asking the legitimate question of the reactivity. Nevertheless, further efforts could be done to replace the bacterial cellulose with energetic matrix.

Crystallisation in solution allows the formation of large crystal by growth, thus allowing more parametric studies about the influence of solvents ; for instance (Li et al. 2015c) has studied the importance of temperature and supersaturation for the crystallisation for HMX in $\gamma$-butyrolactone, revealing that low temperatures and highly supersaturated solutions trend to increase the defects in HMX crystals.

### 2.1.2 Solvent substitution using reverse micelles

Dabin et al. (1999) have developed an ingenious method to prepare nanometre RDX using a simple technique: the crystallisation is triggered by a solvent substitution, and the nanometre scale is obtained by restricting the reactor volume to such a scale with reverse micelles. NaAOT (Sodium 1,4-bis(2-ethylhexoxy)-1,4-dioxobutane-2-sulfonate) into isooctane forms reverse micelles, then RDX in DMF is added to one solution containing these micelles, and water to another solution of micelles. Both are finally mixed together to form the nano RDX with a diameter of 70 nm to 100 nm .

### 2.1.3 Sol-Gel

Energetic materials processed by sol-gel method, are desensitized by embedding in a matrix, usually a silica matrix. Developed by Gash et al. (2000), Tillotson et al. (2001), and Tillotson et al. (1997), the silica-explosive gel is prepared by dissolving the energetic compound, the silica precursor and a catalyst, in a co-solvent. After the gelification, an anti-solvent of the explosive is injected to replace the solvent in the pores and precipitate the explosives in that silica matrix. By drying with heating or at low pressure, a xerogel with higher density is obtained; if supercritical $\mathrm{CO}_{2}$ is used to extract the solvent, an aerogel with low density is formed. Therefore, the nanostructuration of the explosive comes from the porous matrix: cavities of mesoporous gels are from 2 to 50 nm large, less than 2 nm for microporous gels. Macroporous materials have pore diameters of greater than 50 nm (Rouquerol et al. 1994).

RDX/Resorcinol-formaldehyde (RF) nano-composite has been synthesized (GUO Qiu-xia 2006): 38 nm large nano-RDX has crystallised in an RF aerogel matrix with a surface area of $551.5 \mathrm{~m}^{2} / \mathrm{g}$ (measure taken without RDX). Wuillaume et al. (2014) trapped AP and RDX in a mesoporous low-density energetic organogel. At the impact test negligible decrease of sensitivity has been measured: $75 \mathrm{wt} \%$ RDX nano gels and macro gels have the same sensitivity and the $90 \mathrm{wt} \%$ nano gels are even more sensitive than the macroscopic counterparts. When compared to pure RDX, the $90 \mathrm{wt} \%$ nano gels are not desensitized. However, SSGT preformed on pressed gels ( $95 \%$ TMD) revealed an improvement of the sensitivity for the $90 \mathrm{wt} \%$ RDX nano-formulation. That nano gel exhibits an uncommon micro-structure of sheets, with micron-sized particles potentially formed by nano primary particles: the lack of desensitization on the loose powder may be explained with the sensitization by the sheet-like shape counteracted by the presence of the gel coating each nanoparticles.

Li et al. (2015a) used a better energetic matrix -Cilycidyl Azide Polymer (GAP) - with a maximum of $40 \mathrm{wt} \%$ of RDX; they noticed a lower sensitivity than the physical mix. However, the claimed nano size is only deduced from porosity without RDX and from XRD patterns which only gives a mean coherence length. They also created NitroCellulose (NC)-RDX-AP nano composites by a technique similar to sol-gel (Jin et al. 2015); the matrix consist of the NC itself solidified by micron-sized AP crystals and cross-linked with Toluene Dilsocyanate (TDI) and Dibutyltin dilaurate (DBTDL), whereas RDX is dissolved in acetone inside that template. The gel and the crystallisation of RDX is triggered by supercritical $\mathrm{CO}_{2}$ drying. Even if the sensitivity and the density were not improved, the increase of the heat of explosion measured and the originality of the approach make promising the formation of nano-composite based entirely on energetic materials through chemical binding.

### 2.1.4 Melting

Many high energetic materials degrade very closely to their melting point. Therefore, only a few such as TNT or TNB can be used in their molten state, since the melting temperature is at least $100^{\circ} \mathrm{C}$ far from the exothermic decomposition. The melt-cast process of TNT-based composition is used for shaping charges or loading them into ammunitions since WW I. Crystallisation from an emulsified molten explosive is an innovative technique used by Anniyappan et al. (2015). 2,4,6-triazido-1,3,5-triazine or cyanuric triazide (CTA) has been processed at $95^{\circ} \mathrm{C}$ to crystallise as micron-sized agglomerates. CTA is a promising primary explosive compliant with the new REACH legislation (Regulation (EC) No 1907/2006 on the Registration, Evaluation, Authorisation and Restriction of Chemicals (REACH) and setting up a European Chemicals Agency 2007) forbidding the use of heavy
metal based materials. Further investigation with surfactants might lead to smaller particles by counteracting the high viscosity of molten droplets.

### 2.1.5 Milling

Redner et al. (2006) developed a batch wet-milling process, producing submicrometer RDX. A mixture of water, isobutanol, a dispersant and RDX is filled into a unspecified mill, resulting in a minimal mean particle size of 310 nm and a crystallite size of about 65 nm . Several milling issues were mentioned such as the yield initially of around $25 \%$ and the importance of the residence time and the drying step.

Liu et al. (2014a, 2013) studied the effect of drying nano-RDX and HMX samples under various conditions. They first obtained nano-RDX in solution from a mixture of water, ethanol, isopropanol and RDX. The suspension is put in a bi-directional rotation mill for 6 h . Just as Rednere experienced, the drying is the critical point to get a nano powder. They dried the RDX under different conditions: freeze drying and supercritical drying led to quite impressive results, with medians at 160 nm and 200 nm respectively from a solution containing an average particle size of 64 nm . After RDX and HMX, CL-20 was successfully processed the same way resulting in a median size of 180 nm determined by SEM (Liu et al. 2014b). For the three compounds, nano powders are less sensitize than their micron-size counterparts.

Spray drying is a less energy intensive drying method studied by Patel et al. (2015). RDX and CL-20 have been bead milled from water with addition of isobutanol and Polyvinyl alcohol (PVOH) to stabilize the colloid by dispersion and coating, and then an unknown polymeric binder is added just before drying the slurry by spray drying. Mean particle sizes down to 400 and 200 nm respectively have been measured by DLS for RDX- and CL-20-based composites after milling. However, no PSD curve has been provided nor dispersion of the results indicated. It has been noticed that for particles of CL-20 at 200 nm , the $\alpha$ phase is obtained. From the same team, nanoscale cocrystal of CL-20:HMX 2:1 has been prepared by bead milling an aqueous suspension of $\varepsilon-C L-20$ and $\beta-\mathrm{HMX}$ in a 2:1 stoichiometric ratio (Qiu et al. 2015a). The progressive conversion of raw materials into the cocrystal is achieved after one hour, resulting in a particle size lower than 200 nm . However, not much attention has been paid to the drying effect of large scale batch; SEM and XRD were made on a drop dried at room temperature, and it is likely that the drying of several grams of such molecular crystal will behave differently. Furthermore, the accuracy of the XRD technique does not allow to conclude that a complete conversion into cocrystal has occurred, but rather indicates that the percentage of $\varepsilon-\mathrm{CL}-20$ and $\beta-\mathrm{HMX}$ is
lower by $10 \%$ approximatively. Full quantification by Rietveld or Full Pattern Matching methods would have been relevant to follow the conversion with time.

### 2.2 Dry production methods

### 2.2.1 Physical Vapor Deposition (PVD)

Frolov and Pivkina have developed together a vacuum condensation process for high energetic material first reported in 2002 (Frolov et al. 2002; Frolov et al. 2010; Pivkina et al. 2004). Vacuum deposition of ammonium nitrate (AN), RDX and a composite AN-RDX was performed on a cooled quartz-glass substrate. The mean particle size was directly measured from AFM: a size of 50 nm was obtained for the three materials, even after processing the nano-powder (removing from the quartz substrate and pressing into tablets).

Mil'chenko et al. (2015) went further in the Physical Vapor Deposition (PVD) process by the deposition of TATB, HMX, RDX, PETN and BTF as thin layers on several substrate such as Plexiglas and copper while changing operative parameters. Critical thickness of the detonating layer is an order of magnitude lower; the sensitivity toward impact and friction is barely mentioned as being similar to the raw materials but the sensitivity to Light Amplification by Stimulated Emission of Radiation (LASER) has been substantially increased.

Therefore, the PVD technique is greatly suitable for "pyrotechnic integrated circuits", whereas mass production of loose powder is not economically viable.

### 2.2.2 Electrospray

Radacsi et al. (2011) crystallised submicrometer RDX using an electrospray. A solution of RDX-acetone is sprayed through a nozzle electrically charged to a grounded plate: the droplet surface is charged, increasing their surface energy and so triggering their fission into smaller droplets. This Coulomb fission phenomenon and the evaporation of the solvent lead to crystallisation and the deposit of non agglomerated particles. The tweaking of the characteristics of the nozzle and the potential difference resulted in various morphology of RDX particles: for instance, micrometer hollow spheres of agglomerated RDX were produced. The minimal mean size obtained was 400 nm : that submicrometer RDX exhibited a clear insensitivity towards friction, but with the same impact sensitivity as conventional micron-sized RDX (Table 2.1, p. 67).

Reus et al. (2014) then processed bi-component systems: proteins and RDX/TNT. XRD patterns of the final products are mentioned to be different from the ones of the raw material, which seems to indicate either a strong

| RDX | Impact [J] | Friction [N] |
| :---: | :---: | :---: |
| Conventional | 7.5 | 120 |
| submicrometer | 10 | $>360$ |

Table 2.1 - Comparison of the sensitivity levels of conventional and 400-nm large RDX.
degradation or a cocrystallisation. Infrared definitely demonstrates a critical partial decomposition of both RDX and TNT due to the electrospray and the same phenomenon has likely happened for Radacsi et al. too. Whatever was really obtained, Reus crystallised very small particles, estimated by me to be under or around 100 nm for any initial ratio of TNT/RDX. AFM could have been much more informative about the size and shape of such nanoparticles already well dispersed on a substrate. Sensitivity tests have been performed on those degraded materials, which were found to be as insensitive as TNT.

Electrospray can create a fine spray of micron-sized charged droplets repealing each others, ideal for crystallisation; the high voltage needed is a major handicap for processing sensitive powders such as energetic materials containing nitro groups.

### 2.2.3 Plasma

During his PhD project (Radacsi 2012), Radacsi used an innovative and advanced technique to crystallise submicrometer RDX: a Collison nebulizer aerosolizes a RDX-acetone solution to a Surface Dielectric Barrier Discharge (SDBD) plate where a cold plasma disrupts the droplet by the Coulomb fission. Like the electrospray, one droplet should crystallise into a unique single-crystal. The minimal mean size obtained was 500 nm , with a range from 200 nm to 900 nm and with prismatic or spherical shapes. Again like the submicrometer powder obtained from electrospray, the 500 nm -sized RDX has been desensitize to friction but not to impact (Table 2.2, p. 67).

| .RDX | Impact <br> $[J]$ | Friction <br> $[\mathrm{N}]$ |
| :---: | :---: | :---: |
| Conventional | 5 | 144 |
| submicrometer | 5 | $>360$ |

Table 2.2 - Comparison of the sensitivity levels of conventional and 500-nm large RDX (Radacsi 2012).

### 2.2.4 Supercritical/Gas Anti-Solvent precipitation

Supercritical Anti-Solvent precipitation (SAS) uses the same principle as liquid crystallisation, substituting the liquid anti-solvent by a supercritical fluid. The very high diffusivity of supercritical fluids leads to a rapid supersaturation and so to a sudden precipitation. Various apparatuses are used in SAS: a specific one is the Gas AntiSolvent (GAS) precipitation, where the liquid solution is first loaded into the vessel, before the addition of the supercritical anti-solvent. For RDX, $\mathrm{CO}_{2}$ is a correct supercritical anti-solvent. Gallagher et al. (1992) first investigated GAS process of RDX in 1992. Supercritical $\mathrm{CO}_{2}$ was injected into RDX-cyclohexanone solution at various injection times, injection quantities and temperatures: in this first use of GAS for RDX, a lot of different particle size distributions and morphologies were obtained, but none under the micrometer size. Since then, several process derived from the GAS process, and which could be referred as SAS sub-process, have been used to reach the submicrometer and nano scale for energetic materials. But from 1992, no GAS/SAS process has been reported to produce energetic materials to a size lower than the micron (Jung et al. 2001; Lee et al. 2009, 2011b; Teipel et al. 1997), excepted for 5-nitro-1,2,4-triazol-3-one (NTO) by Lim et al. (1998) (Reverchon et al. 2005).

### 2.2.5 Aerosol Solvent Extraction System (ASES) process

Aerosol Solvent Extraction System (ASES) process involves spraying the solution to precipitate through an atomization nozzle into supercritical $\mathrm{CO}_{2}$. Lee et al. (2011b) used GAS and ASES apparatus to crystallise $\beta$-HMX: undesirables shapes (needle-like, irregular and aggregated) were produced by ASES at any operating conditions, whereas GAS led to regular shape and the most desired $\beta$ phase. Dou et al. (2013) sprayed RDX dissolved in DMF obtaining micronsized particles highly polydispersed. However, submicron-sized polymers and biopolymers produced by ASES have been reported since the nineties by Dixon et al. (1993) and Reverchon (1999). Nevertheless, that technique could be used on NC based composite due to its polymer-like behaviour.

### 2.2.6 Solution Enhanced Dispersion by Supercritical fluids (SEDS)

Solution Enhanced Dispersion by Supercritical fluids (SEDS) process was developed and patented by the Bradfort University to achieve a smaller droplet size compared to the previously described SAS methods. For SEDS process, a solution with the compound solvated is sprayed into supercritical anti-solvent gas $\left(\mathrm{CO}_{2}\right.$ for RDX$)$ through a nozzle with two coaxial passages: this technique
can be seen as a specific implementation of the ASES process, where $\mathrm{CO}_{2}$ is introduced through the nozzle continuously with the solution. Shang et al. (2014) produced by SEDS spherical RDX particles with a mean particle size of 770 nm , therefore finally lowering the particle size under the micron.

### 2.2.7 Particles from Gas-Saturated Solutions (PGSS)

Both patents "Conditioning of finely divided crude organic pigments" (1984) and "Finely dispersed carotenoid pigments prodn. - by dissolving carotenoid in a supercritical gas, pref. carbon di:oxide, and dispersing the soln. in an aq. colloidal matrix" (1981) first described a procedure that today is called Particles from Gas-Saturated Solutions (PGSS). The PGSS technique consists in dissolving a compressed gas into a solution of the substrate in a solvent, then passing it through a nozzle: the sudden decompression leads to crystallisation thus to the formation of solid particles. Although this method is widely used at large scale with a wide range of products from inorganic powder to pharmaceutical compounds (Pourmortazavi et al. 2005), nothing has been reported (Jung et al. 2001) concerning energetic materials processed by PGSS.

### 2.2.8 Rapid Expansion of Supercritical Solutions (RESS)

The RESS concept has been first described by Hannay and Hogart more than a century ago (Hannay et al. 1879) but studied by Krukonis (1984) and the Battelle Institute research team (Matson et al. 1987a,b). The RESS process consists in spraying in a lower pressure chamber (60-0 bar) through a nozzle a supercritical (sc) fluid containing the substrate. The sudden drop of pressure leads to rapid nucleation and so small (from micron- to nano-sized) particles which are finally collected. The use of a supercritical fluid like $\mathrm{CO}_{2}$ allows the direct production of a dry and pure powder. Teipel et al. $(1997,2001)$ first reported the use of RESS for energetic materials: $10 \mu \mathrm{~m}$ large TNT particle were crystallised in those preliminary experiments. They mentioned parameters which influence strongly the crystallisation from a RESS apparatus: pressures, temperatures, geometry of the nozzle and mass flow. Stepanov in the group of Krasnoperov succeeded in the fine tuning of the RESS process to prepare dried n-RDX (Stepanov 2003, 2008; Stepanov et al. 2006, 2005). The formed RDX particles had a mean particle diameter ranging from 110 nm to 220 nm and an irregular spherical morphology. He performed an up-scaling of the RESS process in order to increase the production capacity of RDX to $6 \mathrm{~g} / \mathrm{h}$ but with a $\mathrm{CO}_{2}$ consumption of $35 \mathrm{~kg} / \mathrm{h}$. By RESS, a slight sensitization to impact and shock stimuli of the 200 nm nano-RDX occurred compared to $500 \mathrm{~nm} n-R D X$ (Stepanov et al. 2011).

CL-20 has also been reported to be processed by RESS from trifluoromethane $\left(\mathrm{CHF}_{3}\right)$ (Reverchon et al. 2005): sc- $\mathrm{CHF}_{3}$ has similar thermodynamic properties and is a better solvent of $\mathrm{CL}-20$ than sc- $\mathrm{CO}_{2}$. Only micron-sized particles were produced and no article reporting the results could have been found. Changing the solvent is a line of research followed by Lee et al. (2011a) using compressed liquid DiMethyl Ether (DME) for RDX. The parametric study points out the role of inlet pressure and temperature and the nozzle diameter: increasing any of those three parameters increases the particle size. Therefore, the two minimal mean particle sizes of 370 and 360 nm were obtained for the lowest mass flow rate of 0.37 and $0.85 \mathrm{~g} / \mathrm{s}$ of DME.

### 2.2.9 RESS-AS (or RESOLV)

After the success of the RESS process, Essel et al. developed a new method from that technique, called Rapid Expansion of Supercritical Solutions into an Aqueous Solution (RESS-AS) first reported in 2010 (Essel et al. 2010). Rapid Expansion of Supercritical Solutions into an Aqueous Solution (RESS-AS) uses the versatility of the RESS process, spraying into an aqueous solution containing a dispersant and/or growth inhibitor (Kuo et al. 2011). They reported (Essel et al. 2012) a production of 30 nm sized RDX using a pH 7 -stabilized solution, although a polymer coating (PEI or PVP) was necessary to avoid any agglomeration and so stabilize the colloid from the Ostwald ripening observed when no polymer was added. No sensitivity tests have been reported about any nano-powder which could be obtained from those colloidal suspensions.

### 2.2.10 Light Amplification by Stimulated Emission of Radiation (LASER) Ablation

Gottfried et al. (2012) successfully produced for the first time nanoparticles of RDX using LASER ablation. Near-infrared, nanosecond pulsed LASER has been focused on military-grade RDX pellets: Scanning Mobility Particle Sizer (SMPS) and SEM analyses showed a particle size distribution around 64 nm for 200 mJ pulse and 75 mJ pulse.

### 2.2.11 Ultrasonic Spray Pyrolysis

Since the nineties, spray crystallisations and synthesis have been performed using several atomizers, and among them piezoelectric transducers (Messing et al. 1993; Okuyama et al. 2003). As a spray technique, the goal is to produce one particle per droplet, but here the crystallisation is controlled by the drying step, an oven just after the atomization. Kim et al. (2011a), Kim et al. (2011b),
and Spitzer et al. $(2011,2010)$ both developed an apparatus to produce dried submicrometer RDX from an ultrasonic transducer. After the droplet generation, the solvent is evaporated by thermal gradient applied on the flux pulled by a pump. Highly agglomerated particles $200 \mathrm{~nm}-500 \mathrm{~nm}$ were produced. Caoo et al. (2014a,b) used the same experimental setup with the exception of the addition of a thermal gradient in the furnace, in order to produce 78 nm FOX-7 particles, and submicron-sized CL-20:HMX cocrystals.

### 2.2.12 Spray Drying

The development of spray drying (Broadhead et al. 1992; Stein 1973) has been expanding since many years and has recently became a suitable commercial solution at both R\&D and industry scales to produce dried particles from microns to nanometres. The pyrotechnic community quickly discerned the advantages of this simple technique to process energetic compounds as pure and composite materials.

The process sprays a solution containing a dissolved compound or particles in suspension into a hot gaseous stream (air or nitrogen) thus crystallising into particles and/or drying the granules. van der Heijden et al. (2008) has proven that spray drying is able to crystallise finer RDX particles ("from 400 nm and larger") than their technique of precipitation into anti-solvent ( $1 \mu \mathrm{~m}$ to $10 \mu \mathrm{~m}$ ). Qiu et al. studied the crystallisation of energetic compounds using the spray drying with ultrasonic (Qiu et al. 2011) or pneumatic (Qiu et al. 2012) nozzle or with both type of nozzles (Qiu et al. 2015b). All their experiments were done with the addition of Polyvinyl acetate (PVAc) and resulted in micron or submicronsized hollow spheres made of nano primary particles; the smallest ones were estimated at 20 nm for RDX/PVAc made from a pneumatic nozzle with a mean droplet size of around $7 \mu \mathrm{~m}$. The versatility of the process allows the production of energetic composites (coating of TATB on micron-sizedHMX, RDX or CL-20 by Ma et al. (2015)), energetic/elastomer composites (micron-sized CL-20/EPDM by Ji et al. (2015), micron-sized spheres of agglomerated HMX/Viton by Shi et al. (2015)), and even cocrystals (micron-sized spheres of agglomerated HMX/TNT by Li et al. (2015b)).

### 2.2.13 Spray Flash Evaporation (SFE)

Risse and Spitzer at the NS3E laboratory developed an innovative process after experimenting the limitations of the Ultrasonic Spray Pyrolysis method: beyond the inherent risk of using a high voltage electrostatic precipitators for energetic powders, the rate of evaporation of droplets is too low to avoid agglomeration and to crystallise submicrometer particles. Risse (Doctoral Thesis 2012) and Risse
et al. (2012) used the flash-evaporation behaviour of droplets to dramatically reduce the life time and the size of droplets. The compound is dissolved in a volatile solvent and that solution is heated just before being sprayed into vacuum, where the crystallisation is triggered by the sudden temperature depression and the solvent evaporation. The process is discussed in more details in Section 2.4.2.

An unconventional application of nanosized explosives used at the NS3E laboratory is the synthesis of nanostructured material by detonation. Pichot et al. (2015) and Pichot et al. (2013) demonstrated that smaller nano diamonds are generated from the detonation of $n-T N T / R D X$ composites produced by SFE than from a physical mixing of micron-sized commercial TNT and RDX.

### 2.3 Discussion on production methods

The smallest size of RDX is either obtained from wet techniques, or from smallscale approaches which cannot be transferred to industry (PVD and LASER). Even if PVD has been successfully used in the semiconductor sector for our everyday electronic devices since decades, PVD for energetic material will never be able to reach a production of several hundred of grams per hour. However, PVD is perfectly suitable for the current trend to create "pyrotechnic integrated circuits". Femto second LASER ablation is used for nanoparticles synthesis of metal in solution at the laboratory scale; the colloids produced are found to be extremely stable. Used in dried conditions, a deposit of nanoparticles on a substrate could be obtained from a gas flow, or a dried powder could be collected within a cyclonic separator: this LASER technique has been used to cut high energetic material quite safely (Roeske et al. 2003) but nanoparticles production would be severely limited to high-added-value industrial applications due to low production rate and high operation cost. Besides those two aspects, neither methods would process advanced composites - with a binder for instance - or would be able to do concomitant or cocrystallisation.

The production of nanoparticles through wet techniques has became a common industrial chemical process. The Sustainable Hydrothermal Manufacturing of Nanomaterials (SHYMAN) European project aims to increase the production rate of a continuous hydrothermal process from 1-10 tons/annum to 100 tons/annum of inorganic nanomaterials (Charitidis et al. 2014). Tsuzuki (2013) statistically studied which method for inorganic nano synthesis are mostly used in industry: vapour (39 \% mainly Chemical Vapor Deposition (CVD)) and liquid (45 \%) phase synthesis are the main type of techniques. Patents or historic skills of the brand can restrain the choice of a technology, so such data should not be taken as indicators of the robustness or versatility of the method. Considering such wide adoption of wet techniques (Sheth et al. 2012) and the knowledge from

| Process | working <br> pres- <br> sure(s) | heating $\left({ }^{\circ} \mathrm{C}\right)$ | continuous | scale-up | limiting <br> step(s) | smallest size ${ }^{1}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Sol-Gel | atmo | no | no | -+ | matrix, drying | 100-150 ${ }^{2}$ |
| Antisolvent | atmo | 70 | could be | - | injection, drying | 38 |
| Milling | atmo | cooling | no | + | drying | $160^{3}$ |
| PVD | $10^{-4} P a^{*}$ | 100-200 | no | - | vacuum | 50 |
| Electrospray | atmo | no | could be | - | mass <br> flow, electric field | 400 |
| ASES | 12 MPa | yes and cooling | no | - | $\mathrm{sCO}_{2}$ | microns |
| SEDS | $35 \mathrm{MPa*}$ | yes | no | - | $\mathrm{sCO}_{2}$ | microns |
| RESS | $\begin{gathered} 35 \mathrm{MPa} \\ \rightarrow 0.1-5 \\ \mathrm{MPa} \end{gathered}$ | yes and cooling | could be | -+ | $\mathrm{sCO}_{2}$ | 200 |
| RESS- <br> AS | 35 MPa <br> $\rightarrow$ atmo | 25 | could be | -+ | $\begin{aligned} & \mathrm{sCO}_{2} \\ & \text { drying } \end{aligned}$ | $30^{4}$ |
| LASER | atmo | no | no | - | mass <br> flow | 64 |
| Ultrasonic | atmo | 50-150 | could be | -+ | transducer | 200-500 |
| Spray drying | atmo | 50-100 | could be | ++ | evaporation ratio | 400 |
| SFE | $\begin{gathered} 5 \mathrm{MPa} \rightarrow \\ 5 \mathrm{mbar} \end{gathered}$ | 150 | yes | ++ | vacuum | 300 |

Table 2.3 - Comparison . ${ }^{1}$ smallest pure RDX mean size reported in nm $\left.\right|^{2}$ XRD measurement | ${ }^{3}$ freeze dried from a 64 nmRDX slurry | ${ }^{4}$ from DLS, no report about dried state | "Not available in the references, so the value is based on usual operating conditions | sCO $\mathrm{SO}_{2}$ : supercritical carbon dioxide
chemical engineering - homogenization in large reactor, processing of liquid flow, versatility, safety ... -, wet crystallisation methods are a logical choice to process organic materials. However, unlike inorganic and metal nanoparticles, organic matter is very sensitive to drying as we previously saw in Section 2.1.5; yet that delicate step is required since the reactivity of high energetic materials fully exhibits at the dried state. Freeze drying and supercritical drying seem to overcome kinetically and partially the crystal growth occurring. Only a complete growth inhibition will lead to the production of smaller nanoparticles under 100 nm from milling or anti-solvent/cooling crystallisation. From an industrial point of view, freeze or supercritical drying are batch-only processes; all current industrial drying process are not designed to tackle down the fast growth of soft-matter. Innovative techniques such as spin freezing (L. De Meyer et al. 2015) or spray drying enhance the processability and potentially the performances, but their reliability need to be tested.

The ball-milling technique raises question about the purity of the product; it is well know that after such an extensive friction process, industrial milled ceramics are not used for hight purity chemical process (Carter et al. 2013). Industry moved to other techniques such as vapour phase ones, to overcome that limitation and others like the lake of control, local heating etc. Even with soft matter, similar issues can be expected; even small quantities of metallic impurities could catalyse the degradation of the explosive and/or sensitize it.

After 25 years of research and 10 years of process engineering, the SuperCritical Fluid (SCF) technology has never convinced the industry and only marginal uses for specific commercial drug products have been reported (Sheth et al. 2012). First, the choice of the gas at industrial scale is falling back to $\mathrm{CO}_{2}$ due to safety and affordability criteria. For instance, gases such as nitrous oxide or ethane have low critical values, but explosive mixtures can be generated. Trifluoromethane is inert, non-flammable and is usually a better solvent but is way more expensive than $\mathrm{CO}_{2}$ and a potent greenhouse gas. Second, the main limitation -the solubility into sc- $\mathrm{CO}_{2}-$ can be overcome by the addition of organic cosolvent: such modification alters the environmentally safe nature of sc- $\mathrm{CO}_{2}$ based SCF and complicates the process by the need to remove any residual organic solvents. The aggregation phenomenon is commonly observed in SCF processes; further investigations on the role of different particle collection environments are needed, but RESS-AS processes greatly avoid the particle aggregation. The use of a liquid anti-solvent with polymeric stabilizers has been found to be very effective. However, it compromises the recovery of a dry pure powder, going back to square one with the drying issues previously discussed.

Spray techniques are commonly used in the industry, such as micro-encapsulation massively used for food (Gibbs et al. 1999; Madene et al. 2006), spray drying in
pulmonary drug delivery for production of uniform and breathable size particles (Bhavesh B. Patel et al. 2014) or even thermal spray deposition of metallic material (Lavernia et al. 2009). Spraying is a method which allows easy implementation of an installation and easy direct control over the injection. However, because of the low technological cost of atomizing nozzles and the low control over the spray itself, details and know-how are much more important than for other processes. Direct spray drying as crystallisation technique for RDX does not produce submicron-sized particles without the help of an additive and the SCF techniques are not suitable for industry: the need for an intermediate method in terms of pressure and temperature leads to the creation of the Spray Flash Evaporation technique, especially tailored for crystallisation. SFE operates from 40 to 100 bars with an RDX solubility in acetone around $5 \mathrm{wt} \%$, whereas sc- $\mathrm{CO}_{2}$ is formed from 74 bar to 500 bars for a solubility from null to $0.025 \mathrm{wt} \%$.

### 2.4 The Spray Flash Evaporation Technique

### 2.4.1 Theoretical Insights on the SFE technology

Flash Evaporation The flash evaporation is the physical phenomenon occurring when the boiling point of a liquid is lower than its actual temperature, due to a sudden drop of pressure and/or a quick increase of temperature. The excess of heat is instantly converted into latent heat of vaporization, cooling both liquid and vapour down to the saturation temperature. Multi Stage Flash (MSF) evaporators of static water have been used since the middle of the $\mathrm{XX}^{\text {th }}$ century ("Combined flash and vapor compression evaporator" 1956; "Flashtype distillation system" 1959; "Method of and apparatus for flash evaporation treatment" 1957) with yield of around $100 \mathrm{~m}^{3}$ per day, receiving a growing interest mainly from the US West Coast (Resources 1969) and Japan (national research program "seawater desalting and by product recovery" launched in 1969, (Sawa et al. 1976)). Current applications are extended from solution concentration such as in wine industry (Sebastian et al. 2002) to heat dissipation of electronic chips and LASER devices (Cheng et al. 2016).

Flash Evaporation of Superheated Liquid Jet Brown and York (Brown et al. 1962) found a critical temperature above which the liquid jet was burst by rapid bubbling. They injected water up to 13 bar through simple single-hole nozzles with a minimal diameter of $500 \mu \mathrm{~m}$ into ambient pressure. The linear mean droplet sizes were found to follow a linear variation of temperature. Then in 1981, Miyatake et al. were pioneers in the field of flash evaporation and published the

(a) Two different disruptions in flashing water jets enlarged 10X from Brown et al. (1962)

(b) Flashing water jets under various superheating from Miyatake et al. (1981a)

Figure 2.2 - Flashing in water liquid jet
first known articles about spray flash evaporation with superheating (Miyatake et al. 1981a,b), after studying flash evaporation from water pool (Miyatake et al. 1972). Many technical limitations restricted their studies for current issues: only straight-lined liquid jets were studied with basic optical techniques where the smallest drops and bubbles could not be indexed. However, Miyatake et al. (1985) interestingly used electrolysis to generate more bubbles into a flashing water jet. Nowadays, not many laboratories still investigate flashing liquid jets; Günther et al. (2013) characterized with modern techniques flashing liquid jets and noticed the formation of bubbles inside a glass nozzle for high superheating. They also demonstrated that a simple acoustic measurement can be used to monitor the atomization of superheated liquids. The current application of flashing liquid jet is the improvement of MSF desalination processes of sea water (Ikegami et al. 2006; Miyatake et al. 2001); a much higher evaporation rate is obtained in contrast to static flash evaporator where the rate is surface dependent.


Figure 2.3 - Empirical diagram of the evaporation of a water drop (Owen et al. 1991)

Flash Evaporation of Droplets Specific studies on the flashing phenomenon are rare. Owen et al. (1991) investigated that specific form of evaporation on isolated drops. A superheat of $0^{\circ} \mathrm{C}$ to $5^{\circ} \mathrm{C}$ triggers only surface evaporation,
then boiling occurs at higher superheat. Flashing is triggered for superheat from $18^{\circ} \mathrm{C}$ to $24^{\circ} \mathrm{C}$ for drop of $1 \mathrm{~mm}-3 \mathrm{~mm}$ and larger drops flash more readily as illustrated in Figure 2.3. Since flash evaporation is closely related to cooling, many theoretical approaches start with a simplified model without superheating: Shin et al. (2000), Satoh et al. (2002) thoroughly described the evaporation behaviour of a water droplet in an abruptly evacuated atmosphere leading to its solidification. Sobac et al. (2015) developed a comprehensive model of the evaporation of a liquid spherical drop but not yet applicable to extremely small droplets as in flashing spray.

Interesting studies close to our SFE process came from Gebauer et al. (2012, 2015a,b, 2016). In their system, a pressurized superheated liquid is atomized through an hollow cone nozzle into a low pressure chamber and micron-size particles are recovered. However, only a partial evaporation occurs and leads to further crystal growth during the flying time and into the sump collected in the bottom of the crystalliser.

### 2.4.2 Comprehensive description of SFE



Figure 2.4 - SFE installation as patented and used in this present work
Figure 2.4 is a schematic diagram of the process, where the high pressure part is the red zone and the low pressure one in blue. One storage tank (4) is filled with technical grade solvent and is used for pre-heating, cooling and washing. The other tank (1) is filled with the solution containing the compound(s) to recrystallize. Both are closed and pressurized with compressed nitrogen at the pre-expansion pressure. Hydraulic tubes bring the fluid inside the atomization chamber; there, a heating jacket superheats the liquid, with a regulation made of thermocouple plugged to a Proportional-Integral-Derivative (PID) controller.

The superheated fluid is sprayed by a hollow cone nozzle (3) into the atomization chamber under a vacuum below 10 mbar. Details can be seen in Figure 2.5: the tip of the thermocouple (type $K \varnothing 1.5 \mathrm{~mm}$ ) measures the temperature after the heating jacket and just before the nozzle mounted on a full flow quick coupling.


Figure 2.5 - Schematic insight of the nozzle and its heating system; from left to right, rear view, longitudinal cross-section and front view.

The gaseous flow from the evaporation and the recrystallized product is pumped to a cyclonic separator. The cyclones are made from the description of (Chen et al. 2006) who found a cut-off diameter of $21.7 \mathrm{~nm}-49.8 \mathrm{~nm}$ in their work. A glass flat flange reaction vessel allows to gather the powder easily as it can be seen in Figure 2.6. Each cyclone unit can be isolated from the vacuum to allow the recovery of the product from one unit and the continuous separation inside the other: the two cyclones in parallel ensure the continuous functioning of the process at any flow rate.

At the end, the flow of gaseous solvent passes through a $35 \mathrm{~m}^{3} / \mathrm{h}$ vacuum pump; a condenser after the pump can recover the solvent for industrial installations.

The standard operating conditions are 40 bar of inlet pressure and $160^{\circ} \mathrm{C}$ at the hollow cone nozzle with an orifice diameter of $60 \mu \mathrm{~m}$.

The maintenance and constant improvements of several SFE installations took a significant part of this research project. The reliability, robustness, ergonomic and life-cycle of the process have been extended by replacing hydraulic and vacuum parts, by understanding phenomena, by developing on-line metrology and by stimulating the necessary feedback and cooperation between the various SFE users at NS3E.

### 2.4.3 Versatility of the SFE

Depending on the solute and the desired particle size range, the SFE can be adapted by changing the following parameters:


Figure 2.6 - System for the product recovery: in orange the cyclonic separator for vacuum and in gray the interchangeable vessel.

Type of solvent The most suitable solvents for SFE are low-boiling solvents with a high molar heat capacity. For easy handling and recovery, the solvents should have a boiling point in the range of $30-70^{\circ} \mathrm{C}$.

Superheating temperature The superheating temperature is proportional to the mass flow and the fluid properties. An increased superheating temperature enables higher evaporation rate.

Pre-expansion pressure The pre-expansion pressure has to be above the vapour pressure of the superheated solvent and compatible with nozzle diameter and type. The droplet size is also known to decrease at higher pressure.

Saturation pressure and temperature Saturation pressure and temperature of the spray cone in the atomization chamber depend mostly on the performance of the vacuum pump.

Nozzle diameter For most nozzles types like hollow cone nozzles, full cone nozzles, or flat jet nozzles, a decreasing orifice diameter decreases the
droplet size, but increases the pre-expansion pressure.

Besides the innovative applications of nano energetic materials such as the synthesis of ultra-fine nano diamonds (Pichot et al. 2015; Pichot et al. 2013) and reactivity enhancement (Comet et al. 2015), the SFE versatility allows the crystallisation at a submicron or nano scale of a wide range of organic compounds. In particular, cocrystals of medical materials are of interest for drug enhancement and were successfully processed through SFE at the nano scale (Spitzer et al. 2014). Inorganic nanoparticles were also produced at the nanoscale through SFE. ZnO was crystallised from the precursor zinc acetate dihydrate dissolved in ethanol with addition of water. From early experiments, nano primary particles of 20 nm were found to be agglomerated in sub-size structures, whereas the slightly larger nanoparticles were found much less agglomerated using the classical wet method. However, the SFE clearly demonstrated the feasibility of faster and quite efficient crystallisation of inorganic particles from precursors. Le Brize et al. (2016) processed energetic composite materials by SFE: a submicron structuration was evidenced from SEM pictures and an higher degree of chemical interaction was also found from Infrared (IR) and Raman spectra.

### 2.5 Scientific goals of the thesis

### 2.5.1 Particle Size Reduction

The first main goal of the project is to reduce further the particle size. During his PhD, Risse studied the effects of the superheating temperature, the inlet pressure, the ratio of MTBE/acetone as solvent, the nozzle diameter and the RDX-concentration. At higher superheating temperature and pressure, the droplets are likely smaller which leads to a noticeable decrease of the particle size. However, the role of solvent was not clarified; furthermore, both nozzle diameter and RDX-concentration need to be correlated with the inlet mass flow and the real superheating temperature - which is the difference between the spray and the inlet liquid - should have been monitored and kept constant. To reduce the particle size, the degree of supersaturation has to be controlled in both space and time resolution. Globally, we can distinguish two main approaches, a chemical one and a more physical one. On the chemical route, polymeric additives are studied to control the nucleation and growth steps. On the other side, different conditions of crystallisation are studied by a mixture of an anti-solvent and a solvent, and also by 'in-spray interactions' where two nozzles with overlapping spray patterns are used.

### 2.5.2 SFE understanding

The crystallisation by SFE results from deep and complex interactions between several physicochemical phenomena. That intricacy is illustrated by the mapping in Figure 2.7. While many parameters are involved, a few bottlenecks emerge: the volume of droplets, the degree of supersaturation and the time of the primary nucleation are keys to achieve a perfect control of the final particle size under flash-evaporation conditions. Therefore, the effort on in situ measurement for SFE technology is focused on those observable variables. In the meantime, other parameters has been changed such as the solvent type to influence the supersaturation and the nucleation time by additives.

### 2.6 Summary of the Chapter

Many crystallisation processes have been applied on RDX and similar energetic organic crystals. The smallest size of RDX is either obtained from wet techniques, or from small-scale approaches which cannot be transferred to industry (PVD and LASER). Finally, the Spray Flash Evaporation (SFE) process is a well balanced method between spray drying unable to process particles lower that the micrometer, and the expensive batch Rapid Expansion of Supercritical Solutions (RESS) process. The SFE relies on the superheating of a solvent sprayed into vacuum and thus flashing. The pressurization of the liquid before the injection provides the stability for the spray pattern and also for the overheated liquid. The flash evaporation is the physical phenomenon occurring when the boiling point of a liquid is lower than its actual temperature, due to a sudden drop of pressure and/or a quick increase of temperature. The excess of heat is instantly converted into latent heat of vaporization, thus provoking the fragmentation of the droplets called "flash". This allows formation of smaller crystallisation reactors (droplets) with a very high rate of evaporation therefore achieving smallest particle size.

From particle size and shape many properties are resulting such as the surface related ones for catalysis but also more physical one like the apparent density and the critical diameter for explosives. However, the definition of a particle is subject to variation; a real powder may be formed of macroscopic soft agglomerates of micron-sized hard agglomerates of nano primary particles. Therefore each characterization technique measures an unique mean distance depending of the physicochemical phenomena involved and the response of the sample. The following explains the characterizations previously in use at NS3E, their scientific criticism through analytical studies and the new methods applied.


Figure 2.7 - Intricacy of the parameters and phenomena involved in the particle crystallisation by the SFE process.

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## Chapter 3

## Definition of Particle and Determination of the Particle Size Distribution of RDX processed by SFE

### 3.1 Size Measurement

### 3.1.1 Sensitivity of nano-organic energetic particles

A particle size distribution can be obtained through many methods: X-Ray Disc Centrifugation (XDC), Photon Correlation Spectroscopy (PCS), Differential Centrifugal Sedimentation (DCS), Laser Scattering (Dynamic or Static), Laser Doppler Electrophoresis, nitrogen adsorption (BET method), Differential Mobility Analysis (Scanning Mobility Particle Sizer), Phase Doppler Particle Analyzer, Electronic Microscopy, Atomic Force Microscopy etc. But only a few are suitable for organic nanoparticles. In molecular crystals, weak forces are holding the molecules together instead of covalent bonds for metals or oxide solids; therefore organic nanoparticles are much more sensitive to solvation issues. Water is commonly misused as an anti-solvent of RDX, whereas the few $\mathrm{mg} / \mathrm{L}$ of solubility is enough to strengthen the growth of crystals through Ostwald ripening or to model a new crystal habit within a few hours or minutes. The liquid alkanes such as hexane are much more often used to precipitate active pharmaceutical ingredients in industry. Besides the solvation, all characterization methods from a colloid are measuring aggregates and agglomerates; some even measure a bigger diameter, a hydraulic one which includes one or several solvations or ionic layer depending of the technique.

In a dried state, measurements can be performed from an aerosol: LASER techniques such as Phase Doppler Analysis (PDA) suffer from a submicron limit of detection. The first stage of a Differential Mobility Analysis (DMA) technique is the neutralization of the aerosol from a radioactive source then particles are sorted by their mobility and so size, then counted by a Condensation Particle Counter (CPC); to overcome the size limitation, the CPS creates vapour from a working fluid (usually butanol, isopropyl alcohol, or water) which condenses onto the particles helping them grow in size and can be optically counted. It is important to notice that hard aggregates in aerosol can not be distinguished through DMA; surface area and volume can be corrected but the primary particle diameter has to be known already. However, DMA provides statistically significant and real time size distributions.

On static dried powder, particle size can also be extracted from BET theory by adsorption of a known gas. Diverse trials to investigate surface area and derive particle sizes from BET were found to be inefficient on n-RDX: no compromise between an appropriate degassing and a prevention of nanomaterial degradation and sintering could be established, due to high vacuum and heating that have to be applied on the sample (Section 1.4.2).

Direct particle observation should always be performed to verify the validity of the assumptions made from the other characterization techniques. Particle aggregation, particle morphology and degradation can be measured or at least reasonably estimated for particles under 50 nm . To reveal details at the nano scale, Atomic Force Microscopy is well suited for insulator nanoparticles. No energy is brought to the material but only a slight mechanical stress; imaging is performed at ambient temperature and pressure. Nevertheless, the tip is not a single point probe: the curvature radius and cone angle lower the heigh and also cause a "profile broadening" effect. Those side effects can be reduced by scanning in tapping mode and selecting a tip with a smaller radius to improve accuracy. However, a balance has to be found between the accuracy and the differential height that the tip can follow without being damaged. Therefore, when the particle size exceeds the hundreds nanometres, electron microscopy allows data acquisition on bigger areas in a minute.

### 3.1.2 AFM

### 3.1.2.1 Methodology

To overcome the difficulties encountered with SEM and to improve the accuracy, Atomic Force Microscopy is a good and obvious choice, especially when a laboratory has both apparatuses. For this reason, a standard procedure has been established prior to my arrival to measure particle size. To minimize the
roughness of the sample surface for an AFM tip, an original technique was introduced. The powder is pressed into pellets then its surface is flatten by the use of a rotary microtome.

A stainless steel tubular mould with an inner diameter of 4 mm is filled with the energetic material then closed with a stainless steel rod; the system is placed under a press where different weights can be hang on the extremity of a lever. The whole apparatus follows the pyrotechnic safety guidelines thanks to a mould with thick walls and a protective transparent screen. In this case, the mass of energetic materials is below 50 mg . The material is maintained under a pressure of 97 MPa for one minute, with transitions slowest as possible to avoid friction heat. Microtomy is done by a succession of cut thinner and thinner on one side of the pellet: five times $20 \mu \mathrm{~m}$, then five times $5 \mu \mathrm{~m}$ and finally five times $1 \mu \mathrm{~m}$ to remove superficial layers and have the smoothest surface. The quality of the surface preparation can be easily seen with the naked eye, by checking its great reflectivity.

The mean apparent density is $1.406 \pm 0.035 \mathrm{~g} / \mathrm{cm}^{3}$ from results reported in Table 3.1 which is in good agreement with densities from Pichot et al. (2015) and shows good reproducibility. The easy shaping of the powder into a cylindrical pellet is only possible thanks to the reduced particle size: pellets of the finer commercial available RDX with a PSD around $6.8 \mu \mathrm{~m}$ break apart (Spitzer et al. 2011). Moreover, pellet of n-RDX exhibits a glassy structure with transparency.

| Height $(\mathrm{mm})$ | Mass $(\mathrm{mg})$ | Density $\left(\mathrm{g} / \mathrm{cm}^{3}\right)$ |
| :---: | :---: | :---: |
| 1.09 | 19.69 | 1.395 |
| 1.61 | 28.42 | 1.377 |
| 0.92 | 17.33 | 1.462 |
| 1.56 | 28.04 | 1.395 |
| 2.08 | 38.89 | 1.451 |
| 1.50 | 26.23 | 1.357 |

Table 3.1 - Several apparent densities of pellets pressed at 97 MPa.

The analysis of height fields obtained by AFM is then made through a semi automatic process with the free and open source software Gwyddion (Nečas et al. 2012). Giwyddion is a modular program for SPM (Scanning Probe Microscopy) data visualization and analysis. It has been chosen thanks to its large number of data processing functions, including all the standard statistical characterization, the levelling and data correction, the filtering or grain marking functions. Among them, the watershed algorithm allows the detection of particles by local minima determination then image segmentation. The grain size analysis is made through several steps:

Grain localisation process the surface is inverted - hills become valleys - then virtual water drops are placed on each point. Then drops fall to the closest local minimum, following the steepest descent. The process is repeated and accumulated drops are forming lakes. Those small lakes filling the inverted surface depressions are the position of grains.

Segmentation While the drops are filling the surface, if a lake touches another one, they are merged in the previous step. In the segmentation step, drops are again falling but the growing lakes are not merged and their border is refined. The quality of grain boundary depends on the drop size set but computing time increases when the drop size is smaller.

Visual checking and corrections The software allows manual marking of grains and several contrast improvements to control and correct the results from the watershed method. The phase and amplitude channels can also help to determine the validity of a grain boundary.

PSD and fitting The software allows the direct display for the PSD but also can export the results. The diameter of a grain is computed from the diameter of a disc with the same surface area. A frequency count on the diameters renders the raw PSD; then the curve is fitted with a log-normal distribution function. Gaussian fitting is in poor accordance. Therefore, the PSD is generated by many small random effects that are multiplicative for the log-normal distributions (Limpert et al. 2001)

### 3.1.2.2 Effect of the concentration on the particle size

During his PhD in our laboratory, Risse studied the RDX concentration from $0.5 \mathrm{wt} \%$ to $2 \mathrm{wt} \%$ in acetone; as the concentration increases, the particle size decreases and so the specific surface increases. This can be linked to the increase of the degree of supersaturation with the concentration, therefore triggering a high nucleation rate. In this context, the first work of my PhD project was to start studying the crystallisation process and so the degree of supersaturation by extending that previous work.

SFE parameters were chosen from the optimized operating conditions: the nozzle temperature is set at $160^{\circ} \mathrm{C}$, the inlet pressure at 40 bar and the nozzle is an hollow cone one with a diameter of $60 \mu \mathrm{~m}$. The walls of the vacuum chamber from the nozzle to the cyclone are heated to $80^{\circ} \mathrm{C}$ to avoid any condensation and to reduce the losses of product by thermophoretic force. The solvent used for all the study is the same lot of acetone CHROMASOLV®, for HPLC, $\geq 99.9 \%$, from Sigma Aldrich. The same lot of RDX provided by Eurenco, labelled as M5, is used all along this study and this PhD project.


Figure 3.1 - Watershed analysis illustrated on simulated 200 nm spheres.

PSDs are determined by the previously mentioned method on pellets. XRD is also performed in order to calculate the apparent volume weighted domain size from the Scherrer equation as described in Section 1.4.2 p. 49. The sensitivity of the energetic powders is also quantified in order to investigate an eventual link with the mean particle size and crystallite size. Also the results are reported in Figure 3.2.

A parabolic trend could be interpreted from Figure 3.2e. However, the statistical significance of the result should be first performed. Thus, statistical analysis are made from the software GraphPad Prism 5 to compare mean particle size obtained from AFM pictures from one concentration to another. Table 3.2 shows that globally these means are not significantly different. Table 3.3 compares mean to each other and still no significance has been found.

The concentration of RDX in solution up to values close to the saturation does not influence the particle size according to the statistical analysis. Moreover, sensitivity remains constant among all samples: to up-scale the SFE process, such constant properties while increasing the RDX content is advantageous to increase the mass flow and so decrease the cost of the process.

The mean crystallite size is also always around 65 nm ; RDX particles are polycrystalline and the nucleation seems to be unchanged while changing concentration.


Figure 3.2 - Parametric study based on the variation of the concentration in solvent.


Figure 3.2 - Parametric study based on the variation of the concentration in solvent.

(e) Particle size against concentration

Figure 3.2 - Parametric study based on the variation of the concentration in solvent.

| $P$ value | 0.5734 |
| :---: | :---: |
| Are means signif. different? $(P<0.05)$ | No |
| Number of groups | 4 |
| $F$ | 0.7087 |
| R squared | 0.2100 |

Table 3.2 - One-way analysis of variance on the particle size from AFM pictures.

| Tukey's Comparison Test | Mean Diff. | q | Significant? | $95 \% \mathrm{Cl}$ of diff |
| :---: | :---: | :---: | :---: | :---: |
| $1 \%$ vs $2 \%$ | -20 | 1.519 | No | -79.64 to 39.64 |
| $1 \%$ vs $3 \%$ | 21 | 1.681 | No | -77.58 to 35.58 |
| $1 \%$ vs $4 \%$ | -6 | 0.4556 | No | -65.64 to 53.64 |
| $2 \%$ vs $3 \%$ | -1 | 0.09076 | No | -50.90 to 48.90 |
| $2 \%$ vs $4 \%$ | 14 | 1.189 | No | -39.35 to 67.35 |
| $3 \%$ vs $4 \%$ | 15 | 1.361 | No | -34.90 to 64.90 |

Table 3.3 - Tukey's multiple comparison test on the particle size from AFM pictures.

### 3.1.2.3 Reliability and accuracy

Risse also found that a crystallite size remained constant around 65 nm . However, the concentration had a significant influence on PSD from BET and SEM characterizations: the particle size decreased while the concentration increased. The mean particle size from SEM was $715 \pm 244 \mathrm{~nm}$ at $0.7 \mathrm{wt} \%$ and $408 \pm 175 \mathrm{~nm}$ at $2 \mathrm{wt} \%$ : those values were much higher than the mean particle size obtained from the AFM method.

No statistical assessment was performed previously and the repeatability of the previously work is questionable. The difference between SEM and AFM was a scientific question previously discussed. The high vacuum decreases the thermal stability of the energetic compounds which also have a very low vapour pressure ( $3.30 \times 10^{-9}$ Torr the vapour pressure of RDX at $25^{\circ} \mathrm{C}$ (Östmark et al. 2012)); it can be assumed that sublimation of the smallest particle leads to that significant difference in mean size. Sintering can also be strongly worsen by the energy brought by the electron beam.

To finally settle those long term doubts and question the reliability and accuracy of the pellet method, a parametric study was performed halfway across this PhD project thanks to the help of the ex-internship, currently PhD student, J-E Berthe. The uncertainty of the Watershed method was estimated and the following two key parameters were studied

- pressure applied
- microtomy

Uncertainty of the Watershed Method As implemented in the current version of Giwyddion (2.45), the Watershed Method suffers from a lack of optimization and synergy between the other correction tools of the software. To study the sole effect of the Watershed method, ideal AFM topographies of a virtual deposit of spherical particles were made through the build-in particle generator. In that way, all instrumental influence (AFM tip geometry, noise etc.) is totally suppressed as it can be seen from the Figure 3.1 p. 99.

Several tests were performed with different particle sizes, picture dimensions and surface sizes: values were taken from the AFM picture usually analysed. An alternative method introduced with the most recent updates was also tried: the threshold algorithm which relies on the height, slope and curvature parameters; those three options can be combined by union or intersection. The result of the algorithm is updated in real time but requires much more attempts. The Table 3.4 shows that the Watershed method is always more accurate than the threshold one due to more rigorous grain boundaries. However, the size is always minimized: this can be easily explained due to the boundary layer of
one pixel to mark grains. So the accuracy decreases with the particle size and the resolution since the missing pixels represent an higher relative area. As rule of thumb the mean particle sizes measured from AFM have to be increased by $10 \%$ for $1024 \mathrm{px} \times 1024 \mathrm{px}$ pictures and by $20 \%$ for $512 \mathrm{px} \times 512 \mathrm{px}$ pictures. The values reported in the previous study on the effect of the concentration are then corrected by $10 \%$.

|  | particle radius | resolution | simul. area | method | nbr. of anal- <br> ysed <br> part. | measured radius | deviation from the initial radius |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| unit | nm | lines | $\mu \mathrm{m}$ |  |  | nm |  |
| trimmed | 50 | $512 \times 512$ | $5 \times 5$ | threshold | 1445 | 36.75 | 27\% |
|  | 50 | 512x512 | $5 \times 5$ | threshold | 1406 | 36.75 | 27\% |
|  | 50 | 512x512 | $5 \times 5$ | watershed | 1474 | 40.25 | 20\% |
| trimmed | 50 | 1024x1024 | $5 \times 5$ | threshold | 1477 | 40.75 | 19\% |
|  | 50 | $1024 \times 1024$ | $5 \times 5$ | threshold | 1416 | 40.75 | 19\% |
|  | 50 | 1024×1024 | $5 \times 5$ | watershed | 1539 | 44.25 | 12\% |
| trimmed | 150 | $512 \times 512$ | $5 \times 5$ | threshold | 215 | 129.75 | 14\% |
|  | 150 | $512 \times 512$ | $5 \times 5$ | threshold | 177 | 129.75 | 14\% |
|  | 150 | $512 \times 512$ | $5 \times 5$ | watershed | 248 | 136.75 | 9\% |
| trimmed | 150 | 1024x1024 | $5 \times 5$ | threshold | 214 | 133.75 | 11\% |
|  | 150 | 1024×1024 | $5 \times 5$ | threshold | 176 | 133.75 | 11\% |
|  | 150 | 1024×1024 | $5 \times 5$ | watershed | 235 | 137.5 | 8\% |

Table 3.4 - Watershed and threshold method tested on simulated data; the 'trimmed' results mean that the grains at the edge of the picture are removed since they are probably trimmed. The Watershed algorithm add a one pixel boundary at the edges too, so trimmed grains cannot be removed easily.

Effect of the Pressure The press used for the compression of energetic materials consists of a lever supported by an hydraulic piston; at the extremity of the lever an hook allows to put several weights on it (from 5 kg to 97 kg ), then the piston is actuated to slowly lower the lever thus forming the pellet. The pressure applied on the sample is calculated according to the weights applied; values are reported in Table 3.5.

In the results reported in Figure 3.3, the same face was always inspected by AFM (the upper one here) and microtomy was not applied. The scan surface is $5 \mu \mathrm{~m} \times 5 \mu \mathrm{~m}$ in $1024 \mathrm{px} \times 1024 \mathrm{px}$. In Figure 3.3a clear drop of the mean size begins at 140 kg and then the value fluctuates around 90 nm : that change is

| Weight (kg) | Pressure (MPa) |
| :---: | :---: |
| 2 | 12 |
| 5 | 26 |
| 10 | 50 |
| 20 | 97 |
| 30 | 140 |
| 45 | 210 |
| 70 | 330 |
| 97 | 460 |

Table 3.5 - Weights used and their calculated corresponding pressures: the leverage follows the law $P=6 \cdot \frac{M}{A}+31$ where $A=\frac{\pi}{4} \cdot \varnothing^{2}$ with $M$ the mass of the weight.
also observed in Figure 3.3b with a shift and a major broadening of the particle distribution. On the AFM pictures in Figures 3.3c and 3.3d, particles are hardly identifiable.

The results from samples processed by microtomy in Figure 3.4 also demonstrate that the pressure has a significant influence on particle size. In that case, the particle size is reduced further and further with increasing pressure. Above $97 \mathrm{MPa}(20 \mathrm{~kg})$, the pellets start to be too glassy for microtomy; due to the the great hardness, the pellet breaks apart when the blade hits the sample.

Raw micron-sizedRDX (M5 Eurenco) were also investigated; the pellets are much less cohesive and were not flatten by microtomy. However, at the highest pressure of 97 MPa , a similar breakage appears with a much lower particle size. Therefore the milling of n-RDX processed by SFE is much easier; for industry, it would be interesting to find a balance between optimization of the SFE conditions and an additional rough milling/mixing step. Also this effect would have an huge impact on energetic pressed charges.

Effect of the Microtome From the curves in Figures 3.3a and 3.4a, the microtomy reduces the size. The surfaces from samples pressed at 97 MPa and processed by microtomy (Figure 3.4e) are quite similar to the samples pressed above the critical pressure and not processed by microtomy (Figure 3.3e).

Pressure reduces the inter-granular void which increases compactivity and hardness. Therefore, the blade of the microtome needs more energy to penetrate the pellet and a surface milling occurs reducing further the particle size.


(c) $26 \mathrm{MPa}(5 \mathrm{~kg})$

(d) $97 \mathrm{MPa}(20 \mathrm{~kg})$

(e) $460 \mathrm{MPa}(97 \mathrm{~kg})$

Figure 3.3 - Effect of the weight; same face, no microtomy, $5 \mu m \times 5 \mu \mathrm{~m}$ for $1024 p x \times 1024 p x$, enhanced contrast.

| Pressure (MPa) | Raw | With Microtomy |
| :---: | :---: | :---: |
| 12 |  | 280 |
| 26 | 180 |  |
| 50 | 170 | 230 |
| 97 | 235 | 140 |
| 140 | 100 |  |
| 210 | 80 |  |
| 330 | 110 |  |
| 460 | 90 |  |

Table 3.6 - Mean Diameters (nm) according to the pressure applied and the pre-treatment by microtomy; by SEM, the mean size is 500 nm .


Figure 3.4 - Effect of the weight; same face, processed by microtomy, $5 \mu \mathrm{~m} \times 5 \mu \mathrm{~m}$ for $1024 p x \times 1024 p x$, enhanced contrast.

### 3.1.2.4 Conclusion on the AFM pellet method

The particle size variation when adding PVP or PolyEthylene Cilycol (PEG) studied from SEM in Chapter 5 where initially discovered from the analysis of pellets by AFM. The exact same trend from SEM was also found from AFM picture analysis whose results can be found in Table 3.7. However, instead of a particle size around 160 nm as found by direct imaging in SEM, a mean value around 70 nm is measured. The content of polymer seems to have no influence on how brittle is the energetic material since PEG samples also have an increasing size with the PEG content: those results show that not only the hardness of the material is a major parameter but also the initial size of the particles. This seems to be valid only when the pressure applied is below the critical pressure. Another interpretation would be that this critical pressure changes; for instance it could
have decreased for RDX/PVP samples, thus leading to one of the smallest PSD ever observed on RDX.

| Compound(s) | Polymer content (wt\%) | Mean Diameter AFM (nm) |
| :--- | :---: | :---: |
| RDX/PVP40K | 1 | 66 |
| RDX/PVP40K | 1 | 73 |
| RDX/PVP40K | 1 | 67 |
| RDX/PVP40K | 0,5 | 165 |
| RDX/PEG400 | 1 | 965 |
| RDX/PEG400 | 0,1 | 180 |

Table 3.7 - Particle size from pellet imaging by AFM of some samples at 97MPa with microtomy.

SEM pictures were taken from pellets made from n-RDX by the pressing technique mentioned above, in order to observe at larger scales their surface. After being pressed and imaged by AFM, the sample is cut in half to be analysed by SEM on one piece; the other is used as a reference.

Thanks to the results in Figure 3.5, the surface of pellets appear to have two different areas: linear grooves and holes. The holes let the inside of the pellet to appear from outside; those are rough and bumpy which is a problem for AFM. However, the particles seen from inside are very similar in size and shape to the ones observed from the loose powder. In the Figure 3.7, the particles inside have the same rounded shape as in the loose powder. On the contrary, the grooves are smooth and made from the smaller particles; those areas are perfect for landing an AFM tip and scan. The AFM method suffers so from an additional bias which is the area segregation. To land the tip, to initialize the scan and to have a correct AFM picture, the tip is moved until the scanning area is flat enough: the biggest particles inside the holes of the pellet are never investigated. Surfaces of pellets of energetic materials are not representative of the loose powder of the same material.

The comparison between AFM and SEM of the same sample clearly illustrates the reason behind the particle size difference between those two techniques. The press hardens the pellet, the microtome mills the surface and scanning by AFM selects the flattest area where the smallest particles lies.


Figure 3.5 - SEM imaging of a 97 MPa pellet of RDX processed with $5 w t \%$ of $P V P$ 40000.


Figure 3.6 - SEM and AFM imaging of a 97 MPa pellet of RDX processed with $5 w t \%$ of PVP 40000.


Figure 3.7 - SEM imaging of one hole of a 97 MPa pellet compared to the loose powder of the same sample of RDX processed with $5 w t \%$ of PVP 40000.

### 3.2 One Technique, One Size

### 3.2.1 XDR

### 3.2.1.1 Determination of the apparent volume weighted domain size

From an XRD pattern, many information can be extracted. The mean crystallite size can easily be calculated from the Scherrer equation, the strain inside the crystal is available from more advanced analysis such as Williamson-Hall, and the morphology of the crystallite can even be 3D-modeled from a fine Rietveld refinement.

The Scherrer equation is a quick method to determine the average coherence length, so it is widely used. However, the value is calculated from the broadening which is influenced by many other physical parameters such as the lattice strain. Williamson et al. (1953) defined a alternative method taking into account the strain contribution into the broadening. Explained in the Section 1.4.2 p. 49, the analysis relies on plotting $\beta \cos (\theta)$ as a function of $\sin (\theta)$ and fitting it to an affine function where the slope is directly related to the strain.

Results in Figure 3.8 show the attempt to fit five n-RDX samples crystallised through SFE in the same operative conditions. The sub-figure A, on the left, illustrates different approaches in measuring the Full Width at Half Maximum (FWHM) according to the angle: due to the poor accuracy of the peak per peak measurement (peak fit from Origin or manual peak marking in EVA), data seems to be linear in the range 0.1-0.2. This also explains the large difference with the Full Pattern Matching (FPM) analysis: FPM relies on the whole pattern allowing a large number of peaks to be analysed by an algorithm. The usual mathematical functions to fit XRD peaks are implemented in the code, and the software compares the experimental data to the theoretical hkl planes calculated from the space group. The FPM is therefore more accurate, computes a large dataset and has a real meaning. Our XRD diffractometer does not filter the $K_{\alpha 2}$ ray of the Cu source: so each peak is actually a double-peak. The FPM as implemented in Fullprof can fit the pattern knowing the peak position for each radiation thus deconvoluting each peak in two. The peaks shape was fitted with a Thompson-Cox-Hastings pseudo-Voigt convoluted with axial divergence asymmetry function (Finger et al. 1994).

In Figure 3.8, only two samples could have been fitted into a linear regression. The other three evolve into parabolas. Such diverging results clearly indicates that the Williamson-Hall theory does not describe accurately the peak broadening.


Figure 3.8 - Williamson-Hall of n-RDX processed by SFE at $2 w t \%$ in acetone.

### 3.2.1.2 Rietveld refinement

The Rietveld refinement allows the fine analysis of the crystals properties (size and strain according to several models, hkl shifts, asymmetry, preferred orientation etc.) but also a complete segregation with instrumental effects on the pattern.

In most implementation of the Rietveld method, to refine crystallite structures, the microstructure (size and strain) of each lattice is modelled by considering only an average crystallite size. Although this technique gives good results, it is important to notice that the real sample has a distribution of the crystallite sizes. Usually such models for the crystallite size approximate the crystallite shape with a sphere. Some even more complicated models consider a specific morphology of the crystallites. But, the best results for the average crystallite size are obtained by modelling its shape in the reciprocal space with an expansion of symmetrized spherical harmonics; then the corresponding crystallite shape obtained in the real space would be the one obtained from direct imaging of the primary particles.

The micro-structural analysis from Rietveld refinement is implemented in several size broadening models into the free software Fullprof. We will be using the Anisotropic Lorentzian size broadening: it considers the size broadening as a linear combination of spherical harmonics (SPH). The anisotropic size is
supposed to contribute to the Lorentzian component of the total Voigt function. After refinement of the coefficients the program calculates the apparent size (in Ångströms) along each reciprocal lattice vectors if the instrumental resolution is provided.

A preliminary calibration of the peak broadening due to the apparatus is performed on $\mathrm{LaB}_{6}$ : the resulting refinement can be seen in Figure 3.9. If the peak broadening is too close to the instrumental resolution, the software will not refine the peak. The Table 3.8 contains the values used for all the following Rietveld refinement. $\mathrm{U}, \mathrm{V}$ and W are parameters used to model the change of the FWHM with the angle from the instrument, by the equation $H^{2}=U \tan (\theta)^{2}+V \tan (\theta)+W$. The peak shape for $L a B_{6}$ is a Pseudo-Voigt; the parameters were adapted from the instrument parameter and input files of the Beamline 11-BM of Argonne National Laboratory. Then, n-RDX patterns are refined using a Thompson-Cox-Hastings pseudo-Voigt convoluted with axial divergence asymmetry function as the peak shape (Finger et al. 1994). Therefore, the FWHM of the Gaussian ( $H_{G}$ ) and Lorentzian $\left(H_{L}\right)$ components are calculated as:

$$
\begin{gather*}
H_{G}^{2}=\left(U+D_{S T}^{2}\right) \tan ^{2} \theta+V \tan \theta+W+\frac{I_{G}}{\cos ^{2} \theta}  \tag{3.1a}\\
H_{L}=X \tan \theta+\frac{\left[Y+F\left(S_{Z}\right)\right]}{\cos \theta} \tag{3.1b}
\end{gather*}
$$

Much more technical details can be found in the manual and help provided with FullProf.

| Uins | Vins | Wins | Xins | Yins | Zins |
| :---: | :---: | :---: | :---: | :---: | ---: |
| 0.001356 | -0.005000 | 0.003910 | 0.063891 | 0.000083 | 0.0 |
| 0.001356 | -0.005000 | 0.003910 | 0.063891 | 0.000083 | 0.0 |

Table 3.8 - Instrumental resolution determined from $L a B_{6}$ pattern refinement.
The Rietveld refinement requires some expertise and patience to analyse with accuracy and avoid any divergence of the parameters toward non physical meanings. The process is made step by step following this sequence:

1. Scale factor
2. Scale factor, zero point of detector, lattice constants. The background is refined if the background subtraction from EVA is not satisfactory.
3. Atomic positions

## ALS 11-BM - NIST SRM 660a LaB6



Figure 3.9 - Rietveld refinement performed on $L a B_{6}$.
4. Peak shape and asymmetry parameters
5. Atom occupancies
6. Microstructural parameters: size and strain effects. The model used is the Anisotropic Lorentzian size broadening (Spherical Harmonic) with the Laue class mmm, which allows the crystallite morphology determination.

The experimental pattern, refinement and residual are frequently checked during the refinement process. The final results are found in the Figures 3.10 to 3.14: the curves in black is the refined pattern, in red the experimental data and in blue below the first two is the residual. The small ticks between the residual and the curves are the hkl positions from $K_{\alpha 1}$ and $K_{\alpha 2}$ rays of the Cu source. The refinement takes a dozen minutes, with an increasing computation time when adding parameters to refine. Also the refinement diverges easily, corrupting the input file. Dozens of refinements were saved per samples with reducing $\chi$; attempts increasing $\chi$ were not saved but are sometimes used to start from original values leading afterwards to a more accurate solution.

The refinements of the sample of $n-R D X$ processed pure at $3 w t \%$ acetone in Figure 3.11 and the one with a $80 \mu \mathrm{~m}$ nozzle in Figure 3.14 are acceptable but
less accurate than others, with a negative residue on the angles at small angles and a positive residue on angles above $20^{\circ}$. Finding a realistic refinement was the most difficult issue to solve: having a refinement accurate enough with no bias -such as that angular dependency- and an acceptable 3D model at the same time. The results shown here are the best refinement possible with a realistic 3D model. The three other refinements are in very good agreement with the experimental data.


Figure 3.10 - Sample of n-RDX processed pure at $2 w t \%$ in acetone.


Figure 3.11 - Sample of n-RDX processed pure at $3 w t \%$ in acetone.
A global appreciation on the refinement would be a more accurate fitted solution with the smallest particles. Beyond the inherent difficulty of the micro-
structural analysis by the Rietveld theory, the organic crystals exhibit a large number of peak with many overlaps, and a natural broadening due to a lattice crystalline less ordered, which is far from the ideal condition.

Nevertheless, all the models seem to converge on spherical particles slightly flattened on two planes (4 faces/extremity). This oblate geometry is correlated to an almost homogeneous growth with no preferential direction growth. Size and morphology found with those analysis are then compared to the particle size and morphology obtained by AFM on pellets and on the smallest particles imaged on SEM.


Figure 3.12 - Sample of n-RDX processed with $0.1 \mathrm{wt} \%$ of PEG.


Figure 3.13 - Sample of n-RDX processed with 10 wt\% PVP.


Figure 3.14 - Sample of n-RDX processed with 1 wt\% PVP with a $80 \mu m$ nozzle

### 3.2.2 Smallest observable object

In order to assess the problem of the particle size and definition of a particle, a new deposit technique for SEM was developed recently in our laboratory: it is based on the rubbing of the powder between two glass sheets. Individual and very small particles have been found to be more easily observed on a glass support. The method is still under investigation, especially to explain the influence of the support. However the spreading due to the rubbing allows the distinct imaging of the smallest particles. The particle size and morphology is studied through SEM and compared to the results from Rietveld refinement. The aim of this study is to answer to the questions of the crystallinity and aggregation of n-RDX processed by SFE.

Spray techniques may produce particles made from much smaller primary particle: Qiu et al. (2015) successfully probed the interior of their micrometer spheres (RDX) to found out a gradient of the primary particle size at the submicrometer scale. Focused ion beam (FIB) is the technique used to make the cross-sections: even if a low probe current helps to preserve the sample (Cierak 2009) no attempt has already been reported on energetic materials. An easiest solution is to use the rubbing deposition technique to image the smallest particles. Results reported in Table 3.9 show that the RDX processed with polymers actually exists as single crystals. On the contrary, the smallest pure n-RDX are still polycrystalline. The oblate shape found by Rietveld seems consistent with morphology imaged by SEM, as it can be seen in Table 3.9.

AFM on pellets of those samples were also analysed. As seen in Figure 3.16,

|  | Average apparent <br> size and standard <br> deviation <br> (anisotropy) <br> $(\AA)$ | Average maximum <br> strain and standard <br> deviation <br> $($ anisotropy $)$ <br> $(\%(\times 10000))$ | Smallest Particle <br> Sizes from SEM <br> $(\mathrm{nm})$ |
| :---: | :---: | :---: | :---: |
| pure at $2 \mathrm{wt} \%$ in | 716 | 5.53 | $180-200$ |
| acetone | $(28)$ | $(0.0039)$ | $125-140$ |
| pure at $3 \mathrm{wt} \%$ in | 814 | 3.23 |  |

Table 3.9 - Smallest particle imaged on SEM compared to the computed average apparent size from Rietveld refinement.


Figure 3.15 - One of the smallest particle ( $63 \times 58 \mathrm{~nm}$ ) observed by SEM on RDX processed with $10 w t \%$ PVP.


Figure 3.16 - n-RDX processed with 10 wt\% PVP.
even much smaller particles were measured -after the surface milling- when adding more polymer and reducing the original particle size (the ones imaged by SEM). For pure n-RDX the sizes of the smallest particles stay in the same range as the particle size from AFM below the critical pressure without microtomy: this confirms that due to the segregation by AFM the smallest particles are scanned, thus implying that below the critical pressure the particles may stay unbroken. Those results raise again the question of the hardness of the nanoparticles. Since the smallest particles imaged in SEM are bigger than the one observed by AFM, the rubbing method does not bring an energy (friction work and pressure) as high as in the case of the AFM pellets: that technique seems suitable to spread the particles without breaking the brittle particles.

### 3.3 Summary of the Chapter

Several sizes have been measured depending on the technique and the conditions. By AFM, pellets are imaged, without or with microtomy to flatten the surface; many samples were analysed by this technique at 97 MPa plus microtomy such as the result reported by Spitzer et al. (2014) or the preliminary study with a range of RDX content. Classical SEM were made on loose powder and pellets, and a rubbing technique has been developed to spread particles on a glass substrate in order to image the smallest particles. The lattice structure and the apparent volume weighted domain size were computed from Rietveld
refinement. All that high amount of data were interpreted and correlations between techniques have been found.
n-RDX can be broken in smaller particles by compression. For pure compounds and below a critical pressure, the particles observed by AFM are about 200 nm with a irregular round shapes; that size and morphology is the same as imaged on the smallest particles, by the rubbing technique by SEM. When using a microtome on n-RDX pellets, the surface is milled and the blade imperfections imprint grooves on the surface or strip off parts which reveal the original particles inside the pellet, as seen by SEM. By AFM a segregation is made by the roughness of the surface: those holes with bigger particles are never scanned on the pellets processed by microtomy, thus only the smallest particles are counted. That bias also explains why size and shapes on AFM can be identical to the smallest particles imaged on SEM.

XRD patterns analysed by Rietveld refinement reveal an average apparent size around 80 nm with an oblate morphology for all samples, meaning that an homogeneous growth occurs in all SFE conditions. The smallest particles imaged by SEM seem to be single crystals in the case of n-RDX processed by polymers.

As the particles sizes after mechanical stress depend on purity and quantity of polymer, the hardness is probably a key property for a deeper comprehension of the phenomenon reported in this chapter. Nano indentation is used to study the mechanical properties of material: Hudson et al. (2012) found that micron-sized crystals with many internal defects have reduced modulus of elasticity, stiffness and prone to greater deformation under applied load, therefore correlate shock sensitivity and stiffness/elasticity. Nano mechanical tests can be done under the direct visualization of an SEM or Transmission Electron Microscopy (TEM). However, due to the already mentioned difficulties to image energetic organic nanoparticles, such experiments would require a dedicated scientific study.

After being able to define an absolute particle size representative of the sample, the reduction of the particle size can be studied without bias; the crystallisation has to be controlled in both space and time resolution. Two main approaches have been established, a chemical one and a more physical one. The next chapter focuses on the physical attempt by the exploration of various supersaturation conditions, just after introducing all the needed concepts for the formation of organic crystal, with a specific focus on the nucleation.

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## Chapter 4

## Crystallisation study and comprehension of the SFE process

### 4.1 Crystallisation, Nucleation and supersaturation

Crystallisation from solution occurs when the concentration of the compound is higher than its solubility, namely in the supersaturation zone. Various strategies can be used since the solubility depends on the temperature, the solvent(s) and other compound(s): temperature change (cooling in the case of a positive gradient $\frac{d C}{d V}$ of the solubility curve or heating in the case of a negative one), solvent removing (evaporation), addition of a drowning-out agent (an anti-solvent) or reaction partners. But achieving the supersaturation may not be enough; to trigger the crystallisation in that metastable system, an external energy (stirring, mechanical shock, friction or extreme pressures) or a seed (impurity or a crystal of the compound) can be brought to the solution. Others stimuli such as electric and magnetic fields, spark discharges, UV light, X-rays and ultrasonic irradiation have also been studied since decades (Atwood et al. 1969) but no application in large-scale crystallisation has been ever reported.

Three types of nucleation can be distinguished. The secondary nucleation occurs when a crystal already exists: a seed triggers the nucleation of the metastable solution or the compound nucleates on the surface of the growing particles. Primary nucleation can be spontaneous -homogeneous nucleation- or triggered by impurities -secondary nucleation-. Since impurity free solutions are virtually impossible, cases are often reported when a system nucleates at a few degrees lower than predicted or than the previous smaller batches (Mullin 2001). The exact formation of nuclei is still not known (Sosso et al. 2016). The molecules have to coagulate, then to resist to re-dissolution but since the lattice faces are not equivalent, the molecules should have the right orientation. Even

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 124the mechanisms are not resolved yet, a nucleus has to achieve a critical size to actually grow into a crystalline particle. From the Classical Nucleation Theory, the critical radius corresponds to the one minimizing the overall excess Cibbs energy $\Delta G$ :

$$
\begin{align*}
\Delta G_{1} & =\Delta G_{S}+\Delta G_{v} \\
= & 4 \pi r^{2} \gamma+4 / 3 \pi r^{3} \Delta G_{v}  \tag{4.1}\\
\Rightarrow>\frac{d \Delta G}{d r} & =8 \pi r \nu+4 \pi r^{2} \Delta G_{v}=0  \tag{4.2a}\\
\Rightarrow r_{c} & =\frac{-2 \gamma}{\delta G_{c}} \tag{4.2b}
\end{align*}
$$

$\Delta G_{I S}$ is the excess Cibbs energy between the surface of the particle and the bulk, and $\Delta G_{V}$ is the volume excess Cibbs energy between a large (infinite) particle and the compound dissolved. $\Delta G_{S}>0$ while $\Delta G_{V}<0 . \Delta G_{S}$ relies on the interfacial tension -also called surface energy- $\gamma$ and $\Delta G_{v}$ is the volumetric volume excess Cibbs energy. Therefore, critical overall excess Cibbs energy can be expressed as:

$$
\begin{equation*}
\Delta G_{c}=\frac{16 \pi \gamma^{3}}{3\left(\Delta G_{v}^{2}\right)} \tag{4.3}
\end{equation*}
$$

The supersaturation $S$ is expressed as a ratio between the concentration $c$ and the solubility $s$ at the given temperature: $S=c / s$. With the Cibbs-Thomson relationship, the supersaturation becomes with $v$ the molecular volume:

$$
\begin{equation*}
\ln S=\frac{2 \gamma V}{R T r}=\frac{2 \gamma v}{k_{B} T r} \tag{4.4}
\end{equation*}
$$

So from the Equations (4.3) and (4.4), we can finally express the critical overall excess Cibbs energy with the supersaturation:

$$
\begin{equation*}
\Delta G_{c}=\frac{16 \pi v^{3} v^{2}}{3\left(k_{B} T \ln S\right)^{2}} \tag{4.5}
\end{equation*}
$$

To go further, the rate of nucleation can be written as an Arrhenius velocity equation $J=A \exp \left(-\Delta G_{1} / k T\right)$, which is given from Equation (4.5)

$$
\begin{equation*}
J=A \exp \left(-\frac{16 \pi \nu^{3} v^{2}}{3\left(k_{B} T\right)^{3}(\ln S)^{2}}\right) \tag{4.6}
\end{equation*}
$$

The rate of nucleation finally relies on the temperature, surface energy and the supersaturation, and has been plotted in Figure 4.1a; after a critical value


Figure 4.1 - Rate of nucleation against the supersaturation.
the rate increases rapidly up to an asymptotic rate. The experimental values in Figure 4.1b are in good agreement with a sudden increase followed by a plateau.

However, many efforts have been devoted since 2010 to extend and improve the Classical Nucleation Theory (CNT) (De Yoreo 2013; Gebauer et al. 2014; Vekilov 2010b; Zahn 2015). On the contrary of melts where the liquid is dense enough to neglect concentration gradients and related phenomena, the case of crystal nucleation of molecules in solution is quite different. A significant concentration fluctuation is required to bring the needed number of molecules to construct the nuclei. That's why a two-step mechanism was developed recently where two free energy barriers have to be overcome instead of an unique one expressed in Equation (4.1) from the CNT: as displayed in Figure 4.2, the first one illustrates the density variation to create a primary cluster of molecules, then the second one describes the ordering of those clusters into the crystalline nuclei. Early stages of the nucleation of organic crystals have been investigated using Molecular Dynamics (MD) backed up with experimental data from singlemolecule real-time transmission electron microscopy (SMRT-TEM); Salvalaglio et al. $(2015,2012)$ demonstrated that different solvents can lead to different
nucleation mechanisms such as a single-step nucleation process favoured for urea molecule in methanol and ethanol and a two-step mechanism in acetonitrile and water.


Figure 4.2 - Two possible scenarios from the two-step nucleation mechanism: the first one involves an intermediate state at a higher energy due to an unstable dense liquid existing as mesoscopic clusters, and the second lower curve applies if the dense liquid is stable $\left(\Delta G_{L-L}^{0}<0\right)$

The link between the rate of nucleation and the crystal size is far of being established since several phenomena follow the nucleation: the firstborn nuclei are subject to growth but also aggregation. Thus an optimal value of the supersaturation exists for each system; a supersaturation too high would lead to aggregation and also to secondary nucleation on growing particles.

### 4.1.1 Increasing Supersaturation in SFE with an Anti-solvent

The key to control crystallisation and so particle size is to determine the supersaturation which is time dependent but also is unique in each droplet. Supersaturation, as a function of time and coordinates, was not available: since we were not able to determine in situ droplet size distribution, extreme variations of the supersaturation are investigated. Therefore, a suitable anti-solvent for RDX and for SFE has been searched in order to increase the supersaturation by reduced solubility. Water is commonly used as drowning out agent for RDX recrystallisation (Essel et al. 2012; Gallagher et al. 1992; Lee et al. 2014), but due
to a high temperature of evaporation and a modest heat capacity ( $75.28 \mathrm{~J} / \mathrm{mol} \mathrm{K}$ at $25^{\circ} \mathrm{C}$ ), such solvent can not be processed by SFE: a flash evaporation can be triggered but a quick condensation will occur thus wetting the particles.

(a) Vapor-Liquid Equilibrium (VLE) diagram

| pressure | temperature $(\mathrm{K})$ | x (acetone) |
| :---: | :---: | :---: |
| 1 bar | 323 | 0.648 |
| 7 mbar | 228.5 | 0.621 |

(b) Azeotropes

Figure 4.3 - VLE of the binary system acetone-hexane at 1 bar (solid lines) and 7 mbar (dashed lines): the data at 1 bar are obtained from the Dortmund Data Bank, and curves at 7 mbar are computed from ProSim.
n-Hexane is a perfect non-polar solvent of RDX (PANT et al. 2013). n-Hexane is miscible with acetone and has a low boiling point of 342 K at atmospheric pressure, a high vaporization enthalpy around $31 \mathrm{~kJ} / \mathrm{mol}$ and a remarkably high heat capacity of $195.8 \mathrm{~J} / \mathrm{mol} \mathrm{K}$ at 298 K . All of those thermodynamic properties are better than any solvent studied by PANT et al. (2013). Moreover, n-hexane forms an azeotrope with acetone: Vapour-Liquid equilibrium data at ambient pressure are plotted in Figure 4.3a. Values at reduced pressure close to the

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ones in the SFE are computed by ProSim using the Non-Random Two-Liquid (NRTL) model for the activity coefficients. The UNIFAC model was also tested, but lowered the bubble point temperatures by 0.2 K with no change on the azeotrope position. The VLE of an n-hexane/acetone system exhibits significant lower bubble points than both of the boiling temperatures: the azeotrope at atmospheric pressure is $7^{\circ}$ lower than the standard boiling point of acetone and $19^{\circ}$ lower than the one of n-hexane.

Beside increasing the supersaturation with a binary system solvent/anti-solvent, an original approach was developed: to understand the flash-evaporation mechanisms, especially the life-time of droplets and the time dependant crystallisation, the SFE system has been upgraded with a second nozzle. An entire second channelling for the new nozzle has been added and build on an existing system. Also the nozzles have to be oriented to effectively overlap the hollow spray cone: to achieve that the piping system has been reconsidered. The Figure 4.4 describes the new system. Due to technical limitations, a lateral distance between the inlet pipe has to be kept and the channelling has to remain parallel up to the heating elements. Therefore the distance between the end of an heater and the nozzle has been minimized and the stainless steel pipes insulated to prevent heat loss. From the experiments made in Section 4.2.2, an optimal angle around $70^{\circ}$ has been found and used here. For the present study, one system is used to spray RDX dissolved at $2 \mathrm{wt} \%$ in acetone through a $60 \mu \mathrm{~m}$ nozzle; the other one sprays n -hexane trough a $80 \mu \mathrm{~m}$ nozzle in order to permanently have a higher flow of hexane over acetone and so to maximize the overlapping. The system was patented in the international version of the patent ("Method for producing cocrystals by means of flash evaporation" 2016).

Several molar ratio were tried: very near the azeotrope at $x_{\text {acetone }}=0.642$ and two others flanking the azeotrope from far. But due to the specific boiling point curve of the acetone/n-hexane, the three ratio $x_{\text {acetone }} 0.573,0.642$ and 0.817 correspond to the same boiling temperature at atmospheric pressure and below. Therefore the driving force of the SFE, the superheating, is kept constant and only the variation of the saturation over time varies. Then after the flash of droplets, it assumed that the nucleation already occurred and classical evaporation applies. Finally, depending on the ratio the rare remaining drops will either enrich in acetone ( $x_{\text {acetone }}=0.817$ ) or in hexane ( $x_{\text {acetone }}=0.573$ ): that phenomenon could provoke the generation of a secondary PSD. Only a single peak following a log-normal distribution is found from the frequency count of particle size determined by SEM. The classical evaporation is negligible.

The overall mean diameter of RDX particles is quite high; for instance the reference -pure RDX at $2 \mathrm{wt} \%$ in acetone- result in a mean diameter of 790 nm instead of the usual 500 nm (Doctoral Thesis Risse 2012). Such an increase


Figure 4.4 - The dual nozzle system.


Figure 4.5 - PSD for RDX processed in the binary system acetone/n-hexane by SFE through one or two nozzles; the legend shows the molar ratio of acetone and in parenthesis the mean diameter in nm.

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suggest a deterioration of the flash-evaporation due to a lower superheating: the dual nozzle is less efficient to keep the solvent superheated from the heaters to the nozzles because the distance induces higher heat losses. However, the flash-evaporation characteristics such as broadened spray and a lower vacuum pressure are still observed.

From Figure 4.5, the ratio of hexane clearly decreases the particles size from around 800 nm down to around 550 nm . That lower bound already appears for $x_{\text {acetone }}=0.642$. Increasing the supersaturation up to a certain degree seems to improve the nucleation rate and therefore the particle size with no drawback due to aggregation. The experiment using two nozzles is very informative: droplets have enough life time for an effective overlapping. A possible interpretation would be that acetone droplets are first in a metastable state with no nucleation and no flashing thus allowing them to collide and merge with hexane droplets. The sudden saturation due to a lower solubility in the system acetone-hexane triggers the nucleation in the same conditions as for the one-nozzle at ratio 0.573 and 0.642 . So the overlapping induces a ratio of acetone lower than 0.817 .

The dual nozzle system has many advantages; in order to increase the mass flow rate, the percentage of the compounds in solution can be raised, then crystallisation is triggered by a second solution containing a drowning out solvent or a crystallisation partner. Advanced chemistry could also be explored when the reactive species should not be mixed until a thermal activation. Two points have to be confirmed first: the droplets interpenetrate each others from both sprays and hexane is not already gaseous thus drying acetone droplets. Therefore a reactive specie is added to the second solution: the cocrystallisation of CL-20:HMX 2:1 is chosen and explained in Section 4.2.

### 4.1.2 Supersaturation Determination

The supersaturation is a key element which will be unveiled by using the latest advances in LASER and phase Doppler analysers. Particle Image Velocimetry (PIV) were first tried at ambient pressure but is not suitable due to the hight density of the spray and limited spatial resolution of the technique. The LASER Doppler technique was first proposed in 1964 by Cummins et al. (1964) but was widely used only in the 70's. The phase Doppler technique exhibited a similar development about 20 years later from Bachdo et al. (1984), Bauckhage et al. (1984), and Saffman et al. (1984). The recent advances in signal filtering and analysis allows now the light-scattering interferometry to simultaneously record in real time object velocities and size distribution. The principle of Phase Doppler Analysis (PDA) is illustrated in Figure 4.6. A measurement volume is defined by the intersection of two focused LASER beams: the light is scattered by the particles passing through this volume. The second refraction order is
specifically used by the three detectors of the PDA probe. Each detector is pre-aligned and converts the optical signal into a Doppler burst with a frequency linearly proportional to the particle velocity. Then the phase shift $\phi$ between the Doppler signals from different detectors allows the calculation of the particle diameter D :

$$
\begin{equation*}
\Phi=\frac{-2 \pi D}{\lambda} \frac{n \sin \theta \sin \psi}{\sqrt{2(1+\cos \theta \cos \psi \cos \varphi)\left(1+n^{2-n} \sqrt{2(1+\cos \theta \cos \psi \cos \varphi)}\right)}} \tag{4.7}
\end{equation*}
$$



Figure 4.6 - Principle of the Phase Doppler analysis (PDA) in a glance (Dantec Documentation).

Preliminary results from a demonstration apparatus are reported in Figure 4.8. No calibration were performed to assess the accuracy of the apparatus. No optimizations nor quantification of the error were done. However, the droplets are clearly extremely small around the microns or even lower; the closer we are to flash evaporation, the smallest are the drops. The velocity is also very


Figure 4.7 - PDA in situ measurements for SFE.
high with an order of magnitude of $2(100 \mathrm{~m} / \mathrm{s})$ : it is one order above the rare velocities reported in flash-evaporation of spray by Gebauer et al. (2015) and Miyatake et al. (1981). Those preliminary data confirm that the SFE process involves high energy and fast crystallisation. It can be estimated than after 1 cm from the nozzle the spray is no more visible, which could implies that after only $0.1 \mu \mathrm{~s}$ the evaporation is complete and the crystallisation performed.

More reliable results were acquired thanks to the work of Mr Lasserre to deliver us an operational PDA apparatus quickly after the purchase. The beams were focused a few millimetre after the nozzle orifice and as closest as possible to the nozzle axe. The PDA were stabilized and operated in coincidence mode (the velocity measured by Laser velocimetry is coupled to the measurement of the diameter by Phase Doppler interferometry, resulting in the exact measure of both for each object in the measurement volume) with a sequence of 10 measurements each with 20k objects measured ; the receiving optics adjusted for the highest rate of coincidence and optimized with the Laser power. About the SFE, the temperature is stabilized for 15 min before each sequence. Each batch from the set of ten is compared to each other: no changes is the PSD has been noticed in a set of measurement for a given temperature so all the 200 k objects measured per temperature are concatenated to render the Figure 4.9.

While the temperature is raised the droplet size clearly decreases close to the detection limit around one micron. Moreover the polydiversity exhibited for each PSD is reduced while increasing the temperature; multi peak fitting reveals three modes centred at 2.1, 2.8 and $3.8 \mu \mathrm{~m}$ at all temperatures. The


Figure 4.8 - Preliminary measurements from a demonstration apparatus inside the SFE under vacuum while spraying acetone. Acquisitions were performed at two different axial distances from the nozzle orifice: at around 4 mm or quite far at around 1 cm

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center of gravity doesn't change with temperature but only the area. Therefore at such temperatures the SFE is under a transition state toward flash evaporation which seems to be the dominant phenomenon at temperatures around $160^{\circ} \mathrm{C}$. To complete this study, the influence of the nozzle type should be study to evidence a potential change in the centre of gravity of the modes.


Figure 4.9 - Particle Size Distribution of droplets of acetone spayed at 100, 140 and $160^{\circ} \mathrm{C}$.

### 4.2 CL-20:HMX 2:1 Cocrystal as a Tool for Understanding Crystallisation by SFE

### 4.2.1 Cocrystallisation

A cocrystal consists in the combination of two or more electrically neutral molecules within a single crystal lattice in a stoichiometric ratio. The exact definition is still under debate (Sun 2013) but hydrates and solvates are usually excluded. The constitutive compounds are often called co-formers. While cocrystals are known to potentially combine the drug effect of two Active Pharmaceutical Ingredient (API)s (Vishweshwar et al. 2006), it is interesting to notice that historically the pharmaceutical industry first avoided cocrystal, the racemic ones (Toda et al. 1997).

The formation of an existing cocrystal and the crystals of the co-formers relies on their solubility. A Phase Solubility Diagram (PhSD) shown in Figure 4.11

(a) $100^{\circ} \mathrm{C}$

(b) $140^{\circ} \mathrm{C}$

(c) $160^{\circ} \mathrm{C}$

Figure 4.10 - Peak fitting of the PSD of droplets of acetone spayed at 100, 140 and $160^{\circ} \mathrm{C}$.


Figure 4.11 - Phase Solubility Diagram (PSD) of a 1:1 AB cocrystal from co-formers $A$ and $B$; in red the solubility curve of the $A$ crystal, in blue the one of $B$, and in green the cocrystal. Arrows illustrate a possible crystallisation by addition of $B$ to the solution followed by the cocrystallisation.
depicts the co-former concentrations in a solvent at equilibrium at a given temperature with the different domain for each crystals (Nehm et al. 2006). The domain I is saturated in A and under saturated with respect of the cocrystal AB : only polymorphs from A can be crystallised. In the domain II both $A_{S}$ and $A B_{S}$ crystallises; the domain IV is situated above the solubility curve of the cocrystal and thus allows the crystallisation of the $A B_{S}$ alone. In the domain III, the solution is under saturated for all species and no crystallisation can occur.

Unlike the PhSD, the triangular phase diagram (TPD) in Figure 4.12 shows the total composition of the system. Chiarella et al. (2007) explained why the formation of cocrystals could not occur while having the appropriate stoichiometry and underlined the need of covering a wide range of ratio when screening for cocrystals (Chadwick et al. 2009).

Beside those thermodynamic properties at equilibrium, kinetics prevail especially when crystallising from multicomponent systems. Ostwald (1897) speculated that the critical cluster to nucleate from a supercooled liquid may not be

### 4.2. CL-20:HMX 2:1 COCRYSTAL AS A TOOL FOR UNDERSTANDING CRYSTALLISATION BY SFE



Figure 4.12 - Ternary Diagram of a 1:1 AB cocrystal from co formers $A$ and $B$; coloured curves are the solubility curves from Figure 4.11.
the most stable polymorph but the polymorph closest in energy to the liquid phase. Since 1897, this behaviour has been observed a number of times (ten Wolde et al. 1999).

### 4.2.2 CL-20:HMX 2:1 Cocrystallisation from SFE

The SFE has already proved to be a suitable method to cocrystallise from a solution at the dried state (Spitzer et al. 2014). However to ensure a complete comprehension of the cocrystallisation by SFE, PhSD at several temperatures should be established for each compound such as the caffeine and acid glutaric from Yu et al. (2010). Unfortunately no PhSD nor ternary diagram exists for the CL-20:HMX 2:1 cocrystal.

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In order to confirm the existence of metastable droplets in a state where no nucleation nor flash-evaporation occurred, an experiment with the co-formers sprayed separately was designed: the first dual-nozzle system was build for those experiments. Instead of an angle of $70^{\circ}$, the nozzles were oriented at $45^{\circ}$ as illustrated in Figure 4.13.


Figure 4.13 - First dual nozzle system with an orientation at $45^{\circ}$.

The solutions of CL-20 and HMX were prepared in the stoichiometric ratio 2:1 of the cocrystal, using acetone (CHROMASOLV $®$, for HPLC, $\geq 99.9 \%$ Sigma Aldrich). The Figure 4.14 shows mean PSD of the samples obtained through that technique; the method used is the AFM on pellets explained in the Section 3.1.2. Therefore, even if the mean size obtained here of 73 nm can not be interpreted as an absolute size, it can be compared to other samples processed by this technique: 73 nm is among the smallest mean sizes counted for $\mathrm{n}-\mathrm{RDX}$-more specifically the RDX processed with PVP- meaning that an absolute size under 300 nm can be excepted.

X-ray Diffraction was performed on samples processed from that dual nozzle setup. The XRD pattern in Figure 4.15 exhibits two crystalline structures: the main crystals present is $\beta$-CL-20 but the cocrystal is confirmed to have crystallised from the overlapped sprays. $\beta$-CL-20 is the least stable polymorph of CL-20; the crystallisation of $\beta$-CL-20 from SFE implies a kinetically controlled crystallisation and an high energy (Ostwald rule previously mentioned). The cocrystal being the minor product could be explained from a thermodynamic point of view from solubilities, but the solubility of CL-20 in acetone is much higher $(100 w t \%)$ than HMX ( $2.8 w t \%$ ). The explanation lies from a more practical issue.

The flow rate is not monitored in real time, but an estimation of the mean flow rate for each nozzle is calculated from the volumes left and the experiment time. It has been found that for all experiments with the dual nozzle at $45^{\circ}$,

### 4.2. CL-20:HMX 2:1 COCRYSTAL AS A TOOL FOR UNDERSTANDING CRYSTALLISATION BY SFE



Figure 4.14 - Mean Particle Size Distribution of the cocrystal CL-20:HMX 2:1 samples processed by SFE (first batch) and counted from pellets analysed by AFM.
the nozzles have a very strong attendance to clog. Due to the angle and the spray broadening under vacuum, nozzles spray on each other; each nozzle forms a solid deposit on the opposite one and, after a while, one nozzle is clogging and blocking entirely the other one. Another system is build afterwards with an angle around $70^{\circ}$ as previously introduced in Section 4.1.1; also to correlate the percentage of each crystal to kinetic or thermodynamic phenomena, the flow rate has to remain constant. Coriolis mass flow meters for high pressure were purchased and installed on the SFE process. To control in real time the flow rate of one inlet based on the variation of the other inlet, a master/slave system was developed: one flow meter read and transmit the flow rate of one nozzle to the second flow meter equipped with a valve and an internal PID controller. A variable resistor allows to set a ratio of flow rate between the inlets, thus allowing to have the compounds in a non stoichiometric ratio -with respect to the cocrystal- in solution but sprayed at the stoichiometric ratio. Those flow meters are currently at the testing stage before performing scientific studies.

An experiment was performed lately by spraying a solution of CL-20 in ethyl acetate and a solution of HMX in acetone at the constant stoichiometric ratio 2:1 by monitoring and controlling both mass flow rate. As it can be seen in Figure 4.16, even introduced with the right proportion with a controlled flow rate, the main product is again $\beta-C L-20$ with the cocrystal as the minor one. The amorphous content has to be calculated from the pattern; several methods

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Figure 4.15 - XRD of a sample processed from dual nozzle system compared to CL20:HMX and to $\beta$-CL-20 both from SFE via a single nozzle.


Figure 4.16 - XRD of a sample processed from a solution of CL-20 in ethyl acetate and a solution of HMX in acetone sprayed at the constant stoichiometric ratio 2:1 by monitoring and controlling mass flow rate; the pattern is compared to the sample from the Figure 4.15, CL-20:HMX and to $\beta-C L-20$ both from SFE via a single nozzle.
exists requiring calibration suite or internal/external standards. All of them would require to analyse the sample(s) with silicon or quartz zero-background sample holder: less than 20 mg are used and so the current sample holder has a strong amorphous contribution. If the $H M X$ is found to be amorphous by chemical analysis such as IR or Raman, the system in the overlapping area is a solubility zone were the cocrystal can not be obtained pure. If no HMX is found, the crystallisation of CL-20 and HMX occurs already before the overlap and almost all crystallised HMX is lost due to a flaw in the process itself (cyclone cut-off, crust on the nozzle, affinity with walls etc.). The overlap should also been monitored to quantify the percentage of droplet interpenetration.

### 4.3 Summary of the Chapter

The crystallisation is a multi-step process not yet fully understood; the critical initial stage -the nucleation- is still under investigation by the crystallisation community with recent advances completing further the Classical Nucleation Theory (CNT). Nevertheless, the supersaturation still plays a major role on the rate and trigger of nucleation. Without a determination of the droplets size and evaporation rate, this present study focused on solvent exchange.

The n-hexane is used as anti-solvent to raise the supersaturation. The system acetone/n-hexane forms an azeotrope with a lower boiling point which increases the superheating. However, while using different ratios at the same boiling point, increasing amounts of n-hexane reduced the final mean particle size: from around 800 nm with pure acetone to a plateau around 550 nm . When spraying the $n$-hexane from a second nozzle, particle size has been improved with a mean particle size of 580 nm .

To confirm that the droplets interpenetrate each other and hexane is not already gaseous thus drying acetone droplets, the cocrystal CL-20:HMX 2:1 is studied. Two solutions of acetone are prepared and sprayed separately; one with CL-20 and another with HMX. The cocrystallisation occurs confirming the overlap. Another similar experiment where CL-20 is dissolved into ethyl acetate supports that interpretation with again a cocrystallisation.

Phase Doppler Analysis (PDA) has been used for the first time for in situ measurement of a superheated fluid sprayed under vacuum. The SFE technology will be studied and on-line monitored; the data acquired from both PDA and Small-Angle X-ray Scattering (SAXS) will be computed to provide evaporation rate and crystallisation kinetics, introducing a breakthrough for theSFE technology.

Size reduction can also be achieved by controlling the nucleation and growth steps by adding agents which will change the supersaturation conditions locally

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or will interact with the solute favourably or not. PolyVinylPyrrolidone (PVP) and PolyEthylene Gilycol (PEG) are two very common polymers identified as food additives - E1201 and E1521 respectively - but also as crystallisation agents for many organic compounds. The new chapter explores the chemical approach for controlling crystallisation by SFE, with a focus on those two polymers, resulting in a new wide range of RDX size available.

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## Chapter 5

## Tunable continuous production of RDX from microns to nanoscale using polymeric additives

The specificity of the SFE process arises from the intracity of many physicochemical phenomena that occur with the spray of superheated and supersaturated solutions. The whole system needs to be resolved in space and time as illustrated in Figure 5.1. Crystallisation itself happens in successive steps, namely primary nucleation, crystal growth and secondary nucleation. The complexity of the flashing behaviour is increased by the lack of both theoretical and empirical bases on flashing droplets. In order to dissociate those dynamic events, one crystallisation step over the others can be promoted by the use of additives; nucleation and growth can be inhibited or favoured selectively by polymers. PolyVinylPyrrolidone (PVP) and PolyEthylene Glycol (PEG) are two very common polymers identified as food additives - E1201 and E1521 respectively - but also as crystallisation tools. Kim et al. $(2013,2011)$ and Lee et al. (2014) clearly identified the PVP as a both growth and nucleation inhibitor of RDX in acetone, although only an alteration of the particles morphology was measured without any reduction of the size under electrospray. McPherson and Cudney (McPherson et al. 2006) proved the great effectiveness of PEG for triggering proteins precipitation, notably by steric exclusion as shown by Bhat and Timasheff (Bhat et al. 1992). By the addition of PVP, a delay of the crystallisation at higher supersaturation degree is expected, thus triggering an homogeneous nucleation with a higher density of nuclei. However in those conditions, aggregation or coalescence of nuclei may occur leading respectively to bigger polycrystalline particles or to bigger single crystals. The PEG would increase the supersaturation too, but with a different mechanism than PVP; PVP trends to adsorb on crystal surfaces thus inhibiting the nucleation and growth,
whereas PEG acts as nucleation promoter due to its steric effect.


Figure 5.1 - Evaporation and crystallisation phenomena throughout the SFE process. The 500 nm limit displayed is roughly the detection limit for Phase Doppler Particle Analyzers, which allows in situ size and velocity measurements on both liquid and solid particles.

### 5.1 Material Er Methods $^{2}$

As mentioned in Chapter 1, the RDX is provided by Eurenco, labelled as M5 and used as is, without further purification; the mean size is $6.8 \mu \mathrm{~m}$. Standard PVP with an average molar weight around $40.000 \mathrm{~mol} / \mathrm{g}$ and PEG $400 \mathrm{~mol} / \mathrm{g}$ (liquid) are purchased from Sigma Aldrich.

RDX and the polymers when needed are dissolved in acetone by stirring one minute and then an ultrasonic bath of ten seconds achieved the dissolution. The concentration of RDX is kept constant at $2 \mathrm{wt} \%$ in acetone and weighted percentages of polymer are per gram of RDX.

The operating conditions of the SFE are 40 bar of inlet pressure and $160^{\circ} \mathrm{C}$ at a hollow cone nozzle with an orifice diameter of $60 \mu \mathrm{~m}$.

### 5.2 Results \& Discussion

### 5.2.1 Quantification by NMR Spectroscopy

The quantification of the amount of polymer in the final RDX products is the preliminary step before further characterizations and interpretation. NRM-H were conducted in cooperation with our colleagues from the ISL specialized in analytical chemistry. The robustness and accuracy of the build-in quantification integrated in the software is first tested. A well-known lot of RDX is chosen as a standard sample, then a mass gradation is performed in two different solvents, acetonitrile and DMSO at $35{ }^{\circ} \mathrm{C}$ to ensure complete dissolution. The linear regressions shown in Figure 5.2 are acceptable. DMSO is also the most suitable solvent.

Subsequently, RDX samples processed with polymer are analysed by NRM-H and the RDX peak integrated. The value for $100 \mathrm{wt} \%$ of RDX is taken from a pure SFE-processed RDX sample. The final results are shown in Table 5.1. All values are close to the initial amount of RDX. However, two trends can be clearly highlighted when calculating the difference between theoretical and experimental amounts. For the samples processed with PVP, when the amount of RDX increases, the final product contains more PVP than initially; on the contrary less PEG is found when increasing the RDX content. Due to the NMR accuracy and the percentages involved, those trends should be confirmed, at least some values, by using another analytical method such as HPLC before any interpretation. Nevertheless, final and initial ratio of RDX/polymer are similar.

| theoretical wt\% of RDX | 90.91 | 95.24 | 99.01 | 99.50 |
| :---: | :---: | :---: | :---: | :---: |
| mean calculated value from NMR | 90.9 | 94.5 | 98.0 | 96.8 |
| difference | 0.0 | -0.7 | -1.0 | -2.7 |

(a) RDX processed with PVP.

| theoretical $w t \%$ of RDX | 90.91 | 99.01 | 99.90 |
| :---: | :---: | :---: | :---: |
| mean calculated value from NMR | 88.6 | 98.5 | 99.9 |
| difference | -2.3 | -0.5 | 0.0 |

(b) RDX processed with PEG.

Table 5.1 - Mass percentage of RDX in the final products compared to the initial loading.


Figure 5.2 - Test of the reliability of quantification byNMR.


Figure 5.3 - NMR-H spectra of various representative samples

### 5.2.2 RDX processed with PEG 400

### 5.2.2.1 Particle Size and Morphology



Figure 5.4 - Sizes - using a logarithmic scale - of samples processed with PEG measured from SEM micrographs; solid lines represent the smallest lengths and the dotted lines the largest. Pure RDX processed by SFE and raw M5 RDX added here for comparison.

Originally pure RDX processed by SFE can be obtained with a mean size in the range of $400 \mathrm{~nm}-900 \mathrm{~nm}$ depending on the conditions; with the parameters chosen for that study, the mean size would be around 500 nm (Doctoral Thesis Risse 2012). Starting with only $0.1 \mathrm{wt} \%$ of PEG per gram of RDX, the mean particle size increases to $670(0.356) \mathrm{nm}$. Then the mean size still increases to $750(0.244) \mathrm{nm}$ with $1 \mathrm{wt} \%$ and reaches $4.9(0.482) \mu \mathrm{m}$ with $10 \mathrm{wt} \%$. The elongation of the particles while increasing PEG content can be clearly seen from Figure 5.4 but also when defining a roundness factor or aspect ratio by dividing the smallest length by the largest one. That width-to-length ratio is 0.94 at $0.11 \mathrm{wt} \%, 0.89$ at $1 \mathrm{wt} \%$ and only 0.64 at $10 \mathrm{wt} \%$, indicating a preferential growth in one direction.

Due to a high solubility in acetone, PEG rapidly increases supersaturation in droplets at the very beginning of the atomization and, considering its influence on particle size, the supersaturation is far from the optimal value where the
nucleation rate is maximal. Vekilov (2010) proposed an explanation of why, while the nucleation rate should be increasing exponentially with the degree of supersaturation, experiments at high supersaturations clearly show unpredictable rate of nucleation; according to the two-step mechanism, the crystalline nucleus appears inside metastable clusters of several hundred nanometres. Those clusters of dense liquid which are suspended in the solution can be favoured by the steric effect of PEG and the rapidly increasing saturation due to the flashing behaviour of droplets. Therefore, the induction time of nuclei is reduced and the nucleation rate low thus allowing the formation of bigger particles. Further characterizations involving Phase Doppler Anemometry has to be conducted to kinetically discriminate the role of PEG in the SFE process. As shown in Figure 5.1, the crystallisation of RDX with PEG would allow the particle size to exceed 500 nm ; kinetic growth from the apparatus detection limit to the final particle size could be established.

Although PEG is liquid at ambient temperature, no significant change of aspect between all the final nano powders of RDX processed either pure or with an additive can be noticed. The samples processed with $10 \mathrm{wt} \%$ of PEG are less electrostatic and slightly yellowish.

### 5.2.2.2 X-Ray Difraction (XRD)

The XRD patterns in Figure 5.6 exhibit a slight different texture when micronsize RDX samples at $10 \mathrm{wt} \%$ of PEG are compared with others. From SEM pictures, morphology and PSD indicates a preferentially oriented growth ; the relative differences of intensity in XRD clearly shows that the face $\{311\}$ is much more prominent whereas others like \{111\}, \{002\}, \{102\}, \{020\} and \{021\} are hindered. Those results are in contradiction with predicted and effective morphologies resulting for RDX growth in acetone; Shim and Koo (Shim et al. 2014) successfully predicted the crystal growth habit of RDX in acetone by the spiral growth model and Chen et al. (2015) went further using molecular dynamic simulations. They explained the increased growth rate of the polar faces \{111\}, $\{200\},\{020\}$ and $\{021\}$ compared to the non-polar face $\{002\}$ in polar solvents like acetone. From our experiment, the use of the chemical affinity of faces toward the solvent does not apply when processed by SFE with PEG; the 311 face illustrated in Figure 5.7 exhibits both methylene and nitro group at the surface, and the non-polar $\{002\}$ peak is also decreased as well as the polar faces while adding PEG, a relatively non polar molecule. A small templating effect involving a preferential organization of PEG at higher concentration could explain those differences.


Figure 5.5 - SEM micrographes of RDX samples processed by SFE in the same operating conditions.


Figure 5.6 - (A) XRD patterns of RDX PEG-processed samples; only isolated peaks of major interest have been indexed for clarity. (B) inset of XRD patterns illustrating the broadening of peaks.


Figure 5.7 - View of the 311 plane (in violet, almost perpendicular to the plane of the drawing) and RDX molecules on the surface: both nitro and methylene group are located at the surface (on the background, the unit cell).

### 5.2.2.3 Thermal Analysis

The DSC results in Figure 5.8 show that the RDX processed by SFE is thermally less stable than the raw micron-size RDX, due to a higher ratio surface/volume for submicron size particles. Those results are in accordance with the work of Rosa et al. (2014) where micron size organic particles show also a similar slight melting depression. From 200 to $20 \mu \mathrm{~m}$, they noticed a drop of $0.8^{\circ}$; from $7 \mu \mathrm{~m}$ to 500 nm , the melting point of pure RDX decreases of $1.2^{\circ}$. Although that ratio is decreasing while adding PEG, DSC curves in Figure 5.8 show that the content of PEG itself decreases the activation energies for melting and decomposition: the temperatures - merged in Table 5.2 - are all decreasing. The PEG 400 melts at $3^{\circ} \mathrm{C}$ (peak minimum) and starts to decompose after $300^{\circ} \mathrm{C}$ (data not shown). The broadening of peaks and decrease of melting temperature is a well-known trend for impure organic particles: the gain of entropy by the creation of a bi component melt drives the melting. This phenomenon appears also in PBX like formex-bonded explosives where BCHMX/Formex melts $5^{\circ} \mathrm{C}$ lower (Yan et al. 2012).


Figure 5.8 - DSC analysis of RDX samples processed with different wt\% of PEG.

|  | $T_{\text {e endo }}$ | $T_{\text {e exo }}$ | $T_{\text {pexo }}$ | $T_{\text {cexo }}$ | $E(\mathrm{~J} / \mathrm{g})$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| M5 RDX | 204,0 | 206,1 | 230,8 | 233,6 | 4550 |
| SFE RDX | 202,8 | 204,6 | 229,6 | 232,1 | 4210 |
| 0.1\%PEG | 202,1 | 204,1 | 230,0 | 233,2 | 4710 |
| 1\% PEG | 200,0 | 201,4 | 227,6 | 230,0 | 4530 |
| 10\% PEG | $\mathrm{n} / \mathrm{a}$ | 193,4 | 223,8 | 227,7 | 4010 |
| $0.5 \%$ PVP | 202,2 | 204,3 | 229,3 | 231,7 | 4120 |
| 1\% PVP | 201,7 | 203,6 | 228,9 | 232,4 | 4190 |
| 5\%PVP | 197,1 | 199,1 | 226,0 | 229,4 | 2990 |
| 10\% PVP | n/a | n/a | 223,5 | 227,4 | 3090 |

Table 5.2 - Melting (endo) and decomposition (exo) temperatures in ${ }^{\circ} \mathrm{C}$ and decomposition energy in J/g for all samples (Te extrapolated peak onset, Tp peak maximum temperature, Tc extrapolated peak offset). See Material \& Methods section for more details.

### 5.2.2.4 Infrared (IR) Spectroscopy

In Figure 5.9, the mid-infrared spectra both $0.1 \mathrm{wt} \%$ and $10 \mathrm{wt} \%$ samples are compared to the raw PEG 400 used, and to pure RDX. The three main specific vibrations of PEG at $1000 \mathrm{~cm}^{-1}-1200 \mathrm{~cm}^{-1}$, at $2800 \mathrm{~cm}^{-1}-3000 \mathrm{~cm}^{-1}$ and at $3200 \mathrm{~cm}^{-1}-3600 \mathrm{~cm}^{-1}$ are broad absorption bands which can be clearly distinguished from RDX spectra; the $10 \mathrm{wt} \%$ sample exhibit those bands, but samples with lower amount such as the $0.1 \mathrm{wt} \%$ one are almost identical to the RDX one. The RDX characteristic bands at 3065 and $3075 \mathrm{~cm}^{-1}$ correspond to C-H stretching aromatic vibrations while $1590 \mathrm{~cm}-1,1570 \mathrm{~cm}-1$ and $1270 \mathrm{~cm}-1$ are assigned to stretching of $\mathrm{NO}_{2}$. A slight shift of $2 \mathrm{~cm}-1$ to lower wavenumber of all bands from $500 \mathrm{~cm}-1$ to $1650 \mathrm{~cm}-1$ can be noticed only for the sample with the higher amount of $P E G$; since that region regroups both nitroamines and ring vibrations it seems more appropriate to consider that shift as negligible or at least not due to a specific interaction between the polymer and RDX.

### 5.2.3 RDX processed with PVP 40K

### 5.2.3.1 Particle Size and Morphology

The processing of RDX with PVP 40K dramatically changes the particles size and morphology as it can be clearly seen when comparing side by side the Figures 5.5a and 5.5d. The PSD of samples processed with PVP in Figure 5.10


Figure 5.9 - FTIR spectra of two relevant RDX samples processed with PEG, compared to raw PEG 400 and pure RDX processed by SFE. (Socrates et al. 2001)
show a stabilized mean size around 160 nm with at least $5 \mathrm{wt} \%$ of PVP. At $1 \mathrm{wt} \%$, the mean particle size is slightly higher at 180 nm and with a little more scattering: the multiplicative standard deviation increases from 0.843 for $5 \mathrm{wt} \%$ to 0.926 can be visualized from the dotted cumulative count curve in Figure 5.10.

It is very interesting to notice that only $0.05 \mathrm{wt} \%$ of PVP decreases the size by $34 \%$, from around 500 nm for pure RDX to 320 nm , and improves the spheric shape in a significant way. No preferential growth has been noticed and XRD (not shown here) confirms by identical intensity ratios within the micron-size raw RDX.

As previously mentioned Kim et al. studied the effect of additives on RDX crystallisation by electrospray and drowning-out and pointed out the role of PVP as nucleation inhibitor and growth inhibitor in acetone. The growth inhibition by PVP was only recently evidenced in their experiments of drowning-out where


Figure 5.10 - Particle size distribution and cumulative counts - using a logarithmic scale - of samples processed with PVP measured from SEM micrographs.
$\mathrm{RDX} /$ acetone is sprayed into water, but not in the case of the electrospray; the difference can lye in longer times of flight in air and life in water of droplets in drowning-out and thus implies a more significant impact of the PVP on crystal growth. In contrast, the SFE process has a much higher mean evaporation rate and a two-step evaporation mechanism. Prior to the flash, the PVP inhibits the crystallisation of RDX until the flash of the droplet or delay the nucleation just before the flash. Then the sudden rise of saturation triggers the nucleation if not already, and implies a high crystal growth rate hindered again by the adsorption of PVP.

The size reaching a minimum at $1 \mathrm{wt} \%$ is certainly due to the mechanism of adsorption of the PVP. PVP possesses hydrophilic polar groups, that will interact preferentially on the crystal by chemical adsorption, thus slowing down crystal growth. The minima is then attained for a maximal surface coverage. Moreover, Patel et al. (2015) found out that the growth inhibition of PVP increased with the supersaturation of indomethacin in water. With the droplet fission, that trend is an additive phenomenon explaining the smaller size of RDX processed by SFE with PVP when compared to Kim's results.

In order to confirm the important role of the PVP, one small set of experiments


Figure 5.11 - Particle size distribution of RDX processed with a $80 \mu \mathrm{~m}$ nozzle at only 20 bar.
was conducted with a $80 \mu \mathrm{~m}$ nozzle at only 20 bar. From an industrial point of view, a higher mass flow at lowest pressure is a significant advantage; instead of a yield between 2 and $3 \mathrm{~g} / \mathrm{h}$ for a $60 \mu \mathrm{~m}$ nozzle at 40 bar, RDX were recovered at a rate of $5-8 \mathrm{~g} / \mathrm{h}$. However, as evidenced by Risse (Doctoral Thesis 2012), bigger particles are produced in those conditions; with only $1 \mathrm{wt} \%$ of PVP , the particle size decreases from 714(0.020) nm to $307(0.027) \mathrm{nm}$ and again improves the sphericity. The increase of the particle size at higher flow rates can be counteracted $y$ the addition of PVP, thus allowing both high production rate and small PSD.

### 5.2.3.2 Thermal Analysis

Figure 5.12 reveals that onset temperatures and temperatures at maximum decrease when adding PVP, following the same trend as the RDX samples processed with PEG. As we already discussed, a melting point depression for organic crystal can occur thanks to a decreasing particle size even above 500 nm and can be thermodynamically favoured: PVP-processed samples have a volumetric mean size well below 500 nm and the transition from a soluble solid formed by RDX and PVP to a liquid miscible solution is favourable. Moreover


Figure 5.12 - DSC analysis of RDX samples processed with different wt\% of PVP.
since PVP 40K has a glass transition temperature around $150-175^{\circ} \mathrm{C}$, solid PVP inclusion in the crystal lattice of RDX may also increase the internal energy. In case of crystal defects, micro-strain can be identified by XRD from peak broadening. Williamson Hall plotting has been found not to be a suitable model therefore a more reliable and calibrated method was required. details were given in Section 3.2.1.1; the Rietveld refinements then performed revealed an apparent volume weighted domain size always around $85 \pm 10 \mathrm{~nm}$ and an average maximum strain around $10 \pm 510^{-4} \%$ for both pure and PVP processed samples. So it is very likely that only the effect of size and the presence of PVP are driving the melting point depression here.

### 5.2.3.3 IR Spectroscopy

In Figure 5.13, the mid-infrared spectrum of a $10 \mathrm{wt} \%$ sample is compared to the raw PVP 40K used, and to pure RDX. The two main specific vibrations of PVP around $1660 \mathrm{~cm}^{-1}$ and at $2850 \mathrm{~cm}^{-1}-2950 \mathrm{~cm}^{-1}$ (CH stretching) are broad absorption bands which can be clearly distinguished from RDX spectra. The absorption at $3200 \mathrm{~cm}^{-1}-3600 \mathrm{~cm}^{-1}$ is the vibration of water, the PVP being very hygroscopic. Only the $10 \mathrm{wt} \%$ samples exhibit a small broad peak around $1660 \mathrm{~cm}^{-1}$ from PVP.


Figure 5.13 - FTIR spectra of the RDX samples processed with 10 wt\% of PVP, compared to raw PVP 40K and pure RDX processed by SFE.

### 5.2.4 Sensitivity

In general, samples of nano-RDX have lower sensitivities with the addition of polymers as shown in the Figure 5.14. Due to the reliability issues raised by the submicrometer scale of the powders tested on macro or micron scale apparatus (Radacsi et al. 2013) and the inherent scattering of the results (Brown et al. 2015), the differences of one level higher or lower has to be moderated.

The threshold at the electrostatic discharge test is increased for all SFE processed RDX, and even further when adding at least $5 \mathrm{wt} \%$ of PVP (+300\% then $+700 \%$ compared to M5 RDX) or $10 \mathrm{wt} \%$ of PEG ( $+1160 \%$ compared to M5 RDX).

The addition of at least $1 \mathrm{wt} \%$ of PVP or PEG desensitizes the RDX toward friction, up to $+57.5 \%$. Taking into account the previously mentioned dispersions of sensitivity values, the slight decreased value for friction at $10 \mathrm{wt} \%$ for both polymers can be not significant enough, due to the inability of the apparatus to process more plasticized compositions or due to the lower thermal stability.

The micron size RDX with $10 \mathrm{wt} \%$ of PEG is twice insensitive at the impact


Figure 5.14 - Sensitivities of RDX processed with PVP and PEG compared with pure nano-RDX and the raw micron size RDX.

| Sample | Impact test (J) | Friction (N) | ESD (mJ) |
| :---: | :---: | :---: | :---: |
| M5 RDX | 3.52 | 160 | 119 |
| SFE RDX | 2.05 | 180 | 359 |
| $0.1 \mathrm{wt} \%$. | 1.56 | 192 | 366 |
| $1 \mathrm{wt}. \mathrm{\%}$ | 3.52 | 252 | 366 |
| $10 \mathrm{wt}. \mathrm{\%}$ | 6.96 | 216 | 1.5 J |

Table 5.3 - Sensitivities of the RDX processed with PEG, compared with pure nano-RDX and the raw micron size RDX.
test than pure nano or micron size RDX; despite a morphology trending to be needle-like when adding PEG and so being more likely sensitive to impact as Chen et al. (2012) demonstrated, the sensitivity decreases due to the polymeric content and the size range.

With the exception of $10 \mathrm{wt} \%$ PVP samples, no loss of reactivity has been noticed during the sensitivity tests, the material has the same response as the pure nano and the raw micron size RDX. An explosion at the impact or discharge can be clearly heard with no residue left, and the friction produces an audible crackling with matter ejection; only the $10 \mathrm{wt} \mathrm{\%}$ PVP samples exhibit a lower reactivity at impact with more residue left and the threshold value reported for impact corresponds to a partial ignition (at the interstice between the steel ring and the steel cylinder, therefore suggesting an ignition by friction).

### 5.2.5 Comparison with mechanically mixed samples

Mechanical mixes with $10 \mathrm{wt} \%$ of PVP or PEG and nano or the raw micron-sized M5 RDX were done: DSC results can be seen in Figure 5.15. Figure 5.15a illustrates effect of the size since the decomposition peak of the $10 \mathrm{wt} \%$ sample $(5 \mu \mathrm{~m})$ is between the nano $(500 \mathrm{~nm})$ and micron $(7 \mu \mathrm{~m})$ size pure RDX, while the fusion starts at lower temperature. That's the same phenomenon for the $0.1 \mathrm{wt} \%$ sample comparable to pure nano and micron size pure RDX. For the PVP mixes in Figure 5.15 b , the comparison between the $10 \mathrm{wt} \%$ sample, the n -mix and the $\mu-m i x$ ask the question of the distribution of polymer across the sample. We will focus on the distribution of polymer in another study when theTip Enhanced Raman Spectroscopy (TERS) apparatus will be available.

Sensitivity tests were conducted with those mechanic mixes: the n-mix of 10 $w t \%$ PEG is very insensitive (it did not react at 37 J ) while the impact sensitivity of the n-mix of $10 \mathrm{wt} \%$ PVP is higher. So in the first case the humidification and coating by the liquid PEG could totally inhibit RDX, and in the second one, the issue comes from the difficult homogenisation of a micron size solid PVP with submicron RDX. This increases the need of a TERS apparatus to have much more reliable and precise interpretation.

### 5.3 Summary of the Chapter

The great versatility of the Spray Flash Evaporation allows the processing of solid (PVP 40K) and liquid (PEC 400) polymers to tune the particle size distribution of the final dried nano, submicron or micron-sized powder. PEG triggers the early nucleation of RDX with low nucleation rate leading to bigger particles up to $5 \mu \mathrm{~m}$. PVP acts as a nucleation inhibitor and a growth inhibitor:

(a) RDX processed with PEG

(b) RDX processed with PVP

Figure 5.15 - DSC analysis of RDX samples processed with PVP and PEG: comparison of mechanical mixes with 10 wt \% of PVP or PEG.

RDX nuclei are formed in less volume available due to the fission and flashing of droplets, and then the crystal growth is slowed, thus allowing the formation of much smaller particles at 160 nm with a spherical shape. The addition of PEG could have increased supersaturation to trigger nucleation at a maximal rate but our results show that the contribution of both the evaporation behaviour and the nucleation inhibition is more effective and probably the safest choice to reduce and stabilize the particle size and morphology.

Despite a lower thermal stability, the synthesized RDX composites exhibit reduced sensitivities in electrostatic discharge, friction and impact without loss of reactivity and are less prone to Ostwald ripening. The present work is a great advance in the processability of composite and organic compounds by the SFE technology. The sample synthesized here are also promising for the control of the reactive properties of RDX. Further studies should be performed by TERS to elucidate the question of the distribution of polymer across the sample.

Linking size of droplets, and so supersaturation, to particle size and kinetics of crystallisation is still of interest. In addition to PDA, experiments under the X-Ray beam from a particle accelerator would provide more information of the crystallisation kinetics; our application for beamtime at the ESRF has been recently approved and scheduled for the end of 2016. SAXS will provide information about existing nuclei in droplets as a function of space by scanning the spray and as a function of temperature

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## Related Work

## Innovations



Figure 5.16 - New model of SFE with a reduced size.

SFE Apparatuses Several models of SFE were build prior to my arrival. In order to increase the number of SFE available, a new SFE model was designed with enhanced ergonomy and compactness in cooperation with Ing J. Urban from ISL. I designed and bought the hydraulic system and took care of the budget and assembly of those machines. With the PhD student Axel Le Brize, we performed the maintenance of all the SFE apparatuses and I manage the purchases and improvements on all models. To study the physicochemical phenomena, a new vacuum chamber was designed for PDA and a whole second injection system was build on an existing apparatus. I have launched and managed the modernization of a laboratory to change the layout, to make available the use of the PDA mounted on an internally designed micrometer traverse and to enhance the whole ergonomy of the pre existing models of SFE.

SFE in situ measurements Additional equipments have to be purchase in order to quantify and study precisely the phenomena occurring in the SFE. The inherent risk of the use of energetic materials makes almost impossible -or at
least very limited- any scientific collaboration. I instigated this project which started by the challenging selection of an appropriate technology to measure on-line velocities and sizes. Then a sizeable budget was allocated from public funding thus delaying the effective acquisition of the PDA.

In the mean time, experiments under the X-Ray beam from a particle accelerator have been planed as part of my PhD project, in order to provide more information of the crystallisation; SAXS measurement will allows us to link existing nuclei in droplets in space by scanning the spray but also as a function of temperature.Thanks to Dr Spitzer who supported that project, our application for beamtime at the ESRF has been quite recently approved and scheduled for the end of 2016, after a long process of approval by an international committee and a Safety group.

With MCF Dr. Lobry and Dr. Bonnot, a project for in situ Fast Scanning Calorimetry on micro chip has also been started. The study aims to quantify the evaporation kinetics under vacuum of the metastable droplets in SFE, to analyse solid particles at different locations and so to map the crystallization and evaporation in or near an SFE spray. Dr. Bonnot conducted preliminary experiments of standard explosives dissolved in solvents, and the support system with fine controls has been designed.

Analysis Improvements The analysis of data acquired from various characterization techniques was improved. For instance, the use of the software Giwyddion increased the accuracy and the time spend on AFM images; the Rietveld method was introduced to colleagues to get more information from XRD patterns. A database of all experiments made from SFE was set to study reproducibility and perform statistical analysis

## Published Work and Communication

Communications

- Europyro 2015, 41st International Pyrotechnic Seminar (Toulouse).
- 4th ISL Budding Science Colloquium (Saint Louis, 2015).
- European Congress and Exhibition on Advanced Materials and Processes EUROMAT 2015, B1.3 Section Nanocrystallisation (Warsaw).
- Material Weekend Warsaw 2015; a PhD student workshop from both E-MRS and FEMS societies.
- exhibitor at the 2016 Eurosatory, Defence and Security International Exhibition (572 exhibitors from 56 countries, 213 official delegations from 94 countries)
- 5th ISL Budding Science Colloquium (Saint Louis, 2016).
- Junior EUROMAT 2016 (Lausanne).
- 6th NANOstructures and nanomaterials SElf-Assembly (NanoSEA) (Ciardini Naxos (ME), Italy 2016).
- 1 poster: 3rd ISL Budding Science Colloquium (2014)


## Publications

- Blas, Lucia, Martin Klaumünzer, Florent Pessina, Silke Braun, and Denis Spitzer. "Nanostructuring of Pure and Composite-Based K6 Formulations with Low Sensitivities." Propellants, Explosives, Pyrotechnics 40, no. 6 (2015): 938-44.
- Florent Pessina, Fabien Schnell, and Denis Spitzer. "Tunable Continuous Production of RDX from Microns to Nanoscale Using Polymeric Addlitives." Chemical Engineering Journal 291 (May 1, 2016): 12-19. doi:10.1016/j.cej.2016.01.083.
- Martin Klaumünzer, Florent Pessina, and Denis Spitzer. "Indicating Inconsistency of Desensitizing High Explosives against Impact through Recrystallisation at the Nanoscale." Journal of Energetic Materials, July 1, 2016, 1-10. doi:10.1080/07370652.2016.1199610.
- Denis Spitzer, Vincent Pichot, Florent Pessina, Fabien Schnell, Martin Klaumünzer, and Lucia Blas. "Continuous and Reactive Nanocrystallisation: New Concepts and Processes for Dual-Use Advances." Comptes Rendus Chimie, July 2016. doi:10.1016/j.crci.2016.06.009.
- Florent Pessina and Denis Spitzer. "The longstanding challenge of the nano crystallization of 1,3,5-trinitroperhydro-1,3,5-triazine (RDX)" Beilstein Journal of Nanotechnology Under Review.


## Patent

- Risse, Benedikt, Florent Pessina, and Denis Spitzer. Method for producing cocrystals by means of flash evaporation. WO 2016001445, issued January 2016.


## Scientific courses

- Sensibilisation à la pyrotechnie 3PSC17C, Centre de Formation de la Défense (Bourges 2013)
- Advanced Functional Materials and Characterization, CNRS-EWHA Winter School (Strasbourg 2014)
- Nano-OptoMechanics, School in Physics (Strasbourg 2014)


## Conclusion

Due to the difficult micronisation and nano crystallisation of classical organic explosives such as RDX, advances in insensitive munitions came mainly from new compounds such as NTO or optimizations of each step of the production process (Klapötke et al. 2016; Nouguez et al. 2016). The size reduction of energetic crystals is still of interest not only to produce particles under the critical hot-spot size but also to provide easier shaping and homogeneous energetic compositions. The extensive review of the crystallisation technique used on RDX performed in the Chapter 2 suggests that the Spray Flash Evaporation (SFE) is a well balanced method between spray drying unable to process particles lower that the micrometer, and the expensive batch Rapid Expansion of Supercritical Solutions (RESS) process. The crystallisation in solution is a competitive approach but limited by the drying conditions and its inability to process propellants, unlike the SFE technology (Le Brize et al. 2016).

The present research project was initially focused in the size reduction of crystals produced by this unique technique created in our laboratory. Many challenges were addressed starting by the difficult to commit characterizations of energetic materials, and of the spray itself. Then the crystallisation from SFE has been unveiled with supersaturation variations by solvent exchanges and by polymeric agents.

The nano-technology took off with the invention of the two crucial characterization methods, the Scanning Tunneling Microscopy (STM) and the Atomic Force Microscopy (AFM). The energetic materials are organic crystals where molecules are held together by weak forces; therefore energetic compounds exhibit high sensitivity towards characterization techniques providing energy to the sample. As a consequence, the pyrotechnic community experiences many limitation to assess accurately the particle morphology, their size, aggregation state etc. By trying several characterization techniques especially the microscopy ones, the Environmental Scanning Electron Microscopy (ESEM) has been found to be a suitable technique to process energetic material.

An original method where pellets are flatten then analysed by AFM was in
use previously (Spitzer et al. 2014) and also at the beginning of this present project. It was found that the size measured that way was not a function of the concentration in solution but more of the condition of preparation of the pellets. The compression breaks the brittle crystals with a critical pressure above which the particles reach an even smaller size; while using a microtome, the surface is milled and grooves appear. Sizes down to the crystallite size were found in those grooves. That phenomenon is much more pronounced for n-RDX processed by SFE than for raw micron-sized RDX, just as Spitzer et al. (2011) experienced about opacity and mechanical strength. Those properties could benefit to pressed charges to tune the apparent density and greatly improve homogeneity.

For the SFE process, particle size and shape depend on the crystallisation itself governed by the supersaturation. The degree of supersaturation is unique in each droplet and thus is a function of time and space. The restriction for in situ characterization of the droplets for SFE has been overcome by focusing on the chemical route to change the supersaturation and by designing a dual injection system. In that latter system, the persistence of droplet is questioned by using the cocrystal CL-20:HMX. Cocrystallisation occurs in any cases: by using a unique solution and nozzle, by using one solvent but two solutions and nozzles, and also by using two different solvents each one sprayed by one nozzle. Droplets effectively collide from both spray permitting the crystallisation; it is however not clear whether the nucleation occurs before the overlap or the Phase Solubility Diagram (PhSD) of the system does not allow the formation of the sole cocrystal. Further investigations will be performed to quantify the relative crystalline phases and the overlap.

The SFE versatility was again taken a step further within the introduction of solid and viscous polymers in solvent. Those polymers are food additives namely PolyVinylPyrrolidone (PVP) and PolyEthylene Cilycol (PEG) and were successfully used to control crystallisation steps. PEG 400 triggers the early nucleation of RDX with low nucleation rate leading to bigger particles up to $5 \mu \mathrm{~m}$. PVP 40K acts as a nucleation inhibitor and a growth inhibitor: RDX nuclei are formed in less volume available due to the fission and flashing of droplets; then the crystal growth is slowed, thus allowing the formation of much smaller particles at 160 nm with a narrow distribution and a spherical shape. The addition of PEG could have increased supersaturation to trigger nucleation at a maximal rate but results show that the contribution of both the evaporation behaviour and the nucleation inhibition is more effective and probably the surest choice to reduce and stabilize both particle size and morphology. Furthermore, those synthesized energetic composites are less sensitive.

The laboratory acquired very recently a Phase Doppler Analysis (PDA) in order to elucidate the question of supersaturation. Droplets size and velocity will be measured as a function of temperature but also in space within the spray. The dual nozzle system will also benefit from PDA analyses to define the evaporation behaviours while using two solvent or an anti-solvent. Pre-results show droplets of a few microns at high speed more than $100 \mathrm{~m} / \mathrm{s}$, suggesting the possible crystallisation from metastable systems.

To summarize, the submicron and nano scales bring to the pyrotechnic community new challenges for the characterization of nano energetic materials. Furthermore, this research project paved the way to global and deeper understanding of the crystallisation aspect of the SFE technology. New apparatuses and designs were explored and implemented as breakthrough for the SFE technology; they led to the control of particle size and shape, and to versatility and industrial-friendly enhancements of the SFE apparatuses.

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3. Nouguez, Bruno and Geneviève Eck (2016). "From Synthesis to Formulation and Final Application". In: Propellants, Explosives, Pyrotechnics 41.3, pp. 548-554. ISsn: 1521-4087. DoI: 10.1002/prep. 201600031.
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## Appendix A

## Rietveld refinement

## A. 1 Calibration

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** PROGRAM FullProf.2k (Version 5.50 - Dec2014-ILL JRC) **
M U L T I _- P A T T E R N
Rietveld, Profile Matching & Integrated Intensity
Refinement of X-ray and/or Neutron Data
Date: 17/02/2015 Time: 13:47:24.271
=> PCR file code: lab6 - Copie (22) - Copie
=> DAT file code: lab6.dat -> Relative contribution: 1.0000
==> CONDITIONS OF THIS RUN FOR PATTERN No.: 1
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=> Global Refinement of X-ray powder diffraction data
=> Global Refinement of $X$-ray powder diffraction data
Flat plate with PSD
$\Rightarrow$ Title: ALS 11-BM - NIST SRM 660a LaB6
=> Number of phases: 1
=> Number of excluded regions:
$\Rightarrow$ Number of scattering factors supplied: 0
$\Rightarrow$ March-Dollase model for preferred orientation
=> Conventional weights: w=1.0/Variance (yobs)
$\Rightarrow$ Asymmetry correction as in J.Appl.Cryst. 26,128(1993)
$\Rightarrow$ Background linearly interpolated between the 7 points given
$\Rightarrow$ The 5 th default profile function was selected
$\Rightarrow$ Pseudo-Voigt function (ETA variable)
$X$-parameter correspond to: ETA $=E T A 0+X * 2$ theta
$\mathrm{pV}(\mathrm{x})=\mathrm{ETA} * \mathrm{~L}(\mathrm{x})+(1-\mathrm{ETA}) * \mathrm{G}(\mathrm{x})$
==> INPUT/OUTPUT OPTIONS:
$\Rightarrow$ Generate bacground file *.bac
$\Rightarrow$ Generate file *.PRF for plot
=> Output Integrated Intensities
$\Rightarrow$ Output Correlation Matrix
$\Rightarrow$ Generate new input file *.PCR
=> Data supplied in free format for pattern: 1
=> Plot pattern at each cycle
$\Rightarrow$ Wavelengths: 1.540591 .54431
$\Rightarrow$ Alpha2/Alpha1 ratio: 0.5000
$\Rightarrow \operatorname{Cos}($ Monochromator angle) $=1.0000$
$\Rightarrow$ Asymmetry correction for angles lower than 90.000 degrees
$\Rightarrow$ Absorption correction (AC), muR-eff = 0.0000 0.0000
$\Rightarrow$ Base of peaks: 2.0*HW* 20.00
=> Number of cycles:
50
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$\Rightarrow$ for halfwidth/strain/size parameters: 1.00
$\Rightarrow$ for lattice constants and propagation vectors: 1.00
=> EPS-value for convergence: 0.0
=> Background ==>
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## Information on Space Group:

=> Number of Space group: 221
$\Rightarrow$ Hermann-Mauguin Symbol: P m 3 m
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$\Rightarrow$ Table Setting Choice:
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Bravais Lattice: P
Lattice Symbol: cP
Reduced Number of S.O.: 24 General multiplicity: 48 Centrosymmetry: Centric (-1 at origin)
Generators (exc. -1\&L): 3
$\Rightarrow \quad$ Asymmetric unit: $0.000<=x<=0.500$
$0.000<=y<=0.500$
$0.000<=z<=0.500$
$\Rightarrow$ List of S.O. without inversion and lattice centring translations

| SYMM | 1) : $x, y, z$ | => SYMM ( | 2) : | $x,-y,-z$ |
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| > SYMM | 3): $-\mathrm{x}, \mathrm{y},-\mathrm{z}$ | $\Rightarrow$ SYMM | 4) : | -x, - y, z |
| => SYMM | 5): $\mathrm{y}, \mathrm{z}, \mathrm{x}$ | $\Rightarrow$ SYMM ( | 6): | -y, $-\mathrm{z}, \mathrm{x}$ |
| $\Rightarrow$ SYMM | 7) : $\mathrm{y},-\mathrm{z},-\mathrm{x}$ | $\Rightarrow$ SYMM | 8) : | -y, z, -x |



$\Rightarrow$ X-ray scattering coeff. (A1, B1, A2,...C, f(0), Z, Dfp,Dfpp)


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844 at 2 theta/TOF/E(KeV) 858 at 2theta/TOF/E(KeV): 885 at 2theta/TOF/E(KeV): 887 at 2 theta/TOF/E(KeV): 896 at 2 theta/TOF/E(KeV) 902 at 2 theta/TOF/E(KeV) 907 at 2theta/TOF/E(KeV) 927 at 2theta/TOF/E(KeV) : 932 at 2 theta/TOF/E(KeV) 934 at 2 theta/TOF/E(KeV) 937 at 2theta/TOF/E(KeV): 941 at 2theta/TOF/E(KeV): 943 at 2theta/TOF/E(KeV): 944 at 2 theta/TOF/E(KeV): 945 at 2theta/TOF/E(KeV) 953 at 2 theta/TOF/E(KeV): 956 at 2theta/TOF/E(KeV): 957 at 2 theta/TOF/E(KeV): 959 at 2theta/TOF/E(KeV): 963 at 2 theta/TOF/E(KeV) 969 at 2theta/TOF/E(KeV) 970 at 2theta/TOF/E(KeV): 982 at 2 theta/TOF/E(KeV) 992 at 2 theta/TOF/E(KeV) 996 at 2 theta/TOF/E(KeV) : 1005 at 2theta/TOF/E(KeV): 1063 at 2theta/TOF/E(KeV): 1068 at 2 theta/TOF/E(KeV): 1070 at 2 theta/TOF/E(KeV): 1071 at 2 theta/TOF/E(KeV): 1074 at 2theta/TOF/E(KeV): 1081 at 2 theta/TOF/E(KeV): 1085 at 2 theta/TOF/E(KeV): 1090 at 2 theta/TOF/E(KeV): 1093 at 2theta/TOF/E(KeV): 1094 at 2 theta/TOF/E(KeV): 1105 at 2theta/TOF/E(KeV): 1107 at 2 theta/TOF/E(KeV): 108 at 2theta/TOF/E(KeV): 1111 at 2theta/TOF/E(KeV): 1112 at 2theta/TOF/E(KeV): 1125 at 2 theta/TOF/E(KeV): 1155 at 2 theta/TOF/E(KeV) 1188 at 2 theta/TOF/E(KeV): 1189 at 2 theta/TOF/E(KeV): 1192 at 2 theta/TOF/E(KeV): 1195 at 2 theta/TOF/E(KeV): 196 at 2 theta/TOF/E(KeV): 1200 at 2 theta/TOF/E(KeV): 1212 at 2theta/TOF/E(KeV): 1214 at 2theta/TOF/E(KeV): 1215 at 2theta/TOF/E(KeV): 1223 at 2 theta/TOF/E(KeV): 1226 at 2 theta/TOF/E(KeV): 1231 at 2theta/TOF/E(KeV): 1238 at 2theta/TOF/E(KeV): 1242 at 2 theta/TOF/E(KeV): 1249 at 2 theta/TOF/E(KeV): 1267 at 2theta/TOF/E(KeV): 1283 at 2theta/TOF/E(KeV): 1284 at 2 theta/TOF/E(KeV): 1292 at 2 theta/TOF/E (KeV) : 1309 at 2theta/TOF/E(KeV): 1396 at 2 theta/TOF/E(KeV): 1418 at 2 theta/TOF/E(KeV): 1419 at 2theta/TOF/E(KeV): 1428 at 2 theta/TOF/E(KeV): 1444 at 2 theta/TOF/E(KeV): 1453 at 2 theta/TOF/E(KeV): 1457 at 2 theta/TOF/E(KeV): 1461 at 2 theta/TOF/E(KeV): 1476 at 2 theta/TOF/E(KeV) 1479 at 2 theta/TOF/E(KeV): 1491 at 2theta/TOF/E(KeV): 1496 at 2 theta/TOF/E(KeV): 1497 at 2theta/TOF/E(KeV): 1508 at 2 theta/TOF/E(KeV): 1515 at 2theta/TOF/E(KeV): 1520 at 2 theta/TOF/E(KeV): 1521 at 2 theta/TOF/E(KeV): 1524 at 2theta/TOF/E(KeV): 1538 at 2 theta/TOF/E(KeV): 1573 at 2theta/TOF/E(KeV): 1663 at 2theta/TOF/E(KeV) 1689 at 2 theta/TOF/E(KeV): 1691 at 2 theta/TOF/E(KeV): 1693 at 2 theta/TOF/E(KeV): 1694 at 2 theta/TOF/E(KeV): 1696 at 2 theta/TOF/E(KeV): 1708 at 2 theta/TOF/E(KeV):
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6905 at 2theta/TOF/E(KeV) : 6910 at 2theta/TOF/E(KeV): 6917 at 2 theta/TOF/E(KeV): 6928 at 2 theta/TOF/E (KeV) :
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Standard deviations have to be multiplied by: 2.1538
(correlated residuals) See references:
-J.F.Berar \& P.Lelann, J. Appl. Cryst. 24, 1-5 (1991)
-J.F.Berar, Acc. in Pow. Diff. II,NIST Sp.Pub. 846, 63(1992)

$==>$ PROFILE PARAMETERS FOR PATTERN\# 1
$\begin{array}{lllll}=> & \text { Overall scale factor: } & 0.000125355 & 0.000000003 & 0.000000635\end{array}$
$\Rightarrow E t a(p-V o i g t)$ or $m(P e a r s o n ~ V I I): \quad 0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Overall tem. factor: 0.0000000 .0000000 .000000
$\Rightarrow$ Halfwidth parameters:
$0.001356 \quad 0.000000 \quad 0.000000$
$-0.005000 \quad 0.000000 \quad 0.000000$
$0.003910 \quad 0.000000 \quad 0.000000$
=> Cell parameters:
$\begin{array}{lll}4.154987 & 0.000000 & 0.000000\end{array}$
$4.154987 \quad 0.000000 \quad 0.000000$
$4.154987 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$\begin{array}{lll}90.000000 & 0.000000 & 0.000000\end{array}$
$90.000000 \quad 0.000000 \quad 0.000000$
=> Preferred orientation:
$1.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Asymmetry parameters:
$-0.032396 \quad 0.000130 \quad 0.031169$
$0.042064 \quad 0.000018 \quad 0.004032$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow X$ and $Y$ parameters:
0.063891 -0.000003 0.001582
$0.0000830 .000000 \quad 0.000000$
$\Rightarrow$ Strain parameters :
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Size parameters (G,L):
$0.000000 \quad 0.0000000 .000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Further shape parameters (S_L and D_L):
$0.0000000 .000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$

```
==> GLOBAL PARAMETERS FOR PATTERN# 1
\begin{tabular}{llll}
\(=>\) & Zero-point: & -0.2111 & 0.0000
\end{tabular}
\(\Rightarrow \operatorname{Cos}(t h e t a)-s h i f t\) parameter \(: 0.07670 .00000 .0034\)
\(=>\operatorname{Sin}(2 t h e t a)-s h i f t\) parameter \(: 0.03870 .00000 .0025\)
\(==>\) RELIABILITY FACTORS WITH ALL NON-EXCLUDED POINTS FOR PATTERN: 1
\(\Rightarrow\) R-Factors: \(20.8 \quad 31.0 \quad\) Chi2: 18.6 DW-Stat.: \(1.2720 \quad\) Patt\#: 1
\(\Rightarrow\) Expected : 7.20 1.9292
\(\Rightarrow\) Deviance : 0.187E+06 Dev*: 26.62
\(\Rightarrow\) GoF-index: \(4.3 \quad\) Sqrt(Residual/N)
\(\Rightarrow \mathrm{N}-\mathrm{P}+\mathrm{C}: 6973\)
\begin{tabular}{lccccr}
\(=>\) & SumYdif & SumYobs & SumYcal & \multicolumn{2}{c}{ SumwYobsSQ } \\
\(0.2802 \mathrm{E}+06\) & \(0.1347 \mathrm{E}+07\) & \(0.1232 \mathrm{E}+07\) & \(0.1347 \mathrm{E}+07\) & \(0.1296 \mathrm{E}+06\) & \(0.5539 \mathrm{E}+19\)
\end{tabular}
\(\Rightarrow\) Conventional Rietveld Rp,Rwp,Re and Chi2: 22.2 \(\quad 32.2 \quad 18.59\)
\(\Rightarrow\) (Values obtained using Ynet, but true sigma(y))
\(\Rightarrow\) SumYnet, Sum (w Ynet**2): 0.1263E+07 0.1250E+07
=> N-sigma of the GoF: 1038.716
```

$==>$ RELIABILITY FACTORS FOR POINTS WITH BRAGG CONTRIBUTIONS FOR PATTERN: 1

| => | R-Factors: | 18.1 | 27.0 | Chi2: | 20.7 | DW-Stat. | 1.7601 | Patt\#: |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Expected |  | 5.94 |  |  |  | 1.9131 |  |
| > | Deviance : | $0.115 \mathrm{E}+06$ | De | 25.16 |  |  |  |  |
| > | GoF-index: | 4.5 | Sqr | esidual |  |  |  |  |
| $\Rightarrow \mathrm{N}-\mathrm{P}+\mathrm{C}$ : 4520 |  |  |  |  |  |  |  |  |
| => | SumYdif | Sum |  | SumYcal |  | YobsSQ | Residual | Con |
|  | $2316 \mathrm{E}+06$ | $0.1282 \mathrm{E}+0$ |  | $6 \mathrm{E}+07$ | 0.12 | 070.93 | $9 \mathrm{E}+05$ | 0. 5539 E |


| $\Rightarrow$ | Conventional Rietveld Rp,Rwp, Re and Chi2: | 18.8 | 27.8 | 6.10 | 20.73 |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |

$\Rightarrow$ (Values obtained using Ynet, but true sigma(y))
$\Rightarrow$ SumYnet, Sum(w Ynet**2): 0.1234E+07 0.1214E+07
$\Rightarrow N-s i g m a$ of the GoF: 937.871
=> Global user-weigthed Chi2 (Bragg contrib.): 28.7

| $\Rightarrow$ | Parameters with Correlation greater that $50 \%==>$ |  |  |  |  |
| :--- | :--- | :--- | :--- | :--- | :--- |
| $->$ Correlation of parameter: | SyCos_pat1 | with: | Asym1_ph1_pat1 | $->$ | $59 \%$ |
| $->$ Correlation of parameter: | U-Cagl_ph1_pat1 | with: | W-Cagl_ph1_pat1 | $->$ | $97 \%$ |
| $->$ Correlation of parameter: | Asym1_ph1_pat1 | with: | Asym2_ph1_pat1 | $->$ | $78 \%$ |

## Pattern\# 1 Phase No: 1 Phase name: NIST SRM 660a LaB6




BRAGG R-Factors and weight fractions for Pattern \# 1
$\Rightarrow$ Phase: 1 NIST SRM 660a LaB6
$\Rightarrow$ Bragg R-factor: 13.0 Vol: $71.731(0.000)$ Fract (\%): 100.00( 0.72 )
$\Rightarrow$ Rf-factor $=8.65$ ATZ: 1630.079 Brindley: 1.0000

SYMBOLIC NAMES AND FINAL VALUES AND SIGMA OF REFINED PARAMETERS:

| - | Parameter number | 1 | : | Zero_pat 1 | -0.21106540 | +/- | 0.32565552E-02 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| - | Parameter number | 2 | : | SyCos_pat1 | 0.76720364E-01 ( | +/- | 0.33641579E-02 |
| -> | Parameter number | 3 | : | SySin_pat1 | $0.38725469 \mathrm{E}-01$ ( | +/ - | 0.24757127E-02 |
| -> | Parameter number | 4 | : | X_B_ph1 | 0.20319004 | +/- | 0.19287585E-02 |
| -> | Parameter number | 5 | : | Scale_ph1_pat1 | $0.12535467 \mathrm{E}-03$ ( | +/- | 0.63530314E-06 |
| -> | Parameter number | 6 | . | U-Cagl_ph1_pat1 | $0.13559998 \mathrm{E}-02($ | +/- | 0.38470202E-09 |
| -> | Parameter number | 7 | . | V-Cagl_ph1_pat1 | -0.49999999E-02 | +/- | 0.13145328E-08 |
| -> | Parameter number | 8 | . | W-Cagl_ph1_pat1 | $0.39100000 \mathrm{E}-02($ | +/ - | 0.10740180E-08 |
| -> | Parameter number | 9 | : | Asym1_ph1_pat1 | -0.32395910E-01 | +/ - | 0.31169372E-01 |
| -> | Parameter number | 10 | : | X -tan_ph1_pat1 | 0.63890785E-01 ( | +/- | 0.15823194E-02 |
| -> | Parameter number | 11 | . | Y-cos_ph1_pat1 | 0.0000000 | +/- | 0.0000000 |
| -> | Parameter number | 12 | . | Asym2_ph1_pat1 | 0.42063739E-01 | +/- | 0.40319548E-02 |

=> Number of bytes for floating point variables: 4
$\Rightarrow$ Dimensions of dynamic allocated arrays in this run of FullProf:
$\Rightarrow$ Total approximate array memory (dynamic + static): 107719993 bytes
MaxPOINT= 60000 Max.num. of points (+int. Inten.)/diffraction pattern
MaxREFLT= 20000 Max.num. of reflections/diffraction pattern
MaxPARAM = 300 Max num of refinableparameters
MaxOVERL= 2096 Max.num. of overlapping reflections
=> Number of bytes for floating point arrays: 4
$\Rightarrow$ Dimensions of fixed arrays in this release of FullProf:

| NPATT | $=$ | 80 Max.num. of powder diffraction patterns |
| :--- | :--- | ---: | :--- |
| NATS | $=$ | 830 Max.num. of atoms (all kind) in asymmetric unit |
| MPAR | $=$ | 1800 Max.num. of non atomic parameters/phase |
| IEXCL | $=$ | 30 Max.num. of excluded regions |
| IBACP | $=$ | 277 Max.num. of background points for interpolation |
| NPHT | $=$ | 16 Max.num. of phases |
| NMAGM | $=$ | 8 Max.num. of rotation-matrices sets for magnetic structure |
| NBASIS | $=$ | 12 Max.num. of basis functions associated to a single atom |
| NIREPS | $=$ | 9 Max.num. of irreducible representations to be combined |
| N_EQ | $=$ | 384 Max.num. of user-supplied symmetry operators/propagation vectors |
| NGL | $=$ | 300 Max.num. of global parameters/diffraction pattern |
| N_LINC | $=$ | 30 Max.num. of global linear restraints |
| NAT_P | $=$ | 64 Max.num. of atomic parameters per atom |
| NCONST | $=$ | 500 Max.num. of slack constraints per phase |
| N_SPE | $=$ | 16 Max.num. of different chemical species |
| N_FORM | $=$ | 60 Max.num. of scattering factor values in a table |
| NPR | $=$ | 150 Max.num. of points defining a numerical profile |
| INPR | $=$ | 25 Max.num. of different numerical peak shapes |

```
NPRC = 150 Max.num. of terms in the table for correcting intensities
NSOL = 10 Max.num. of solutions to be stored in Montecarlo searchs
CPU Time: 5.328 seconds
0.089 minutes
=> Run finished at:
Date: 17/02/2015 Time: 13:47:29.606
%\end{Verbatim}
```


## A. 2 Sample of n-RDX processed pure at $2 \mathrm{wt} \%$ in acetone

```
** PROGRAM FulProf 2k (Version 5 60 - Jan2015-ILL JRC) **
*****************
M U L T I -- P A T T E R N
Rietveld, Profile Matching & Integrated Intensity
Refinement of X-ray and/or Neutron Data
Date: 15/06/2015 Time: 11:00:34.452
=> PCR file code: v203
=> DAT file code: v203.dat -> Relative contribution: 1.0000
==> CONDITIONS OF THIS RUN FOR PATTERN No.: 1
=> Global Refinement of X-ray powder diffraction data
=> Global Refinement of X-ray powder diffraction data
Flat plate with PSD
=> Title:RDX
=> Number of phases: 1
=> Number of excluded regions: 0
=> Number of scattering factors supplied: 0
=> March-Dollase model for preferred orientation
=> Conventional weights: w=1.0/Variance(yobs)
=> Asymmetry correction as in J.Appl.Cryst. 26,128(1993)
=> Background refined by polynomial function
> The 5th default profile function was selected
> Pseudo-Voigt function (ETA variable)
X-parameter correspond to: ETA=ETAO+X*2theta
pV(x)= ETA*L(x) +(1-ETA)*G(x)
==> INPUT/OUTPUT OPTIONS:
=> Generate file *.PRF for plot
=> Output Integrated Intensities
=> Generate new input file *.PCR
=> Data supplied in free format for pattern: 1
=> Plot pattern at each cycle
=> Wavelengths: 1.54056 1.54439
=> Alpha2/Alpha1 ratio: 0.5000
C Cos(Monochromator angle)= 1.0000
=> Asymmetry correction for angles lower than 90.000 degrees
=> Absorption correction (AC), muR-eff = 0.0000 0.0000
=> Base of peaks: 2.0*HW* 20.00
=> Number of cycles: 50
=> Relaxation factors ==> for coordinates: 1.00
=> for anisotropic temperature factors: 1.00
=> for halfwidth/strain/size parameters: 1.00
> for lattice constants and propagation vectors: 1.00
=> EPS-value for convergence: 0.0
=> Instrumental Resolution read from file: xray-res.irf
=> Title of data: Approximate resolution function of a conventional X-ray diffractometer CuKalpha1,2
> The resolution function is IRESOL: 1 for profile function # 5
Input resolution parameters:
\begin{tabular}{lccccc} 
U-inst & V-inst & W-inst & X-inst & Y-inst & Z-inst \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000 \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000
\end{tabular}
=> Number of Least-Squares parameters varied: 60
=>-----------------------------
=>-------> PATTERN number: 1
=> Global parameters and codes ==>
=> Zero-point: -0.2016 21.0000
=> Background parameters and codes ==>
=> Origin of polynomial at 2theta/TOF/E(KeV): 70.000
0.11847E+06 0.72376E+06 -47087. -0.18536E+07-0.14029E+07 -35943.
0.00 0.00 0.00 0.00 0.00
=> Displacement peak-shift parameter and code: 0.00 0.00
# Transparency peak-shift parameter and code: 
```

```
=> Reading Intensity data =>>
==> Angular range, step and number of points:
2Thmin: 10.000000 2Thmax: 49.998600 Step: 0.003700 No. of points: 10811
# Phase No. 1
rdx
=>------> Pattern# 1
=> Crystal Structure Refinement
=> The 7th profile function was selected for phase no. 1
=> Preferred orientation vector: 0.0000 0.0000 1.0000
=>-------> Data for PHASE: 1
=> Number of atoms: 21
=> Number of distance constraints: 0
=> Number of angle constraints: 0
=> Symmetry information on space group: P b c a
-> The multiplicity of the general position is: 8
-> The space group is Centric (-1 at origin)
-> Lattice type P: { 000 }
-> Reduced set of symmetry operators:
\begin{tabular}{|c|c|c|c|c|c|c|}
\hline No. IT & Sy & -1 & Rotation part & Assoc & & \\
\hline 1: ( 1) & 1 & --> & ( \(x, y, z\) ) + \{ & 0.0000 & 0.0000 & \(0.0000\}\) \\
\hline 2: ( 4) & 2 ( x, 0, & 0) --> & \((x,-y,-z)+\{\) & 0.5000 & 0.5000 & \(0.0000\}\) \\
\hline ( 3) & 2 ( 0, y, & 0) --> & \((-x, y,-z)+\{\) & 0.0000 & 0.5000 & \(0.5000\}\) \\
\hline : ( 2) & 2 ( 0, 0, & z) --> & (-x,-y, z) + \{ & 0.5000 & 0.0000 & \(0.5000\}\) \\
\hline
\end{tabular}
```



| Codes: | $\mathrm{H}^{501.00000}$ |  | 511.00000 | 521.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  | 0 | 0 | 0 | 8 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| H (1A) |  |  |  | . 40289 |  | 0.52 | 2403 |  | 0.2 | 20773 |  | 5.13220 | 1.00000 |  |  |  |  |
| Codes: | 0.00000 |  | 0.00000 | 0.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  |  |  |  |  |
| H (1B) | H | 0.00000 |  | . 29071 |  | 0.42 | 2024 |  | 0.2 | 23991 |  | 4.84270 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  |  | 0.00000 | 0.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  |  |  |  |  |
| H (2A) | H | 0.00000 |  | . 44331 |  | 0.1 | 3918 |  | 0.1 | 14950 |  | 4.60580 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  |  | 0.00000 | 0.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  |  |  |  |  |
| H (2B) | H | 0.00000 |  | . 31742 |  | 0.19 | 9390 |  | 0.2 | 20730 |  | 4.97430 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  |  | 0.00000 | 0.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  |  |  |  |  |
| H (3A) | H | 0.00000 |  | . 20936 |  | 0.35 | 35364 |  | 0.0 | . 2527 |  | 4.50050 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  |  | 0.00000 | 0.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  |  |  |  |  |
| H (3B) | H |  |  | . 17213 |  | 0.32 | 2091 |  | 0.1 | 10070 |  | 3.92150 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.0 | 000 |  | 0.0 | 0000 |  | 0.0 |  |  |  |  |  |  |  |

$\Rightarrow$ IT IS ASSUMED THAT THE FIRST GIVEN SITE IS FULLY OCCUPIED
OR THE FIRST AND SECOND ATOMS ARE IN THE SAME SITE WITH TOTAL FULL OCCUPATION
(If this is not the case, change the order of atoms to obtain correct values for the content of the unit cell)
The given occupation factors have been obtained mutiplying m/M by 1.0000
$\rightarrow$ Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: O Atomic Mass: 15.9994
$\rightarrow$ Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
$\rightarrow$ Atom: 0, Chemical element: 0 Atomic Mass: 15.9994
-> Atom: N , Chemical element: N Atomic Mass: 14.0067
-> Atom: N , Chemical element: N Atomic Mass: 14.0067
-> Atom: N , Chemical element: N Atomic Mass: 14.0067
$\rightarrow$ Atom: N , Chemical element: N Atomic Mass: 14.0067
$\rightarrow$ Atom: N , Chemical element: N Atomic Mass: 14.0067
$\rightarrow$ Atom: N , Chemical element: N Atomic Mass: 14.0067
-> Atom: C , Chemical element: C Atomic Mass: 12.0110
$\rightarrow$ Atom: C , Chemical element: C Atomic Mass: 12.0110
$\rightarrow$ Atom: C , Chemical element: C Atomic Mass: 12.0110
-> Atom: H , Chemical element: H Atomic Mass: 1.0080
-> Atom: H , Chemical element: H Atomic Mass: 1.0080
-> Atom: H , Chemical element: H Atomic Mass: 1.0080
-> Atom: H , Chemical element: H Atomic Mass: 1.0080
$\rightarrow$ Atom: H , Chemical element: H Atomic Mass: 1.0080
$\rightarrow$ Atom: H , Chemical element: H Atomic Mass: 1.0080
$\Rightarrow$ The given value of ATZ is 1776.94 the program has calculated: 1776.94
The value of ATZ given in the input PCR file will be used for quantitative analysis
$\Rightarrow$ The chemical content of the unit cell is:
$8.00000+8.00000+8.00000+8.00000+8.00000$ $8.0000 \mathrm{~N}+8.0000 \mathrm{~N}+8.0000 \mathrm{~N}$
$8.0000 \mathrm{~N}+8.0000 \mathrm{~N}+8.0000 \mathrm{C}+$
$+8.0000$
$8.0000 \mathrm{C}+8.0000 \mathrm{C}+8.0000 \mathrm{H}+8.0000 \mathrm{H}+\quad$ 2 $8.0000 \mathrm{H}+8.0000 \mathrm{H}$
$+$ 8.0000 H
$\Rightarrow$ The normalized site occupation numbers in $\%$ are:

| 100.0000 (1) | : |  | 100.0000 0(2) |  | 100.0000 0(3) | : |  | 100.0000 0(4) | : |  | 100.0000 0(5) | : |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 100.0000 | O(6) | : | $100.0000 \mathrm{~N}(1)$ | : | 100.0000 | N(2) | : | 100.0000 | N(3) | : | 100.0000 | N (4) | : |
| $100.0000 \mathrm{~N}(5)$ | : |  | $100.0000 \mathrm{~N}(6)$ |  | 100.0000 C (1) | : |  | 100.0000 C(2) | : |  | 100.0000 C (3) | : |  |
| 100.0000 | H (1 A ) | : | $100.0000 \mathrm{H}(1 \mathrm{~B})$ | : | 100.0000 | H (2A) | : | 100.0000 | H (2B) | : | 100.0000 | H (3A) | : |

$100.0000 \mathrm{H}(3 \mathrm{~B})$
$\Rightarrow$ The density (volumic mass) of the compound is: $1.818 \mathrm{~g} / \mathrm{cm} 3$
=>-------> PROFILE PARAMETERS FOR PATTERN: 1
$\Rightarrow$ Overall scale factor: $0.366470 \mathrm{E}-02$
$\Rightarrow$ ETA (p-Voigt) OR M (Pearson VII): 0.0000
$\Rightarrow$ Overall temperature factor: 0.00000
$\Rightarrow$ Halfwidth U,V,W: $\quad-0.01481 \quad 0.00000$
$\Rightarrow X$ and $Y$ parameters: $\quad 0.0000 \quad 0.0000$
$\begin{array}{lllllllllllll}\Rightarrow \text { Direct cell parameters: } & 11.5606 & 10.6800 & 13.1449 & 90.0000 & 90.0000 & 90.0000\end{array}$
$\Rightarrow$ Preferred orientation parameters: 1.00000 .0000
$\begin{array}{lllllll}\Rightarrow \text { Asymmetry parameters } & : & 0.20251 & 0.04985 & 0.00000 & 0.00000\end{array}$
$\begin{array}{lllll}\Rightarrow & \text { Strain parameters } & : & 0.00000 & 0.00000\end{array} 0.00000$
$\begin{array}{llrll}\Rightarrow & \text { Size parameters } & : & 0.01453 & 0.00000 \\ => & \text { Further shape parameters } & \left(S \_L\right. & \text { and } \operatorname{D} \text { L) : } & 0.00000\end{array}$
S_L is source width/detector distance
D_L is detector width/detector distance
$=\Rightarrow$ CODEWORDS FOR PROFILE PARAMETERS of PATTERN\# 1
=> Overall scale factor: 31.000
$\Rightarrow$ ETA (p-Voigt) OR M (Pearson VII): 0.000
$\Rightarrow$ Overall temperature factor: 0.000
$\begin{array}{llll}\Rightarrow & H a l f w i d t h ~ U, V, W: & 41.000 & 0.000 \\ 0.000\end{array}$
$\Rightarrow X$ and Y parameters: 0.0000 .000
$\begin{array}{llllllllllll}\Rightarrow \text { Direct cell parameters: } & 51.000 & 61.000 & 71.000 & 0.000 & 0.000 & 0.000\end{array}$
$\begin{array}{llll}\Rightarrow & P r e f e r r e d ~ o r i e n t a t i o n ~ p a r a m e t e r s: ~ & 0.000 & 0.000\end{array}$
$\begin{array}{llllllll}\Rightarrow & \text { Asymmetry parameters } & : & 531.000 & 541.000 & 0.000 & 0.000\end{array}$
$\Rightarrow$ Strain parameters : 0.000 0.000 0.000
=> Size parameters : 11.000551 .000
$\Rightarrow$ The 18 th model for size is used
$\Rightarrow$ Orthorhombic Anisotropic Broadening using Spherical Harmonics up
to 4 -th order (Laue class: mmm, SPG:16-74, only lorentzian comp.)
Ylm's up to 4th order: Y00,Y20,Y22+,Y40,Y42+,Y44+
RJP - Ref: M. Jarvinen, J. Appl. C. (1993), p. 527
$\Rightarrow$ Coefficients of Spherical Harmonics for anisotropic size


SYMBOLIC NAMES AND INITIAL VALUES OF PARAMETERS TO BE VARIED:


| -> | Parameter number |
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| Symbolic | Name: | Z_0 (6) _ph1 | $0.53580001 \mathrm{E}-01$ |
| :---: | :---: | :---: | :---: |
| > Symbolic | Name: | X_N (1) _ph1 | 0.44586000 |
| -> Symbolic | Name: | Y_N (1) _ph1 | 0.33585000 |
| > Symbolic | Name: | Z_N (1) _ph1 | 0.17310999 |
| > Symbolic | Name: | X_N (2) _ph1 | 0.32971999 |
| Symbolic | Name: | Y_N (2) _ph1 | 0.23289999 |
| Symbolic | Name: | $\mathrm{Z}_{-} \mathrm{N}$ (2) _ ph 1 | $0.54719999 \mathrm{E}-01$ |
| Symbolic | Name: | $\mathrm{X}_{-} \mathrm{N}$ (3) _ ph 1 | 0.30485001 |
| Symbolic | Name: | Y_N (3) _ph1 | 0.45556000 |
| Symbolic | Name: | Z_N (3) _ph1 | $0.82680002 \mathrm{E}-01$ |
| > Symbolic | Name: | X_N (4) _ph1 | 0.53974003 |
| -> Symbolic | Name: | Y_N (4) _ph1 | 0.33263999 |
| -> Symbolic | Name: | Z_N (4) _ph1 | 0.23717000 |
| -> Symbolic | Name: | X_N (5) _ph1 | 0.38532999 |
| -> Symbolic | Name: | Y_N (5) _ph1 | 0.20298000 |
| -> Symbolic | Name: | Z_N (5) _ph1 | -0.42270001E-01 |
| > Symbolic | Name: | $\mathrm{X}_{-} \mathrm{N}$ (6) _ ph 1 | 0.35655001 |
| > Symbolic | Name: | Y_N (6) _ph1 | 0.54262000 |
| > Symbolic | Name: | Z_N (6) _ph1 | $0.10490000 \mathrm{E}-01$ |
| -> Symbolic | Name: | $\mathrm{X}_{-} \mathrm{C}$ (1) _ ph 1 | 0.34604999 |
| -> Symbolic | Name: | Y_C (1) _ph1 | 0.43641999 |
| -> Symbolic | Name: | Z_C (1) _ph1 | 0.19790000 |
| -> Symbolic | Name: | X_C (2) _ph1 | 0.38722000 |
| -> Symbolic | Name: | Y_C (2) _ph1 | 0.21280000 |
| -> Symbolic | Name: | Z_C (2) _ph1 | 0.15753999 |
| -> Symbolic | Name: | X_C (3) _ph1 | 0.23514999 |
| -> Symbolic | Name: | Y_C (3) _ph1 | 0.33774999 |
| -> Symbolic | Name: | Z_C (3) _ph1 | $0.52490000 \mathrm{E}-01$ |
| -> Symbolic | Name: | Asym1_ph1_pat1 | 0.20251000 |
| -> Symbolic | Name: | Asym2_ph1_pat1 | $0.49849998 \mathrm{E}-01$ |
| -> Symbolic | Name: | L-Size_ph1_pat1 | 0.0000000 |
| -> Symbolic | Name: | Size2_ph1_pat1 | 0.0000000 |
| -> Symbolic | Name: | Size3_ph1_pat1 | 0.0000000 |
| -> Symbolic | Name: | Size4_ph1_pat1 | 0.0000000 |
| -> Symbolic | Name: | Size5_ph1_pat1 | 0.0000000 |
| -> Symbolic | Name: | Size6_ph1_pat1 | 0.0000000 |

$0.53580001 \mathrm{E}-01$

- 0.44586000
0.33585000
$\mathrm{X}_{-} \mathrm{N}(2)$ _ph1 0.32971999
$Y_{-} N(2)$ _ph1 0.23289999
_N (2) _ph1 0.54719999E-01
0.30485001

Y_N (3) _ph1 0.45556000
02E-01
Y N (4) ph1
Z_N (4) _ph1 0.23717000
$X_{-} N(5)$ _ph1 0.38532999
Z_N(5)_ph1 -0.42270001E-01
X_N (6) _ph1 0.35655001
Y_N (6) _ph1 0.54262000
X_C (1) _ph1 0.34604999
Y_C (1) _ph1 0.43641999
Z_C(1)_ph1 0.19790000
X_C (2) _ph1 0.38722000
$Z_{-} C(2)$ _ph1 0.15753999
X_C (3) _ph1 0.23514999
Y_C (3) _ph1 0.33774999
Asym1_ph1_pat1 0.20251000
Asym2_ph1_pat1 0.49849998E-01
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1 at 2 theta/TOF/E (KeV):
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97 at 2theta/TOF/E(KeV): 101 at 2theta/TOF/E(KeV): 104 at 2 theta/TOF/E (KeV): 105 at 2 theta/TOF/E (KeV): 107 at 2 theta/TOF/E (KeV): 116 at 2 theta/TOF/E (KeV): 118 at 2 theta/TOF/E (KeV) : 119 at 2theta/TOF/E (KeV): 122 at 2 theta/TOF/E (KeV) : 126 at 2 theta/TOF/E (KeV) : 130 at 2 theta/TOF/E(KeV): 132 at 2 theta/TOF/E (KeV): 144 at 2 theta/TOF/E (KeV): 148 at 2 theta/TOF/E (KeV): 155 at 2 theta/TOF/E (KeV): 168 at 2theta/TOF/E(KeV): 176 at 2 theta/TOF/E (KeV): 180 at 2 theta/TOF/E (KeV): 182 at 2 theta/TOF/E (KeV): 185 at 2 theta/TOF/E (KeV): 198 at 2theta/TOF/E(KeV): 200 at 2 theta/TOF/E (KeV): 204 at 2 theta/TOF/E (KeV) :
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12.2126 Intensity fixed to 1.0 and variance to 1E6

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16.8931 16.8968 16.9079 16.9153 16.9264 16.9560 17.9069 17.9106 17.9254 17.9328 17.9365 17.9402 17.9439 17.9550 17.9772 17.9809 17.9846 17.9883 17.9920

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2168 at 2 theta/TOF/E(KeV) 2169 at 2 theta/TOF/E(KeV) : 2171 at 2 theta/TOF/E(KeV): 2172 at 2 theta/TOF/E(KeV): 2173 at 2theta/TOF/E(KeV): 2174 at 2theta/TOF/E(KeV): 2175 at 2theta/TOF/E(KeV): 2176 at 2 theta/TOF/E(KeV) 2177 at 2 theta/TOF/E(KeV): 2178 at 2 theta/TOF/E(KeV): 2180 at 2 theta/TOF/E(KeV): 2181 at 2theta/TOF/E(KeV): 2182 at 2theta/TOF/E(KeV): 2183 at 2 theta/TOF/E(KeV): 2184 at 2 theta/TOF/E(KeV): 2185 at 2 theta/TOF/E(KeV): 2186 at 2 theta/TOF/E(KeV): 2187 at 2 theta/TOF/E(KeV): 2188 at 2theta/TOF/E(KeV): 2189 at 2theta/TOF/E(KeV): 2190 at 2theta/TOF/E(KeV): 2191 at 2theta/TOF/E(KeV): 2192 at 2 theta/TOF/E(KeV): 2194 at 2theta/TOF/E(KeV): 2195 at 2 theta/TOF/E(KeV): 2196 at 2 theta/TOF/E(KeV): 2197 at 2 theta/TOF/E(KeV) 2198 at 2 theta/TOF/E(KeV): 2199 at 2 theta/TOF/E(KeV) : 2201 at 2 theta/TOF/E(KeV): 2202 at 2theta/TOF/E(KeV): 2203 at 2theta/TOF/E(KeV): 2204 at 2theta/TOF/E(KeV): 2205 at 2 theta/TOF/E(KeV): 2206 at 2theta/TOF/E(KeV): 2207 at 2theta/TOF/E(KeV): 2208 at 2 theta/TOF/E(KeV): 2209 at 2theta/TOF/E(KeV): 2210 at 2 theta/TOF/E(KeV): 2212 at 2theta/TOF/E(KeV): 2213 at 2theta/TOF/E(KeV): 2214 at 2theta/TOF/E(KeV): 2215 at 2 theta/TOF/E(KeV): 2216 at 2theta/TOF/E(KeV): 2217 at 2theta/TOF/E(KeV): 2219 at 2theta/TOF/E(KeV) 2222 at 2 theta/TOF/E(KeV): 2223 at 2 theta/TOF/E(KeV): 2224 at 2theta/TOF/E(KeV): 2225 at 2theta/TOF/E(KeV): 2226 at 2 theta/TOF/E(KeV): 2227 at 2 theta/TOF/E(KeV): 2228 at 2 theta/TOF/E(KeV): 2229 at 2theta/TOF/E(KeV): 2230 at 2theta/TOF/E(KeV): 2231 at 2theta/TOF/E(KeV): 2232 at 2theta/TOF/E(KeV): 2234 at 2 theta/TOF/E(KeV): 2235 at 2theta/TOF/E(KeV): 2236 at 2theta/TOF/E(KeV): 2237 at 2theta/TOF/E(KeV): 2238 at 2theta/TOF/E(KeV): 2239 at 2theta/TOF/E(KeV): 2240 at 2 theta/TOF/E(KeV): 2241 at 2theta/TOF/E(KeV): 2242 at 2 theta/TOF/E(KeV): 2243 at 2 theta/TOF/E(KeV) : 2244 at 2theta/TOF/E(KeV): 2245 at 2theta/TOF/E(KeV): 2246 at 2theta/TOF/E(KeV): 2247 at 2 theta/TOF/E(KeV): 2248 at 2 theta/TOF/E(KeV): 2249 at 2theta/TOF/E(KeV): 2252 at 2theta/TOF/E(KeV): 2253 at 2 theta/TOF/E(KeV): 2254 at 2theta/TOF/E(KeV): 2255 at 2theta/TOF/E(KeV): 2256 at 2theta/TOF/E(KeV): 2257 at 2 theta/TOF/E(KeV): 2258 at 2theta/TOF/E(KeV): 2259 at 2theta/TOF/E(KeV): 2260 at 2theta/TOF/E(KeV): 2261 at 2theta/TOF/E(KeV): 2262 at 2theta/TOF/E(KeV): 2263 at 2theta/TOF/E(KeV): 2264 at 2 theta/TOF/E(KeV) 2265 at 2theta/TOF/E(KeV): 2267 at 2 theta/TOF/E(KeV) 2269 at 2 theta/TOF/E(KeV): 2270 at 2 theta/TOF/E(KeV):
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2440 at 2 theta/TOF/E(KeV): 2441 at 2theta/TOF/E(KeV): 2442 at 2theta/TOF/E(KeV): 2444 at 2theta/TOF/E(KeV): 2445 at 2theta/TOF/E(KeV): 2446 at 2theta/TOF/E(KeV): 2447 at 2theta/TOF/E(KeV): 2448 at 2theta/TOF/E(KeV): 2449 at 2 theta/TOF/E(KeV): 2450 at 2 theta/TOF/E(KeV): 2451 at 2 theta/TOF/E(KeV): 2453 at 2theta/TOF/E(KeV): 2454 at 2theta/TOF/E(KeV): 2455 at 2 theta/TOF/E(KeV): 2456 at 2 theta/TOF/E(KeV): 2457 at 2 theta/TOF/E(KeV): 2458 at 2 theta/TOF/E(KeV): 2459 at 2theta/TOF/E(KeV): 2461 at 2theta/TOF/E(KeV): 2462 at 2 theta/TOF/E(KeV): 2463 at 2theta/TOF/E(KeV): 2464 at 2theta/TOF/E(KeV): 2465 at 2 theta/TOF/E(KeV): 2467 at 2 theta/TOF/E(KeV): 2468 at 2 theta/TOF/E(KeV): 2469 at 2theta/TOF/E(KeV): 2470 at 2theta/TOF/E(KeV): 2471 at 2 theta/TOF/E(KeV): 2472 at 2 theta/TOF/E(KeV): 2473 at 2 theta/TOF/E(KeV): 2476 at 2 theta/TOF/E(KeV): 2482 at 2theta/TOF/E(KeV): 2483 at 2theta/TOF/E(KeV): 2485 at 2 theta/TOF/E(KeV): 2487 at 2theta/TOF/E(KeV): 2488 at 2theta/TOF/E(KeV): 2489 at 2theta/TOF/E(KeV): 2491 at 2theta/TOF/E(KeV): 2493 at 2theta/TOF/E(KeV): 2494 at 2theta/TOF/E(KeV): 2536 at 2theta/TOF/E(KeV): 2538 at 2theta/TOF/E(KeV): 2539 at 2 theta/TOF/E(KeV): 2542 at 2theta/TOF/E(KeV): 2544 at 2theta/TOF/E(KeV): 2548 at 2theta/TOF/E(KeV): 2549 at 2 theta/TOF/E(KeV): 2551 at 2 theta/TOF/E(KeV): 2552 at 2theta/TOF/E(KeV): 2553 at 2theta/TOF/E(KeV): 2554 at 2theta/TOF/E(KeV): 2555 at 2theta/TOF/E(KeV): 2557 at 2 theta/TOF/E(KeV): 2559 at 2theta/TOF/E(KeV): 2560 at 2 theta/TOF/E(KeV): 2561 at 2theta/TOF/E(KeV): 2562 at 2theta/TOF/E(KeV): 2563 at 2theta/TOF/E(KeV): 2565 at 2theta/TOF/E(KeV): 2566 at 2 theta/TOF/E(KeV): 2567 at 2 theta/TOF/E(KeV): 2568 at 2 theta/TOF/E(KeV): 2569 at 2theta/TOF/E(KeV): 2570 at 2 theta/TOF/E(KeV): 2571 at 2 theta/TOF/E(KeV): 2572 at 2 theta/TOF/E(KeV): 2574 at 2theta/TOF/E(KeV): 2575 at 2 theta/TOF/E(KeV): 2577 at 2 theta/TOF/E(KeV): 2578 at 2theta/TOF/E(KeV): 2579 at 2 theta/TOF/E(KeV): 2582 at 2 theta/TOF/E(KeV): 2583 at 2 theta/TOF/E(KeV): 2584 at 2theta/TOF/E(KeV): 2585 at 2 theta/TOF/E(KeV): 2586 at 2theta/TOF/E(KeV): 2587 at 2 theta/TOF/E(KeV): 2588 at 2theta/TOF/E(KeV): 2589 at 2theta/TOF/E(KeV): 2591 at 2 theta/TOF/E(KeV): 2594 at 2 theta/TOF/E(KeV): 2595 at 2theta/TOF/E(KeV): 2597 at 2theta/TOF/E(KeV): 2598 at 2 theta/TOF/E(KeV) 2600 at 2 theta/TOF/E(KeV): 2601 at 2 theta/TOF/E(KeV) 2602 at 2 theta/TOF/E(KeV): 2603 at 2theta/TOF/E(KeV): 2604 at 2 theta/TOF/E(KeV) 2606 at 2 theta/TOF/E(KeV):
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19.2241
19.3795 19.3869 19.3906 19.4017 19.4091 19.4239 19.4276 19.4350 19.4387 19.4424 19.4461 19.4498 9.4572 19.4646 19.4683 19.4720 19.4757 19.4794 19.4868 19.4905 19.4942 19.4979 19.5016 19.5053 19.5090 19.5127 19.5201 19.5238 19.5312 19.5349 19.5386 19.5497 19.5534 19.5571 19.5608 19.5645 19.5682 19.5719 19.5756 19.5830 19.5941 19.5978 19.6052 19.6089 19.6163 19.6200 19.6237 19.6274 19.6311
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2934 at 2 theta/TOF/E(KeV) 2936 at 2theta/TOF/E(KeV): 2938 at 2theta/TOF/E(KeV): 2939 at 2theta/TOF/E(KeV): 2947 at 2theta/TOF/E(KeV): 2951 at 2theta/TOF/E(KeV): 2954 at 2theta/TOF/E(KeV): 2956 at 2theta/TOF/E(KeV): 2957 at 2 theta/TOF/E(KeV): 2960 at 2 theta/TOF/E(KeV): 2962 at 2theta/TOF/E(KeV): 2963 at 2theta/TOF/E(KeV): 2964 at 2theta/TOF/E(KeV): 2965 at 2theta/TOF/E(KeV): 2966 at 2 theta/TOF/E(KeV): 2971 at 2theta/TOF/E(KeV): 2974 at 2theta/TOF/E(KeV): 2975 at 2 theta/TOF/E(KeV): 3070 at 2theta/TOF/E(KeV): 3079 at 2theta/TOF/E(KeV): 3081 at 2theta/TOF/E(KeV): 3086 at 2 theta/TOF/E(KeV): 3089 at 2 theta/TOF/E(KeV): 3091 at 2theta/TOF/E(KeV): 3092 at 2 theta/TOF/E(KeV): 3094 at 2theta/TOF/E(KeV): 3097 at 2theta/TOF/E(KeV): 3099 at 2theta/TOF/E(KeV): 3100 at 2theta/TOF/E(KeV): 3101 at 2 theta/TOF/E(KeV) 3102 at 2theta/TOF/E(KeV): 3105 at 2theta/TOF/E(KeV): 3106 at 2theta/TOF/E(KeV): 3108 at 2 theta/TOF/E(KeV): 3109 at 2theta/TOF/E(KeV): 3113 at 2theta/TOF/E(KeV): 3115 at 2 theta/TOF/E(KeV): 3121 at 2theta/TOF/E(KeV): 3124 at 2theta/TOF/E(KeV): 3273 at 2 theta/TOF/E(KeV): 3276 at 2theta/TOF/E(KeV): 3282 at 2 theta/TOF/E(KeV): 3285 at 2 theta/TOF/E(KeV): 3287 at 2 theta/TOF/E(KeV): 3288 at 2theta/TOF/E(KeV): 3289 at 2theta/TOF/E(KeV): 3293 at 2theta/TOF/E(KeV): 3294 at 2 theta/TOF/E(KeV) 3295 at 2theta/TOF/E(KeV): 3303 at 2theta/TOF/E(KeV): 3305 at 2 theta/TOF/E(KeV): 3310 at 2theta/TOF/E(KeV): 3311 at 2 theta/TOF/E(KeV): 3312 at 2theta/TOF/E(KeV): 3431 at 2theta/TOF/E(KeV): 3432 at 2theta/TOF/E(KeV): 3434 at 2theta/TOF/E(KeV): 3438 at 2 theta/TOF/E(KeV) 3440 at 2theta/TOF/E(KeV): 3441 at 2theta/TOF/E(KeV): 3444 at 2theta/TOF/E(KeV): 3447 at 2 theta/TOF/E(KeV): 3449 at 2theta/TOF/E(KeV): 3450 at 2 theta/TOF/E(KeV): 3452 at 2theta/TOF/E(KeV): 3453 at 2 theta/TOF/E(KeV): 3459 at 2theta/TOF/E(KeV): 3460 at 2 theta/TOF/E(KeV): 3461 at 2 theta/TOF/E(KeV) : 3462 at 2theta/TOF/E(KeV): 3463 at 2theta/TOF/E(KeV): 3464 at 2theta/TOF/E(KeV): 3467 at 2 theta/TOF/E(KeV): 3468 at 2theta/TOF/E(KeV): 3469 at 2 theta/TOF/E(KeV): 3470 at 2 theta/TOF/E(KeV): 3471 at 2 theta/TOF/E(KeV): 3472 at 2theta/TOF/E(KeV): 3474 at 2theta/TOF/E(KeV): 3477 at 2 theta/TOF/E(KeV): 3480 at 2 theta/TOF/E(KeV) 3481 at 2 theta/TOF/E(KeV): 3483 at 2theta/TOF/E(KeV): 3485 at 2theta/TOF/E(KeV): 3486 at 2 theta/TOF/E(KeV): 3555 at 2 theta/TOF/E(KeV) 3561 at 2 theta/TOF/E(KeV): 3563 at 2theta/TOF/E(KeV): 3564 at 2 theta/TOF/E(KeV) 3566 at 2theta/TOF/E(KeV):
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29.9763

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$\Rightarrow$ Optimizations for routine tasks applied:
=> Calculation mode for patter\#: 1 CM_PSEUDO_VOIGT
$=>$ Lorentzian FWHM < 0 at 2theta:
$=>$ Lorentzian FWHM < 0 at 2theta:
=> Lorentzian FWHM < 0 at 2theta:
$=>$ Lorentzian FWHM < 0 at 2theta:
=> Lorentzian FWHM < 0 at 2theta:
17.921 for phase no 17.966 for phase no 17.921 for phase no.
29.9837 29.9874 29.9948 30.0059 30.0096 30.0133 30.0577 33.5283 33.5357 33.5431 33.7725 33.8095 33.8169 33.8317 33.8354 33.8428 33.8465 33.8502 34.2313 34.2461 34.2535 34.2609 34.2683 34.2720 34.2757 34.2868 34.2905 34.3090 34.3164 34.3238 34.3312 34.3497 34.3608 34.3682 34.3756 34.3941 34.4311 34.4422 35.4042 35.4708 35.9666 36.0221 36.0295 36.0443 36.0628 36.0665 36.0702 36.0813 36.0850 36.0998 36.1035 36.1072 36.1146 36.1183 36.1479 36.1516 36.1627 36.1738 36.1886 36.1923 36.1997 36.2256 36.2515 36.2589 36.2700 36.2737 36.2774 36.2848 36.3292 36.3514 36.3625 36.3736 36.3921 37.2468 38.4789 38.5233 38.5418 38.5455 38.5492 38.6454 38.8822
39.0043
49.5308

Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to $1 E 6$ Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6
(
1 -> Fixing to $\mathrm{HL}=1.0 \mathrm{e}-10$
1 -> Fixing to $H L=1.0 \mathrm{e}-10$
$1->$ Fixing to $H L=1.0 \mathrm{e}-10$
$1->$ Fixing to $H L=1.0 \mathrm{e}-10$

17.966 for phase no. 17.921 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.964 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.964 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no. 17.920 for phase no. 17.965 for phase no.
-> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 $->$ Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to $\mathrm{HL}=1.0 \mathrm{e}-10$ -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 $->$ Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to HL=1.0e-10 -> Fixing to $\mathrm{HL}=1.0 \mathrm{e}-10$ -> Fixing to HL=1.0e-10
-> Fixing to HL=1.0e-10

Standard deviations have to be multiplied by:15.9393 (correlated residuals) See references:
-J.F.Berar \& P.Lelann, J. Appl. Cryst. 24, 1-5 (1991)
-J.F.Berar, Acc. in Pow. Diff. II,NIST Sp.Pub. 846, 63(1992)
$\Rightarrow$ CYCLE No.: 50
=> Phase 1 Name: rdx
$\Rightarrow$ New parameters, shifts, and standard deviations


$==>$ PROFILE PARAMETERS FOR PATTERN\# 1
$\begin{array}{llll}=> & \text { Overall scale factor: } 0.003677659 & -0.000000780 \quad 0.000011493\end{array}$
$\Rightarrow$ Eta(p-Voigt) or m(Pearson VII): 0.000000 0.000000 0.000000
$\Rightarrow$ Overall tem. factor: 0.0000000 .0000000 .000000
$\Rightarrow$ Halfwidth parameters:
$0.014150 \quad 0.000261 \quad 0.003446$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Cell parameters:
$\begin{array}{lll}11.557671 & 0.000021 & 0.000273\end{array}$
$10.676690 \quad 0.000017 \quad 0.000281$
$13.141932 \quad 0.000026 \quad 0.000305$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
=> Preferred orientation:
1.0000000 .0000000 .000000
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Asymmetry parameters:
$0.165592-0.000072 \quad 0.008782$
$0.053462-0.000027 \quad 0.001781$ $0.000000 \quad 0.000000 \quad 0.000000$ $0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow X$ and $Y$ parameters
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Strain parameters:
$0.000000 \quad 0.0000000 .000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Size parameters (G,L):
$0.012007-0.000010 \quad 0.000086$
$-0.025048 \quad 0.000745 \quad 0.004665$
$\Rightarrow$ Further shape parameters (S_L and D_L) :
$0.0000000 .000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Spherical Harmonics coeff. (size) :

| -0.025048 | 0.000745 | 0.004665 | 0.019418 | -0.001630 | 0.013391 | 0.197667 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0.010955 | 0.000007 | 0.013803 | -0.039622 | -0.001868 | 0.013335 | 0.019753 |  |
| 0.210143 | 0.011426 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.0000 | 0.000 |

$==>$ GLOBAL PARAMETERS FOR PATTERN\# 1
=> Zero-point: -0.2154 0.0001 0.0022
=> Background Polynomial Parameters ==>
$\begin{array}{lll}0.11847 \mathrm{E}+060.0000 & 0.0000\end{array}$

| $0.72376 \mathrm{E}+06$ | 0.0000 | 0.0000 |
| :--- | :--- | :--- |
| -47087. | 0.0000 | 0.0000 |
| $-0.18536 \mathrm{E}+07$ | 0.0000 | 0.0000 |
| $-0.14029 \mathrm{E}+07$ | 0.0000 | 0.0000 |
| -35943. | 0.0000 | 0.0000 |

$\Rightarrow \operatorname{Cos}($ theta)-shift parameter $: 0.00000 .00000 .0000$
$\Rightarrow \operatorname{Sin}(2 t h e t a)-s h i f t$ parameter $: 0.00000 .00000 .0000$
$==>$ RELIABILITY FACTORS WITH ALL NON-EXCLUDED POINTS FOR PATTERN: 1


| $=>$ | Conventional Rietveld Rp,Rwp,Re and Chi2: | 14.1 | 23.3 | 1.44 | 263.3 |
| :--- | :--- | :--- | :--- | :--- | :--- |

$\Rightarrow$ (Values
$\Rightarrow$ SumYnet, Sum (w Ynet**2): $0.5204 \mathrm{E}+08 \quad 0.5204 \mathrm{E}+08$
=> N -sigma of the GoF: $* * * * * * * *$
$==>$ RELIABILITY FACTORS FOR POINTS WITH BRAGG CONTRIBUTIONS FOR PATTERN: 1

$\Rightarrow$ (Values obtained using Ynet, but true sigma(y) )
$\Rightarrow$ SumYnet, Sum (w Ynet**2): 0.5204E+08 0.5203E+08
=> N-sigma of the GoF: 19232.480
=> Global user-weigthed Chi2 (Bragg contrib.): 264.


$\begin{array}{llcccc}61 & 1 & 2 & 4 & 0 & 4\end{array} 0.139729$

| 26.295 | 477.2 | 468.6 | 8.507 | 0.127464 | 0.008127 | 0.082439 | $\checkmark$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 26.448 | 155.3 | 169.9 | 16.049 | 0.127506 | 0.008555 | 0.086508 | $\checkmark$ |
| 26.803 | 238.4 | 281.9 | 51.333 | 0.127608 | 0.018097 | 0.171977 | $\checkmark$ |
| 26.847 | 919.2 | 1051.8 | 151.421 | 0.127620 | 0.011554 | 0.114468 | $\checkmark$ |
| 27.057 | 3627.0 | 3717.6 | 92.802 | 0.127682 | 0.006239 | 0.063979 | $\checkmark$ |
| 27.118 | 2486.4 | 2612.2 | 131.679 | 0.127700 | 0.027363 | 0.245424 | $\checkmark$ |
| 27.422 | 1171.2 | 1287.3 | 127.507 | 0.127790 | 0.008230 | 0.083217 | $\checkmark$ |
| 28.097 | 23.2 | 22.8 | 4.775 | 0.127997 | 0.017384 | 0.165495 | 2 |
| 28.215 | 0.1 | 0.1 | 0.046 | 0.128034 | 0.023806 | 0.217723 | $\checkmark$ |
| 29.362 | 4563.9 | 4918.6 | 381.135 | 0.128409 | 0.019979 | 0.186618 | $\checkmark$ |
| 29.451 | 3494.9 | 3560.3 | 66.512 | 0.128439 | 0.012778 | 0.124866 | $\swarrow$ |
| 29.451 | 6978.2 | 7140.8 | 165.994 | 0.128439 | 0.020550 | 0.191234 | $\checkmark$ |
| 29.548 | 161.6 | 159.0 | 2.566 | 0.128472 | 0.005875 | 0.060035 | $\checkmark$ |
| 30.242 | 3.7 | 2.0 | 1.291 | 0.128713 | 0.011779 | 0.115616 | $\checkmark$ |
| 30.572 | 2758.7 | 2709.9 | 47.994 | 0.128831 | 0.010324 | 0.102197 | $\checkmark$ |
| 30.923 | 1299.6 | 1311.4 | 11.983 | 0.128958 | 0.034495 | 0.294131 | $\checkmark$ |
| 31.292 | 2039.8 | 1894.2 | 134.858 | 0.129095 | 0.018797 | 0.176039 | $\checkmark$ |
| 31.688 | 522.2 | 458.6 | 55.691 | 0.129245 | 0.016572 | 0.157202 | $\checkmark$ |
| 31.959 | 117.9 | 99.8 | 15.267 | 0.129349 | 0.015927 | 0.151586 | $\checkmark$ |
| 32.027 | 431.8 | 412.0 | 18.845 | 0.129375 | 0.015661 | 0.149279 | 2 |
| 32.064 | 1102.2 | 1112.0 | 9.881 | 0.129390 | 0.032849 | 0.282068 | $\checkmark$ |
| 32.422 | 3338.3 | 3440.9 | 105.543 | 0.129530 | 0.017398 | 0.163870 | $\checkmark$ |
| 32.511 | 3523.3 | 3602.1 | 80.514 | 0.129566 | 0.010517 | 0.103425 | $\checkmark$ |
| 32.798 | 425.0 | 376.3 | 42.985 | 0.129681 | 0.030543 | 0.265378 | $\checkmark$ |
| 32.908 | 305.6 | 299.0 | 6.479 | 0.129726 | 0.015334 | 0.146104 | 2 |
| 33.323 | 1831.2 | 1906.9 | 78.738 | 0.129896 | 0.008330 | 0.082886 | $\checkmark$ |
| 33.546 | 480.4 | 496.1 | 16.214 | 0.129989 | 0.009777 | 0.096312 | $\checkmark$ |
| 33.862 | 60.0 | 46.5 | 10.628 | 0.130122 | 0.026491 | 0.235129 | $\checkmark$ |
| 34.252 | 507.9 | 372.5 | 99.203 | 0.130290 | 0.009406 | 0.092680 | $\checkmark$ |
| 34.918 | 433.3 | 440.3 | 7.320 | 0.130582 | 0.025893 | 0.229955 | $\checkmark$ |
| 34.967 | 2357.7 | 2417.3 | 61.202 | 0.130604 | 0.019059 | 0.176388 | 2 |
| 35.146 | 12.1 | 12.7 | 0.641 | 0.130685 | 0.010799 | 0.105165 | $\checkmark$ |
| 35.257 | 2207.0 | 2394.2 | 202.655 | 0.130734 | 0.015524 | 0.146704 | $\checkmark$ |
| 35.292 | 432.8 | 477.0 | 48.558 | 0.130750 | 0.029701 | 0.257600 | $\downarrow$ |
| 35.621 | 11.9 | 8.5 | 2.600 | 0.130900 | 0.015219 | 0.143933 | $\checkmark$ |
| 35.893 | 441.0 | 525.6 | 100.615 | 0.131026 | 0.018461 | 0.170986 | $\checkmark$ |
| 35.967 | 311.8 | 328.8 | 17.971 | 0.131061 | 0.028134 | 0.245796 | $\checkmark$ |
| 36.008 | 13.1 | 12.4 | 0.665 | 0.131080 | 0.011414 | 0.110410 | $\checkmark$ |
| 36.008 | 64.0 | 60.7 | 3.126 | 0.131080 | 0.027048 | 0.237803 | $\checkmark$ |
| 36.297 | 12.7 | 5.9 | 6.289 | 0.131217 | 0.009202 | 0.090185 | $\checkmark$ |
| 36.898 | 49.9 | 73.2 | 34.195 | 0.131505 | 0.018076 | 0.167275 | $\checkmark$ |
| 36.977 | 726.8 | 849.2 | 142.751 | 0.131544 | 0.017201 | 0.159991 | $\checkmark$ |

2theta Icalc Iobs Sigma HwG HwL ETA $~$ H


| 37.149 | 488.4 | 455.9 | 30.297 | 0.131628 | 0.010448 | 0.101293 | $\swarrow$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 37.718 | 417.5 | 375.2 | 37.881 | 0.131911 | 0.014708 | 0.138575 | $\checkmark$ |
| 37.932 | 2.0 | 3.1 | 1.691 | 0.132019 | 0.024890 | 0.220317 | $\checkmark$ |
| 38.048 | 2.2 | 2.9 | 0.929 | 0.132078 | 0.013285 | 0.126126 | $\checkmark$ |
| 38.132 | 403.0 | 419.6 | 17.278 | 0.132121 | 0.023255 | 0.207719 | $\checkmark$ |
| 38.222 | 1692.6 | 1640.2 | 50.692 | 0.132167 | 0.022666 | 0.203114 | $\checkmark$ |
| 38.530 | 25.4 | 31.0 | 6.909 | 0.132326 | 0.023891 | 0.212316 | $\checkmark$ |
| 38.949 | 8.8 | 20.8 | 28.151 | 0.132546 | 0.022495 | 0.201292 | $\checkmark$ |
| 39.502 | 139.8 | 138.8 | 1.122 | 0.132842 | 0.010603 | 0.101815 | $\checkmark$ |
| 39.608 | 691.6 | 672.3 | 18.744 | 0.132899 | 0.014028 | 0.131817 | $\checkmark$ |
| 39.783 | 234.7 | 278.8 | 52.341 | 0.132994 | 0.017661 | 0.162214 | $\checkmark$ |
| 40.136 | 92.2 | 145.1 | 82.930 | 0.133189 | 0.016644 | 0.153619 | $\checkmark$ |
| 40.167 | 9.4 | 14.2 | 7.327 | 0.133206 | 0.027673 | 0.239153 | $\checkmark$ |
| 40.296 | 266.8 | 410.4 | 220.572 | 0.133278 | 0.011579 | 0.110176 | $\checkmark$ |
| 40.462 | 15.3 | 26.6 | 19.638 | 0.133370 | 0.014877 | 0.138621 | $\checkmark$ |
| 40.480 | 59.6 | 105.4 | 80.546 | 0.133381 | 0.037264 | 0.304463 | $\swarrow$ |
| 40.773 | 253.2 | 366.1 | 162.566 | 0.133546 | 0.026738 | 0.231839 | $\checkmark$ |
| 41.028 | 78.9 | 143.1 | 116.093 | 0.133691 | 0.022595 | 0.200563 | $\swarrow$ |
| 41.180 | 270.2 | 346.2 | 96.974 | 0.133778 | 0.036414 | 0.298241 | 2 |
| 41.318 | 6.5 | 7.4 | 0.990 | 0.133858 | 0.021430 | 0.191331 | 2 |
| 41.373 | 205.2 | 250.3 | 54.811 | 0.133890 | 0.034177 | 0.283304 | $\checkmark$ |
| 41.589 | 6.6 | 20.0 | 40.716 | 0.134016 | 0.022543 | 0.199743 | $\checkmark$ |
| 41.702 | 9.7 | 36.5 | 100.091 | 0.134083 | 0.020426 | 0.183187 | $\checkmark$ |
| 41.947 | 410.9 | 483.1 | 84.542 | 0.134227 | 0.034800 | 0.286870 | $\checkmark$ |
| 42.267 | 2.2 | 10.5 | 40.534 | 0.134418 | 0.033734 | 0.279447 | $\checkmark$ |
| 42.450 | 14.8 | 27.2 | 22.546 | 0.134528 | 0.022844 | 0.201384 | $\checkmark$ |
| 42.480 | 218.1 | 352.4 | 216.317 | 0.134546 | 0.022498 | 0.198718 | $\swarrow$ |
| 42.550 | 276.5 | 416.9 | 211.109 | 0.134588 | 0.024753 | 0.215702 | $\checkmark$ |
| 42.603 | 119.1 | 182.5 | 96.935 | 0.134621 | 0.014503 | 0.134305 | $\checkmark$ |
| 42.832 | 8.6 | 56.8 | 317.859 | 0.134760 | 0.033085 | 0.274517 | $\swarrow$ |
| 43.164 | 0.6 | 12.6 | 246.240 | 0.134965 | 0.035583 | 0.290752 | 2 |
| 43.448 | 61.2 | 262.6 | 862.094 | 0.135141 | 0.019444 | 0.174196 | $\swarrow$ |
| 43.477 | 1.5 | 5.6 | 14.663 | 0.135159 | 0.019537 | 0.174911 | 2 |
| 43.615 | 78.4 | 151.3 | 140.411 | 0.135247 | 0.015831 | 0.144812 | $\checkmark$ |
| 43.655 | 233.7 | 408.4 | 304.666 | 0.135272 | 0.014041 | 0.129816 | $\checkmark$ |
| 44.183 | 234.0 | 461.2 | 445.975 | 0.135607 | 0.031470 | 0.262177 | $\checkmark$ |
| 44.240 | 28.9 | 48.7 | 33.306 | 0.135644 | 0.018353 | 0.164943 | $\checkmark$ |
| 44.388 | 50.9 | 114.7 | 143.656 | 0.135739 | 0.014707 | 0.135001 | $\checkmark$ |
| 44.683 | 44.9 | 139.9 | 295.294 | 0.135931 | 0.030099 | 0.252217 | $\checkmark$ |
| 44.864 | 116.7 | 201.2 | 145.092 | 0.136050 | 0.032881 | 0.271036 | $\checkmark$ |
| 45.033 | 381.8 | 504.5 | 161.474 | 0.136161 | 0.030379 | 0.253806 | $\checkmark$ |
| 45.038 | 16.5 | 21.3 | 6.253 | 0.136164 | 0.022053 | 0.193276 | $\checkmark$ |
| 45.066 | 284.6 | 367.8 | 107.263 | 0.136183 | 0.022680 | 0.198019 | $\checkmark$ |
| 45.117 | 180.2 | 237.5 | 75.063 | 0.136217 | 0.030455 | 0.254243 | $\checkmark$ |
| 45.234 | 3.6 | 5.5 | 2.959 | 0.136295 | 0.019062 | 0.169870 | $\checkmark$ |


| 107 | 1 | 1 | 5 |  | 8 | 0.144726 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 2.000154 |  | 43.714397 |  |  |  |
| 108 | 1 | 4 | 3 | 3 | 8 | 0.148983 |
|  | 1.996637 |  | 43.527786 |  |  |  |
| 109 | 1 | 1 | 2 | 6 | 8 | 0.152351 |
|  | 1.995937 |  | 43.488667 |  |  |  |
| 110 | 1 | 2 | 3 | 5 | 8 | 0.147379 |
|  | 1.985559 |  | 42.952629 |  |  |  |
| 111 | 1 | 2 | 5 | 1 | 8 | 0.146777 |
|  | 1.980102 |  | 42.675720 |  |  |  |
| 112 | 1 | 3 | 4 | 3 | 8 | 0.147295 |
|  | 1.961735 |  | 41.732731 |  |  |  |
| 113 | 1 | 4 | 4 | 0 | 4 | 0.151994 |
|  | 1.960631 |  | 20.838533 |  |  |  |
| 114 | 1 | 2 | 4 | 4 | 8 | 0.146202 |
|  | 1.950139 |  | 41.143612 |  |  |  |
| 115 | 1 | 4 | 4 | 1 | 8 | 0.152075 |
|  | 1.939170 |  | 40.591351 |  |  |  |
| 116 | 1 | 6 | 0 | 0 | 2 | 0.162899 |
|  | 1.926275 |  | 9.985799 |  |  |  |
| 117 | 1 | 5 | 3 | 1 | 8 | 0.156524 |
|  | 1.917771 |  | 39.521759 |  |  |  |
| 118 | 1 | 2 | 5 | 2 | 8 | 0.147731 |
|  | 1.915934 |  | 39.433163 |  |  |  |
| 119 | 1 | 4 | 1 | 5 | 8 | 0.151386 |
|  | 1.912836 |  | 39.274673 |  |  |  |
| 120 | 1 | 2 | 2 | 6 | 8 | 0.153063 |
|  | 1.912226 |  | 39.244450 |  |  |  |
| No. | Code |  | K | $\begin{aligned} & \mathrm{L} \quad \text { Mult } \\ & \text { CORR } \end{aligned}$ |  | Hw |
|  |  | hkl |  |  |  |  |
| 121 | 1 | 5 | 2 | 3 | 8 | 0.154413 |
|  | 1.909163 |  | 39.094662 |  |  |  |
| 122 | 1 | 3 | 0 | 6 | 4 | 0.153864 |
|  | 1.904096 |  | 19.421478 |  |  |  |
| 123 | 1 | 6 | 1 | 0 | 4 | 0.163132 |
|  | 1.895669 |  | 19.215900 |  |  |  |
| 124 | 1 | 1 | 5 | 3 | 8 | 0.146969 |
|  | 1.893506 |  | 38.329342 |  |  |  |
| 125 | 1 | 5 | 0 | 4 | 4 | 0.154006 |
|  | 1.890512 |  | 19.089468 |  |  |  |
| 126 | 1 | 4 | 4 | 2 | 8 | 0.152597 |
|  | 1.878781 |  | 37.612156 |  |  |  |
| 127 | 1 | 6 | 1 | 1 | 8 | 0.162876 |
|  | 1.876250 |  | 37.487667 |  |  |  |
| 128 | 1 | 3 | 1 | 6 | 8 | 0.154167 |
|  | 1.874519 |  | 37.402283 |  |  |  |
| 129 | 1 | 0 | 4 | 5 | 4 | 0.148898 |
|  | 1.872800 |  | 18.661100 |  |  |  |
| 130 | 1 | 5 | 1 | 4 | 8 | 0.154620 |
|  | 1.861554 |  | 36.780247 |  |  |  |
| 131 | 1 | 5 | 3 | 2 | 8 | 0.156642 |
|  | 1.859300 |  | 36.674236 |  |  |  |
| 132 | 1 | 3 | 3 | 5 | 8 | 0.150943 |
|  | 1.853503 |  | 36.396729 |  |  |  |
| 133 | 1 | 4 | 3 | 4 | 8 | 0.151822 |
|  | 1.852572 |  | 36.352833 |  |  |  |
| 134 | 1 | 3 | 5 | 1 | 8 | 0.151793 |
|  | 1.849062 |  | 36.189026 |  |  |  |
| 135 | 1 | 1 | 4 | 5 | 8 | 0.149623 |
|  | 1.848687 |  | 36.168797 |  |  |  |
| 136 | 1 | 6 | 0 | 2 | 4 | 0.162073 |
|  | 1.848485 |  | 18.078987 |  |  |  |
| 13 | 1 | 1 | 3 | 6 | 8 | 0.153527 |
|  | $1.841518$ |  |  | 827 |  |  |
| 13 | 1 | 4 | 2 | 5 | 8 | 0.153203 |
|  | 1.826896 |  |  | 140 |  |  |
| 13 | 1 | 1 | 1 | 7 | 8 | 0.161109 |
|  | 1.825828 |  |  | 089 |  |  |
| 14 | 1 | 3 | 4 | 4 | 8 | 0.150733 |
|  | 1.824592 |  |  | 034 |  |  |
| 14 | 1 | 2 | 5 | 3 | 8 | 0.149882 |
|  | 1.821587 |  |  | 896 |  |  |
| 142 | 1 | 6 | 1 | 2 | 8 | 0.162498 |
|  | 1.821389 |  |  | 884 |  |  |

45.301
45.385
45.402
45.653 45.786 46.239 46.267
46.530
46.809
47.141
47.363
47.411
47.493
47.509

$$
2 \text { theta }
$$

47.590

| 13.1 | 26.9 | 28.187 | 0.137926 | 0.030357 | 0.250960 | $\swarrow$ |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| 28.3 | 87.7 | 183.311 | 0.138023 | 0.029210 | 0.242893 |  |

47.950
48.008
48.089
48.408
48.478
48.525
48.573
48.885
48.949
49.112
49.138

$$
49.238
$$

| 4.0 | 8.0 | 7.976 | 0.136340 | 0.015646 | 0.142244 |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 48.2 | 133.9 | 237.399 | 0.136396 | 0.023351 | 0.202813 |
| 15.6 | 45.2 | 85.406 | 0.136407 | 0.029381 | 0.246491 |
| 110.4 | 290.6 | 472.772 | 0.136575 | 0.020099 | 0.177704 |
| 26.0 | 74.3 | 137.757 | 0.136666 | 0.018829 | 0.167624 |
| 2.5 | 3.3 | 0.968 | 0.136975 | 0.019213 | 0.170313 |
| 1084.3 | 1397.4 | 402.098 | 0.136994 | 0.027700 | 0.233777 |
| 7.1 | 19.9 | 35.734 | 0.137177 | 0.016829 | 0.151086 |
| 423.6 | 524.9 | 125.033 | 0.137371 | 0.027174 | 0.229487 |
| 3.2 | 13.1 | 40.673 | 0.137605 | 0.045561 | 0.347164 |
| 324.0 | 462.4 | 196.551 | 0.137763 | 0.034363 | 0.278069 |
| 87.0 | 110.0 | 29.080 | 0.137798 | 0.018504 | 0.163835 |
| 4.7 | 6.7 | 2.766 | 0.137856 | 0.025063 | 0.213579 |
| 1.8 | 2.7 | 1.322 | 0.137868 | 0.028056 | 0.235041 |
| Icalc | Iobs | Sigma | HwG | HwL | ETA |

$$
49.248
$$

$$
49.254
$$

$$
49.453
$$

$$
49.875
$$

49.907
49.943
50.031
50.037

| 72.1 | 175.1 | 248.695 | 0.138186 | 0.044986 | 0.342748 |  |  |
| :--- | ---: | ---: | ---: | ---: | ---: | ---: | :---: |
| 14.8 | 35.8 | 50.545 | 0.138229 | 0.016303 | 0.145807 |  |  |
| 29.1 | 81.0 | 144.198 | 0.138288 | 0.028994 | 0.241001 | , |  |

[^0]$\Rightarrow$ Bragg R-factor: $6.97 \quad$ Vol: $1621.684(0.069)$ Fract (\%): 100.00( 0.44 )
$\Rightarrow$ Rf-factor $=9.79 \quad$ ATZ: $1776.939 \quad$ Brindley: 1.0000

## SYMBOLIC NAMES AND FINAL VALUES AND SIGMA OF REFINED PARAMETERS:

-> Parameter number 1 : G-Size_ph1_pat1 0.12007418E-01 ( +/- 0.85642365E-04)

| -> | Parameter number | 2 | : | Zero_pat1 | -0.21540712 | +/- | 0.21793407E-02 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| -> | Parameter number | 3 | : | Scale_ph1_pat1 | $0.36776587 \mathrm{E}-02($ | +/- | 0.11493407E-04 |
| -> | Parameter number | 4 | : | U-Cagl_ph1_pat 1 | 0.14149698E-01( | +/ - | 0.34455676E-02 |
| -> | Parameter number | 5 | : | Cell_A_ph1_pat 1 | 11.557671 ( | +/- | 0.27274666E-03 |
| -> | Parameter number | 6 | : | Cell_B_ph1_pat 1 | 10.676690 ( | +/- | 0.28143937E-03 |
| -> | Parameter number | 7 | : | Cell_C_ph1_pat | 13.141932 ( | +/- | 0.30492945E-03 |
| -> | Parameter number | 8 | : | $\mathrm{x}_{\mathrm{O}} \mathrm{O}(1)-\mathrm{ph} 1$ | 0.57030642 | +/- | 0.50944550E-03 |
| -> | Parameter number | 9 | : | Y_O(1) _-ph1 | 0.44054043 | +/- | 0.58024272E-03 |
| -> | Parameter number | 10 | : | Z_O(1) _-ph1 | 0.26806968 | +/- | 0.53565676E-03 |
| -> | Parameter number | 11 | : | $\mathrm{x}_{\text {_ }} \mathrm{O}(2)$ _ ph 1 | 0.59821874 | +/- | 0.59325760E-03 |
| -> | Parameter number | 12 | : | Y_O(2) _-ph1 | 0.23070036 ( | +/- | 0.58002409E-03 |
| -> | Parameter number | 13 | : | Z_O(2) _ph 1 | 0.22521888 | +/- | 0.52235578E-03 |
| -> | Parameter number | 14 | : | $\mathrm{X}_{\mathrm{O}} \mathrm{O}$ (3)-ph1 | 0.47699246 | +/- | 0.58257120E-03 |
| -> | Parameter number | 15 | : | Y_O (3) _ Ph 1 | 0.13119514 | +/- | 0.53428166E-03 |
| -> | Parameter number | 16 | : | Z_O(3)_-ph1 | -0.16466578E-01( | +/- | 0.51274599E-03 |
| -> | Parameter number | 17 | : | X_0 (4) _ ph 1 | 0.34888738 ( | +/- | 0.59821649E-03 |
| -> | Parameter number | 18 | : | Y_O (4) - ph 1 | 0.25898808 | +/- | $0.66673080 \mathrm{E}-03$ |
| -> | Parameter number | 19 | : | $\mathrm{Z}_{\mathrm{O}} \mathrm{O}(4)$ _ ph 1 | -0.11068642 | +/- | 0.58052666E-03 |
| -> | Parameter number | 20 | : | X_O(5)_ph1 | 0.30777898 | +/- | 0.54655079E-03 |
| -> | Parameter number | 21 | : | Y_O (5) _-ph1 | 0.51705146 | +/- | $0.63611532 \mathrm{E}-03$ |
| -> | Parameter number | 22 | : | Z_O(5)_ph1 | -0.79056025E-01( | +/- | $0.50401402 \mathrm{E}-03$ |
| -> | Parameter number | 23 | : | $\mathrm{X}_{\text {_ }} 0(6)$ _ ph 1 | 0.42721874 | +/- | 0.51176769E-03 |
| -> | Parameter number | 24 | : | Y_O(6)_Ph1 | 0.60060859 ( | +/- | $0.74724230 \mathrm{E}-03$ |
| -> | Parameter number | 25 | : | $\mathrm{Z}_{-} 0(6)$ _ph 1 | $0.52727856 \mathrm{E}-01($ | +/- | $0.53174264 \mathrm{E}-03$ |
| -> | Parameter number | 26 | : | $\mathrm{X}_{\text {_ }} \mathrm{N}(1)$ - ph 1 | 0.44408569 | +/- | $0.76306117 \mathrm{E}-03$ |
| -> | Parameter number | 27 | : | Y_N(1) _Ph1 | 0.33099678 | +/- | 0.98512415E-03 |
| -> | Parameter number | 28 | : | $\mathrm{Z}_{\text {_ }} \mathrm{N}(1)$ _ ph 1 | 0.17287177 | +/- | 0.62338362E-03 |
| -> | Parameter number | 29 | : | $\mathrm{X}_{\mathbf{N}} \mathrm{N}$ (2) _ ph 1 | 0.32741672 ( | +/- | $0.94491179 \mathrm{E}-03$ |
| -> | Parameter number | 30 | : | Y_N (2)_Ph1 | 0.23490509 ( |  | 0.88645355E-03 |
| -> | Parameter number | 31 | : | $\mathrm{Z}_{\mathrm{N}} \mathrm{N}$ (2) _ ph 1 | 0.53277619E-01( | +/- | $0.72490342 \mathrm{E}-03$ |
| -> | Parameter number | 32 | : | $\mathrm{X}_{-} \mathrm{N}$ (3) _ ph 1 | 0.30725399 ( | +/- | $0.85900084 \mathrm{E}-03$ |
| -> | Parameter number | 33 | : | Y_N (3) _- Ph 1 | 0.45634460 | +/- | $0.81957324 \mathrm{E}-03$ |
| -> | Parameter number | 34 | : | $\mathrm{Z}_{\text {- }} \mathrm{N}(3)$ _ ph 1 | $0.82887992 \mathrm{E}-01($ | +/- | $0.67181664 \mathrm{E}-03$ |
| -> | Parameter number | 35 | : | $\mathrm{X}_{\text {_ }} \mathrm{N}(4)$ _ ph 1 | 0.53932601 ( | +/- | $0.68082550 \mathrm{E}-03$ |
| -> | Parameter number | 36 | : | Y_N (4) _Ph1 | 0.33542445 ( | +/- | $0.69672387 \mathrm{E}-03$ |
| -> | Parameter number | 37 | : | $\mathrm{Z}_{\text {_ }} \mathrm{N}(4)$ _ ph 1 | 0.23514608 ( |  | $0.67948614 \mathrm{E}-03$ |
| -> | Parameter number | 38 | : | $\mathrm{X}_{\text {_ }} \mathrm{N}(5)$ _ ph 1 | 0.38598049 ( |  | $0.79134514 \mathrm{E}-03$ |
| -> | Parameter number | 39 | : | Y_N (5)_-ph1 | 0.20331475 | +/- | 0.91921864E-03 |
| -> | Parameter number | 40 | : | Z_N (5)_ph1 | -0.41405533E-01( | +/- | $0.79785188 \mathrm{E}-03$ |
| -> | Parameter number | 41 | : | $\mathrm{X}_{\mathbf{N}} \mathrm{N}$ (6) _ ph 1 | 0.35495391 | +/- | $0.68654644 \mathrm{E}-03$ |
| -> | Parameter number | 42 | : | Y_N (6) _ph 1 | 0.54360700 | +/- | $0.92109625 \mathrm{E}-03$ |
| -> | Parameter number | 43 | : | $\mathrm{Z}_{\text {- }} \mathrm{N}(6)$ _ph1 | $0.99107744 \mathrm{E}-02($ | +/- | $0.78920758 \mathrm{E}-03$ |
| -> | Parameter number | 44 | : | $\mathrm{X}_{-} \mathrm{C}(1)$ _ ph 1 | 0.34678712 ( | +/- | 0.84853295E-03 |
| -> | Parameter number | 45 | : | Y_C (1) _- Ph 1 | 0.43853557 ( | +/- | $0.93395612 \mathrm{E}-03$ |
| -> | Parameter number | 46 | : | $\mathrm{Z}_{\mathrm{C}} \mathrm{C}(1)$ _- ph 1 | 0.19867958 ( |  | $0.73884765 \mathrm{E}-03$ |
| -> | Parameter number | 47 | : | $\mathrm{X}_{\mathrm{C}} \mathrm{C}(2)$ _- ph 1 | 0.38558781 |  | 0.87032176E-03 |
| -> | Parameter number | 48 | : | Y_C (2)_-ph1 | 0.21305369 ( | +/- | $0.93864364 \mathrm{E}-03$ |
| -> | Parameter number | 49 | : | $\mathrm{z}_{-} \mathrm{C}(2)$ _ph1 | 0.15540366 ( | +/- | 0.96520188E-03 |
| -> | Parameter number | 50 | : | $\mathrm{X}_{\text {_ }} \mathrm{C}$ (3) $\mathrm{S}^{\text {Ph } 1}$ | 0.23576419 ( | +/- | $0.71329746 \mathrm{E}-03$ |
| -> | Parameter number | 51 | : | Y_C (3) _- Ph 1 | 0.34061772 ( | +/- | 0.13099160E-02 |
| - | Parameter number | 52 | : | $\mathrm{Z}_{\text {_ }} \mathrm{C}$ (3) _ ph 1 | 0.52318119E-01 ( | +/- | $0.63173153 \mathrm{E}-03$ |
| -> | Parameter number | 53 | : | Asym1_ph1_pat 1 | 0.16559245 ( | +/- | $0.87822555 \mathrm{E}-02$ |
| -> | Parameter number | 54 | : | Asym2_ph1_pat1 | $0.53462289 \mathrm{E}-01($ |  | 0.17806906E-02 |
| -> | Parameter number | 55 | : | L-Size_ph1_pat 1 | -0.25047939E-01( |  | 0.46645673E-02 |
| -> | Parameter number | 56 | : | Size2_ph1_pat1 | 0.19417906E-01 ( | +/- | 0.13390562E-01 |
| -> | Parameter number | 57 | : | Size3_ph1_pat 1 | 0.19766724 ( | +/- | 0.10954754E-01 |
| -> | Parameter number | 58 | : | Size4_ph1_pat1 | 0.21014285 | +/- | $0.13802625 \mathrm{E}-01$ |
| -> | Parameter number | 59 | : | Size5_ph1_pat 1 | -0.39622393E-01 | +/- | 0.13335176E-01 |
| -> | Parameter number | 60 | : | Size6_ph1_pat1 | 0.19753376E-01( | +/- | 0.11426117E-01 |

=> Number of bytes for floating point variables: 4
=> Dimensions of dynamic allocated arrays in this run of FullProf:
$\Rightarrow$ Total approximate array memory (dynamic + static): 107719993 bytes
MaxPOINT= 60000 Max.num. of points(+int. Inten.)/diffraction pattern MaxREFLT $=20000$ Max.num. of reflections/diffraction pattern
Maxparam $=$
MaxOVERL $=2096$ Max.num. of overlapping reflections
$\Rightarrow$ Number of bytes for floating point arrays: 4
$\Rightarrow$ Dimensions of fixed arrays in this release of FullProf:

| NPATT | $=$ | 80 Max.num. of powder diffraction patterns |
| :--- | :--- | ---: | :--- |
| NATS | $=$ | 830 Max.num. of atoms (all kind) in asymmetric unit |
| MPAR | $=$ | 1800 Max.num. of non atomic parameters/phase |
| IEXCL | $=$ | 30 Max.num. of excluded regions |
| IBACP | $=$ | 277 Max.num. of background points for interpolation |
| NPHT | $=$ | 16 Max.num. of phases |
| NMAGM | $=$ | 8 Max.num. of rotation-matrices sets for magnetic structure |
| NBASIS | $=$ | 12 Max.num. of basis functions associated to a single atom |
| NIREPS | $=$ | 9 Max.num. of irreducible representations to be combined |
| N_EQ | $=$ | 384 Max.num. of user-supplied symmetry operators/propagation vectors |
| NGL | $=300$ Max.num. of global parameters/diffraction pattern |  |
| N_LINC | $=$ | 30 Max.num. of global linear restraints |
| NAT_P | $=$ | 64 Max.num. of atomic parameters per atom |



## A. 3 Sample of n-RDX processed pure at $3 \mathrm{wt} \%$ in acetone

```
**********************************************************
** PROGRAM FullProf.2k (Version 5.50 - Dec2014-ILL JRC) **
***********************************************************
M U L T I -- P A T T E R N
Rietveld, Profile Matching & Integrated Intensity
Refinement of X-ray and/or Neutron Data
Date: 18/02/2015 Time: 13:16:26.953
=> PCR file code: 3b
=> DAT file code: 3b.dat -> Relative contribution: 1.0000
==> CONDITIONS OF THIS RUN FOR PATTERN No.: 1
=> Global Refinement of X-ray powder diffraction data
=> Global Refinement of X-ray powder diffraction data
Flat plate with PSD
=> Title:RDX
=> Number of phases: 1
> Number of excluded regions: 0
=> Number of scattering factors supplied: 0
=> March-Dollase model for preferred orientation
=> Conventional weights: w=1.0/Variance(yobs)
=> Asymmetry correction as in J.Appl.Cryst. 26,128(1993)
=> Background linearly interpolated between the 6 points given
=> The 5th default profile function was selected
> Pseudo-Voigt function (ETA variable)
X-parameter correspond to: ETA=ETAO+X*2theta
pV(x)= ETA*L(x)+(1-ETA)*G(x)
==> INPUT/OUTPUT OPTIONS:
=> Generate file *.PRF for plot
=> Output Integrated Intensities
=> Generate new input file *.PCR
=> Data supplied in free format for pattern: 1
=> Plot pattern at each cycle
=> Wavelengths: 1.54056 1.54439
=> Alpha2/Alpha1 ratio: 0.5000
C Cos(Monochromator angle)= 1.0000
> Asymmetry correction for angles lower than 90.000 degrees
=> Absorption correction (AC), muR-eff = 0.0000 0.0000
=> Base of peaks: 2.0*HW* 20.00
=> Number of cycles: 50
=> Relaxation factors ==> for coordinates: 1.00
=> for anisotropic temperature factors: 1.00
=> for halfwidth/strain/size parameters: 1.00
> for lattice constants and propagation vectors: 1.00
=> EPS-value for convergence: 0.0
=> Background ==>
Position Intensity
\(15.00 \quad 16.91 \quad 0.00\)
\begin{tabular}{lll}
10.00 & -27.69 & 0.00
\end{tabular}
rrrer
30.00 13.02 0.00
35.00 -2.55 0.00
\begin{tabular}{lll}
38.00 & 37.25 & 0.00
\end{tabular}
```

=> Instrumental Resolution read from file: xray-res.irf
$\Rightarrow$ Title of data: Approximate resolution function of a conventional X-ray diffractometer CuKalpha1, 2
$\Rightarrow$ The resolution function is IRESOL: 1 for profile function \# 5
Input resolution parameters:

| U-inst | V-inst | W-inst | X-inst | Y-inst | Z-inst |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 0.00136 | -0.00500 | 0.00391 | 0.06389 | 0.00008 | 0.00000 |
| 0.00136 | -0.00500 | 0.00391 | 0.06389 | 0.00008 | 0.00000 |

```
=> Number of Least-Squares parameters varied: 5
=>-----------------------------
=>-------> PATTERN number: 1
---->
=> Global parameters and codes ==>
=> Zero-point: -0.0410 0.0000
=> Displacement peak-shift parameter and code: -0.10 0.00
=> Transparency peak-shift parameter and code: 0.26 0.00
=> Reading Intensity data =>>
==> Angular range, step and number of points:
2Thmin: 12.113000 2Thmax: 38.910702 Step: 0.024900 No. of points: 1077
=> Phase No. 
rdx
--------------------------------- Pattern# 1
=> Crystal Structure Refinement
=> The 7th profile function was selected for phase no. 1
=> Preferred orientation vector: 0.0000 0.0000 1.0000
=>-------> Data for PHASE: 1
=> Number of atoms: 21
=> Number of distance constraints: 0
=> Number of angle constraints: 0
=> Symmetry information on space group: P b c a
-> The multiplicity of the general position is:
-> The space group is Centric (-1 at origin)
-> Lattice type P: { 000 }
-> Reduced set of symmetry operators:
\begin{tabular}{|c|c|c|c|c|c|c|}
\hline No. IT & Symmetry & symbol & Ro & \multicolumn{3}{|l|}{Associated Translation} \\
\hline ( 1) & 1 & > & ( \(x, y, z\) ) + \{ & 0.0000 & 0.0000 & \(0.0000\}\) \\
\hline ( 4) & 2 ( \(\mathrm{x}, 0\), & 0) --> & \((x,-y,-z)+\{\) & 0.5000 & 0.5000 & \(0.0000\}\) \\
\hline ( 3) & 2 ( 0, y, & 0) --> & \((-x, y,-z)+\{\) & 0.0000 & 0.5000 & \(0.5000\}\) \\
\hline ( 2) & & z) --> & & 0.5000 & & \\
\hline
\end{tabular}
```

Information on Space Group:
$\Rightarrow$ Number of Space group: 61
$\Rightarrow$ Number of Space group:
$\Rightarrow$ Hermann-Mauguin Symbol: p b c a
$\begin{array}{lrl}\Rightarrow & \text { Hermann-Mauguin Symbol: } P \text { b c } a \\ \Rightarrow & \text { Hall Symbol: }-\mathrm{P} 2 \mathrm{ac} 2 \mathrm{ab}\end{array}$
$\Rightarrow \quad$ Table Setting Choice:
$\Rightarrow \quad$ Setting Type: IT (Generated from Hermann-Mauguin symbol)
$\Rightarrow \quad$ Crystal System: Orthorhombic
$\Rightarrow \quad$ Laue Class: mmm
$\Rightarrow \quad$ Bravais Lattice: $\Rightarrow$
$\Rightarrow \quad$ Lattice Symbol: oP
$\Rightarrow$ Reduced Number of S.O.: 4
$\Rightarrow \quad$ General multiplicity: $\quad 8$
$\Rightarrow$ Generators (exc. -1\&L): 2
$\Rightarrow \quad$ Asymmetric unit: $0.000<=x<=0.500$
$0.000<=y<=0.500$
$0.000<=\mathrm{z}<=0.500$
$\Rightarrow$ List of S.O. without inversion and lattice centring translations

=> Initial parameters ==>


| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 00.0 | $00 \quad 0.000$ |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| N (5) | N |  |  | 0.38834 | 0.20759 | -0.03308 | 3.09700 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 00.0 | $00 \quad 0.00$ |  |  |  |  |  |  |
| N (6) | N |  |  | 0.352990 | 0.52971 | 0.01650 | 3.43200 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | 00.0 .00 |  |  |  |  |  |  |
| C (1) | C |  |  | 0.357990 | 0.43950 | 0.18450 | 2.89510 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 00.0 | 00.0 .00 |  |  |  |  |  |  |
| C (2) | C |  |  | $0.38140 \quad 0$ | 0.21557 | 0.14950 | 2.70030 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 00.0 | 000.000 |  |  |  |  |  |  |
| C (3) | C |  |  | 0.24458 | 0.33936 | 0.05038 | 2.55740 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0 0.0 | 00.0 .000 |  |  |  |  |  |  |
| H (1A) | H |  |  | 0.402890 | 0.52403 | 0.20773 | 5.13220 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | 00.000 |  |  |  |  |  |  |
| H (1B) | H |  |  | 0.29071 0 | 0.42024 | 0.23991 | 4.84270 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | 00.000 |  |  |  |  |  |  |
| H (2A) | H |  |  | 0.44331 | 0.13918 | 0.14950 | 4.60580 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | 00.000 |  |  |  |  |  |  |
| H (2B) | H |  |  | 0.31742 | 0.19390 | 0.20730 | 4.97430 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | 00.0 .00 |  |  |  |  |  |  |
| H (3A) | H |  |  | 0.209360 | 0.35364 | -0.02527 | 4.50050 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | $00 \quad 0.000$ |  |  |  |  |  |  |
| H (3B) | H |  |  | 0.17213 | 0.32091 | 0.10070 | 3.92150 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: |  | 0.00000 | 0.00000 | 0.00000 | 0.0 | $00 \quad 0.00$ |  |  |  |  |  |  |

$\Rightarrow$ IT IS ASSUMED THAT THE FIRST GIVEN SITE IS FULLY OCCUPIED
OR THE FIRST AND SECOND ATOMS ARE IN THE SAME SITE WITH TOTAL FULL OCCUPATION
(If this is not the case, change the order of atoms to obtain correct values for the content of the unit cell)
The given occupation factors have been obtained mutiplying m/m by 1.0000

$\Rightarrow$ The given value of ATZ is $\quad 1776.94$ the program has calculated: $\quad 1776.94$
The value of ATZ given in the input PCR file will be used for quantitative analysis
$\Rightarrow$ The chemical content of the unit cell is:
 $8.0000 \mathrm{~N}+8.0000 \mathrm{~N}+8.0000 \mathrm{~N}$
$8.0000 \mathrm{~N}+8.0000 \mathrm{~N}+8.0000 \mathrm{C}+$ $8.0000 \mathrm{H}+8.0000 \mathrm{H}+8.0000 \mathrm{H}+$
8.0000 H
$\Rightarrow$ The normalized site occupation numbers in $\%$ are:

| 100.0000 0(1) | : |  | 100.0000 0(2) | : |  | 100.0000 0(3) | : |  | 100.0000 0(4) | : |  | 100.0000 0(5) | : |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 100.0000 | O(6) |  | 100.0000 | N(1) | : | 100.0000 | N(2) | . | 100.0000 | N(3) |  | 100.0000 | N (4) | : |
| $100.0000 \mathrm{~N}(5)$ | : |  | $100.0000 \mathrm{~N}(6)$ | : |  | $100.0000 \mathrm{C}(1)$ | : |  | 100.0000 C(2) | : |  | 100.0000 C(3) | : |  |
| 100.0000 | H (1 A ) |  | 100.0000 | H (1B) |  | 100.0000 | H (2A) |  | 100.0000 | H (2B) |  | 100.0000 | H (3A) |  |


$100.0000 \mathrm{H}(3 \mathrm{~B})$
$\Rightarrow$ The density (volumic mass) of the compound is: $1.785 \mathrm{~g} / \mathrm{cm} 3$
=>-------> PROFILE PARAMETERS FOR PATTERN: 1
$\Rightarrow$ Overall scale factor: 0.666440E-03
$\Rightarrow$ ETA (p-Voigt) OR M (Pearson VII): 0.0000
$\Rightarrow$ Overall temperature factor: 0.00000
$\begin{array}{lll}\Rightarrow \text { Halfwidth U,V,W: } & -0.00587 & 0.00000\end{array}$
$\begin{array}{lll}\Rightarrow X & \text { and } Y \text { parameters: } & 0.0000\end{array} 0.0000$
$\begin{array}{lllllllllllll}\Rightarrow> & \text { Direct cell parameters: } & 11.6304 & 10.7431 & 13.2279 & 90.0000 & 90.0000 & 90.0000\end{array}$
$\Rightarrow$ Preferred orientation parameters: 1.0000 0.0000
$\begin{array}{lllllll}\Rightarrow \text { Asymmetry parameters } & : & -0.21721 & 0.00510 & 0.00000 & 0.00000\end{array}$
$\Rightarrow$ Strain parameters $\quad: \quad 0.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{lllll}\Rightarrow & \text { Size parameters } & : & 0.00000 & 0.00000 \\ => & \text { Further shape parameters } & \left(S \_L \text { and D_L): }\right. & 0.00000 & 0.00000\end{array}$
S_L is source width/detector distance
D_L is detector width/detector distance
$==>$ CODEWORDS FOR PROFILE PARAMETERS of PATTERN\# 1
$\Rightarrow$ Overall scale factor: 11.000
$\Rightarrow$ ETA (p-Voigt) OR M (Pearson VII): 0.000
$\Rightarrow$ Overall temperature factor: 0.000
$\begin{array}{lllll}\Rightarrow & H a l f w i d t h ~ U, V, W: & 21.000 & 0.000 & 0.000\end{array}$
$\Rightarrow X$ and $Y$ parameters: 0.0000 .000
$\begin{array}{llllllllll}\Rightarrow \text { Direct cell parameters: } 0.000 & 0.000 & 0.000 & 0.000 & 0.000 & 0.000\end{array}$
$\begin{array}{llll}\Rightarrow \text { Preferred orientation parameters: } & 0.000 & 0.000\end{array}$

| $\Rightarrow$ Asymmetry parameters | $:$ | 41.000 | 51.000 | 0.000 | 0.000 |
| :--- | :--- | ---: | ---: | ---: | ---: |
| $=$ | Strain parameters | $:$ | 0.000 | 0.000 | 0.000 |
| $\Rightarrow$ Size parameters | $:$ | 31.000 | 0.000 |  |  |
| $\Rightarrow$ Cell constraints according to Laue symmetry: mmm |  |  |  |  |  |

Metric information:
=> Direct cell parameters:


| $\mathrm{a} *=$ | 0.085981 | $\mathrm{~b} *=$ | 0.093083 | $\mathrm{c} *=$ | 0.075598 |
| :--- | :---: | :---: | :---: | :---: | :---: |
| $\mathrm{alpha}=$ | 90.000 | beta $*=$ | 90.000 | gamma $*=$ | 90.000 |
| Reciprocal Cell Volume | $=$ | 0.00060504 |  |  |  |

Reciprocal Cell Volume $=0.00060504$
=> Direct and Reciprocal Metric Tensors:

| GD |  | GR |  |  |  |
| :--- | ---: | ---: | :---: | :---: | ---: |
| 135.2666 | 0.0000 | 0.0000 | 0.007393 | 0.000000 | 0.000000 |
| 0.0000 | 115.4133 | 0.0000 | 0.000000 | 0.008665 | 0.000000 |
| 0.0000 | 0.0000 | 174.9783 | 0.000000 | 0.000000 | 0.005715 |

$\Rightarrow$ Cartesian frame: $x / / a ; y$ is in the $a b-p l a n e ; ~ z i s ~ x-y$
Crystal_to_Orthonormal_Matrix

| Cr_Orth_cel |  |  |
| :--- | ---: | ---: |
| 11.6304 | 0.0000 | 0.0000 |
| 0.0000 | 10.7431 | 0.0000 |
| 0.0000 | 0.0000 | 13.2279 |

Busing-Levy B-matrix: $H c=B . H$
BL_M

| BL_M | BL_Minv |  |  |  |  |
| :--- | ---: | ---: | ---: | ---: | ---: |
| 0.085981 | 0.000000 | 0.000000 | 11.6304 | 0.0000 | 0.0000 |
| 0.000000 | 0.093083 | 0.000000 | 0.0000 | 10.7431 | 0.0000 |
| 0.000000 | 0.000000 | 0.075598 | 0.0000 | 0.0000 | 13.2279 |

$\Rightarrow$ Laue symmetry mmm will be used to generate HKL for pattern\# 1
$\Rightarrow$ Reflections generated between $S(1 / d) \min : 0.1366$ A-1 and $S(1 / d) \max : \quad 0.4324$ A-1
$\Rightarrow \quad \operatorname{dmax}: \quad 7.3188 \mathrm{~A}$ and $\mathrm{dmin}: \quad 2.3127 \mathrm{~A}$
$\Rightarrow$ The number of reflections generated is: 69
$\Rightarrow$ The max. scatt. variable (gen.ref.) is: 38.9107
$\Rightarrow$ Scattering coefficients from internal table
$\Rightarrow X$-ray scattering coeff. (A1, B1, A2, .. C, f(0), Z, Dfp,Dfpp)

| 0 | 3.0485 | 13.2771 | 2.2868 | 5.7011 | 1.5463 | 0.3239 | 0.8670 | 32.9089 | 0.2508 | 7.9994 | 8.0000 | 0.0470 | $\swarrow$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0.0320 |  |  |  |  |  |  |  |  |  |  |  |  |
| N | 12.2126 | 0.0057 | 3.1322 | 9.8933 | 2.0125 | 28.9975 | 1.1663 | 0.5826 | -11.5290 | 6.9946 | 7.0000 | 0.0290 | $\swarrow$ |
| C | $\begin{aligned} & 0.0180 \\ & 2.3100 \end{aligned}$ | 20.8439 | 1.0200 | 10.2075 | 1.5886 | 0.5687 | 0.8650 | 51.6512 | 0.2156 | 5.9992 | 6.0000 | 0.0170 | $\swarrow$ |
|  | 0.0090 |  |  |  |  |  |  |  |  |  |  |  |  |
| H | 0.4930 | 10.5109 | 0.3229 | 26.1257 | 0.1402 | 3.1424 | 0.0408 | 57.7997 | 0.0030 | 1.0000 | 1.0000 | 0.0000 | $\swarrow$ |
|  | 0.0000 |  |  |  |  |  |  |  |  |  |  |  |  |

SYMBOLIC NAMES AND INITIAL VALUES OF PARAMETERS TO BE VARIED:

| $->$ | Parameter number | 1 | $->$ Symbolic Name: | Scale_ph1_pat1 | $0.66644000 \mathrm{E}-03$ |
| :--- | :--- | :--- | :--- | :--- | :--- |
| $->$ Parameter number | 2 | $->$ Symbolic Name: | U-Cagl_ph1_pat1 | $-0.58700000 \mathrm{E}-02$ |  |
| $->$ Parameter number | 3 | $->$ Symbolic Name: | G-Size_ph1_pat1 | 0.0000000 |  |
| $->$ Parameter number | 4 | $->$ Symbolic Name: | Asym1_ph1_pat1 | -0.21720999 |  |
| $->$ Parameter number | 5 | $->$ Symbolic Name: | Asym2_ph1_pat1 | $0.51000002 \mathrm{E}-02$ |  |

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| 12.1628 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 12.1877 | Intensity | fixed | to | 1.0 | and | e | to | 1 E6 |
| 12.2126 | Intensity | fixed | to | 1.0 | and | va | to | 1 E6 |
| 12.2375 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 12.3122 | Intensity | fixed | to | 1.0 | and | variance | to | 1E6 |
| 12.3371 | Intensity | fixed | to | 1.0 | and | variance | to | 1E6 |
| 12.3620 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 12.4367 | Intensity | fixed | to | 1.0 | and | varianc | to | 1 E6 |
| 12.4616 | Intensity | fixed | to | 1.0 | and | varianc | to | 1 E6 |
| 12.6359 | Intensity | fixed | to | 1.0 | an | $v$ | to | 1 E6 |
| 13.6070 | Intensity | fixed | to | 1.0 | and | varianc | to | 1 E6 |
| 13.6319 | Intensity | fixed | to | 1.0 | and | va | - | 1 E6 |
| 13.8062 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 14.0054 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 14.0552 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 14.1050 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 14.2295 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 14.2544 | Intensity | fixed | to | 1.0 | and | variance | to | 1 E6 |
| 14.4038 | Intensity | fixed | to | 1.0 | and | variance | O | 1 E6 |

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38.7809

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```
=> Optimizations for routine tasks applied:
=> Calculation mode for patter#: 1 CM_PSEUDO_VOIGT
```

Standard deviations have to be multiplied by: 3.5344
(correlated residuals) See references:
-J.F.Berar \& P.Lelann, J. Appl. Cryst. 24, 1-5 (1991)
-J.F.Berar, Acc. in Pow. Diff. II,NIST Sp.Pub. 846, 63(1992)

```
=> CYCLE No.: }1
=> Convergence reached at this CYCLE !!!!
=> Parameter shifts set to zero
```

=> Phase 1 Name: rdx
$\Rightarrow$ New parameters, shifts, and standard deviations

$\begin{array}{lllllllllllllllllll}1.00000 & 0.00000 & 0.43427 & 0.00000 & 0.00000 & 0.26465 & 0.00000 & 0.00000 & 3.70830 & 0.00000 & 0.00000\end{array}$
(2) $\quad 0.59453 \quad 0.00000 \quad 0.0000$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{lllllllllllllllllllll}0.47340 & 0.00000 & 0.00000 & 0.13880 & 0.00000 & 0.00000 & -0.02250 & 0.00000 & 0.00000 & 4.98480 & 0.00000 & 0.00000\end{array}$
1.000000 .000000 .00000
$\begin{array}{lllllllllllllll}0.35580 & 0.00000 & 0.00000 & 0.24950 & 0.00000 & 0.00000 & -0.11238 & 0.00000 & 0.00000 & 4.76640 & 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{llllllllllllllllllll}0.31810 & 0.00000 & 0.00000 & 0.53030 & 0.00000 & 0.00000 & -0.06806 & 0.00000 & 0.00000 & 5.32170 & 0.00000 & 0.00000\end{array}$
1.000000 .000000 .00000
1.00000 0.000000 .00000
$\begin{array}{llllllllllllll}0.43638 & 0.00000 & 0.00000 & 0.33385 & 0.00000 & 0.00000 & 0.17584 & 0.00000 & 0.00000 & 2.73980 \quad 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{lllllllllllllllllllll}0.32231 & 0.00000 & 0.00000 & 0.23197 & 0.00000 & 0.00000 & 0.05389 & 0.00000 & 0.00000 & 2.40240 & 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{lllllllllllll}0.29900 & 0.00000 & 0.00000 & 0.45348 & 0.00000 & 0.00000 & 0.08838 & 0.00000 & 0.00000 & 2.59240 & 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{llllllllllllllllllllll}0.53777 & 0.00000 & 0.00000 & 0.33516 & 0.00000 & 0.00000 & 0.22628 & 0.00000 & 0.00000 & 2.76530 & 0.00000 & 0.00000\end{array}$
1.000000 .000000 .00000
$\begin{array}{llllllllllllllllllllll}0.38834 & 0.00000 & 0.00000 & 0.20759 & 0.00000 & 0.00000 & -0.03308 & 0.00000 & 0.00000 & 3.09700 & 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{llllllllllllll}0.35299 & 0.00000 & 0.00000 & 0.52971 & 0.00000 & 0.00000 & 0.01650 & 0.00000 & 0.00000 & 3.43200 & 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
00000.357990 .000000 .00
$0.38140 \quad 0.00000 \quad 0.0000$
$1.00000 \quad 0.00000 \quad 0.00000$
$1.00000 \quad 0.00000 \quad 0.00000$
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{lllllllllll}\mathrm{H}(1 \mathrm{~B}) & 0.29071 & 0.00000 & 0.00000 & 0.42024 & 0.00000 & 0.00000 & 0.23991 & 0.00000 & 0.00000 & 4\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
H (2A) $0.44331 \quad 0.00000 \quad 0.00000$
$1.00000 \quad 0.00000 \quad 0.00000$

$1.00000 \quad 0.00000 \quad 0.00000$
H(3A) 0.20936 0.00000 0.00000
$1.00000 \quad 0.00000 \quad 0.00000$
$\begin{array}{lllllllllllllll}\mathrm{H}(3 \mathrm{~B}) & 0.17213 & 0.00000 & 0.00000 & 0.32091 & 0.00000 & 0.00000 & 0.10070 & 0.00000 & 0.00000 & 3.92150 & 0.00000 & 0.00000\end{array}$
$1.00000 \quad 0.00000 \quad 0.00000$
$==>$ PROFILE PARAMETERS FOR PATTERN\# 1

| $\Rightarrow$ Overall scale factor: | 0.000451821 | 0.000000000 | 0.000003839 |
| :--- | :--- | :--- | :--- |

$\Rightarrow$ Eta(p-Voigt) or m(Pearson VII): $0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Overall tem. factor: 0.000000 0.000000 0.000000
$\Rightarrow$ Halfwidth parameters:
$-0.0048470 .000000 \quad 0.013262$
$\begin{array}{lll}-0.000000 & 0.000000 & 0.000000\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Cell parameters:
$11.630419 \quad 0.000000 \quad 0.000000$
$\begin{array}{lll}11.630419 & 0.000000 & 0.000000 \\ 10.743058 & 0.000000 & 0.000000\end{array}$
$\begin{array}{lll}10.743058 & 0.000000 & 0.000000 \\ 13.227938 & 0.000000 & 0.000000\end{array}$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Preferred orientation :
$\begin{array}{lll}\text { 1.000000 } & 0.000000 & 0.000000\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Asymmetry parameters:
$0.032918 \quad 0.000000 \quad 0.006054$
$\begin{array}{lll}0.032918 & 0.000000 & 0.006054 \\ 0.042103 & 0.000000 & 0.003202\end{array}$

==> GLOBAL PARAMETERS FOR PATTERN\# 1

| $=>$ | Zero-point: | -0.0410 | 0.0000 |
| :--- | :--- | :--- | :--- |

$=>\operatorname{Cos}($ theta)-shift parameter : -0.1020 0.0000 0.0000
$\Rightarrow \operatorname{Sin}(2 t h e t a)-$ shift parameter $: 0.26300 .00000 .0000$
$==>$ RELIABILITY FACTORS WITH ALL NON-EXCLUDED POINTS FOR PATTERN: 1

$==>$ RELIABILITY FACTORS FOR POINTS WITH BRAGG CONTRIBUTIONS FOR PATTERN: 1




| 0.123082 | 21.291 |
| :---: | :---: |
| 0.123227 | 21.952 |
| 0.123352 | 22.515 |
| 0.123379 | 22.635 |
| 0.123482 | 23.087 |
| 0.123579 | 23.509 |
| 0.124006 | 25.314 |
| 0.124205 | 26.125 |
| 0.124243 | 26.278 |
| 0.124331 | 26.630 |
| 0.124341 | 26.672 |
| 0.124395 | 26.886 |
| 0.124408 | 26.939 |
| 0.124486 | 27.244 |
| 0.124659 | 27.916 |
| 0.124688 | 28.028 |
| 0.124991 | 29.175 |
| 0.125013 | 29.257 |
| 0.125015 | 29.265 |
| 0.125041 | 29.359 |
| 0.125229 | 30.050 |
| 0.125318 | 30.374 |
| 0.125415 | 30.724 |
| 0.125517 | 31.085 |
| 0.125629 | 31.483 |
| 0.125705 | 31.749 |
| 0.125725 | 31.818 |
| 0.125737 | 31.859 |
| 0.125838 | 32.208 |
| 0.125865 | 32.302 |
| 0.125948 | 32.587 |
| 0.125979 | 32.691 |
| 0.126102 | 33.107 |
| 0.126169 | 33.333 |
| 0.126262 | 33.643 |
| 0.126380 | 34.034 |
| 0.126582 | 34.692 |
| 0.126597 | 34.742 |
| 0.126653 | 34.922 |
| 0.126686 | 35.027 |
| 0.126698 | 35.064 |
| 0.126798 | 35.386 |
| 0.126884 | 35.655 |
| 0.126909 | 35.735 |
| 0.126919 | 35.767 |


35.767
68.1 775. 144.3 39.2 27.2 148.2 902.6 37.3
9.1
6.6
146.0
522.6
325.3
146.
3.2
0.1
586.2
889.3

451 ．
3.1

402 ． 2
184.3
253.8
61.1
134.1
431.3
465.1
48.8
36.1
290.6
6.
45.
66.2
306.6
0.
280.9
0.1

$$
\begin{array}{llll}
33.725 & 0.116603 & 0.012094 & 0.129725
\end{array}
$$

$$
\begin{array}{lllll}
843.0 & 85.375 & 0.116543 & 0.012476 & 0.133524
\end{array}
$$

55
43
43.5
$8.932 \quad 0.115843 \quad 0.018825 \quad 0.193840$
312

| 6.6 | 5.4 | 19.513 | 0.115808 | 0.019403 | 0.199051 | $\swarrow$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 45.1 | 56.9 | 27.961 | 0.115795 | 0.019641 | 0.201187 | $\checkmark$ |
| 66.2 | 78.5 | 15.767 | 0.115775 | 0.020043 | 0.204774 | $\checkmark$ |
| 306.6 | 360.7 | 66.180 | 0.115774 | 0.020074 | 0.205047 | $\checkmark$ |
| 0.0 | 0.0 | 0.002 | 0.115769 | 0.020184 | 0.206025 | $\swarrow$ |
| 280.9 | 388.9 | 149.247 | 0.115766 | 0.020248 | 0.206597 | $\swarrow$ |
| 41.3 | 57.5 | 22.622 | 0.115765 | 0.020271 | 0.206800 | $\checkmark$ |
| 0.0 | 0.0 | 0.038 | 0.115757 | 0.020468 | 0.208545 | $\checkmark$ |
| 86.7 | 101.1 | 20.860 | 0.115750 | 0.020634 | 0.210009 | $\checkmark$ |
| 20.1 | 23.9 | 5.495 | 0.115748 | 0.020683 | 0.210440 | $\checkmark$ |
| 0.1 | 0.2 | 0.035 | 0.115748 | 0.020703 | 0.210613 | $\swarrow$ |

$\begin{array}{lllllll}86.7 & 101.1 & 20.860 & 0.115750 & 0.020634 & 0.210009\end{array}$
$\begin{array}{llllll}20.1 & 23.9 & 5.495 & 0.115748 & 0.020683 & 0.210440\end{array}$

$$
86
$$135.

$23.581 \quad 0.116493 \quad 0.012802 \quad 0.136755$

| 34.2 | 6.470 | 0.116482 | 0.012872 | 0.137447 |
| :--- | :--- | :--- | :--- | :--- |


| 20.6 | 9.583 | 0.116443 | 0.013134 | 0.140032 |
| :--- | :--- | :--- | :--- | :--- |
| 155.7 | 46.760 | 0.116408 | 0.013379 | 0.142440 |

$1096.9241 .947 \quad 0.116265 \quad 0.014433 \quad 0.152701$

| 64.9 | 47.910 | 0.116206 | 0.014909 | 0.157288 |  |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 16.6 | 13.432 | 0.116195 | 0.014999 | 0.158154 | 々 |


|  | 3.570 | 0.116170 | 0.015206 | 0.160138 |
| :--- | :--- | :--- | :--- | :--- |
| 189.7 | 56.634 | 0.116167 | 0.015231 | 0.160373 |


| 614.0 | 107.796 | 0.116153 | 0.015357 | 0.161577 |  |
| ---: | ---: | ---: | ---: | ---: | ---: |
| 373.2 | 55.441 | 0.116149 | 0.015388 | 0.161874 | 々 |


| 784.3 | 264.693 | 0.116011 | 0.016713 | 0.174392 |
| :--- | :--- | :--- | :--- | :--- | :--- |

$1121.2 \quad 292.295 \quad 0.116006 \quad 0.016762 \quad 0.174849$

| 568.8 | 147.410 | 0.116006 | 0.016767 | 0.174891 |
| ---: | ---: | ---: | ---: | ---: | ---: |
| 4.2 | 1.385 | 0.116000 | 0.016823 | 0.175419 |


| 0.2 | 4.321 | 0.115963 | 0.017235 | 0.179258 |  |
| ---: | ---: | ---: | ---: | ---: | ---: |
| 432.9 | 37.902 | 0.115947 | 0.017429 | 0.181055 | 々 |

$205.123 .261 \quad 0.115929 \quad 0.017639 \quad 0.182997$ 々
$305.4 \quad 61.928 \quad 0.115912 \quad 0.017856 \quad 0.184993 \quad \downarrow$

| 1.4 | 1.141 | 0.115882 | 0.018255 | 0.188655 |
| :--- | :--- | :--- | :--- | :--- | :--- |


| 171.3 | 47.391 | 0.115877 | 0.018321 | 0.189260 |
| :--- | :--- | :--- | :--- | :--- | :--- |


| 549.7 | 150.424 | 0.115862 | 0.018532 | 0.191184 |
| :--- | :--- | :--- | :--- | :--- | :--- |

0.2
$0.035 \quad 0.115748$
0.02070
0.21061


```
BRAGG R-Factors and weight fractions for Pattern # 1
=> Phase: 1 rdx
> Bragg R-factor: 17.2 Vol: 1652.781( 0.000) Fract(%): 100.00( 1.20)
=> Rf-factor= 9.62 ATZ: 1776.939 Brindley: 1.0000
```

SYMBOLIC NAMES AND FINAL VALUES AND SIGMA OF REFINED PARAMETERS:

| -> | Parameter number | 1 |  | Scale_ph1_pat1 | $0.45182102 \mathrm{E}-03($ | +/- | 0.38391618E-05 | ) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| -> | Parameter number | 2 | : | U-Cagl_ph1_pat1 | -0.48470786E-02 | +/- | $0.13262363 \mathrm{E}-01$ | ) |
| -> | Parameter number | 3 | : | G-Size_ph1_pat1 | 0.10384443E-01 ( | +/ - | 0.25276333E-03 | ) |
| -> | Parameter number | 4 | : | Asym1_ph1_pat1 | 0.32917723E-01 ( | +/- | $0.60544414 \mathrm{E}-02$ | ) |
| -> | Parameter number | 5 | : | Asym2_ph1_pat1 | $0.42102702 \mathrm{E}-01$ ( | +/- | 0.32015643E-02 |  |

$\Rightarrow$ Number of bytes for floating point variables: 4
$\Rightarrow$ Dimensions of dynamic allocated arrays in this run of FullProf:
$\Rightarrow$ Total approximate array memory (dynamic + static): 107719993 bytes
MaxPOINT= 60000 Max.num. of points (+int. Inten.)/diffraction pattern
MaxREFLT $=20000$ Max.num. of reflections/diffraction pattern
MaxPARAM= 300 Max.num. of refinable parameters
MaxOVERL $=2096$ Max.num. of overlapping reflections
=> Number of bytes for floating point arrays: 4
=> Dimensions of fixed arrays in this release of FullProf:

| NPATT | = | 80 | Max.num. of | powder diffraction patterns |
| :---: | :---: | :---: | :---: | :---: |
| NATS | = | 830 | Max.num. of | atoms (all kind) in asymmetric unit |
| MPAR | = | 1800 | Max.num. of | non atomic parameters/phase |
| IEXCL | = | 30 | Max.num. of | excluded regions |
| IBACP | = | 277 | Max.num. of | background points for interpolation |
| NPHT | = | 16 | Max.num. of | phases |
| NMAGM | = | 8 | Max.num. of | rotation-matrices sets for magnetic structure |
| NBASIS | = | 12 | Max.num. of | basis functions associated to a single atom |
| NIREPS | = | 9 | Max.num. of | irreducible representations to be combined |
| N_EQ | = | 384 | Max.num. of | user-supplied symmetry operators/propagation vectors |
| NGL | = | 300 | Max.num. of | global parameters/diffraction pattern |
| N_LINC | = | 30 | Max.num. of | global linear restraints |
| NAT_P | = | 64 | Max.num. of | atomic parameters per atom |
| NCONST | = | 500 | Max.num. of | slack constraints per phase |
| N_SPE | = | 16 | Max.num. of | different chemical species |
| N_FORM | = | 60 | Max.num. of | scattering factor values in a table |
| NPR | = | 150 | Max.num. of | points defining a numerical profile |
| INPR | = | 25 | Max.num. of | different numerical peak shapes |
| NPRC | = | 150 | Max.num. of | terms in the table for correcting intensities |
| NSOL | = |  | Max.num. of | solutions to be stored in Montecarlo searchs |
| CPU Tim |  | 6.645 | seconds |  |

## A. 4 Sample of n-RDX processed with $0.1 \mathrm{wt} \%$ of PEG.

```
** PROGRAM FullProf.2k (Version 5.60 - Jan2015-ILL JRC) **
*************************************************************
M U L T I -- P A T T E R N
Rietveld, Profile Matching & Integrated Intensity
Refinement of X-ray and/or Neutron Data
Date: 06/07/2015 Time: 15:52:37.093
=> PCR file code: rpg4std2e
=> DAT file code: rpg4std2e.dat -> Relative contribution: 1.0000
==> CONDITIONS OF THIS RUN FOR PATTERN No.: 1
=> Global Refinement of X-ray powder diffraction data
=> Global Refinement of X-ray powder diffraction data
Flat plate with PSD
=> Title:RDX
=> Number of phases: 1
=> Number of excluded regions: 1
=> Number of scattering factors supplied: 0
=> March-Dollase model for preferred orientation
=> Conventional weights: w=1.0/Variance(yobs)
=> Asymmetry correction as in J.Appl.Cryst. 26,128(1993)
=> Background refined by polynomial function
=> The 7th default profile function was selected
=> T-C-H Pseudo-Voigt function
This function is convoluted with asymmetry due to axial
divergence as formulated by:
van Laar and Yelon, J. Appl. Cryst. 17, 47(1984).
and using the method of:
Finger, Cox and Jephcoat, J. Appl. Cryst. 27, 892 (1994).
Fortran 90 module adapted from function PROFVAL (in F77) :
L.W. Finger, J. Appl. Cryst. 31, 111 (1998).
==> INPUT/OUTPUT OPTIONS:
=> Generate file *.PRF for plot
=> Output Integrated Intensities
=> Generate new input file *.PCR
=> Data supplied in free format for pattern: 1
=> Plot pattern at each cycle
=> Wavelengths: 1.54056 1.54439
=> Alpha2/Alpha1 ratio: 0.5000
=> Cos(Monochromator angle)= 1.0000
=> Asymmetry correction for angles lower than 90.000 degrees
=> Absorption correction (AC), muR-eff = 0.0000 0.0000
=> Base of peaks: 2.0*HW* 20.00
=> Number of cycles: 50
=> Relaxation factors ==> for coordinates: 1.00
=> for anisotropic temperature factors: 1.00
=> for halfwidth/strain/size parameters: 1.00
=> for lattice constants and propagation vectors: 1.00
=> EPS-value for convergence: 0.0
=> Excluded regions for Pattern# 1
From to
39.0000 50.0000
=> Instrumental Resolution read from file: xray-res.irf
=> Title of data: Approximate resolution function of a conventional X-ray diffractometer CuKalpha1,2
=> The resolution function is IRESOL: 1 for profile function # 7
Input resolution parameters:
\begin{tabular}{llllll} 
U-inst & V-inst & W-inst & X-inst & Y-inst & Z-inst \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000 \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000
\end{tabular}
\(\Rightarrow\) Number of Least-Squares parameters varied: 58
-
\(\Rightarrow\) P---> PATTERN number: 1
=> Global parameters and codes ==>
\(\Rightarrow\) Zero-point: \(\quad-0.3162 \quad 541.0000\)
```




| Codes: | 431.00000 | 441.00000451 .00000 | 0.000 | $00 \quad 0.00$ |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| C (2) | C | 0.384790 | 0.21557 | 0.14692 | 2.70030 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 461.00000 | 471.00000481 .00000 | 0.00 | $00 \quad 0.00$ |  |  |  |  |  |  |
| C (3) | C | $0.23190 \quad 0$ | 0.33513 | 0.04874 | 2.55740 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 491.00000 | 501.00000511 .00000 | 0.00 | 00.0 .00 |  |  |  |  |  |  |
| H (1A) | H | 0.402890 | 0.52403 | 0.20773 | 5.13220 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 0.00000 | 0.000000 .00000 | 0.00 | 00.000 |  |  |  |  |  |  |
| H (1B) | H | 0.290710 | 0.42024 | 0.23991 | 4.84270 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 0.00000 | 0.000000 .00000 | 0.00 | 00.000 |  |  |  |  |  |  |
| H (2A) | H | 0.443310 | 0.13918 | 0.14950 | 4.60580 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 0.00000 | 0.000000 .00000 | 0.00 | $00 \quad 0.00$ |  |  |  |  |  |  |
| H (2B) | H | 0.317420 | 0.19390 | 0.20730 | 4.97430 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 0.00000 | 0.000000 .00000 | 0.000 | $00 \quad 0.00$ |  |  |  |  |  |  |
| H (3A) | H | 0.209360 | 0.35364 | -0.02527 | 4.50050 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 0.00000 | 0.000000 .00000 | 0.00 | 00.00 | 0 |  |  |  |  |  |
| H (3B) | H | 0.172130 | 0.32091 | 0.10070 | 3.92150 | 1.00000 | 0 | 0 | 0 | 8 |
| Codes: | 0.00000 | $0.00000 \quad 0.00000$ | 0.00 | $00 \quad 0.00$ |  |  |  |  |  |  |

$\Rightarrow$ IT IS ASSUMED THAT THE FIRST GIVEN SITE IS FULLY OCCUPIED
or the first and second atoms are in the same site with total full occupation
(If this is not the case, change the order of atoms to obtain correct values for the content of the unit cell) The given occupation factors have been obtained mutiplying m/M by 1.0000

$\Rightarrow$ The given value of ATZ is $\quad 1776.94$ the program has calculated: 1776.94

The value of ATZ given in the input PCR file will be used for quantitative analysis
$\Rightarrow$ The chemical content of the unit cell is:

| 8.00000 | + | 8.00000 | + | 8.00000 | + | 8.0000 | 0 | + | 8.0000 | 0 |  | 8.0000 | 0 | + | 8.0000 | N | + | $\checkmark$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 8.0000 | N | $+8.0000$ | N | $+8.0000$ | N | + |  |  |  |  |  |  |  |  |  |  |  |  |
| 8.0000 N | + | 8.0000 N | + | 8.0000 C | + | 8.0000 | C | + | 8.0000 | C | + | 8.0000 | H | + | 8.0000 | H | + | $\swarrow$ |
| 8.0000 | H | $+8.0000$ | H | + 8.0000 | H | + |  |  |  |  |  |  |  |  |  |  |  |  |

8.0000 H
$\Rightarrow$ The normalized site occupation numbers in $\%$ are:

| 100.0000 0(1) |  | 100.0000 0(2) |  | 100.0000 0(3) | : |  | 100.0000 0(4) | : |  | 100.0000 0(5) | : |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 100.0000 0(6) | : | $100.0000 \mathrm{~N}(1)$ | : | 100.0000 | $\mathrm{N}(2)$ | : | 100.0000 | N(3) | : | 100.0000 | N(4) | : |
| $100.0000 \mathrm{~N}(5)$ |  | $100.0000 \mathrm{~N}(6)$ |  | 100.0000 C(1) | : |  | 100.0000 C(2) | : |  | 100.0000 C (3) | : |  |
| $100.0000 \mathrm{H}(1 \mathrm{~A})$ | : | $100.0000 \mathrm{H}(1 \mathrm{~B})$ | : | 100.0000 | H (2A) | : | 100.0000 | H (2B) | : | 100.0000 | H (3A) | : |

$100.0000 \mathrm{H}(3 \mathrm{~B})$
$\Rightarrow$ The density (volumic mass) of the compound is: $1.826 \mathrm{~g} / \mathrm{cm} 3$
=>-------> PROFILE PARAMETERS FOR PATTERN: 1


S_L is source width/detector distance
D_L is detector width/detector distance
$==>$ CODEWORDS FOR PROFILE PARAMETERS of PATTERN\# 1
=> Overall scale factor: 521.000
$\Rightarrow$ ETA (p-Voigt) OR M (Pearson VII): 0.000
$\Rightarrow$ Overall temperature factor: 0.000
$\Rightarrow$ Halfwidth U,V,W: 551.000 $0.000 \quad 0.000$
$\Rightarrow X$ and $Y$ parameters: 0.0000 .000
$\begin{array}{lllllllllllll}\Rightarrow & \text { Direct cell parameters: } 531.000 & 561.000 & 571.000 & 0.000 & 0.000 & 0.000\end{array}$
$\begin{array}{ll}\Rightarrow \text { Preferred orientation parameters: } 0.000 & 0.000\end{array}$
$\begin{array}{lllllll}\Rightarrow \text { Asymmetry parameters } & : & 0.000 & 0.000 & 0.000 & 0.000\end{array}$
$\begin{array}{llrrr}\Rightarrow \text { Strain parameters } & : & 0.000 & 0.000 & 0.000\end{array}$
$\Rightarrow$ Size parameters : 581.00011 .000
$\Rightarrow$ The 18 th model for size is used
$\Rightarrow$ Orthorhombic Anisotropic Broadening using Spherical Harmonics up


SYMBOLIC NAMES AND INITIAL VALUES OF PARAMETERS TO BE VARIED:


-> Parameter number | Parameter number |
| :--- |
| $->$ Parameter number |
| $->$ Pararamer number |
| $->$ Parameter |
| -> |

| 21 | -> Symbolic Name: |
| :---: | :---: |
| 22 | -> Symbolic Name: |
| 23 | -> Symbolic Name: |
| 24 | -> Symbolic Name: |
| 25 | -> Symbolic Name: |
| 26 | -> Symbolic Name |
| 27 | -> Symbolic Name |
| 28 | -> Symbolic Name |
| 29 | -> Symbolic Name |
| 30 | -> Symbolic Name |
| 31 | -> Symbolic Name |
| 32 | -> Symbolic Name |
| 33 | -> Symbolic Name |
| 34 | -> Symbolic Name |
| 35 | -> Symbolic Name |
| 36 | -> Symbolic Name |
| 37 | -> Symbolic Name |
| 38 | Symbolic Name |
| 39 | Symbolic Name |
| 40 | Symbolic Name |
| 41 | -> Symbolic Name |
| 42 | -> Symbolic Name |
| 43 | -> Symbolic Name |
| 44 | -> Symbolic Name |
| 45 | -> Symbolic Name |
| 46 | -> Symbolic Name |
| 47 | -> Symbolic Name |
| 48 | -> Symbolic Name |
| 49 | -> Symbolic Name |
| 50 | -> Symbolic Name |
| 51 | -> Symbolic Name |
| 52 | -> Symbolic Name |
| 53 | -> Symbolic Name |
| 54 | -> Symbolic Name |
| 55 | -> Symbolic Name |
| 56 | -> Symbolic Name |
| 57 | -> Symbolic Name |
| 58 | -> Symbolic Name |


| Z_0 (5) _ph1 | -0.79350002E-01 |
| :---: | :---: |
| X_0 (6) _ph1 | 0.42897001 |
| Y_0 (6) _ph1 | 0.59175998 |
| Z_0 (6) _ph1 | $0.52010000 \mathrm{E}-01$ |
| X_N (1) _ph1 | 0.44549999 |
| Y_N (1) _ph1 | 0.33186999 |
| Z_N (1) _ph1 | 0.17883000 |
| X_N (2) _ph1 | 0.33004999 |
| Y_N (2) _ph1 | 0.24334000 |
| Z_N (2) _ph1 | $0.51729999 \mathrm{E}-01$ |
| X_N (3) _ph1 | 0.30372000 |
| Y_N (3) _ph1 | 0.45297000 |
| Z_N (3) _ph1 | $0.79810001 \mathrm{E}-01$ |
| X_N (4) _ph1 | 0.53996998 |
| Y_N (4) _ph1 | 0.33763999 |
| Z_N (4) _ph1 | 0.23203000 |
| X_N (5) _ph1 | 0.38995001 |
| Y_N (5) _ph1 | 0.20392001 |
| Z_N (5) _ph1 | -0.40810000E-01 |
| $\mathrm{X}_{-} \mathrm{N}$ (6) _ ph 1 | 0.35080001 |
| Y_N (6) _ph1 | 0.55348003 |
| Z_N (6) _ph1 | $0.11820000 \mathrm{E}-01$ |
| X_C (1) _ph1 | 0.34908000 |
| Y_C (1) _ph1 | 0.43663001 |
| Z_C (1) _ph1 | 0.19413000 |
| $\mathrm{X}_{\text {_ }} \mathrm{C}$ (2) _ ph 1 | 0.38479000 |
| Y_C (2) _ph1 | 0.21557000 |
| Z_C (2) _ph1 | 0.14692000 |
| $\mathrm{X}_{-} \mathrm{C}$ (3) _ ph 1 | 0.23190001 |
| Y_C (3) _ph1 | 0.33513001 |
| Z_C (3) _ph1 | $0.48740000 \mathrm{E}-01$ |
| Scale_ph1_pat1 | $0.76621003 \mathrm{E}-03$ |
| Cell_A_ph1_pat1 | 11.543573 |
| Zero_pat1 | -0.31615999 |
| U-Cagl_ph1_pat 1 | -0.25444999E-01 |
| Cell_B_ph1_pat 1 | 10.663886 |
| Cell_C_ph1_pat1 | 13.126143 |
| G-Size_ph1_pat1 | $0.10217000 \mathrm{E}-01$ |

1 at 2theta/TOF/E(KeV): 3 at 2theta/TOF/E(KeV):
4 at 2theta/TOF/E(KeV):
9 at 2theta/TOF/E(KeV)
10 at 2 theta/TOF/E(KeV)
15 at 2theta/TOF/E(KeV):
20 at 2theta/TOF/E(KeV): 25 at 2 theta/TOF/E(KeV): 29 at 2 theta/TOF/E(KeV)
32 at 2 theta/TOF/E(KeV):
36 at 2theta/TOF/E(KeV):
39 at 2theta/TOF/E(KeV):
41 at 2 theta/TOF/E(KeV):
48 at 2 theta/TOF/E(KeV) :
49 at 2theta/TOF/E(KeV):
52 at 2theta/TOF/E(KeV):
53 at 2theta/TOF/E(KeV):
54 at 2 theta/TOF/E(KeV):
60 at 2 theta/TOF/E(KeV)
67 at 2theta/TOF/E(KeV):
79 at 2theta/TOF/E(KeV):
81 at 2theta/TOF/E(KeV):
182 at 2 theta/TOF/E(KeV): 192 at 2theta/TOF/E(KeV): 193 at 2theta/TOF/E(KeV): 194 at 2theta/TOF/E(KeV): 199 at 2theta/TOF/E(KeV): 203 at 2theta/TOF/E(KeV): 205 at 2 theta/TOF/E(KeV): 208 at 2theta/TOF/E(KeV): 210 at 2theta/TOF/E(KeV): 211 at 2 theta/TOF/E(KeV): 214 at 2theta/TOF/E(KeV): 215 at 2 theta/TOF/E(KeV): 217 at 2 theta/TOF/E(KeV): 219 at 2 theta/TOF/E(KeV): 221 at 2 theta/TOF/E(KeV): 224 at 2 theta/TOF/E(KeV): 226 at 2 theta/TOF/E(KeV): 230 at 2 theta/TOF/E(KeV): 233 at 2theta/TOF/E(KeV): 235 at 2 theta/TOF/E(KeV) : 237 at 2 theta/TOF/E(KeV): 239 at 2theta/TOF/E(KeV): 241 at 2 theta/TOF/E(KeV): 246 at 2 theta/TOF/E(KeV): 247 at 2 theta/TOF/E(KeV): 248 at 2theta/TOF/E(KeV) 250 at 2 theta/TOF/E(KeV): 254 at 2 theta/TOF/E(KeV): 263 at 2theta/TOF/E(KeV):

| 12.0000 | ty | fixed | 1.0 |  | to 1E6 |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 12.0148 | Intensity | fixed to | 1.0 and | iance | to 1E6 |
| 12.0222 | Intensity | fixed | 1.0 and |  | - 1E6 |
| 12.0592 | Intensity | fixed | 1.0 and |  | 1E6 |
| 12.0666 | Intensity | fixed | 1.0 |  | 1 E 6 |
| 12.1036 | Intensity | fixed | 1.0 and | variance | 1E6 |
| 12.1406 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 12.1776 | Intensity | fixed | 1.0 and | ce | to 1E6 |
| 12.2072 | Intensity | fixed | 1.0 and | ce | 1E6 |
| 12.2294 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 12.2590 | Intensity | fixed | 1.0 and | variance | 1E6 |
| 12.2812 | Intensity | fix | 0 and | variance | to 1E6 |
| 12.2960 | Intensity | fixed | 0 and |  | to 1E6 |
| 12.3478 | Intensity | fixed | 0 and |  | to 1E6 |
| 12.3552 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 12.3774 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 12.3848 | Intensity | fixed | 1.0 and | ce | to 1E6 |
| 12.3922 | Intensity | fixed | 1.0 and | c | to 1E6 |
| 12.4366 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 12.4884 | Intensity | fix | 0 | variance | to 1E6 |
| 12.5772 | Intensity | fixed | 0 and | variance | to 1E6 |
| 12.5920 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.3394 | Intensity | fixed | 1.0 and | e | to 1E6 |
| 13.4134 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.4208 | Intensity | fixed | 1.0 and | ance | to 1E6 |
| 13.4282 | Intensity | fixed | 1.0 and | ce | to 1E6 |
| 13.4652 | Intensity | fixed | 1.0 | variance | to 1E6 |
| 13.4948 | Intensity | fixed | 1.0 | variance | to 1E6 |
| 13.5096 | Intensity | fixed | 0 | variance | to 1E6 |
| 13.5318 | Intensity | fixed | 1.0 and | variance | 1E6 |
| 13.5466 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.5540 | Intensity | fixed | 1.0 and | ce | to 1E6 |
| 13.5762 | Intensity | fixed | 1.0 and | ce | to 1E6 |
| 13.5836 | Intensity | fixed | 1.0 and | c | to 1E6 |
| 13.5984 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.6132 | Intensity | fixed | 1.0 | variance | to 1E6 |
| 13.6280 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.6502 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.6650 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.6946 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.7168 | Intensity | fixed | 1.0 and | variance | to 1E6 |
| 13.7316 | Intensity | fixed | 1.0 and | ce | to 1E6 |
| 13.7464 | Intensity | fixed to | 1.0 and | ariance | to 1E6 |
| 13.7612 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.7760 | Intensity | fixed to | 1.0 and | varianc | to 1E6 |
| 13.8130 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.8204 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.8278 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.8426 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.8722 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.9388 | Intensity | fixed | 1.0 and | variance | to 1E6 |

$\Rightarrow$ Zero counts at step no. $\Rightarrow$ Zero counts at step no.
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936 at 2theta/TOF/E(KeV): 941 at 2 theta/TOF/E(KeV) 945 at 2theta/TOF/E(KeV): 946 at 2 theta/TOF/E(KeV): 947 at 2 theta/TOF/E(KeV) 948 at 2 theta/TOF/E(KeV): 950 at 2theta/TOF/E(KeV): 952 at 2theta/TOF/E(KeV) 953 at 2 theta/TOF/E(KeV): 954 at 2 theta/TOF/E(KeV) 956 at 2 theta/TOF/E(KeV): 957 at 2theta/TOF/E(KeV): 959 at 2 theta/TOF/E(KeV): 960 at 2 theta/TOF/E(KeV): 963 at 2theta/TOF/E(KeV) 964 at 2 theta/TOF/E(KeV): 965 at 2theta/TOF/E(KeV): 966 at 2 theta/TOF/E(KeV): 968 at 2theta/TOF/E(KeV): 969 at 2 theta/TOF/E(KeV) 971 at 2theta/TOF/E(KeV): 977 at 2theta/TOF/E(KeV): 986 at 2 theta/TOF/E(KeV): 994 at 2 theta/TOF/E(KeV) 996 at 2 theta/TOF/E(KeV): 997 at 2theta/TOF/E(KeV) 998 at 2theta/TOF/E(KeV): 000 at 2theta/TOF/E(KeV): 1001 at 2 theta/TOF/E (KeV) 1002 at 2 theta/TOF/E(KeV): 1003 at 2theta/TOF/E(KeV): 1004 at 2 theta/TOF/E(KeV): 1006 at 2 theta/TOF/E(KeV): 1008 at 2 theta/TOF/E(KeV): 1009 at 2theta/TOF/E(KeV): 1011 at 2 theta/TOF/E(KeV): 1013 at 2theta/TOF/E(KeV): 1017 at 2theta/TOF/E(KeV): 1018 at 2theta/TOF/E(KeV): 1024 at 2 theta/TOF/E(KeV): 1027 at 2 theta/TOF/E(KeV): 1028 at 2 theta/TOF/E(KeV): 1029 at 2 theta/TOF/E(KeV) 1030 at 2 theta/TOF/E (KeV): 1031 at 2theta/TOF/E(KeV): 1032 at 2 theta/TOF/E(KeV): 1034 at 2theta/TOF/E(KeV): 1035 at 2 theta/TOF/E(KeV): 1036 at 2 theta/TOF/E(KeV): 1038 at 2theta/TOF/E(KeV): 1039 at 2 theta/TOF/E(KeV): 1040 at 2 theta/TOF/E(KeV): 1042 at 2 theta/TOF/E(KeV): 1043 at 2theta/TOF/E(KeV): 1045 at 2theta/TOF/E(KeV): 1046 at 2 theta/TOF/E(KeV): 1048 at 2theta/TOF/E(KeV): 1050 at 2 theta/TOF/E(KeV): 1052 at 2 theta/TOF/E(KeV) 1053 at 2theta/TOF/E(KeV): 1054 at 2 theta/TOF/E(KeV): 1055 at 2 theta/TOF/E (KeV) : 1056 at 2 theta/TOF/E(KeV): 1058 at 2 theta/TOF/E(KeV) : 1062 at 2 theta/TOF/E(KeV): 1063 at 2theta/TOF/E(KeV): 1068 at 2theta/TOF/E(KeV): 1071 at 2 theta/TOF/E(KeV): 1072 at 2theta/TOF/E(KeV): 1076 at 2 theta/TOF/E(KeV): 1134 at 2 theta/TOF/E(KeV): 1135 at 2 theta/TOF/E(KeV): 1142 at 2 theta/TOF/E(KeV): 1143 at 2theta/TOF/E(KeV): 1144 at 2 theta/TOF/E(KeV): 1146 at 2 theta/TOF/E(KeV): 1147 at 2 theta/TOF/E(KeV): 1149 at 2theta/TOF/E(KeV): 1150 at 2 theta/TOF/E(KeV): 1152 at 2 theta/TOF/E(KeV): 1153 at 2 theta/TOF/E(KeV): 1157 at 2 theta/TOF/E(KeV): 1158 at 2 theta/TOF/E(KeV): 1159 at 2theta/TOF/E(KeV): 1161 at 2 theta/TOF/E(KeV): 1164 at 2 theta/TOF/E(KeV) 1171 at 2 theta/TOF/E(KeV): 1172 at 2 theta/TOF/E(KeV): 1174 at 2 theta/TOF/E(KeV): 1175 at 2theta/TOF/E(KeV):
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176 at 2 theta/TOF/E(KeV) 178 at 2 theta/TOF/E(KeV): 1179 at 2 theta/TOF/E(KeV): 1181 at 2theta/TOF/E(KeV): 1182 at 2theta/TOF/E(KeV): 1185 at 2theta/TOF/E(KeV): 187 at 2 theta/TOF/E(KeV): 1189 at 2theta/TOF/E(KeV): 1190 at 2theta/TOF/E(KeV): 1193 at 2theta/TOF/E(KeV): 1195 at 2 theta/TOF/E(KeV): 1197 at 2theta/TOF/E(KeV): 1202 at 2 theta/TOF/E(KeV): 1203 at 2 theta/TOF/E(KeV): 1206 at 2 theta/TOF/E(KeV): 1208 at 2theta/TOF/E(KeV): 1211 at 2 theta/TOF/E(KeV): 1213 at 2 theta/TOF/E(KeV): 1215 at 2 theta/TOF/E(KeV): 1221 at 2 theta/TOF/E(KeV): 1224 at 2theta/TOF/E(KeV): 1255 at 2 theta/TOF/E(KeV): 1256 at 2 theta/TOF/E(KeV): 1257 at 2 theta/TOF/E(KeV): 1258 at 2theta/TOF/E(KeV): 1259 at 2theta/TOF/E(KeV): 1262 at 2 theta/TOF/E(KeV): 1264 at 2 theta/TOF/E(KeV): 1267 at 2 theta/TOF/E(KeV): 1269 at 2 theta/TOF/E(KeV): 1271 at 2theta/TOF/E(KeV): 1272 at 2 theta/TOF/E(KeV): 1274 at 2 theta/TOF/E(KeV): 1278 at 2 theta/TOF/E(KeV) 1282 at 2 theta/TOF/E(KeV): 1283 at 2theta/TOF/E(KeV): 1284 at 2theta/TOF/E(KeV): 1286 at 2theta/TOF/E(KeV): 1287 at 2 theta/TOF/E(KeV): 1288 at 2 theta/TOF/E(KeV): 1289 at 2theta/TOF/E(KeV): 1294 at 2 theta/TOF/E(KeV): 1297 at 2theta/TOF/E(KeV): 1298 at 2theta/TOF/E(KeV): 1363 at 2theta/TOF/E(KeV): 1364 at 2theta/TOF/E(KeV): 1365 at 2 theta/TOF/E(KeV): 1366 at 2theta/TOF/E(KeV): 1368 at 2 theta/TOF/E(KeV): 1369 at 2 theta/TOF/E(KeV): 1377 at 2 theta/TOF/E(KeV): 1378 at 2 theta/TOF/E(KeV): 1383 at 2 theta/TOF/E(KeV): 1435 at 2theta/TOF/E(KeV): 1437 at 2theta/TOF/E(KeV): 1439 at 2theta/TOF/E(KeV): 1441 at 2 theta/TOF/E(KeV): 1444 at 2theta/TOF/E(KeV): 1447 at 2 theta/TOF/E(KeV): 1449 at 2 theta/TOF/E(KeV): 1451 at 2 theta/TOF/E(KeV): 1452 at 2 theta/TOF/E(KeV): 1454 at 2 theta/TOF/E(KeV): 1456 at 2 theta/TOF/E(KeV): 1457 at 2 theta/TOF/E(KeV): 1463 at 2theta/TOF/E(KeV): 1465 at 2 theta/TOF/E(KeV): 1467 at 2 theta/TOF/E(KeV) : 1498 at 2theta/TOF/E(KeV): 1499 at 2theta/TOF/E(KeV): 1500 at 2 theta/TOF/E(KeV): 1502 at 2 theta/TOF/E(KeV): 1503 at 2 theta/TOF/E(KeV) 1504 at 2theta/TOF/E(KeV): 1505 at 2 theta/TOF/E(KeV): 1507 at 2 theta/TOF/E(KeV): 1510 at 2 theta/TOF/E(KeV): 1511 at 2theta/TOF/E(KeV): 1518 at 2 theta/TOF/E(KeV): 1519 at 2 theta/TOF/E(KeV): 1522 at 2 theta/TOF/E(KeV): 1564 at 2 theta/TOF/E(KeV): 1565 at 2theta/TOF/E(KeV): 1567 at 2theta/TOF/E(KeV): 1569 at 2 theta/TOF/E(KeV): 1571 at 2 theta/TOF/E(KeV) 1572 at 2 theta/TOF/E(KeV): 1577 at 2 theta/TOF/E(KeV): 1579 at 2 theta/TOF/E(KeV) 1581 at 2theta/TOF/E(KeV):
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1583 at 2 theta/TOF/E(KeV): 1584 at 2theta/TOF/E(KeV): 1590 at 2theta/TOF/E(KeV): 1593 at 2theta/TOF/E(KeV): 1599 at 2theta/TOF/E(KeV): 1602 at 2 theta/TOF/E(KeV): 1604 at 2 theta/TOF/E(KeV): 1606 at 2 theta/TOF/E(KeV) : 1609 at 2 theta/TOF/E(KeV): 1610 at 2 theta/TOF/E(KeV): 1613 at 2 theta/TOF/E(KeV): 1620 at 2 theta/TOF/E(KeV): 1624 at 2theta/TOF/E(KeV): 1626 at 2 theta/TOF/E(KeV): 1632 at 2 theta/TOF/E(KeV): 1633 at 2theta/TOF/E(KeV): 1634 at 2 theta/TOF/E(KeV): 1650 at 2 theta/TOF/E(KeV): 1660 at 2theta/TOF/E(KeV): 1664 at 2 theta/TOF/E(KeV): 1665 at 2 theta/TOF/E(KeV): 1684 at 2 theta/TOF/E(KeV): 1691 at 2 theta/TOF/E(KeV): 1708 at 2 theta/TOF/E(KeV): 2098 at 2theta/TOF/E(KeV): 2104 at 2theta/TOF/E(KeV): 2112 at 2theta/TOF/E(KeV): 2115 at 2theta/TOF/E(KeV): 2118 at 2theta/TOF/E(KeV): 2145 at 2 theta/TOF/E(KeV) : 2147 at 2theta/TOF/E(KeV): 2149 at 2theta/TOF/E(KeV): 2153 at 2 theta/TOF/E(KeV): 2155 at 2 theta/TOF/E(KeV): 2157 at 2theta/TOF/E(KeV): 2161 at 2theta/TOF/E(KeV): 2177 at 2 theta/TOF/E(KeV): 2182 at 2theta/TOF/E(KeV): 2184 at 2theta/TOF/E(KeV): 2205 at 2theta/TOF/E(KeV): 2221 at 2theta/TOF/E(KeV): 2235 at 2theta/TOF/E(KeV): 2247 at 2 theta/TOF/E(KeV): 2248 at 2 theta/TOF/E(KeV): 2251 at 2theta/TOF/E(KeV): 2252 at 2 theta/TOF/E(KeV): 2386 at 2 theta/TOF/E(KeV): 2393 at 2theta/TOF/E(KeV): 2399 at 2theta/TOF/E(KeV): 2404 at 2theta/TOF/E(KeV): 2407 at 2theta/TOF/E(KeV): 2408 at 2theta/TOF/E(KeV): 2409 at 2 theta/TOF/E(KeV): 2411 at 2theta/TOF/E(KeV): 2421 at 2theta/TOF/E(KeV): 2423 at 2theta/TOF/E(KeV): 2424 at 2theta/TOF/E(KeV): 2425 at 2 theta/TOF/E(KeV): 2426 at 2theta/TOF/E(KeV): 2427 at 2theta/TOF/E(KeV): 2431 at 2theta/TOF/E(KeV): 2435 at 2 theta/TOF/E(KeV): 2437 at 2theta/TOF/E(KeV): 2438 at 2theta/TOF/E(KeV): 2901 at 2theta/TOF/E(KeV): 2902 at 2theta/TOF/E(KeV): 2906 at 2theta/TOF/E(KeV): 2907 at 2 theta/TOF/E(KeV): 2909 at 2 theta/TOF/E(KeV): 2915 at 2theta/TOF/E(KeV): 2932 at 2theta/TOF/E(KeV): 2937 at 2 theta/TOF/E(KeV) 2939 at 2theta/TOF/E(KeV): 2941 at 2theta/TOF/E(KeV): 2944 at 2theta/TOF/E(KeV): 2950 at 2theta/TOF/E(KeV): 2996 at 2theta/TOF/E(KeV): 2997 at 2 theta/TOF/E(KeV) 2999 at 2theta/TOF/E(KeV): 3001 at 2theta/TOF/E(KeV): 3003 at 2 theta/TOF/E(KeV): 3004 at 2theta/TOF/E(KeV): 3005 at 2theta/TOF/E(KeV): 3007 at 2 theta/TOF/E(KeV) : 3009 at 2 theta/TOF/E(KeV): 3012 at 2 theta/TOF/E(KeV) 3013 at 2 theta/TOF/E(KeV) : 3014 at 2theta/TOF/E(KeV): 3015 at 2 theta/TOF/E(KeV) 3016 at 2theta/TOF/E(KeV):
23.7068 3. 7142 23.7586 23.7808 23.8252 23.8474 23.8622 23.8770 23.8992 23.9066 23.9288 23.9806 24.0102 24.0250 24.0694 24.0768 24.0842 24.2026 24.2766 24.3062 24.3136 24.4542 24.5060 24.6318 27.5178 27.5622 27.6214 27.6436 27.6658 27.8656 27.8804 27.8952 27.9248 27.9396 27.9544 27.9840 28.1024 28.1394 28.1542 28.3096 28.4280 28.5316 28.6204 28.6278 28.6500 28.6574 29.6490 29.7008 29.7452 29.7822 29.8044 29.8118 29.8192 29.8340 29.9080 29.9228 29.9302 29.9376 29.9450 29.9524 29.9820 30.0116 30.0264 30.0338 33.4600 33.4674 33.4970 33.5044 33.5192 33.5636 33.6894 33.7264 33.7412 33.7560 33.7782 33.8226 34.1630 34.1704 34.1852 34.2000 34.2148 34.2222 34.2296 34.2444 34.2592 34.2814 34.2888 34.2962 34.3036
34.3110

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3017 at 2 theta/TOF/E(KeV): 3022 at 2theta/TOF/E(KeV): 3026 at 2 theta/TOF/E(KeV): 3147 at 2 theta/TOF/E(KeV): 3154 at 2 theta/TOF/E (KeV) : 3158 at 2 theta/TOF/E (KeV): 3166 at 2 theta/TOF/E (KeV): 3170 at 2 theta/TOF/E (KeV): 3230 at 2 theta/TOF/E (KeV) : 3233 at 2 theta/TOF/E (KeV) 3237 at 2 theta/TOF/E (KeV) : 3238 at 2 theta/TOF/E (KeV): 3244 at 2 theta/TOF/E (KeV): 3246 at 2 theta/TOF/E (KeV): 3247 at 2 theta/TOF/E (KeV): 3252 at 2 theta/TOF/E(KeV): 3254 at 2theta/TOF/E (KeV) : 3258 at 2 theta/TOF/E (KeV): 3261 at 2 theta/TOF/E (KeV): 3262 at 2 theta/TOF/E (KeV): 3263 at 2 theta/TOF/E (KeV): 3272 at 2 theta/TOF/E (KeV) : 3275 at 2 theta/TOF/E(KeV): 3277 at 2 theta/TOF/E (KeV) : 3279 at 2 theta/TOF/E (KeV): 3287 at 2 theta/TOF/E (KeV): 3301 at 2theta/TOF/E(KeV): 3399 at 2 theta/TOF/E(KeV): 3410 at 2 theta/TOF/E (KeV) 3411 at 2 theta/TOF/E(KeV): 3414 at 2theta/TOF/E (KeV): 3416 at 2 theta/TOF/E (KeV) : 3554 at 2 theta/TOF/E (KeV): 3571 at 2 theta/TOF/E (KeV) : 3572 at 2 theta/TOF/E (KeV): 3574 at 2theta/TOF/E(KeV): 3589 at 2 theta/TOF/E(KeV) : 3591 at 2 theta/TOF/E (KeV) : 3594 at 2 theta/TOF/E (KeV) : 3596 at 2 theta/TOF/E(KeV): 3597 at 2 theta/TOF/E(KeV): 3599 at 2 theta/TOF/E(KeV): 3601 at 2 theta/TOF/E (KeV) 3610 at 2 theta/TOF/E (KeV) : 3614 at 2 theta/TOF/E(KeV): 3619 at 2 theta/TOF/E (KeV) : 3622 at 2 theta/TOF/E (KeV): 3632 at 2 theta/TOF/E (KeV) 3635 at 2 theta/TOF/E (KeV): 3637 at 2theta/TOF/E(KeV): 3640 at 2 theta/TOF/E (KeV):
34.3184 34.3554 34.3850 35.2804 35.3322 35.3618 35.4210 35.4506 35.8946 35.9168 35.9464 35.9538 35.9982 36.0130 36.0204 36.0574 36.0722 36.1018 36.1240 36.1314 36.1388 36.2054 36.2276 36.2424 36.2572 36.3164 36.4200 37.1452 37.2266 37.2340 37.2562 37.2710 38.2922 38.4180 38.4254 38.4402 38.5512 38.5660 38.5882 38.6030 38.6104 38.6252 38.6400 38.7066 38.7362 38.7732 38.7954 38.8694 38.8916 38.9064 38.9286

Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to $1 E 6$ Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1E6 Intensity fixed to 1.0 and variance to 1 E6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6 Intensity fixed to 1.0 and variance to 1 E 6
$\Rightarrow$ Optimizations for routine tasks applied:
=> Calculation mode for patter\#: 1 CM_PSEUDO_VOIGT

Standard deviations have to be multiplied by: 2.8680
(correlated residuals) See references:
-J.F.Berar \& P.Lelann, J. Appl. Cryst. 24, 1-5 (1991)
-J.F.Berar, Acc. in Pow. Diff. II,NIST Sp.Pub. 846, 63(1992)
=> CYCLE No.: 50
=> Phase 1 Name: rdx
$\Rightarrow$ New parameters, shifts, and standard deviations



| $\Rightarrow$ Overall scale factor: 0.000769464 | 0.000000243 | 0.000004678 |
| :--- | :--- | :--- | :--- | :--- |

$\Rightarrow$ Eta(p-Voigt) or m(Pearson VII): 0.000000 0.000000 0.000000
$\Rightarrow$ Overall tem. factor: 0.000000 0.000000 0.000000
$\Rightarrow$ Halfwidth parameters:
$\begin{array}{lll}-0.014575 & 0.000012 & 0.004497\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Cell parameters:
$\begin{array}{lll}11.545714 & -0.000002 & 0.000240\end{array}$
$\begin{array}{lll}10.665313 & 0.000007 & 0.000249\end{array}$
$13.129634 \quad 0.000005 \quad 0.000308$
$90.000000 \quad 0.000000 \quad 0.000000$
$\begin{array}{lll}90.000000 & 0.000000 & 0.000000\end{array}$
$90.000000 \quad 0.000000 \quad 0.000000$
=> Preferred orientation :
1.0000000 .0000000000
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Asymmetry parameters:
$0.034020 \quad 0.0000000 .000000$
$0.049140 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow X$ and $Y$ parameters :
$\begin{array}{lll}0.000000 & 0.000000 & 0.000000\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Strain parameters:
$0.000000 \quad 0.000000 \quad 0.000000$
$\begin{array}{lll}0.000000 & 0.000000 & 0.000000\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Size parameters (G,L):
$0.009228 \quad 0.000000 \quad 0.000107$
$0.003242 \quad-0.000001 \quad 0.007229$
$\Rightarrow$ Further shape parameters (S_L and D_L):
$0.000000 \quad 0.0000000 .000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Spherical Harmonics coeff.(size):

| $\begin{aligned} & 0.003242 \\ & 0.014164 \end{aligned}$ | -0.000001 | 0.007229 | -0.004081 | 0.000619 | 0.018743 | 0.077268 | -0.000633 | $\swarrow$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{aligned} & 0.118944 \\ & 0.015851 \end{aligned}$ | -0.000412 | 0.019819 | -0.100242 | 0.000038 | 0.018840 | 0.021744 | -0.000283 | $\swarrow$ |
| $\begin{aligned} & 0.000000 \\ & 0.000000 \end{aligned}$ | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | $\checkmark$ |

$==>$ GLOBAL PARAMETERS FOR PATTERN\# 1
$\begin{array}{llll}=> & \text { Zero-point: } & -0.3110 .0000 & 0.0008\end{array}$
$\Rightarrow$ Background Polynomial Parameters ==>
0.00000 .00000 .000
$\begin{array}{lll}0.0000 & 0.0000 & 0.0000\end{array}$
$\begin{array}{lll}0.0000 & 0.0000 & 0.0000\end{array}$
$0.0000 \quad 0.0000 \quad 0.0000$
$\begin{array}{lll}0.0000 & 0.0000 & 0.0000\end{array}$
$\begin{array}{lll}0.0000 & 0.0000 & 0.0000\end{array}$
$\Rightarrow \operatorname{Cos}(t h e t a)-s h i f t$ parameter $: 0.00000 .00000 .0000$
$\Rightarrow$ Sin(2theta)-shift parameter : 0.00000 .00000 .0000
$==>$ RELIABILITY FACTORS WITH ALL NON-EXCLUDED POINTS FOR PATTERN: 1

$==>$ RELIABILITY FACTORS FOR POINTS WITH BRAGG CONTRIBUTIONS FOR PATTERN: 1




| 27.144 | 548.0 |
| :--- | :--- |
| 27.450 | 256.7 |


| 27.450 | 256.7 |
| :--- | ---: |
| 28.126 | 10.2 |

$28.242 \quad 0.5$

| 29.394 | 1024.5 |
| ---: | ---: |
| 29.483 | 791.1 |

1326.3

$$
509.0
$$

$$
35.330
$$

$$
35.657
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$$
35.929
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| 4 | 0 | 4 | 0.114804 |
| :---: | :---: | :---: | :---: |
| 34.072071 |  |  |  |
| 4 | 2 | 8 | 0.114771 |
| 67.825462 |  |  |  |
| 4 | 1 | 8 | 0.114806 |
| 65.588745 |  |  |  |
| 2 | 2 | 8 | 0.117713 |
| 64.771576 |  |  |  |
| 3 | 4 | 8 | 0.116825 |
| 64.337578 |  |  |  |
| 2 | 5 | 4 | 0.119243 |
|  | . 0 |  |  |

322.5 94.1 76.8

| 331.5 | 10.798 | 0.104923 | 0.018322 | 0.206312 | $\swarrow$ |
| ---: | ---: | ---: | ---: | ---: | ---: |
| 88.8 | 5.271 | 0.104895 | 0.018314 | 0.206276 | $\swarrow$ |
| 89.1 | 14.661 | 0.104690 | 0.018745 | 0.210802 | $\swarrow$ |
| 3.6 | 3.562 | 0.104613 | 0.024079 | 0.260416 | $\swarrow$ |
| 5.8 | 2.527 | 0.104571 | 0.022580 | 0.246999 | $\swarrow$ |
| 99.7 | 15.297 | 0.104541 | 0.026889 | 0.285045 | $\swarrow$ |



BRAGG R-Factors and weight fractions for Pattern \# 1

| $=>$ | Phase: 1 | rdx |  |  |  |
| :--- | :---: | :---: | :---: | :---: | :---: |
| $=>$ | Bragg R-factor: | 4.39 | Vol: | $1616.766(0.063)$ | Fract (\%): |
| $=>$ | Rf-factor $=$ | 3.29 |  | ATZ: | 1776.939 |
|  |  |  | Brindley: | $1.000(0.86)$ |  |

SYMBOLIC NAMES AND FINAL VALUES AND SIGMA OF REFINED PARAMETERS:

| -> | Parameter number | 1 | : | L-Size_ph1_pat1 | $0.32420373 \mathrm{E}-02($ | +/- | 0.72292127E-02 ) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| -> | Parameter number | 2 | : | Size2_ph1_pat1 | -0.40812818E-02 | +/- | 0.18743467E-01 ) |
| -> | Parameter number | 3 | : | Size3_ph1_pat1 | 0.77267610E-01 | +/- | 0.14163993E-01 ) |
| -> | Parameter number | 4 | : | Size4_ph1_pat1 | 0.11894368 | +/- | 0.19819405E-01 ) |
| -> | Parameter number | 5 | : | Size5_ph1_pat1 | -0.10024197 | +/- | 0.18839633E-01 ) |
| - | Parameter number | 6 | : | Size6_ph1_pat1 | 0.21744350E-01 ( | +/- | 0.15851058E-01 ) |
| -> | Parameter number | 7 | : | X_0 (1) _ph1 | 0.57541239 | +/- | 0.11092700E-02 ) |
| -> | Parameter number | 8 | : | Y_0 (1) _ph1 | 0.43966007 | +/- | $0.12116111 \mathrm{E}-02$ |
| -> | Parameter number | 9 | : | Z_0 (1) _ph1 | 0.27099708 | +/- | 0.11624396E-02 |
| -> | Parameter number | 10 | : | X_0 (2) _ph1 | 0.59412211 | +/- | 0.10898095E-02 ) |
| -> | Parameter number | 11 | : | Y_0 (2) _ph1 | 0.22895293 | +/- | 0.12537022E-02 ) |
| -> | Parameter number | 12 | : | Z_0 (2) _ph1 | 0.22888340 | +/- | 0.11001484E-02 ) |
| -> | Parameter number | 13 | : | $\mathrm{X}_{-} 0$ (3) _ph1 | 0.47338510 | +/- | 0.12744585E-02 ) |
| -> | Parameter number | 14 | : | Y_0 (3) _ph 1 | 0.13057353 | +/- | 0.92790980E-03 ) |
| -> | Parameter number | 15 | : | Z_0 (3) _ph 1 | -0.19450795E-01 | +/- | 0.10155203E-02 |
| -> | Parameter number | 16 | : | X_0 (4)_ph1 | 0.34381583 | +/- | 0.14120982E-02 |
| -> | Parameter number | 17 | : | Y_0 (4)_ph1 | 0.25728008 | +/- | 0.12697025E-02 |
| -> | Parameter number | 18 | : | Z_0 (4) _ph1 | -0.11679447 | +/- | 0.15248761E-02 ) |
| -> | Parameter number | 19 | : | $\mathrm{X}_{-} 0$ (5) _ ph 1 | 0.31070611 | +/- | 0.94801566E-03) |
| -> | Parameter number | 20 | : | Y_0 (5) _ph1 | 0.51081645 | +/- | 0.12307854E-02 ) |
| -> | Parameter number | 21 | : | Z_0 (5) _ph1 | -0.79970337E-01 | +/- | 0.10943528E-02 ) |
| -> | Parameter number | 22 | : | X_0 (6) _ph1 | 0.42943338 | +/- | 0.13071131E-02 ) |
| -> | Parameter number | 23 | : | Y_0 (6) _ph 1 | 0.59145427 | +/- | 0.18751499E-02 ) |
| -> | Parameter number | 24 | : | Z_0 (6) _ph1 | 0.52474596E-01 ( | +/- | 0.96871122E-03 ) |
| -> | Parameter number | 25 | : | $\mathrm{X}_{-} \mathrm{N}$ (1) _ ph 1 | 0.44482139 | +/- | 0.17220172E-02 ) |
| -> | Parameter number | 26 | : | Y_N (1) _ph1 | 0.33536911 | +/- | 0.43182792E-02 ) |
| -> | Parameter number | 27 | : | Z_N (1) _ph1 | 0.17979442 | +/- | 0.17772377E-02 ) |
| -> | Parameter number | 28 | . | $\mathrm{X}_{-} \mathrm{N}$ (2) _ ph 1 | 0.33223259 | +/- | 0.32609324E-02 ) |
| -> | Parameter number | 29 | : | Y_N (2) _ph 1 | 0.24144928 | +/- | 0.34579535E-02 ) |
| -> | Parameter number | 30 | : | Z_N (2)_ph1 | 0.51606905E-01 ( | +/- | 0.23675738E-02 ) |
| -> | Parameter number | 31 | : | X_N (3)_ph1 | 0.30316588 | +/- | 0.21229470E-02 ) |
| -> | Parameter number | 32 | : | Y_N (3) _ph1 | 0.45272210 | +/- | 0.28552911E-02 ) |
| -> | Parameter number | 33 | : | Z_N (3)_ph1 | $0.78225881 \mathrm{E}-01$ ( | +/- | 0.29536241E-02 ) |
| -> | Parameter number | 34 | : | X_N (4)_ph1 | 0.54015791 | +/- | 0.11990828E-02 ) |
| -> | Parameter number | 35 | : | Y_N (4)_ph1 | 0.33695599 | +/- | 0.19951391E-02 ) |
| -> | Parameter number | 36 | : | Z_N (4) _ph1 | 0.23162104 | +/- | 0.14471047E-02 ) |
| -> | Parameter number | 37 | : | X_N (5)_ph1 | 0.38837519 | +/- | 0.16739216E-02 ) |
| -> | Parameter number | 38 | : | Y_N (5) _ph1 | 0.20530595 | +/- | 0.22275527E-02 ) |
| -> | Parameter number | 39 | : | Z_N (5) _ph1 | -0.39772190E-01 | +/- | 0.16845398E-02 ) |
| -> | Parameter number | 40 | : | X_N (6) _ph1 | 0.35083801 | +/- | 0.17355493E-02 ) |
| -> | Parameter number | 41 | : | Y_N (6)_ph1 | 0.55482548 | +/- | 0.27362476E-02 ) |
| -> | Parameter number | 42 | : | Z_N (6) _ph1 | 0.11853519E-01 ( | +/- | 0.16991830E-02 ) |
| -> | Parameter number | 43 | . | $\mathrm{X}_{-} \mathrm{C}$ (1) _ ph 1 | 0.34745705 | +/- | 0.27718858E-02 ) |
| -> | Parameter number | 44 | : | Y_C (1) _ph1 | 0.43892241 | +/- | 0.30111372E-02 ) |
| -> | Parameter number | 45 | : | Z_C (1) _ph1 | 0.19351751 | +/- | 0.17470347E-02 ) |
| -> | Parameter number | 46 | : | X_C (2)_ph1 | 0.38531837 | +/- | 0.24003256E-02 ) |
| -> | Parameter number | 47 | : | Y_C (2)_ph1 | 0.21723603 | +/- | 0.21812750E-02 ) |
| -> | Parameter number | 48 | : | Z_C (2)_ph1 | 0.14879125 | +/- | 0.24698584E-02 ) |
| -> | Parameter number | 49 | : | X_C (3)_ph1 | 0.23212539 | +/- | 0.12938807E-02 ) |
| -> | Parameter number | 50 | : | Y_C (3)_ph1 | 0.33450860 | +/- | 0.39550792E-02 ) |
| -> | Parameter number | 51 | : | Z_C (3) _ph1 | $0.49307033 \mathrm{E}-01$ ( | +/- | 0.11598649E-02 ) |
| -> | Parameter number | 52 | . | Scale_ph1_pat1 | $0.76946447 \mathrm{E}-03$ ( | +/- | 0.46780219E-05 ) |
| -> | Parameter number | 53 | : | Cell_A_ph1_pat1 | 11.545714 | +/- | 0.23961758E-03 ) |
| -> | Parameter number | 54 | : | Zero_pat1 | -0.31102592 | +/- | 0.82943856E-03 ) |
| -> | Parameter number | 55 | : | U-Cagl_ph1_pat1 | -0.14575286E-01 | +/- | 0.44974512E-02 ) |
| -> | Parameter number | 56 | : | Cell_B_ph1_pat1 | 10.665313 | +/- | 0.24886982E-03 ) |
| -> | Parameter number | 57 |  | Cell_C_ph1_pat1 | 13.129634 ( | +/- | 0.30849580E-03 ) |
| -> | Parameter number | 58 | : | G-Size_ph1_pat1 | $0.92282938 \mathrm{E}-02$ ( | +/- | 0.10682658E-03 ) |

[^1]$\Rightarrow$ Total approximate array memory (dynamic + static): 107719993 bytes

MaxPOINT= 60000 Max.num. of points (+int. Inten.)/diffraction pattern
MaxREFLT= 20000 Max.num. of reflections/diffraction pattern
MaxPARAM= 300 Max.num. of refinable parameters
MaxOVERL $=2096$ Max.num. of overlapping reflections

```
=> Number of bytes for floating point arrays: 4
=> Dimensions of fixed arrays in this release of FullProf:
NPATT = 80 Max.num. of powder diffraction patterns
NATS
MPAR
IEXCL
IEXCL
IBACP
NPHT
NMAGM
NBASIS
NBASIS
NIREPS
N_EQ
NGL
N_LINC=
NAT_P
NCONST
N_SPE
N_FORM
NPR
INPR
NPRC
NSOL=
8 3 0 ~ M a x . n u m . ~ o f ~ a t o m s ~ ( a l l ~ k i n d ) ~ i n ~ a s y m m e t r i c ~ u n i t ~
1800 Max.num. of non atomic parameters/phase
    30 Max.num. of excluded regions
\begin{tabular}{llrl} 
NPATT & \(=\) & 80 Max.num. of powder diffraction patterns \\
NATS & \(=\) & 830 Max.num. of atoms (all kind) in asymmetric unit \\
MPAR & \(=\) & 1800 Max.num. of non atomic parameters/phase \\
IEXCL & \(=\) & 30 Max.num. of excluded regions \\
IBACP & \(=\) & 277 Max.num. of background points for interpolation \\
NPHT & \(=\) & 16 Max.num. of phases \\
NMAGM & \(=\) & 8 Max.num. of rotation-matrices sets for magnetic structure \\
NBASIS & \(=\) & 12 Max.num. of basis functions associated to a single atom \\
NIREPS & \(=\) & 9 Max.num. of irreducible representations to be combined \\
N_EQ & \(=\) & 384 Max.num. of user-supplied symmetry operators/propagation vectors \\
NGL & \(=\) & 300 Max.num. of global parameters/diffraction pattern \\
N_LINC & \(=\) & 30 Max.num. of global linear restraints \\
NAT_P & \(=\) & 64 Max.num. of atomic parameters per atom \\
NCONST & \(=\) & 500 Max.num. of slack constraints per phase \\
N_SPE & \(=\) & 16 Max.num. of different chemical species \\
N_FORM & \(=\) & 60 Max.num. of scattering factor values in a table \\
NPR & \(=\) & 150 Max.num. of points defining a numerical profile \\
INPR & \(=\) & 25 Max.num. of different numerical peak shapes \\
NPRC & \(=\) & 150 Max.num. of terms in the table for correcting intensities \\
NSOL & \(=\) & 10 Max.num. of solutions to be stored in Montecarlo searchs
\end{tabular}
CPU Time: 26.688 seconds
0.445 minutes
=> Run finished at: Date: 06/07/2015 Time: 15:53:03.785
```


## A. 5 Sample of n-RDX processed with 10 wt\% of PVP

```
** PROGRAM FullProf.2k (Version 5.60 - Jan2015-ILL JRC) **
**************************************************************
M U L T I -- P A T T E R N
Rietveld, Profile Matching & Integrated Intensity
Refinement of X-ray and/or Neutron Data
Date: 15/06/2015 Time: 14:26:29.403
=> PCR file code: rpvp102a
=> DAT file code: rpvp102a.dat -> Relative contribution: 1.0000
=> CONDITIONS OF THIS RUN FOR PATTERN No.: 1
=> Global Refinement of X-ray powder diffraction data
=> Global Refinement of X-ray powder diffraction data
Flat plate with PSD
=> Title:RDX
=> Number of phases: 1
=> Number of excluded regions: 1
> Number of scattering factors supplied: 0
=> March-Dollase model for preferred orientation
=> Conventional weights: w=1.0/Variance(yobs)
=> Asymmetry correction as in J.Appl.Cryst. 26,128(1993)
=> Background refined by polynomial function
=> The 5th default profile function was selected
=> Pseudo-Voigt function (ETA variable)
X-parameter correspond to: ETA=ETAO+X*2theta
pV(x)= ETA*L(x) +(1-ETA)*G(x)
==> INPUT/OUTPUT OPTIONS:
```

=> Generate file *.PRF for plot
$\Rightarrow$ Output Integrated Intensities
$\Rightarrow$ Generate new input file *.PCR
$\Rightarrow$ Data supplied in free format for pattern: 1
=> Plot pattern at each cycle
$\Rightarrow$ Wavelengths: 1.540561 .54439
$\Rightarrow$ Alpha2/Alpha1 ratio: 0.5000
$\Rightarrow \operatorname{Cos}$ (Monochromator angle)= 1.0000
$\Rightarrow$ Asymmetry correction for angles lower than 90.000 degrees
$\Rightarrow$ Absorption correction (AC), muR-eff $=0.0000$ 0.0000
$\Rightarrow$ Base of peaks: $2.0 * \mathrm{HW}$ * 20.00
$\Rightarrow$ Number of cycles: 10
$\Rightarrow$ Relaxation factors $==>$ for coordinates: 1.00
$\Rightarrow$ for anisotropic temperature factors: 1.00
$\Rightarrow$ for halfwidth/strain/size parameters: 1.00
$\Rightarrow$ for lattice constants and propagation vectors: 1.00

```
=> EPS-value for convergence: 0.0
=> Excluded regions for Pattern# 1
From to
50.0000
=> Instrumental Resolution read from file: xray-res.irf
=> Title of data: Approximate resolution function of a conventional X-ray diffractometer CuKalpha1,2
=> The resolution function is IRESOL: 1 for profile function # 5
Input resolution parameters:
\begin{tabular}{llllll} 
U-inst & V-inst & W-inst & X-inst & Y-inst & Z-inst \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000 \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000
\end{tabular}
=> Number of Least-Squares parameters varied: 10
```



```
=>-------> PATTERN number: 1
=> Global parameters and codes ==>
=> Zero-point: -0.2646 0.0000
=> Background parameters and codes ==>
= Origin of polynomial at 2theta/TOF/E(KeV): 40.000
499.36 17910. 54941. 47295. 0.0000 0.0000
101.00 91.00 81.00 0.0.00
=> Displacement peak-shift parameter and code: 0.00 0.00
# Transparency peak-shift parameter and code: 0.00 0.00
=> Reading Intensity data =>>
==> Angular range, step and number of points:
2Thmin: 12.000000 2Thmax: 43.012600 Step: 0.012900 No. of points: 2405
# Phase No. 1
rdx
--------------------------------
=> Crystal Structure Refinement
> The 7th profile function was selected for phase no. 1
=> Preferred orientation vector: 0.0000 0.0000 1.0000
=>-------> Data for PHASE: 1
> Number of atoms: 21
=> Number of distance constraints: 0
=> Number of angle constraints: 0
=> Symmetry information on space group: P b c a
-> The multiplicity of the general position is: 8
-> The space group is Centric (-1 at origin)
-> Lattice type P: { 000 }
-> Reduced set of symmetry operators:
\begin{tabular}{|c|c|c|c|c|c|c|c|}
\hline N & IT & \multicolumn{2}{|l|}{Symmetry symbol} & Rotation part & \multicolumn{3}{|l|}{Associated Translation} \\
\hline & 1) & 1 & --> & ( \(\mathrm{x}, \mathrm{y}, \mathrm{z}\) ) + \{ & 0.0000 & 0.0000 & \(0.0000\}\) \\
\hline & 4) & 2 ( \(\mathrm{x}, 0\) & 0) & \((x,-y,-z)+\{\) & 0.5000 & 0.5000 & \(0.0000\}\) \\
\hline & 3) & 2 ( 0, y, & 0) & \((-x, y,-z)+\{\) & 0.0000 & 0.5000 & \(0.5000\}\) \\
\hline 4: & 2) & 2 ( 0, 0, & z) & (-x,-y, z) + \{ & 0.5000 & 0.0000 & 0.5000 \\
\hline
\end{tabular}
```

```
Information on Space Group:
```

$\Rightarrow$ Number of Space group: 61
$\Rightarrow$ Hermann-Mauguin Symbol: p b c a
Hall Symbol: -P 2ac 2 ab
$\Rightarrow \quad$ Table Setting Choice:
$\Rightarrow \quad$ Setting Type: IT (Generated from Hermann-Mauguin symbol)
$\Rightarrow \quad$ Crystal System: Orthorhombic
Laue Class: mmm
Point Group: mmm
Bravais Lattice: P
Lattice Symbol: oP
Reduced Number of S.O.: 4
General multiplicity: 8
Centrosymmetry: Centric (-1 at origin)
Generators (exc. -1\&L): 2
$\Rightarrow \quad$ Asymmetric unit: $0.000<=x<=0.500$
$0.000<=\mathrm{y}<=0.500$
$0.000<=z<=0.500$
$\Rightarrow$ List of S.O. without inversion and lattice centring translations
$\Rightarrow \operatorname{SYMM}(1): x, y, z \quad \Rightarrow \operatorname{SYMM}(2): x+1 / 2,-y+1 / 2,-z$


| $=>$ |  |  |  |  |  |  |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| Atomitial parameters | Ntyp |  | X | Y | Z | B |


| Atom | Ntyp |  | X | Y | Z | B | occ. |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| B11 | B22 | B33 | B12 | B13 | B23 | in | Spc |


$\Rightarrow$ IT IS ASSUMED THAT THE FIRST GIVEN SITE IS FULLY OCCUPIED
OR THE FIRST AND SECOND ATOMS ARE IN THE SAME SITE WITH TOTAL FULL OCCUPATION
(If this is not the case, change the order of atoms to obtain correct values for the content of the unit cell)
The given occupation factors have been obtained mutiplying m/M by 1.0000

| Atom: 0 | Chemical element: 0 | Atomic Mass | 15.9994 |
| :---: | :---: | :---: | :---: |
| -> Atom: 0 | Chemical element: 0 | Atomic Mass: | 15.9994 |
| -> Atom: 0 | Chemical element: 0 | Atomic Mass: | 15.9994 |
| -> Atom: 0 | Chemical element: 0 | Atomic Mass: | 15.9994 |
| -> Atom: 0 | Chemical element: 0 | Atomic Mass: | 15.9994 |
| -> Atom: 0 | Chemical element: 0 | Atomic Mass: | 15.9994 |
| -> Atom: N | Chemical element: N | Atomic Mass: | 14.0067 |
| -> Atom: N | Chemical element: N | Atomic Mass: | 14.0067 |
| -> Atom: N | Chemical element: $N$ | Atomic Mass: | 14.0067 |
| -> Atom: N | Chemical element: $N$ | Atomic Mass: | 14.0067 |
| -> Atom: N | Chemical element: $N$ | Atomic Mass: | 14.0067 |
| -> Atom: N | Chemical element: N | Atomic Mass: | 14.0067 |
| -> Atom: C | , Chemical element: C | Atomic Mass: | 12.0110 |
| -> Atom: C | Chemical element: C | Atomic Mass: | 12.0110 |
| -> Atom: C | Chemical element: C | Atomic Mass: | 12.0110 |
| -> Atom: H | Chemical element: H | Atomic Mass: | 1.0080 |
| -> Atom: H | Chemical element: H | Atomic Mass: | 1.0080 |
| -> Atom: H | Chemical element: H | Atomic Mass: | 1.0080 |
| -> Atom: H | Chemical element: H | Atomic Mass: | 1.0080 |
| -> Atom: H | Chemical element: H | Atomic Mass: | 1.0080 |
| $\rightarrow$ Atom: H |  |  | 1.0080 |

$\Rightarrow$ The given value of $A T Z$ is $\quad 1776.94$ the program has calculated: 1776.94
The value of $A T Z$ given in the input PCR file will be used for quantitative analysis
$\Rightarrow$ The chemical content of the unit cell is:

| 8.00000 | + | 8.00000 | + | 8.0000 | 0 | + | 8.0000 | 0 | + | 8.0000 | 0 | + | 8.0000 | 0 | + | 8.0000 | N | + | $\swarrow$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 8.0000 | N | $+8.0000$ | N | + 8 | . 0000 | N | + |  |  |  |  |  |  |  |  |  |  |  |  |
| 8.0000 N | $+$ | 8.0000 N | + | 8.0000 | 0 C | + | 8.0000 | C | + | 8.0000 | C | + | 8.0000 | H | + | 8.0000 | H | + | $\checkmark$ | $8.0000 \mathrm{H}+8.0000 \mathrm{H}$ 8.0000 H

$\Rightarrow$ The normalized site occupation numbers in $\%$ are:

| 100.0000 (1) | : |  | 100.0000 0(2) | : |  | 100.0000 0(3) | : |  | 100.0000 0(4) | : |  | 100.0000 0(5) | : |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 100.0000 | O(6) | : | 100.0000 | N(1) | : | 100.0000 | N(2) | : | 100.0000 | N(3) | : | 100.0000 | N (4) | : |
| $100.0000 \mathrm{~N}(5)$ | : |  | $100.0000 \mathrm{~N}(6)$ | : |  | 100.0000 C(1) | : |  | 100.0000 C (2) | : |  | 100.0000 C (3) | : |  |
| 100.0000 | H (1A) | : | 100.0000 | H (1B) | : | 100.0000 | H (2A) | : | 100.0000 | H (2 B ) | : | 100.0000 | H (3A) | : |

$100.0000 \mathrm{H}(3 \mathrm{~B})$
$\Rightarrow$ The density (volumic mass) of the compound is: $1.806 \mathrm{~g} / \mathrm{cm} 3$
=>-------> PROFILE PARAMETERS FOR PATTERN: 1
$=>$ Overall scale factor: $0.380410 E-03$
$=>$ ETA (p-Voigt) OR M (Pearson VII): 0.0000
$=>$ Overall temperature factor: 0.00000
$\begin{array}{lrrr}=> & \text { Halfwidth U,V,W: } & 0.03415 & 0.00000\end{array}$


| 0 | $\begin{aligned} & 3.0485 \\ & 0.0320 \end{aligned}$ | 13.2771 | 2.2868 | 5.7011 | 1.5463 | 0.3239 | 0.8670 | 32.9089 | 0.2508 | 7.9994 | 8.0000 | 0.0470 | $\checkmark$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| N | $\begin{aligned} & 12.2126 \\ & 0.0180 \end{aligned}$ | 0.0057 | 3.1322 | 9.8933 | 2.0125 | 28.9975 | 1.1663 | 0.5826 | -11.5290 | 6.9946 | 7.0000 | 0.0290 | $\swarrow$ |
| C | $\begin{aligned} & 2.3100 \\ & 0.0090 \end{aligned}$ | 20.8439 | 1.0200 | 10.2075 | 1.5886 | 0.5687 | 0.8650 | 51.6512 | 0.2156 | 5.9992 | 6.0000 | 0.0170 | $\swarrow$ |
| H | $\begin{aligned} & 0.4930 \\ & 0.0000 \end{aligned}$ | 10.5109 | 0.3229 | 26.1257 | 0.1402 | 3.1424 | 0.0408 | 57.7997 | 0.0030 | 1.0000 | 1.0000 | 0.0000 | $\checkmark$ |

Symbolic names and initial values of parameters to be varied:
-> Parameter number
$->$ Parameter number
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-> Parameter number
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L-Size_ph1_pat1 Size2_ph1_pat1 Size3_ph1_pat1 Size4_ph1_pat1 Size5_ph1_pat1 Size6_ph1_pat1 Bck_3_pat1 Bck_2_pat1 Bck_1_pat1 Bck_0_pat1
0.0000000 0.0000000 0.0000000 0.0000000 0.0000000 0.0000000 47294.730 54940.645 17910.160 499.36499

1 at 2theta/TOF/E(KeV): 110 at 2 theta/TOF/E (KeV): 112 at 2 theta/TOF/E (KeV): 113 at 2 theta/TOF/E (KeV) 118 at 2 theta/TOF/E (KeV): 121 at 2 theta/TOF/E(KeV): 123 at 2 theta/TOF/E (KeV): 128 at 2 theta/TOF/E (KeV) 129 at 2 theta/TOF/E (KeV) 136 at 2 theta/TOF/E (KeV): 140 at 2 theta/TOF/E (KeV): 145 at 2 theta/TOF/E (KeV): 146 at 2 theta/TOF/E (KeV) 147 at 2 theta/TOF/E (KeV): 155 at 2 theta/TOF/E (KeV): 157 at 2 theta/TOF/E (KeV): 158 at 2 theta/TOF/E (KeV): 160 at 2 theta/TOF/E (KeV) 165 at 2 theta/TOF/E (KeV): 166 at 2 theta/TOF/E(KeV): 167 at 2 theta/TOF/E (KeV) : 168 at 2 theta/TOF/E (KeV) : 179 at 2 theta/TOF/E (KeV) 203 at 2theta/TOF/E(KeV): 204 at 2 theta/TOF/E (KeV): 206 at 2 theta/TOF/E (KeV) : 216 at 2 theta/TOF/E (KeV) 217 at 2 theta/TOF/E (KeV) : 219 at 2 theta/TOF/E(KeV): 222 at 2 theta/TOF/E(KeV): 266 at 2 theta/TOF/E (KeV) : 267 at 2 theta/TOF/E (KeV) : 268 at 2 theta/TOF/E (KeV) : 272 at 2theta/TOF/E(KeV): 273 at 2 theta/TOF/E(KeV): 275 at 2 theta/TOF/E (KeV) : 277 at 2 theta/TOF/E (KeV) : 279 at 2 theta/TOF/E (KeV): 280 at 2 theta/TOF/E(KeV): 284 at 2theta/TOF/E(KeV): 286 at 2 theta/TOF/E (KeV) : 288 at 2 theta/TOF/E (KeV) : 289 at 2 theta/TOF/E(KeV): 290 at 2 theta/TOF/E (KeV): 292 at 2 theta/TOF/E(KeV): 294 at 2 theta/TOF/E (KeV) 295 at 2 theta/TOF/E (KeV): 301 at 2theta/TOF/E (KeV): 302 at 2 theta/TOF/E (KeV): 303 at 2 theta/TOF/E (KeV) 307 at 2 theta/TOF/E (KeV) : 308 at 2 theta/TOF/E(KeV): 309 at 2theta/TOF/E (KeV): 310 at 2 theta/TOF/E (KeV) 312 at 2 theta/TOF/E (KeV): 314 at 2 theta/TOF/E (KeV) 320 at 2 theta/TOF/E(KeV): 344 at 2 theta/TOF/E(KeV): 354 at 2 theta/TOF/E (KeV) : 355 at 2 theta/TOF/E (KeV): 356 at 2 theta/TOF/E (KeV) 357 at 2theta/TOF/E(KeV) 358 at 2 theta/TOF/E(KeV): 359 at 2 theta/TOF/E (KeV): 362 at 2 theta/TOF/E(KeV) 363 at 2 theta/TOF/E (KeV) 364 at 2theta/TOF/E(KeV): 365 at 2 theta/TOF/E (KeV): 369 at 2 theta/TOF/E (KeV) : 370 at 2 theta/TOF/E (KeV) 371 at 2 theta/TOF/E(KeV) 373 at 2theta/TOF/E (KeV): 374 at 2 theta/TOF/E (KeV): 375 at 2 theta/TOF/E (KeV):
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19.8432 20.5269 20.5398 20.5656 20.6043 20.6172 20.6301 20.6817 20.6946 20.7462 20.7591 20.7720 20.7978 20.8107 20.8365 20.8623 20.9397 20.9526
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33.6849 33.6978 33.7494 33.7623 34.1106 34.2138 34.2396 34.2654 35.2845 35.3232 35.9166 35.9424 35.9553 35.9682 35.9940 36.0456 36.0585 36.0714 36.0843 36.2391 36.2778 37.0389 37.1163 38.1096 38.1870 38.4966 38.5611 38.5740 38.6514 38.6772 38.7030 38.7159 38.8965 38.9868 39.6060 41.8119 41.8248 41.8764 42.4698 42.6117 42.6504 42.6633 42.6891 42.7149 42.7278 42.7665 42.8697 42.8826 42.9213 42.9342 42.9471 42.9858 42.9987

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$\Rightarrow$ Optimizations for routine tasks applied:
$\Rightarrow$ Calculation mode for patter\#: 1 CM_PSEUDO_VOIGT

Standard deviations have to be multiplied by: 2.6583 (correlated residuals) See references:
-J.F.Berar \& P.Lelann, J. Appl. Cryst. 24, 1-5 (1991)
-J.F.Berar, Acc. in Pow. Diff. II,NIST Sp.Pub. 846, 63(1992)
=> CYCLE No.: 10

$1.00000 \quad 0.00000 \quad 0.00000$

| N (2) | 0.33383 | 0.00000 | 0.00000 | 0.24622 | 0.00000 | 0.00000 | 0.06392 | 0.00000 | 0.00000 | 2.40240 | 0.00000 | 0.00000 | $\checkmark$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $1.00000 \quad 0.00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (3) | 0.30468 | 0.00000 | 0.00000 | 0.46123 | 0.00000 | 0.00000 | 0.06171 | 0.00000 | 0.00000 | 2.59240 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (4) | 0.54554 | 0.00000 | 0.00000 | 0.33062 | 0.00000 | 0.00000 | 0.23341 | 0.00000 | 0.00000 | 2.76530 | 0.00000 | 0.00000 | $\checkmark$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (5) | 0.38005 | 0.00000 | 0.00000 | 0.19333 | 0.00000 | 0.00000 | -0.02755 | 0.00000 | 0.00000 | 3.09700 | 0.00000 | 0.00000 | $\swarrow$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (6) | 0.35044 | 0.00000 | 0.00000 | 0.55394 | 0.00000 | 0.00000 | 0.00906 | 0.00000 | 0.00000 | 3.43200 | 0.00000 | 0.00000 | $\swarrow$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| C (1) | 0.33877 | 0.00000 | 0.00000 | 0.43604 | 0.00000 | 0.00000 | 0.17023 | 0.00000 | 0.00000 | 2.89510 | 0.00000 | 0.00000 | $\swarrow$ |
| $1.00000 \quad 0.00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| C (2) | 0.38264 | 0.00000 | 0.00000 | 0.20846 | 0.00000 | 0.00000 | 0.14721 | 0.00000 | 0.00000 | 2.70030 | 0.00000 | 0.00000 | $\checkmark$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| C (3) | 0.23896 | 0.00000 | 0.00000 | 0.33552 | 0.00000 | 0.00000 | 0.05796 | 0.00000 | 0.00000 | 2.55740 | 0.00000 | 0.00000 | $\swarrow$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (1A) | 0.40289 | 0.00000 | 0.00000 | 0.52403 | 0.00000 | 0.00000 | 0.20773 | 0.00000 | 0.00000 | 5.13220 | 0.00000 | 0.00000 | $\swarrow$ |
| $1.00000 \quad 0.00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (1B) | 0.29071 | 0.00000 | 0.00000 | 0.42024 | 0.00000 | 0.00000 | 0.23991 | 0.00000 | 0.00000 | 4.84270 | 0.00000 | 0.00000 | $\imath$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (2A) | 0.44331 | 0.00000 | 0.00000 | 0.13918 | 0.00000 | 0.00000 | 0.14950 | 0.00000 | 0.00000 | 4.60580 | 0.00000 | 0.00000 | $\checkmark$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (2 B ) | 0.31742 | 0.00000 | 0.00000 | 0.19390 | 0.00000 | 0.00000 | 0.20730 | 0.00000 | 0.00000 | 4.97430 | 0.00000 | 0.00000 | $\swarrow$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (3A) | 0.20936 | 0.00000 | 0.00000 | 0.35364 | 0.00000 | 0.00000 | -0.02527 | 0.00000 | 0.00000 | 4.50050 | 0.00000 | 0.00000 | $\checkmark$ |
| $1.000000 .00000 \quad 0.00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (3B) | 0.17213 | 0.00000 | 0.00000 | 0.32091 | 0.00000 | 0.00000 | 0.10070 | 0.00000 | 0.00000 | 3.92150 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |

==> PROFILE PARAMETERS FOR PATTERN\# 1
$\Rightarrow$ Overall scale factor: $0.000380410 \quad 0.000000000 \quad 0.000000000$
$\Rightarrow$ Eta(p-Voigt) or m(Pearson VII): $0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Overall tem. factor: 0.0000000 .0000000 .000000
=> Halfwidth parameters:
$0.034153 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Cell parameters:
$11.589819 \quad 0.000000 \quad 0.000000$
$\begin{array}{lll}10.700219 & 0.000000 & 0.000000\end{array}$
$13.173317 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Preferred orientation :
$\begin{array}{lll}1.000000 & 0.000000 & 0.000000\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Asymmetry parameters:
$0.083780 \quad 0.0000000 .000000$
$0.041530 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> $X$ and $Y$ parameters
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Strain parameters:
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.0000000 .000000 \quad 0.000000$
$\Rightarrow$ Size parameters (G, L) :
$0.010621 \quad 0.000000 \quad 0.000000$
0.047821 -0.000006 0.014780
=> Further shape parameters (S_L and D_L):
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Spherical Harmonics coeff.(size):

| $\begin{aligned} & 0.047821 \\ & 0.029142 \end{aligned}$ | -0.000006 | 0.014780 | 0.072264 | -0.000017 | 0.040111 | 0.124992 | 0.000011 | $\swarrow$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{aligned} & 0.079216 \\ & 0.033870 \end{aligned}$ | 0.000001 | 0.041181 | 0.006204 | 0.000018 | 0.040141 | 0.011800 | 0.000014 | $\swarrow$ |
| $\begin{aligned} & 0.000000 \\ & 0.000000 \end{aligned}$ | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | $\swarrow$ |

==> GLOBAL PARAMETERS FOR PATTERN\# 1
$\Rightarrow$ Zero-point: $\quad-0.2646 \quad 0.0000 \quad 0.0000$
=> Background Polynomial Parameters ==>
20303. $236.60 \quad 74.327$
64170. $915.43 \quad 244.22$
$55266 . \quad 790.96 \quad 223.17$
$0.0000 \quad 0.0000 \quad 0.0000$
$\begin{array}{lll}0.0000 & 0.0000 & 0.0000\end{array}$
$\Rightarrow \operatorname{Cos}($ theta)-shift parameter : 0.00000 .00000 .0000
$\Rightarrow \operatorname{Sin}(2 t h e t a)-$ shift parameter : $0.0000 \quad 0.0000 \quad 0.0000$




| 66 | 2.368560 |  | . 8 |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 10 | 2 | 5 | 4 | 0.149967 | 38.039 | 57.6 | 58.0 | 1.712 | 0.135236 | 0.027209 | 0.232800 | $\checkmark$ |
|  | 2.363609 |  | 32.274525 |  |  |  |  |  |  |  |  |  |  |
| 67 | ${ }^{1} \quad{ }^{4} .358914$ | 1 | 3 | 8 | 0.150496 | 38.118 | 148.1 | 151.8 | 6.447 | 0.135312 | 0.028018 | 0.238495 | $\checkmark$ |
|  |  |  | 64.255211 |  |  |  |  |  |  |  |  |  |  |
| 68 | 12 | 1 | 5 | 8 | 0.151800 | 38.432 | 3.0 | 5.6 | 7.937 | 0.135619 | 0.029797 | 0.250596 | $\swarrow$ |
|  | 2.340343 | 63.099045 |  |  |  |  |  |  |  |  |  |  |  |
| 69 | 11 | 2 | 5 | 8 | 0.150892 | 38.853 | 2.1 | 4.9 | 15.308 | 0.136034 | 0.027441 | 0.233313 | $\checkmark$ |
|  | 2.315939 |  | 61.594719 |  |  |  |  |  |  |  |  |  |  |

BRAGG R-Factors and weight fractions for Pattern \# 1
$\Rightarrow$ Phase: 1 rdx
$\Rightarrow$ Bragg R-factor: $7.51 \quad$ Vol: $1633.671(0.000)$ Fract (\%): 100.00( 0.00)

SYMBOLIC NAMES AND FINAL VALUES AND SIGMA OF REFINED PARAMETERS:

| -> | Parameter | number | 1 | : | L-Size_ph1_pat1 | $0.47820579 \mathrm{E}-01($ | +/ - | $0.14780403 \mathrm{E}-01$ | ) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| -> | Parameter | number | 2 |  | Size2_ph1_pat1 | 0.72263569E-01 ( | +/- | $0.40111270 \mathrm{E}-01$ | ) |
| -> | Parameter | number | 3 | . | Size3_ph1_pat1 | 0.12499154 | +/- | 0.29142125E-01 | ) |
| -> | Parameter | number | 4 | . | Size4_ph1_pat1 | 0.79216398E-01 | +/- | $0.41180771 \mathrm{E}-01$ | ) |
| -> | Parameter | number | 5 |  | Size5_ph1_pat1 | $0.62037650 \mathrm{E}-02($ | +/ - | $0.40140565 \mathrm{E}-01$ | ) |
| -> | Parameter | number | 6 | . | Size6_ph1_pat1 | 0.11800204E-01 ( | +/- | 0.33870187E-01 | ) |
| -> | Parameter | number | 7 | . | Bck_3_pat1 | 55265.500 ( | +/- | 223.17101 | ) |
| -> | Parameter | number | 8 | . | Bck_2_pat1 | 64169.578 | +/- | 244.21664 | ) |
| -> | Parameter | number | 9 | : | Bck_1_pat1 | 20303.109 | +/- | 74.326691 | ) |
| -> | Parameter | number | 10 | . | Bck_0_pat1 | 564.83319 ( | +/ - | 5.4257102 | ) |

$\Rightarrow$ Number of bytes for floating point variables: 4
$\Rightarrow$ Dimensions of dynamic allocated arrays in this run of FullProf:
$\Rightarrow$ Total approximate array memory (dynamic + static): 107719993 bytes

| MaxPOINT $=$ | 60000 Max.num. of points (+int. Inten.)/diffraction pattern |
| :--- | ---: | :--- |
| MaxREFLT $=$ | 20000 Max.num. of reflections/diffraction pattern |
| MaxPARAM $=$ | 300 Max.num. of refinable parameters |
| MaxOVERL $=$ | 2096 Max.num. of overlapping reflections |

$\Rightarrow$ Number of bytes for floating point arrays: 4
$\Rightarrow$ Dimensions of fixed arrays in this release of FullProf:

| NPATT | $=$ | 80 Max.num. of powder diffraction patterns |
| :--- | :--- | ---: | :--- |
| NATS | $=$ | 830 Max.num. of atoms (all kind) in asymmetric unit |
| MPAR | $=$ | 1800 Max.num. of non atomic parameters/phase |
| IEXCL | $=$ | 30 Max.num. of excluded regions |
| IBACP | $=$ | 277 Max.num. of background points for interpolation |
| NPHT | $=$ | 16 Max.num. of phases |
| NMAGM | $=$ | 8 Max.num. of rotation-matrices sets for magnetic structure |
| NBASIS | $=$ | 12 Max.num. of basis functions associated to a single atom |
| NIREPS | $=$ | 9 Max.num. of irreducible representations to be combined |
| N_EQ | $=$ | 384 Max.num. of user-supplied symmetry operators/propagation vectors |
| NGL | $=$ | 300 Max.num. of global parameters/diffraction pattern |
| N_LINC | $=$ | 30 Max.num. of global linear restraints |
| NAT_P | $=$ | 64 Max.num. of atomic parameters per atom |
| NCONST | $=$ | 500 Max.num. of slack constraints per phase |
| N_SPE | $=$ | 16 Max.num. of different chemical species |
| N_FORM | $=$ | 60 Max.num. of scattering factor values in a table |
| NPR | $=$ | 150 Max.num. of points defining a numerical profile |
| INPR | $=$ | 25 Max.num. of different numerical peak shapes |
| NPRC | $=$ | 150 Max.num. of terms in the table for correcting intensities |
| NSOL | $=10$ Max.num. of solutions to be stored in Montecarlo searchs |  |

CPU Time: $\quad 6.805$ seconds
0.113 minutes
$\Rightarrow$ Run finished at: Date: 15/06/2015 Time: 14:26:36.221

## A. 6 Sample of n-RDX with $1 \mathrm{wt} \%$ of PVP through a 80 micron nozzle

[^2]```
Date: 20/02/2015 Time: 16:02:20.266
=> PCR file code: rpvp1_80_2a_woB_stillKa2_fullprof
=> DAT file code: rpvp1_80_2a_woB_stil -> Relative contribution: 1.0000
==> CONDITIONS OF THIS RUN FOR PATTERN No.: 1
=> Global Refinement of X-ray powder diffraction data
=> Global Refinement of X-ray powder diffraction data
Flat plate with PSD
=> Title:RDX
=> Number of phases: 1
=> Number of excluded regions: 0
=> Number of scattering factors supplied: 0
=> March-Dollase model for preferred orientation
=> Conventional weights: w=1.0/Variance(yobs)
=> Asymmetry correction as in J.Appl.Cryst. 26,128(1993)
=> Background linearly interpolated between the 2 points given
=> The 5th default profile function was selected
=> Pseudo-Voigt function (ETA variable)
X-parameter correspond to: ETA=ETAO +X*2theta
pV}(\textrm{x})=\textrm{ETA}*\textrm{L}(\textrm{x})+(1-\textrm{ETA})*G(x
==> INPUT/OUTPUT OPTIONS:
=> Generate file *.PRF for plot
=> Output Integrated Intensities
=> Generate new input file *.PCR
=> Data supplied in free format for pattern: 1
> Plot pattern at each cycle
=> Wavelengths: 1.54056 1.54439
=> Alpha2/Alpha1 ratio: 0.5000
C Cos(Monochromator angle)= 1.0000
> Asymmetry correction for angles lower than 90.000 degrees
> Absorption correction (AC), muR-eff = 0.0000 0.0000
=> Base of peaks: 2.0*HW* 20.00
> Number of cycles: 50
=> Relaxation factors ==> for coordinates: 1.00
=> for anisotropic temperature factors: 1.00
=> for halfwidth/strain/size parameters: 1.00
> for lattice constants and propagation vectors: 1.00
=> EPS-value for convergence: 0.0
=> Instrumental Resolution read from file: xray-res.irf
=> Title of data: Approximate resolution function of a conventional X-ray diffractometer CuKalpha1,2
=> The resolution function is IRESOL: 1 for profile function # 5
Input resolution parameters:
\begin{tabular}{llllll} 
U-inst & V-inst & W-inst & X-inst & Y-inst & Z-inst \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000 \\
0.00136 & -0.00500 & 0.00391 & 0.06389 & 0.00008 & 0.00000
\end{tabular}
=> Number of Least-Squares parameters varied: 6
=>--------------------------->
=>-------> PATTERN number: 1
>>--------------------------------
=> Global parameters and codes ==>
=> Zero-point: -0.0558 0.0000
=> Displacement peak-shift parameter and code: -0.12 11.00
# Transparency peak-shift parameter and code: 
=> Reading Intensity data =>>
==> Angular range, step and number of points:
2Thmin: 12.000000 2Thmax: 38.784801 Step: 0.012900 No. of points: 2077
=> Phase No. 1
rdx
=>-------> Pattern# 1
=> Crystal Structure Refinement
> The 7th profile function was selected for phase no. 1
=> Preferred orientation vector: 0.0000 0.0000 1.0000
=>-------> Data for PHASE: 1
=> Number of atoms: 21
=> Number of distance constraints: 0
=> Number of angle constraints: 0
=> Symmetry information on space group: P b c a
-> The multiplicity of the general position is: 8
-> The space group is Centric (-1 at origin)
-> Lattice type P: { 000 }
-> Reduced set of symmetry operators:
```

| No. IT | Symmetry symbol |  | Rotation part | Associated Translation |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1: ( 1) | 1 | --> | ( x, y, z) + \{ | 0.0000 | 0.0000 | $0.0000\}$ |
| 2: ( 4) | 2 ( $\mathrm{x}, 0$ | , 0) | x,-y,-z) + \{ | 0.5000 | 0.5000 | $0.0000\}$ |
| 3: ( 3) | 2 ( 0, y | , 0) | (-x, y,-z) + \{ | 0.0000 | 0.5000 | $0.5000\}$ |
| 4: ( 2 ) | 2 ( 0, 0 | , z) -- | (-x,-y, z) + \{ | 0.5000 | 0.0000 | $0.5000\}$ |


$\Rightarrow$ IT IS ASSUMED THAT THE FIRST GIVEN SITE IS FULLY OCCUPIED
or the first and second atoms are in the same site with total full occupation
(If this is not the case, change the order of atoms to obtain correct values for the content of the unit cell)
The given occupation factors have been obtained mutiplying m/m by 1.0000
$\rightarrow$ Atom: 0, Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994
-> Atom: 0 , Chemical element: 0 Atomic Mass: 15.9994

=>-------> PROFILE PARAMETERS FOR PATTERN: 1


S_L is source width/detector distance
D_L is detector width/detector distance
$==>$ CODEWORDS FOR PROFILE PARAMETERS of PATTERN\# 1
$\Rightarrow$ Overall scale factor: 0.000
$\Rightarrow$ ETA (p-Voigt) OR M (Pearson VII): 0.000
$\Rightarrow$ Overall temperature factor: 0.000
$\begin{array}{lllll}\Rightarrow H a l f w i d t h ~ U, V, W: & 21.000 & 0.000 & 0.000\end{array}$
$\Rightarrow X$ and Y parameters: 0.0000 .000
$\begin{array}{lllllllll}\Rightarrow & \text { Direct cell parameters: } & 0.000 & 0.000 & 0.000 & 0.000 & 0.000 & 0.000\end{array}$
$\begin{array}{llll}\Rightarrow & P r e f e r r e d ~ o r i e n t a t i o n ~ p a r a m e t e r s: ~ & 0.000 & 0.000\end{array}$
$\begin{array}{lllllll}\Rightarrow \text { Asymmetry parameters } & : & 41.000 & 61.000 & 0.000 & 0.000\end{array}$
$\begin{array}{lllll}\Rightarrow \text { Strain parameters } & : & 0.000 & 0.000 & 0.000\end{array}$
=> Size parameters : 51.000 0.000
$=>$ The 18 th model for size is used
$\Rightarrow$ Orthorhombic Anisotropic Broadening using Spherical Harmonics up
to 4-th order (Laue class: mmm, SPG:16-74, only lorentzian comp.)
Ylm's up to 4 th order: YOO,Y20, Y22+,Y40, Y42+,Y44+
RJP - Ref: M. Jarvinen, J. Appl. C. (1993), p. 527
$\Rightarrow$ Coefficients of Spherical Harmonics for anisotropic size
broadening for an orthorhombic lattice

| Y00 | Y20 | Y22 | Y40 | Y42+ | Y44+ |
| :--- | :--- | :--- | :--- | :--- | :--- |
| 0.052419 | 0.087274 | 0.142427 | 0.127726 | -0.069125 | -0.017749 |
| 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 | 0.0000 |

$=>$ Cell constraints according to Laue symmetry: mmm
Metric information:
=> Direct cell parameters:
$\begin{array}{lllll}\mathrm{a}= & 11.6304 & \mathrm{~b}= & 10.7431 & \mathrm{c}= \\ 13.2279\end{array}$
alpha $=\begin{aligned} & 90.000 \quad \text { beta }= 90.000 \quad \text { gamma }= \\ & 90.000\end{aligned}$
Direct Cell Volume $=1652.7814$
=> Reciprocal cell parameters:
$\mathrm{a} *=0.085981 \quad \mathrm{~b} *=\quad 0.093083 \quad \mathrm{c} *=0.075598$

| $\mathrm{alpha} *=$ | $90.000 \quad$ beta $*=\quad 90.000 \quad$ gamma* $=\quad 90.000$ |
| :--- | :--- |

Reciprocal Cell Volume $=0.00060504$
$\Rightarrow$ Direct and Reciprocal Metric Tensors:

GD

| GD | GR |  |  |  | GR |
| :--- | ---: | ---: | :---: | ---: | :--- |
| 135.2666 | 0.0000 | 0.0000 | 0.007393 | 0.000000 | 0.000000 |
| 0.0000 | 115.4133 | 0.0000 | 0.000000 | 0.008665 | 0.000000 |
| 0.0000 | 0.0000 | 174.9783 | 0.000000 | 0.000000 | 0.005715 |


Crystal_to_Orthonormal_Matrix Cr_Orth_cel

| Cr_Orth_cel |  |  |
| :--- | ---: | ---: |
| 11.6304 | 0.0000 | 0.0000 |
| 0.0000 | 10.7431 | 0.0000 |
| 0.0000 | 0.0000 | 13.2279 |

Busing-Levy $B$-matrix: $H c=B . H$ BL_M

$\Rightarrow X$-ray scattering coeff. (A1, B1, A2, ..C, f(0), Z, Dfp,Dfpp)

| 0 | $\begin{aligned} & 3.0485 \\ & 0.0320 \end{aligned}$ | 13.2771 | 2.2868 | 5.7011 | 1.5463 | 0.3239 | 0.8670 | 32.9089 | 0.2508 | 7.9994 | 8.0000 | 0.0470 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| N | $\begin{aligned} & 12.2126 \\ & 0.0180 \end{aligned}$ | 0.0057 | 3.1322 | 9.8933 | 2.0125 | 28.9975 | 1.1663 | 0.5826 | -11.5290 | 6.9946 | 7.0000 | 0.0290 |
| C | $\begin{aligned} & 2.3100 \\ & 0.0090 \end{aligned}$ | 20.8439 | 1.0200 | 10.2075 | 1.5886 | 0.5687 | 0.8650 | 51.6512 | 0.2156 | 5.9992 | 6.0000 | 0.0170 |
| H | $\begin{aligned} & 0.4930 \\ & 0.0000 \end{aligned}$ | 10.5109 | 0.3229 | 26.1257 | 0.1402 | 3.1424 | 0.0408 | 57.7997 | 0.0030 | 1.0000 | 1.0000 | 0.0000 |

SYMBOLIC NAMES AND INITIAL VALUES OF PARAMETERS TO BE VARIED:
-> Parameter number
-> Parameter number
-> Parameter number
-> Parameter number
-> Parameter number
-> Parameter number
-> Symbolic Name:
-> Symbolic Name:
-> Symbolic Name:
-> Symbolic Name:
-> Symbolic Name:
-> Symbolic Name:

| SyCos_pat1 | -0.12224000 |
| ---: | :--- |
| U-Cagl_ph1_pat1 | $-0.32860001 \mathrm{E}-02$ |
| SySin_pat1 | 0.24594000 |
| Asym1_ph1_pat1 | $0.50910000 \mathrm{E}-01$ |
| G-Size_ph1_pat1 | $0.90079997 \mathrm{E}-02$ |
| Asym2_ph1_pat1 | $0.49320001 \mathrm{E}-01$ |

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| 12.0000 | Intensity | fixed | 1.0 and | variance | 1 E 6 |
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| 12.0129 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 12.0516 | Intensity | fixed to | 1.0 and | variance | 1 E6 |
| 12.0903 | Intensity | fixed to | 1.0 and | c | to 1E6 |
| 12.1419 | Intensity | fixed | 1.0 and | variance | - 1E6 |
| 12.1548 | Intensity | fixed | 1.0 and |  | 1 E 6 |
| 12.1677 | Intensity | fixed | 1.0 | variance | 1E6 |
| 12.1806 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 12.1935 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 12.2322 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 12.2709 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 12.3483 | Intensity | fixed to | 1.0 and | ce | - 1E6 |
| 12.4386 | Intensity | fixed | 1.0 an | variance | 1 E 6 |
| 12.4515 | Intensity | fixed | 1.0 and | variance | 1E6 |
| 12.4644 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 12.4773 | Intensity | fixed to | 1.0 and | variance | 1E6 |
| 12.5160 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.5222 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.5996 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.6125 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 13.6254 | Intensity | fixed | 1.0 and | variance | - 1E6 |
| 13.7028 | Intensity | fixed | 1.0 and | variance | 1 E 6 |
| 13.7544 | Intensity | fixed | 1.0 and | variance | 1 E 6 |
| 13.7802 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 13.8447 | Intensity | fixed to | 1.0 an | variance | 1 E 6 |
| 13.8834 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 13.9221 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.0124 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.0382 | Intensity | fixed | 1.0 and | e | 1E6 |
| 14.0640 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 14.0769 | Intensity | fixed to | 1.0 and | variance | 1 E 6 |
| 14.1027 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.1672 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.1801 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.2317 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.2704 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.2962 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.3349 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.3994 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.4252 | Intensity | fixed to | 1.0 and | variance | to 1E6 |
| 14.4897 | Intensity | fixed to | 1.0 and | variance | to 1E6 |

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15.0444
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15.5604
15.5991
15.6249
15.6636 15.6765 15.6894 15.7023
15.7152 15.7410 15.7539 15.7668 15.7797
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16.1538
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16.9278
16.9536
16.9665 16.9794 17.9340
17.9985
18.0114
18.0243 18.0759
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$\Rightarrow$ Optimizations for routine tasks applied:
$\Rightarrow$ Calculation mode for patter\#: 1 CM_PSEUDO_VOIGT

Standard deviations have to be multiplied by: 4.9699 (correlated residuals) See references:
-J.F.Berar \& P.Lelann, J. Appl. Cryst. 24, 1-5 (1991)
-J.F.Berar, Acc. in Pow. Diff. II,NIST Sp.Pub. 846, 63(1992)

```
=> CYCLE No.: 17
```

$\Rightarrow$ Convergence reached at this CYCLE !!!!
$\Rightarrow$ Parameter shifts set to zero
=> Phase 1 Name: rdx
$\Rightarrow$ New parameters, shifts, and standard deviations

| Atom | x | dx | sx | y | dy | sy | z | dz | sz | B | dB | sB | occ. |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| docc. socc. |  |  |  |  |  |  |  |  |  |  |  |  |  |
| O(1) | 0.56846 | 0.00000 | 0.00000 | 0.43427 | 0.00000 | 0.00000 | 0.26465 | 0.00000 | 0.00000 | 3.70830 | 0.00000 | 0.00000 | $\swarrow$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| O(2) | 0.59453 | 0.00000 | 0.00000 | 0.24040 | 0.00000 | 0.00000 | 0.23053 | 0.00000 | 0.00000 | 4.41110 | 0.00000 | 0.00000 | $\swarrow$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| O(3) | 0.47340 | 0.00000 | 0.00000 | 0.13880 | 0.00000 | 0.00000 | -0.02250 | 0.00000 | 0.00000 | 4.98480 | 0.00000 | 0.00000 | $\swarrow$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| O(4) | 0.35580 | 0.00000 | 0.00000 | 0.24950 | 0.00000 | 0.00000 | -0.11238 | 0.00000 | 0.00000 | 4.76640 | 0.00000 | 0.00000 | $\imath$ |

1.000000 .000000 .00000

| O(5) | 0.31810 | 0.00000 | 0.00000 | 0.53030 | 0.00000 | 0.00000 | -0.06806 | 0.00000 | 0.00000 | 5.32170 | 0.00000 | 0.00000 | 2 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| O(6) | 0.42860 | 0.00000 | 0.00000 | 0.60110 | 0.00000 | 0.00000 | 0.04920 | 0.00000 | 0.00000 | 5.10850 | 0.00000 | 0.00000 | ? |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N(1) | 0.43638 | 0.00000 | 0.00000 | 0.33385 | 0.00000 | 0.00000 | 0.17584 | 0.00000 | 0.00000 | 2.73980 | 0.00000 | 0.00000 | $\downarrow$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (2) | 0.32231 | 0.00000 | 0.00000 | 0.23197 | 0.00000 | 0.00000 | 0.05389 | 0.00000 | 0.00000 | 2.40240 | 0.00000 | 0.00000 | $\prec$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (3) | 0.29900 | 0.00000 | 0.00000 | 0.45348 | 0.00000 | 0.00000 | 0.08838 | 0.00000 | 0.00000 | 2.59240 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (4) | 0.53777 | 0.00000 | 0.00000 | 0.33516 | 0.00000 | 0.00000 | 0.22628 | 0.00000 | 0.00000 | 2.76530 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N(5) | 0.38834 | 0.00000 | 0.00000 | 0.20759 | 0.00000 | 0.00000 | -0.03308 | 0.00000 | 0.00000 | 3.09700 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| N (6) | 0.35299 | 0.00000 | 0.00000 | 0.52971 | 0.00000 | 0.00000 | 0.01650 | 0.00000 | 0.00000 | 3.43200 | 0.00000 | 0.00000 | $\checkmark$ |
| $1.00000 \quad 0.000000 .00000$ |  |  |  |  |  |  |  |  |  |  |  |  |  |
| C (1) | 0.35799 | 0.00000 | 0.00000 | 0.43950 | 0.00000 | 0.00000 | 0.18450 | 0.00000 | 0.00000 | 2.89510 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| C (2) | 0.38140 | 0.00000 | 0.00000 | 0.21557 | 0.00000 | 0.00000 | 0.14950 | 0.00000 | 0.00000 | 2.70030 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| C (3) | 0.24458 | 0.00000 | 0.00000 | 0.33936 | 0.00000 | 0.00000 | 0.05038 | 0.00000 | 0.00000 | 2.55740 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (1A) | 0.40289 | 0.00000 | 0.00000 | 0.52403 | 0.00000 | 0.00000 | 0.20773 | 0.00000 | 0.00000 | 5.13220 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H(1B) | 0.29071 | 0.00000 | 0.00000 | 0.42024 | 0.00000 | 0.00000 | 0.23991 | 0.00000 | 0.00000 | 4.84270 | 0.00000 | 0.00000 | $\swarrow$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (2A) | 0.44331 | 0.00000 | 0.00000 | 0.13918 | 0.00000 | 0.00000 | 0.14950 | 0.00000 | 0.00000 | 4.60580 | 0.00000 | 0.00000 | $\checkmark$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (2B) | 0.31742 | 0.00000 | 0.00000 | 0.19390 | 0.00000 | 0.00000 | 0.20730 | 0.00000 | 0.00000 | 4.97430 | 0.00000 | 0.00000 | 2 |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (3A) | 0.20936 | 0.00000 | 0.00000 | 0.35364 | 0.00000 | 0.00000 | -0.02527 | 0.00000 | 0.00000 | 4.50050 | 0.00000 | 0.00000 | $\imath$ |
| 1.000000 .000000 .00000 |  |  |  |  |  |  |  |  |  |  |  |  |  |
| H (3B) | 0.17213 | 0.00000 | 0.00000 | 0.32091 | 0.00000 | 0.00000 | 0.10070 | 0.00000 | 0.00000 | 3.92150 | 0.00000 | 0.00000 | $\checkmark$ |
|  | 0000.00 | 0000 | 000 |  |  |  |  |  |  |  |  |  |  |

==> PROFILE PARAMETERS FOR PATTERN\# 1
$\begin{array}{llll}\Rightarrow \text { Overall scale factor: } \quad 0.000484280 & 0.000000000 & 0.000000000\end{array}$
$\Rightarrow$ Eta(p-Voigt) or m(Pearson VII): 0.0000000 .0000000 .000000
=> Overall tem. factor: 0.0000000 .0000000 .000000
=> Halfwidth parameters:
$\begin{array}{lll}-0.021873 & 0.000000 \quad 0.008126\end{array}$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Cell parameters:
$\begin{array}{lll}11.630419 & 0.000000 & 0.000000\end{array}$
$10.743058 \quad 0.000000 \quad 0.000000$
$13.227938 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
$90.000000 \quad 0.000000 \quad 0.000000$
=> Preferred orientation:
$1.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Asymmetry parameters:
$0.016548 \quad 0.000000 \quad 0.022682$
$0.042495 \quad 0.000000 \quad 0.004085$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> X and Y parameters :
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Strain parameters:
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
=> Size parameters (G,L):
$0.009841 \quad 0.000000 \quad 0.000166$
$0.052419 \quad 0.000000 \quad 0.000000$
=> Further shape parameters (S_L and D_L):
$0.000000 \quad 0.000000 \quad 0.000000$
$0.000000 \quad 0.000000 \quad 0.000000$
$\Rightarrow$ Spherical Harmonics coeff.(size):

| $\begin{aligned} & 0.052419 \\ & 0.000000 \end{aligned}$ | 0.000000 | 0.000000 | 0.087274 | 0.000000 | 0.000000 | 0.142427 | 0.000000 | $\checkmark$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\begin{aligned} & 0.127726 \\ & 0.000000 \end{aligned}$ | 0.000000 | 0.000000 | -0.069125 | 0.000000 | 0.000000 | -0.017749 | 0.000000 | $\checkmark$ |
| $\begin{aligned} & 0.000000 \\ & 0.000000 \end{aligned}$ | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | 0.000000 | $\checkmark$ |


| $\Rightarrow$ | Zero-point: $-0.0558 \quad 0.0000$ | 0.0000 |  |  |  |
| :--- | :--- | :--- | :--- | :--- | :--- |
| $\Rightarrow$ | Cos (theta)-shift parameter | $:$ | -0.1317 | 0.0000 | 0.0059 |
| $\Rightarrow$ | Sin(2theta)-shift parameter | $:$ | 0.2589 | 0.0000 | 0.0079 |



Pattern\# 1 Phase No: 1 Phase name: rdx




BRAGG R-Factors and weight fractions for Pattern \# 1


SYMBOLIC NAMES AND FINAL VALUES AND SIGMA OF REFINED PARAMETERS:
$\left.\begin{array}{lllllll} & & & \\ -> & \text { Parameter number } & 1 & : & \text { SyCos_pat1 } & -0.13173719 & (+/- \\ -> & \text { Parameter number } & 2 & : & \text { U-Cagl_ph1_pat1 } & -0.21872528 \mathrm{E}-01(+/- & 0.88904295 \mathrm{E}-02\end{array}\right)$
=> Number of bytes for floating point variables: 4
$\Rightarrow$ Dimensions of dynamic allocated arrays in this run of FullProf:
$\Rightarrow$ Total approximate array memory (dynamic + static): 107719993 bytes

| MaxPOINT $=$ | 60000 Max.num. of points (+int. Inten.)/diffraction pattern |
| :--- | ---: | :--- |
| MaxREFLT $=$ | 20000 Max.num. of reflections/diffraction pattern |
| MaxPARAM $=$ | 300 Max.num. of refinable parameters |
| MaxOVERL $=$ | 2096 Max.num. of overlapping reflections |

$\Rightarrow$ Number of bytes for floating point arrays: 4
$\Rightarrow$ Dimensions of fixed arrays in this release of FullProf:


## Glossary

ADN Ammonium DiNitramide 46
AFM Atomic Force Microscopy 4, 40, 66, 67, 97, 99, 102-105, 107, 108, 110, 116, 117, 119, 120, 138, 139, 170, 173, 282, 283, 285

AN Ammonium Nitrate 32, 66
AP Ammonium Perchlorate 32, 64
API Active Pharmaceutical Ingredient 134
ASES Aerosol Solvent Extraction System 68, 69, 73
BAM Bundesanstalt für Materialprüfung 43-45, 281
BET Brunauer-Emmett-Teller theory 40, 52, 95, 96, 103, 285
CL-20 2,4,6,8,10,12-hexanitro-2,4,6,8,10,12-hexaazaisowurtzitane 32, 35-38, 46, $47,49,54,55,62,65,70,71,138-141,281,283$

CL-20:HMX co-crystal from CL-20 and HMX 36, 38, 65, 71, 130, 137, 139-141, 174, 283

CNT Classical Nucleation Theory 125, 141
CTA 2,4,6-triazido-1,3,5-triazine or cyanuric triazide 64
CVD Chemical Vapor Deposition 72
DBTDL Dibutyltin dilaurate 64
DLS Dynamic Light Scaterring 53, 55, 62, 65, 73, 281, 285
DMA Differential Mobility Analysis 96
DME DiMethyl Ether 70

DMF DiMethylFormamide 33, 34, 63, 68
DMSO dimethylsulfoxide 33, 34, 149
DSC Differential Scanning Calorimetry 4
ESD Electrostatic Discharge 43-45, 47, 163, 281
ESEM Environmental Scanning Electron Microscopy 51, 55, 173, 281
FOX-7 1,1-diamino-2,2-dinitroethene 46, 62, 71
FPM Full Pattern Matching 50, 111
FTIR Fourier Transform Infrared Spectroscopy 42, 158, 162, 284
FWHM Full Width at Half Maximum 111, 113

GAP GIlycidyl Azide Polymer 64
GiAS Gas AntiSolvent 68

HMX octahydro-1,3,5,7-tetranitro-1,3,5,7-tetrazocine 32, 34, 36-38, 46-48, 55, $62,63,65,66,71,138,281$

IM Insensitive Munitions 46
IR Infrared 81

LASER Light Amplification by Stimulated Emission of Radiation 66, 70, 72, 73, 75, 82, 96, 130

MD Molecular Dynamics 125
MSF Multi Stage Flash 75, 77

NC NitroCellulose 64, 68
NMP N-Methyl-2-pyrrolidone 33, 34
NMR Nuclear Magnetic Resonance 9, 42, 149, 150, 283
NRTL Non-Random Two-Liquid 128
NTO 5-nitro-1,2,4-triazol-3-one 68, 173

ONC Octanitrocubane 46

PDA Phase Doppler Analysis 5, 12, 96, 130-132, 141, 166, 169, 170, 175, 283
PEG PolyEthylene Gilycol 5, 12, 107, 116, 118, 142, 147-149, 151-158, 160, 162-166, 174, 282, 284, 286

PGSS Particles from Gas-Saturated Solutions 69
PhSD Phase Solubility Diagram 134, 136, 137, 174
PID Proportional-Integral-Derivative 78, 139
PIV Particle Image Velocimetry 130
PSD Particle Size Distribution 22, 48, 53, 55, 65, 97, 98, 103, 106-108, 128, 129, 132, 133, 138, 153, 157, 160, 281, 283

PVAc Polyvinyl acetate 71
PVD Physical Vapor Deposition 66, 72, 73, 82
PVOH Polyvinyl alcohol 65
PVP PolyVinylPyrrolidone 5, 12, 52, 53, 70, 107-110, 116-119, 138, 142, 147-149, 151, 154, 157-165, 174, 281, 282, 284

RDX 1,3,5-trinitroperhydro-1,3,5-triazine 4, 11, 12, 31-34, 37, 45-48, 50, 51, 54-56, 61-73, 75, 81, 82, 95, 97-99, 103, 105, 108-110, 117-119, 126-129, 138, 147-150, 152-166, 173, 174, 281-286

RESS Rapid Expansion of Supercritical Solutions 47, 69, 70, 73, 82, 173
RESS-AS Rapid Expansion of Supercritical Solutions into an Aqueous Solution 70, 74

RfD reference dose 54

SAS Supercritical Anti-Solvent precipitation 68
SATP Standard Ambient Temperature and Pressure as a temperature of 298.15 K and an absolute pressure of 100 kPa (1 bar) 34, 35

SAXS Small-Angle X-ray Scattering 141, 166, 170
SCF SuperCritical Fluid 74, 75

SDBD Surface Dielectric Barrier Discharge 67
SEDS Solution Enhanced Dispersion by Supercritical fluids 68, 69, 73
SEM Scanning Electron Microscopy 39, 51, 62, 65, 70, 81, 96, 103, 106-110, 116-120, 128, 152-154, 159, 281, 282, 284, 285

SFE Spray Flash Evaporation 4, 46, 48, 72, 73, 75, 78-83, 98, 99, 105, 111, 112, 117, 120, 126-129, 132, 137-141, 147-149, 152-154, 156-159, 162, 163, 166, 173-175, 282-284

SHYMAN Sustainable Hydrothermal Manufacturing of Nanomaterials 72
SMPS Scanning Mobility Particle Sizer 70
SMRT-TEM single-molecule real-time transmission electron microscopy 125
STM Scanning Tunneling Microscopy 4, 173
TDI Toluene Dilsocyanate 64
TEM Transmission Electron Microscopy 120
TERS Tip Enhanced Raman Spectroscopy 164, 166
TIL Threshold Initiation Level 45
TNAZ 1,3,3-trinitroazetidine 46
TNT 2,4,6-trinitrotoluene 4, 11, 13, 64, 67, 69, 72

VLE Vapor-Liquid Equilibrium 127, 128, 283
XRD X-Ray Difraction 36, 39, 40, 49, 50, 64-66, 73, 99, 111, 120, 138, 140, 153, 155, 158, 161, 170, 281, 283-285

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Florent PESSINA

# Toward Particle Size Reduction by Spray Flash Evaporation the case of organic energetic crystals and cocrystals 

## Résumé

La cristallisation en continu de nanoparticules énergétiques est un défi de longue date. Le Spray Flash Evaporation (SFE) est une technique majeure développée et brevetée en interne, pour la production en continu de matériaux énergétiques submicroniques ou nanométriques; la technologie se base sur la surchauffe d'un solvant pulvérisé dans le vide et s'évaporant alors de manière flash.

Ce présent travail de recherche a pour but de comprendre et contrôler la cristallisation au sein du procédé SFE, ceci afin de réduire encore la taille de particules de cristaux énergétiques. Le RDX est choisi comme matériaux de référence ; le cocristal CL-20:HMX 2:1 a été également étudié pour aller au-delà des limitations de mesures in-situ. La sursaturation gouverne la cristallisation, et concernant le SFE, est une fonction du temps et de l'espace liée aux tailles et vitesses de gouttes. La sursaturation fut variée par un anti-solvant et par l'amélioration du SFE avec un système double buse. Finalement, un Interféromètre Phase Doppler fut utilisé pour résoudre cette question de la sursaturation.

Dans un second temps, PVP 40K et PEG 400 ont été utilisés afin de contrôler les deux étapes de la cristallisation, nommément la nucléation et la croissance. Les particules ont pu être ajustées d'une taille de 160 nm à $5 \mu \mathrm{~m}$, avec des morphologies facettées ou sphériques. De plus, les échantillons de RDX ainsi cristallisés furent aussi moins sensibles, notamment de manière très marquée à la décharge électrostatique.

Mots clés: Spray Flash Evaporation, 1,3,5-trinitroperhydro-1,3,5-triazine, RDX, CL-20, HMX, cristallisation, nanoparticules, particules fines, explosif, cocristal

## Résumé en anglais

The continuous formation of nanosized energetic material is a long-standing challenge. Spray Flash Evaporation (SFE) is a major technique, internally developed and patented, for continuously producing energetic materials at submicron or nano scale; it relies on the superheating of a solvent sprayed into vacuum and thus flashing.

This present research project aims to understand and control the crystallisation occurring in the SFE process, in order to reduce further the particle size of energetic crystals. RDX has been chosen as a reference material; the cocrystal CL-20:HMX 2:1 was studied overcome the limited in situ characterizations also. The supersaturation governs the crystallization and is a function of time and space in SFE, linked to the size distribution and velocity of droplets. Supersaturation was raised with an anti-solvent and by the enhancement of the SFE with a dual nozzle system. Later, a Phase Doppler Interferometer was used to elucidate the question of supersaturation.

Another route to control the crystallisation is the addition of chemical agent. PVP 40K and PEG 400 were successfully used to alter the two steps of the crystallisation, namely the nucleation and the growth. The particle was subsequently tuned from 160 nm spheres to $5 \mu \mathrm{~m}$ grains. Additionally, the synthesized RDX samples were less sensitive, especially toward electrostatic discharge.

Keywords: Spray Flash Evaporation, 1,3,5-trinitroperhydro-1,3,5-triazine, RDX, CL-20, HMX, crystallisation, nanoparticles, fine particles, nanoparticles, explosive, cocrystal


[^0]:    BRAGG R-Factors and weight fractions for Pattern \# 1

[^1]:    => Number of bytes for floating point variables: 4
    $\Rightarrow$ Dimensions of dynamic allocated arrays in this run of Fullprof:

[^2]:    $* * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * * ~$
    ** PROGRAM FullProf. 2 k (Version 5.50- Dec2014-ILL JRC) **
    M U L T I - P A T T E R N
    Rietveld, Profile Matching \& Integrated Intensity
    Refinement of $X$-ray and/or Neutron Data

